

PROBABLE LEAK AREAS
CONTAINMENT PLAN
FOR THE
SARS STUDY

U.S. DEPARTMENT OF HEALTH & HUMAN SERVICES
Centers for Disease Control and Prevention
October 1997

P R E L I M I N A R Y
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PROBABLE LEAK AREAS
in
CONTAINMENT EFAs
for the
SARP STUDY

by
Gandhi National Laboratories
October 1991

PRELIMINARY
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PROBABLE LEAK AREAS
CONTAINING
SILICON
STUDY

U.S. AIR FORCE
WALLINGFORD AIRCRAFT RESEARCH CENTER
OCTOBER 1961

P R E L I M I N A R Y

PROBABLE LEAK AREAS
IN
CONTAINMENT WALL
FOR THE
SARP STUDY

by
J. L. Smith
Sandia National Laboratories
October 1991

P R E L I M I N A R Y
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The first part of the report describes the experimental setup and the results of the tests. The second part discusses the theoretical aspects of the problem and compares the experimental results with the theoretical predictions. The third part presents the conclusions of the study and suggests directions for future research.

The experimental setup consisted of a test chamber of diameter 1.0 inch and length 1.5 inches. The chamber was filled with a liquid of viscosity η and density ρ . The liquid was driven through a hole of diameter d by a pump. The flow rate was measured by a flowmeter. The pressure drop across the hole was measured by a manometer.

The theoretical analysis is based on the Navier-Stokes equations for the flow of a viscous fluid. The flow is assumed to be steady and axisymmetric. The velocity profile is assumed to be parabolic. The pressure drop is calculated by integrating the Navier-Stokes equations over the length of the hole.

The experimental results show that the flow rate increases with the pressure drop. The theoretical predictions agree well with the experimental results. The conclusions of the study are that the flow of a viscous fluid through a hole is governed by the Navier-Stokes equations and that the flow rate is proportional to the pressure drop.

$$Q = 0.011 \text{ cm}^3/\text{sec} \quad (\text{at } \Delta P = 100 \text{ mm Hg})$$

$$\text{or } Q = 0.0000 \text{ cm}^3/\text{sec} \quad (\text{at } \Delta P = 0 \text{ mm Hg})$$

In the present study, the flow of a viscous fluid through a hole of diameter 1.0 mm was investigated. The flow rate was measured for a range of pressure drops. The results show that the flow rate is proportional to the pressure drop. The theoretical predictions agree well with the experimental results. The conclusions of the study are that the flow of a viscous fluid through a hole is governed by the Navier-Stokes equations and that the flow rate is proportional to the pressure drop.

$$Q = 0.011 \text{ cm}^3/\text{sec} \quad (\text{at } \Delta P = 100 \text{ mm Hg})$$

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PROBABLE LEAK AREAS UNDER SEVERE ACCIDENT CONDITIONS -
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in order to meet the requirements of the design. Although the welds are not expected to be subjected to high temperatures, they are expected to be subjected to high temperatures during the welding process.

The design of the welds is based on the assumption that the welds will be subjected to high temperatures during the welding process. The design of the welds is based on the assumption that the welds will be subjected to high temperatures during the welding process.

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Since the primary welds for all the non-EPA are non-organic, they are expected to be subjected very little by aging and will have a high temperature capability.

SURRY 1 2 2 - The surry EPAs are designed to be mounted in a 1 inch diameter schedule 40 nozzle. The nozzle is 19.75 inches long and welded to a 1 inch thick stainless steel plate. The nozzle is mounted in the center of the plate. The nozzle is mounted in the center of the plate. The nozzle is mounted in the center of the plate.

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Appendix I

Containment Purge and Vent

Area for Eton 1 and 2

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50-504

BROOKHAVEN NATIONAL LABORATORY

ASSOCIATED UNIVERSITIES, INC.

Upton, Long Island, New York 11973

Department of Nuclear Energy

7203

June 20, 1983

Mr. Goutam Bagchi
Equipment Qualification Branch
Division of Engineering
U.S. Nuclear Regulatory Commission
Washington, DC 20555

Dear Goutam:

As you requested, attached is Brookhaven National Laboratory's (BNL's) evaluation of the leakage area associated with containment supply and exhaust valves for Zion 1 and 2. If you have questions or if we may be of further assistance, please feel free to call.

Sincerely,

Bruce E. Miller
Engineering Analysis and
Human Factors Group

SEM/smm
Attached

cc: R. A. Bari (wo/att.)
R. E. Hall
W. J. Luckas, Jr.
J. H. Taylor
File

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CONTAINMENT PURGE AND VENT VALVE
LEAKAGE AREA FOR ZION 1 AND 2

Brookhaven National Laboratory

Upton, NY 11973

June 20, 1983

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CONTAINMENT PURGE AND VENT VALVE
LEAKAGE AREA
FOR ZION 1 AND 2

Objective

Estimate the potential leakage area associated with the containment purge and vent valves installed at the Zion Nuclear Power Station, Units 1 and 2.

Discussion

The containment purge supply and exhaust air duct are each equipped with two (2) 42-inch isolation valves in series. One valve is inside containment and one valve is outside containment. These valves are manufactured by H. Pratt and are Model RIA valves.

The purchase specification for these valves stipulates a normal inside containment temperature of 66°F to 120°F and approximately a 50% relative humidity. After an incident the specification stipulates that a saturated steam air mixture will exist such that the valve design shall be based on 70 psia, 300°F which will decay to approximately 5 psia, 120°F in 24 hours and will remain at this condition one year thereafter."

During normal operation, the specification further states "...the neutron-proton (gamma) radiation exposure rate" is to be 10^{-1} rads/hour resulting in a total exposure of 4×10^4 rads based on a 40-year plant life. After an incident, the radiation exposure is specified to be 2×10^6 rads during the first three hours and a total exposure of 1×10^9 rads, with an average weighted value of 1.0 meV, based on a one year operating period for system decay. A dilute mixture of sodium hydroxide and boric acid is also specified (containment spray system).

The purchase specification calls for each valve to be hydrostatically tested at the vendor's plant for leakage at 300 psi with each valve seat to be hydrostatically tested to a pressure of 150 psid across the disc to prove it drop-tight.

Conversations with H. Pratt, the valve manufacturer, have revealed that the metal to metal clearance between the valve disc and body range from 1/16 to 1/8 inch. The seating surface or seal ring is Ethylene Propylene Terepolymer. Shaft bearing clearance is .015 inches when the bearing material is bronze. When calculating the area, it was assumed that the bearing is a corrosion resistant sleeve-type. The disc diameter is approximately 40.9 inches and the shaft diameter approximately 4.24 inches.

Potential leakage areas are between the shaft and bearing and the valve disc and body. The total area surrounding the shaft is .1008 square inches. Leakage past the shaft bearing is considered to be negligible, since total failure of the shaft seal, packing retainer ring, packing, lantern gland ring, and bonnet assembly must occur for there to be leakage through an area of .1008 square inches.

Disc and body clearance is 1/16 to 1/8 inch. With a 41-inch disc, total failure of the seal ring, assuming the valve closed, reveals an area around the disc of 4.0282 square inches or 8.0622 square inches, respectively.

When determining the disc area, it was assumed that the valve is closed, that there is a straight run of pipe upstream of the valve, and total failure of the valve seat ring occurs.

Results

When determining leakage rate for the purge and vent valves, the most conservative approach would be to assume total failure of the valves inside containment (valve failed open). Thus, with an area varying from 8.06 to 4.03 square inches per valve, the total leakage area for the two valves located outside containment would be:

1. Past the disc - 16.12 to 8.06 square inches
2. Past the shaft - .2 square inches
3. Total - 8.26 to 16.32 square inches.

Zions containment is designed for 62 psia; 2-1/2 times this pressure is 155 psia. The purchase specification calls for a disc hydrostatic test, to prove that it is drop-tight, at 150 psig, or approximately 165 psia. Thus, it is concluded that total disc failure at 2-1/2 times P_d , design pressure, is unlikely.

The following information was obtained from the records of the
 Department of the Interior, Bureau of Land Management, and the
 Department of the Interior, Bureau of Reclamation, regarding the
 land ownership and management of the area described in the
 preceding pages.

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1. The first part of the document discusses the importance of maintaining accurate records of all transactions and the role of the accounting system in providing reliable financial information. It emphasizes the need for transparency and accountability in financial reporting.

2. The second part of the document outlines the various components of the accounting system, including the general ledger, subsidiary ledgers, and the trial balance. It explains how these components work together to ensure the accuracy and integrity of the financial data.

3. The third part of the document focuses on the process of closing the books at the end of each accounting period. It details the steps involved in transferring balances from the temporary accounts to the permanent accounts, ensuring that the financial statements reflect the correct financial position of the company.

4. The fourth part of the document discusses the importance of internal controls in preventing fraud and errors. It highlights the need for a strong internal control system that includes segregation of duties, authorization, and regular monitoring.

5. The fifth part of the document provides a summary of the key points discussed and offers recommendations for improving the accounting system. It stresses the importance of ongoing education and training for accounting personnel to stay up-to-date with the latest practices and technologies.

Plant	Material	Qty	Unit	Value	Value
Station 1 2 2	Glass/Welded (36 2 38)	300		10-7	10-7
Station 1 2 2	Glass/Welded (22) Glass/Welded (11) Glycol/Vest (9)	7 100/400 340		10-7 10-7 10-7	10-7 10-7 10-7
Repair Bottom	Epoxy (?)	230		10-7	10-7
Crane Oil 1 1	Epoxy/Gel (17)	230		10-7	10-7
Substation 1 2 2	Epoxy/Welded (47)	230		10-7	10-7

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Station	Time	Lat	Long	Alt	Temp	Wind	Clouds	Pressure	Humidity	Visibility	Remarks
Station 1	0800	10° 15' N	156° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 2	0900	10° 30' N	156° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 3	1000	10° 45' N	156° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 4	1100	11° 00' N	157° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 5	1200	11° 15' N	157° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 6	1300	11° 30' N	157° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 7	1400	11° 45' N	157° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 8	1500	12° 00' N	158° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 9	1600	12° 15' N	158° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 10	1700	12° 30' N	158° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 11	1800	12° 45' N	158° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 12	1900	13° 00' N	159° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 13	2000	13° 15' N	159° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 14	2100	13° 30' N	159° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 15	2200	13° 45' N	159° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 16	2300	14° 00' N	160° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 17	2400	14° 15' N	160° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 18	2500	14° 30' N	160° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 19	2600	14° 45' N	160° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 20	2700	15° 00' N	161° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 21	2800	15° 15' N	161° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 22	2900	15° 30' N	161° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 23	3000	15° 45' N	161° 45' W	100	28.5	10	0	1010	85	10	Clear
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Station 25	3200	16° 15' N	162° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 26	3300	16° 30' N	162° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 27	3400	16° 45' N	162° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 28	3500	17° 00' N	163° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 29	3600	17° 15' N	163° 15' W	100	28.5	10	0	1010	85	10	Clear
Station 30	3700	17° 30' N	163° 30' W	100	28.5	10	0	1010	85	10	Clear
Station 31	3800	17° 45' N	163° 45' W	100	28.5	10	0	1010	85	10	Clear
Station 32	3900	18° 00' N	164° 00' W	100	28.5	10	0	1010	85	10	Clear
Station 33	4000	18° 15' N	164° 15' W	100	28.5	10	0	1010	85	10	Clear

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REFERENCES

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Air by Aerosols from the Operation of Industrial
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