



UNION CARBIDE CORPORATION  
METALS DIVISION  
URAVAN, COLORADO 81436

WM-34

July 8, 1980

Colorado Department of Health  
Air Pollution Control Division  
James S. Geier, Public Health Engineer

Dear Sir:

This information is being submitted, in conjunction with our letter of April 28, 1980, concerning the new air pollution control equipment we are planning to install at the Uravan facility and in reply to your comments of May 23, 1980. This data, along with the first letter, is also being submitted to the Colorado Department of Health Radiological and Hazardous Wastes Division in application for a source material license minor health and safety amendment.

Attachment A is a discussion of the present yellowcake calciner and associated scrubber system. Attachment B discusses in more detail the proposed system to be installed along with copies of the scrubber bid specifications and calculations on emission rates.

Construction of the shell of this building and mounting of the seven hearth rotary calciner is scheduled to begin in Mid-July and operational by the first of February of 1981.

If you have any questions concerning this submittal, please contact me at (303) 862-7301.

Sincerely,

A handwritten signature in cursive script, appearing to read "R. K. Jones", with a checkmark at the end.

R. K. Jones  
Environmental Engineer

RKJ:ns  
enclosures

8106040523

## ATTACHMENT A

### Current Yellow Cake Calciner Description

Yellowcake, in solution, is precipitated from the feed liquor through adjusting the pH of the solution with either hydrogen peroxide, caustic soda, or anhydrous ammonia. This thickened solution is pumped into one of four horizontal plate and frame filter presses where it is washed under pressure and a certain amount of liquor is forced from the cake.

The plate and frame presses, each containing approximately 40 plates, are cleaned manually by scraping the dewatered cake off each plate. The cake falls into a scoop which in turn transfers it to a repulper bin. By the nature of the work, occupational exposure to fresh yellowcake is dominant in the operation, providing extraneous pathways of introducing uranium contamination to employees. The cake is repulped, utilizing only the liquor remaining in the cake, and pumped by a diaphragm pump to the top of the calciner where it dumps onto one of the hearths. Plate 4.0 illustrates the current calciner and scrubber arrangement.

This calciner is a ten hearth rotary roaster constructed in the late 1930 era. The emergency exhaust stack shown on Plate 4.0 was the initial venting from the calciner, with no emission controls system; a manual damper shuts off this stack. An add-on ventilation duct, sixteen inches in diameter, is connected to the second to the top hearth, providing suction to the calciner of zero point seven inches of static pressure.

Employee exposure to airborne uranium dust is prevalent due to required maintenance of drop cleaning for each hearth through the calciner access doors. Negative static pressure throughout the calciner is not maintained due to development of back pressure caused by partially plugged drops, resulting in employee exposures during the cleaning of those drops. The access doors are not equipped with the double door plenum arrangement that is designed for the new calciner to minimize employee exposure.

Emissions from the current calciner are exhausted through a Ducon three tiered wet packed tower, consisting of three water sprayed beds of ceramic beryls, saddles, and marbles, and on the exhaust side of the fan, through an additional set of sprays and a demister. Liquor flows from the scrubbing circuit are recycled through a settler.

# CURRENT URAVAN YELLOWCAKE CALCINER

SCHEMATIC

CENTER COLUMN  
EXHAUST

3330 A.C.F.M.  
1220 F. SAT.  
0.0035 lbs/min.  
DUST

EMERGENCY EXHAUST  
STACK

Roof

THREE TIER  
PACKED  
TOWER

FOURTH FLOOR

6500 A.C.F.M.  
518 °F  
0.7" H<sub>2</sub>O S.P.

THIRD FLOOR

TEN HEARTH  
ROTARY FURNACE

UNDERFLOW  
RECYCLED

SECOND FLOOR

600 A.C.F.M.

SHAFT COOLING FAN

OUTSIDE AIR  
INTAKE  
825 A.C.F.M.

FIRST FLOOR

PRODUCT PKG.

DEMISTER

4.7" H<sub>2</sub>O  
STATIC PRESS.

MAKE UP  
WATER

NOT TO SCALE

UNION CARBIDE CORP.

URAVAN, COLO.

PLATE 4.0

Attachment A, continued

Measurements of particle size obtained through a 1979 survey made by the E.P.A. Las Vegas Radiation Branch indicated the mean particle diameter at the scrubber inlet was between nine and ten microns. The discharge mean particle diameter was around three microns. The following information is a tabulation of emission monitoring completed through March 1980. The E.P.A. figures of 1977 were utilized for the 1977 updated APEN report, a copy of which is attached. On an annual average, the feed rate is not expected to exceed a theoretical feed ratio of 1.25 with a maximum operation of 1.50\*.

EMISSION RATE SUMMARY - YELLOW CAKE CALCINER

Sampler Date	Calciner Feed Rate Ratio*	Discharge Vol. <sup>5</sup> Flow Rate x 10 <sup>5</sup> (DSCFH)	Emmision Rate Pounds U308/hr.	Emission Rate Tons/Year	
EPA-Las	10/13/77	1.125	2.1	0.14	0.61
Vegas Rad.	10/14/77	0.800	2.0	0.11	0.48
Branch	10/15/77	1.215	2.0	0.18	0.79
	10/16/77	1.155	1.9	0.25	1.10
	10/17/77	1.310	1.9	0.18	0.79
	10/18/77	1.715	1.9	0.31	1.36
	10/19/77	<u>0.795</u>	<u>1.9</u>	<u>0.28</u>	<u>1.23</u>
MEAN		1.159	1.96	0.21	0.91
NUS	3/4/80	1.163	1.04	0.26	1.14
CORP.	3/4/80	1.163	1.06	0.10	0.44
	3/5/80	<u>1.60</u>	<u>1.48</u>	<u>0.37</u>	<u>1.62</u>
MEAN		1.309	1.19	0.24	1.07
UNION	4/29/69	0.905	2.46	0.33	1.45
CARBIDE	9/14/76	0.480	3.31	0.45	1.98
	9/23/76	2.500	0.90	0.20	1.06
	12/5/76	1.410	2.10	0.17	0.76
	2/16/77	1.360	2.0	0.17	0.76
	2/21/77	<u>0.965</u>	<u>1.9</u>	<u>0.14</u>	<u>0.61</u>
MEAN		1.27	2.1	0.24	1.09
TOTAL MEAN		1.23	1.87	0.23	1.01

\* An arbitrary feed rate was utilized as a denomination to develop a ratio between known feed rates for production versus emission comparisons.

## ATTACHMENT B

### New Yellow Cake Calciner Description

The precipitated yellow cake from the precipitation circuit, as described in the 1978 Uravan Environmental Report, is thickened and the overflow solution from the thickeners is pumped to a horizontal vacuum belt filter, located on the top floor of the new calciner building, where the yellow cake is sprayed onto a moving belt filter with suction applied to the underside of the filter. At the end of the horizontal belt travel, the moist cake drops vertically into a hopper which in turn feeds a screw conveyor. The enclosed screw conveyor transfers the pressed cake to the top of the calciner, eliminating any personnel exposure to supplying the material to the calciner.

The calciner consists of a seven hearth rotary furnace with access doors at each hearth to allow access for cleaning drops and rake arms. The access doors consist of a double door arrangement with approximately one foot clearance between doors. The plenum area between the two doors is maintained under negative pressure. When cleaning drops or rakes does occur, the negative pressure pulls any generated dust away from the personnel's breathing zone area and to the scrubbing system. Heavy particles, not entrained by the negative pressure system fall down the plenum chute, between the doors, to an enclosed five gallon container. This system has been designed specifically to minimize employee exposure during this required operating maintenance.

The product being discharged, from the base of the calciner, drops vertically through a lump breaker and magnetic trap onto the revolving screws of a screw conveyor which transports the product to a storage bin. The bin is emptied daily from the bottom by actuating a valve which discharges the yellow cake into a product shipping drum, 55-gallon capacity. The drum is enclosed at the top by a hood that maintains a negative pressure on the drum, drawing airborne particulates through a duct work to the calciner emission scrubbing system. The product drums, upon filling, roll on a horizontal roller conveying system where they are weighed, inspected, allowed to cool, and sealed. The drums are transported by this manner into another room for immediate storage and labeling.

Emissions from the calciner, product barreling, and calciner drop plenums pass through a dry cyclone, a venturi scrubber and a cyclonic separator prior to being vented to atmosphere.

Work area atmosphere is maintained under negative pressure by a separate ventilation system which includes a reverse jet fabric filter collector.



## EMISSION CALCULATIONS

### I. Proposed Yellow Cake Calciner Scrubber

#### 1.0 Inlet Source #1

1.1 Calciner maximum production - 5.0 lb/min.  
(corresponds to calciner feed rate ratio of 1.5)

1.2 Estimated dust lost to ventilation system - 2%  
 $5 \text{ lb/min.} \times 0.02 = 0.10 \text{ lb/min.}$

#### 2.0 Inlet Source #2

2.1 Drum packing (drum hood, surge bin, conveyor system)  
Assume 1.2 grains per cubic foot in 600 cfm.  
$$\frac{1.2 \times 600}{7000} = 0.10 \text{ lb/min.}$$

3.0 Total scrubber system feed - 0.20 lb/min.

#### 4.0 Scrubber system reduction

4.1 Reduction in dry cyclone - 80% design efficiency  
 $0.20 \text{ lb/min.} \times 0.80 = 0.16 \text{ lb/min.}$

4.2 Cyclone loss to Venturi scrubber  $0.20 - 0.16 = 0.04 \text{ lb/min.}$

4.3 Venturi scrubber at 25" pressure drop is estimated to be 95% efficient for collecting the cyclone exhaust.

4.4 Therefore, stack emission rate is 0.04 lb/min. times 5% or 0.002 lb/min. or 0.12 lbs/hr. or 0.53 tons per year

### II Proposed Yellow Cake Calciner Building Air Ventilation Scrubber

#### 1.0 Inlet Source - Single hood

Estimated 0.001 grains/cubic foot dust in room atmosphere

#### 2.0 Scrubber Efficiency

Fabri-Pulse Reverse jet baghouse design efficiency is 99.9%

#### 3.0 Emission Rate

Calculation:  $0.001 \times 0.0001 = 1 \times 10^{-6}$  grains/cubic foot

$$\frac{1 \times 10^{-6} \times 3800 \text{ cfm} \times 60 \times 24 \times 365}{7000} = 0.28 \text{ lbs./yr.}$$



UNION CARBIDE CORPORATION  
METALS DIVISION  
URAVAN, COLORADO 81415

April 28, 1980

Air Pollution Control Division  
Colorado Department of Health  
4210 East 11th Avenue  
Denver, Colorado 80220

Attention: Mr. John Plog

Re: Union Carbide Corporation  
Uravan, Colorado  
Air Pollutant Emission Notice

Gentlemen:

Enclosed are two air pollutant emission notices and filing fees for new scrubbing systems at the Uravan Mill operated by Union Carbide Corporation.

The primary scrubbing system described under the first notice is the main replacement system for the packed tower scrubber itemized as emission number five in the Air Contaminant Emission Notice filed on June 25, 1970. Plates 1.0 and 2.0 illustrate the basic design of the system and describe designed flow rates and dust concentrations. The second notice is for a general room air dust ventilation and scrubbing system for the new yellowcake drier calciner for which the first notice scrubber will be operating from. Plates 3.0 illustrate the design, flow rates, and concentrations of this system. The combination of the two systems essentially replace emission number five of the 1970 notice.

The anticipated emissions of the combined replacement system is 0.53 tons per year (2.88 lb/hr) in comparison with the current systems 2.3 tons per year.

It is our interpretation that because this is a replacement of an existing scrubber and that because the higher efficiency of the replacement results in a significant decrease in emissions, that no emission permit is required as long as the attached Air Contaminant Emissions Notice, Form APC-200A-20, is filed.

Sincerely,

*G. L. Schierman*  
G. L. Schierman  
Plant Superintendent

*Roger Jones*  
R. K. Jones  
Environmental Engineer

GLS/RKJ:ns  
enclosures

MAIL ADDRESS ..... P.O. BOX 94, URAVAN, COLORADO 81436 PLANT LOCATION ..... URAVAN

PERSON TO CONTACT REGARDING THIS INFORMATION ..... MR. G. L. SCHIERMAN TITLE ..... PLANT SUPERINTENDENT

GENERAL DESCRIPTION OF THIS PLANT'S FUNCTION ..... URANIUM AND VANADIUM EXTRACTION

PHONE (303) 862-7301  
Will you accept only the following hours to call? (Yes) 8:30 - 4:00

A. GENERAL INFORMATION		Normal Operation of Plant*			Seasonal Throughput (% of Annual)				Specify any significantly different schedule of a unit or process which emits air pollutants
No. of Employees	Land Area	Hours/Day	Days/Week	Weeks/Year	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	
225	806	24	7	52	23.7	24.7	25.4	26.2	22.8; 27.0; 24.3; 25.9

B. STACK OR VENT INFORMATION FOR						(Identify which stack if plant has two or more; refer to attached sketch of plant layout)
Height	Diameter	Temperature	Flow Rate	Velocity	Humidity	
47.25 ft	1 ft	150 °r	3000 ACFT	3820 ft/min	100%	

C. FUEL INFORMATION		Design Rate (10 <sup>6</sup> BTU/Hr)	Kind of Fuel Burned	Annual Consumption (Tons, 10 <sup>6</sup> cal, or 10 <sup>6</sup> SCF)	Heating Value (10 <sup>6</sup> BTU/Annual Unit)	Per Cent by Weight		Seasonal Use (% of Annual Use)				Space Heat (2. And)
Description of Combustion Unit						Sulfur (A, %)	Ash (A, %)	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	
Seven Hearth Rotary Furnace		Nat. Available	Nat. Gas Fuel Oil	N/A	N/A	N/A	N/A	24.6	20.6	33.4	21.4	0
Four Burners								57.8	42.2	0	0	0

D. PROCESS INFORMATION		Raw Materials, Solvents, Cleaning Agents, Waste, etc. Involved in Process	Annual Consumption (Specify Units)	Design Rate (Specify Units/Hour)	Finished Products		Annual Output	(AFCH Use) SCC
Description of Processing Unit					Product Name or Description			
Seven Hearth Rotary Furnace		Uranium as Yellowcake	Proprietary Information	Proprietary Information	Yellowcake	Prop. Info		

E. POLLUTION CONTROL EQUIPMENT			Overall Collection Efficiency	Cost of Control		(To be completed by Air Pollution Control Division)			
Pollutant	Type of Control Equipment			Initial Installation	Annual Total Operating Cost	Annual Energy Used (Specify Units & Type)	Estimated Emissions (Tons/Year)	Uncontrolled Emissions (Tons/Year)	Allowable Emissions (Tons/Year)
Particulate	Dry Cyclone	Wet Venturi	99	\$190,000					
SO <sub>x</sub>									
NO <sub>x</sub>									
HCl									
CO									
PS									
Others									

REMARKS: Design Emission Rate: 0.002 lb/min - 2.88 lbs/day

Signature of Person Legally Authorized to Supply Data .....  
Typed Name & Title ..... Mr. G. L. Schierman, Plant Superintendent

COLORADO DEPARTMENT OF HEALTH  
AIR POLLUTION CONTROL DIVISION  
6210 East 11th Avenue  
Denver, Colorado 80220  
(303) 370-6100



MAIL ADDRESS ..... P.O. BOX 94, URAVAN, COLORADO 81436 ..... PLANT LOCATION ..... URAVAN ..... COUNTY MONTROSE  
PERSON TO CONTACT REGARDING THIS INFORMATION ..... MR. G. L. SCHIERMAN ..... TITLE ..... PLANT SUPERINTENDENT ..... PHONE (303) 862-7301  
GENERAL DESCRIPTION OF THIS PLANT'S FUNCTION ..... Uranium and Vanadium Extraction ..... Will you accept collect calls? Yes  
Best hours to call: .....

A. GENERAL INFORMATION		Normal Operation of Plant*			Seasonal Throughput (% of Annual)				Specify any significantly different schedule of a unit or process which emits air pollutants
No. of Employees	Land Area	Hours/Day	Days/Week	Days/Year	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	
225	806	24	7	52	23.7	24.7	25.4	26.2	25; 25; 25; 25

B. STACK OR VENT INFORMATION FOR .....						(Identify which stack if plant has two or more; refer to attached sketch of plant layout)	
Height	Diameter	Temperature	Flow Rate	Velocity	Moisture		
47.25 ft	1	Ambient	3800 acfm	ft/min	Ambient		

C. FUEL INFORMATION		Design Rate (10 <sup>6</sup> BTU/Hr)	Kind of Fuel Burned	Annual Consumption (Tons, 10 <sup>6</sup> gal, or 10 <sup>6</sup> scf)	Heating Value (10 <sup>6</sup> BTU/Annual Unit)	Per Cent by Weight		Seasonal Use (% of Annual Use)				Space Heat (% Annual)
Description of Combustion Unit						Sulfur (A, AB)	Ash (AA, AL)	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	
Not Applicable												

D. PROCESS INFORMATION		Raw Materials, Solvents, Cleaning Agents, Waste, etc. Involved in Process	Annual Consumption (Specify Units)	Design Rate (Specify Units/Hour)	Finished Products		(AFCD Use) SCC
Description of Processing Unit					Product Name or Description	Annual Output	
Rotary Furnace.....		.....Not Applicable.....					
Building Gen.Ventilation.....							

E. POLLUTION CONTROL EQUIPMENT		Overall Collection Efficiency	Cost of Control Equipment			(To be completed by Air Pollution Control Division)			
Pollutant	Type of Control Equipment		Initial Installation	Annual Total Operating Cost	Annual Energy Used (Specify Units & Type)	Exhaustion Estimate	Uncontrolled Emissions	Allowable Emissions	Estimation Method
	Primary					Tons/Year	Tons/Year	Tons/Year	
Particulate	AAF Model 4-168-400	99.9	27,000						
SO <sub>x</sub>	"m" Fabric Pulse Reverse								
NO <sub>x</sub>	Jet Baghouse								
HC									
CO									
PN									
Other									

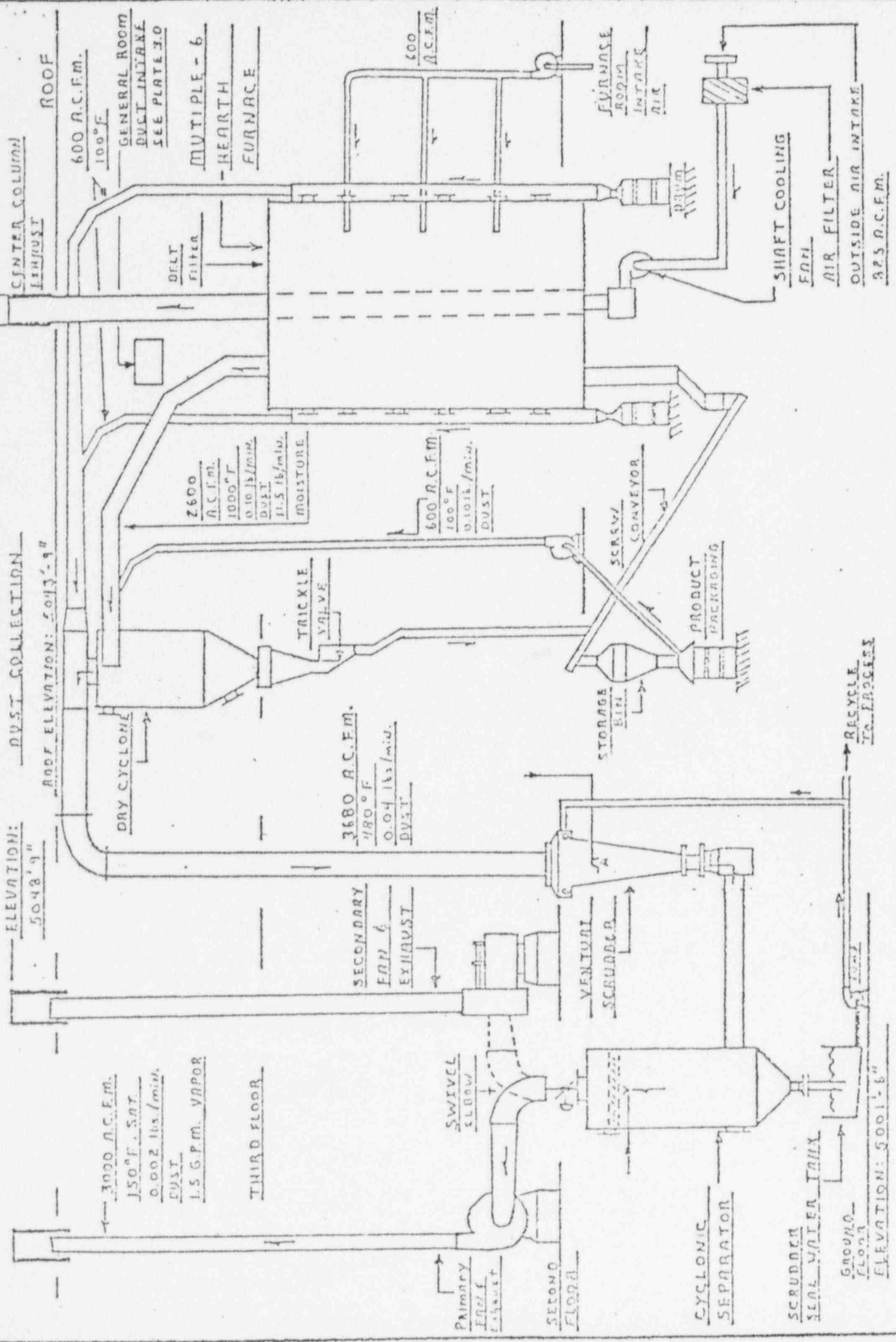
0120731

Signature of Person Legally Authorized to Supply Data .....  
Typed Name & Title ..... Mr. G. L. Schierman, Plant Superintendent

COLORADO DEPARTMENT OF HEALTH  
AIR POLLUTION CONTROL DIVISION  
4210 East 11th Avenue  
Denver, Colorado 80220  
(303) 770-4100

# URAVAN YELLOWCAKE COLLECTION DUST COLLECTION

NOT TO SCALE



3000 ACFM.  
150°F SAT.  
0.002 lb./min. SOLID  
1.5 G.P.M. VAPOR  
1480 D.S.F.M.

# PROPOSED YELLOWCAKE SCRUBBER LIQUID AND MATERIAL BALANCE

3680 A.C.F.M.  
635°F  
0.040 lb./min.

7 G.P.M. @ 15 P.S.I.  
0.029 lb./min.  
0.05%

m.w.  
3 G.P.M.  
30 P.S.I.

10 G.P.M. m.w.  
1 min. ea. hr.

25 G.P.M. 5 P.S.I.  
0.20 lb./min.  
0.10%

THICKENER

1.5 G.P.M.

EMERGENCY m.w.

FLOWMETER

8.5 G.P.M.  
0.067 lb./min.  
0.10%

33.5 G.P.M.  
0.265 lb./min.  
0.10%

33.5 G.P.M.  
0.265 lb./min.  
0.10%

MILL W. MAKEUP

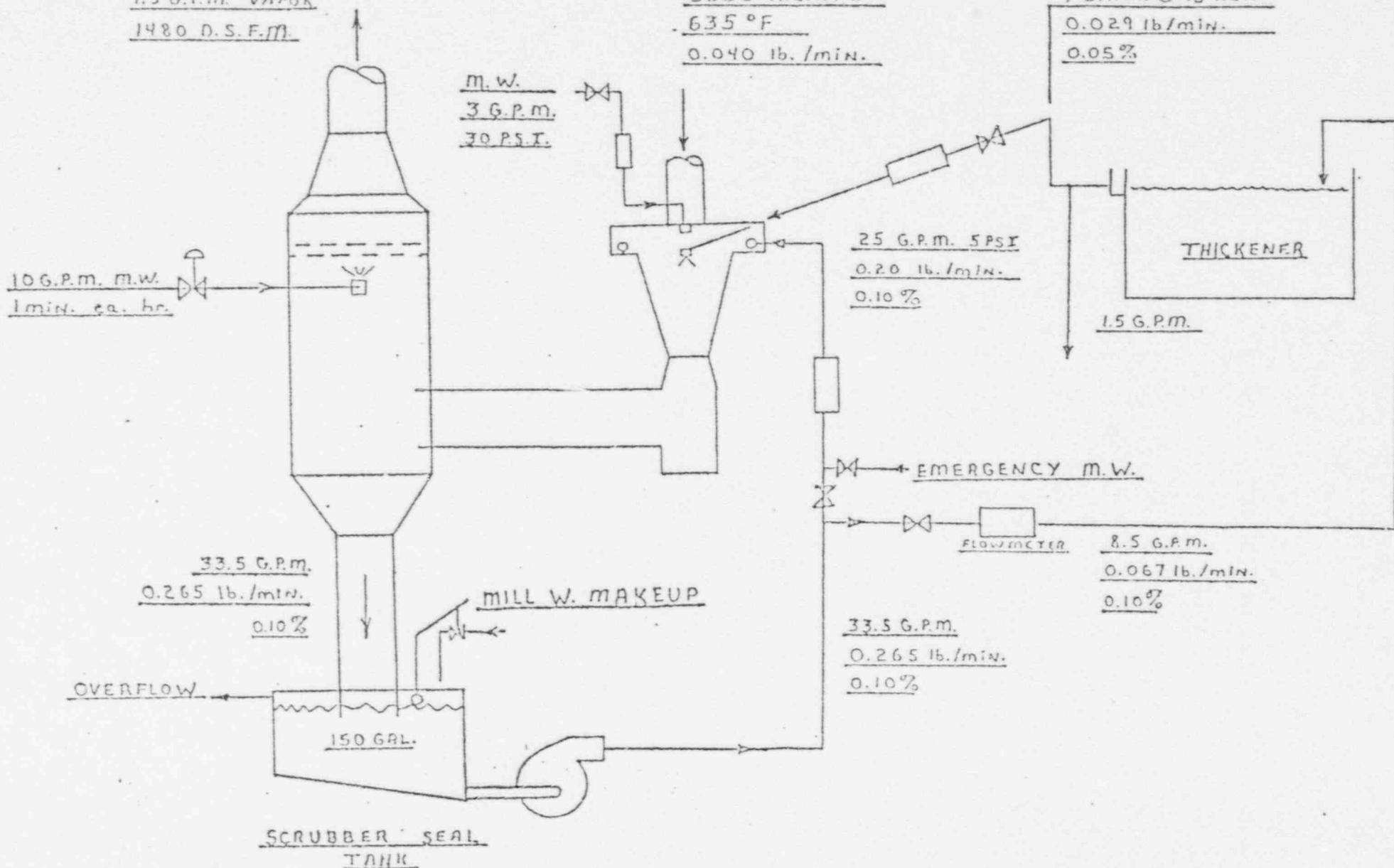
OVERFLOW

150 GAL.

SCRUBBER SEAL  
TANK

PLATE: 2.0

UNION CARBIDE CORP.  
URAVAN, COLORADO



PROPOSED Y.C. DRYER BLDG.  
AIR VENTILATION EMISSION

SCRUBBER

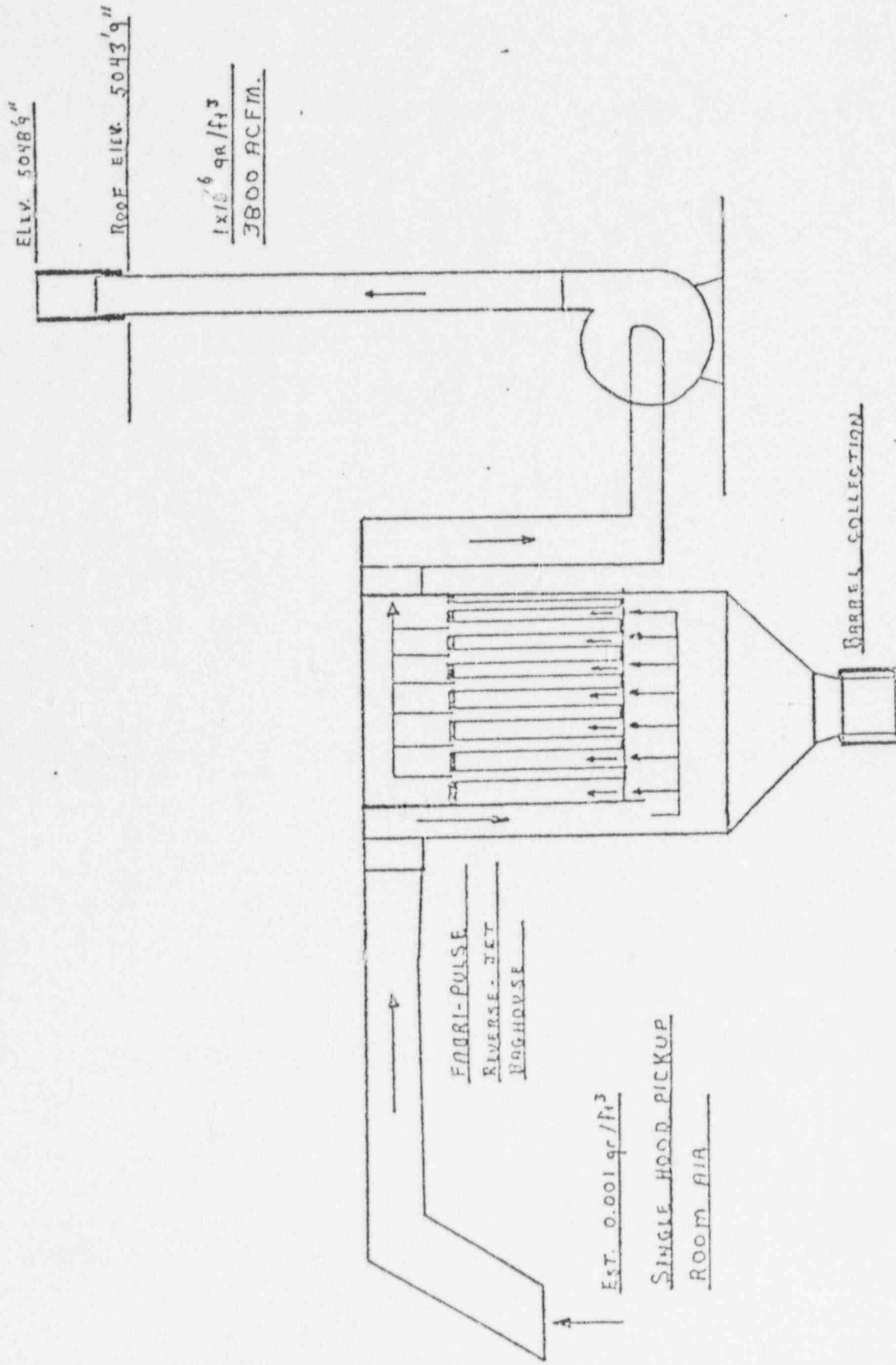


PLATE 3.0

NOT TO SCALE

UNION CARBIDE CORP.  
 URAVAN, COLO.

# URAVAN DRAWER FUND

P. O. Box 94 - 862-7301  
 Uravan, Colorado 81436

Nº 2718

THE MONTROSE COUNTY BANK  
 NATURALITA, COLORADO  
 82-186/1021

PAY Forty & no/100 ----- dollars

TO  
 THE  
 ORDER  
 OF

Colorado Department of Health  
 Air Pollution Control Division

DATE 29 April 1980

AMOUNT \$ 40.00

Uravan Drawer Fund

*[Signature]*  
*R. A. Burt*

⑆102101865⑆ 00236 7⑈

PAYEE: DETACH THIS STATEMENT BEFORE DEPOSITING CHECK

Uravan Drawer Fund

DATE	INVOICE NO.	DESCRIPTION	AMOUNT	DISCOUNT OR DEDUCTION	NET AMOUNT
4-29-80		Filing Fee for Air Pollutant Emissions Notice			40.00
		Acct # 2305-06-03			



URAVAN DRAWER FUND

P. O. Box 94 - 862-7301  
Uravan, Colorado 81436

Nº 2717

THE MONTROSE COUNTY BANK  
NATURITA, COLORADO  
82-186/1021

PAY Forty & no/100 -----dollars

TO  
THE  
ORDER  
OF

Colorado Department of Health  
Air Pollution Control Division

DATE  
29 April 1980

AMOUNT  
\$ 40.00

Uravan Drawer Fund

*W. L. Scherman*  
*R. A. Bell*

⑆102101865⑆ 00236 7⑈

PAYEE: DETACH THIS STATEMENT BEFORE DEPOSITING CHECK

Uravan Drawer Fund

DATE	INVOICE NO.	DESCRIPTION	AMOUNT	DISCOUNT OR DEDUCTION	NET AMOUNT
4-29-80		Filing Fee for Air Pollutant Emissions Notice			40.00
		Acct # 2305-06-03			

## 2.0 PROPOSED CALCINER - TECHNICAL DESCRIPTION

### 2.1 Detailed Drawings

The proposed yellowcake calciner general arrangement, elevations, flow diagrams, and scrubber instrumentation design are represented in detail on the following attached drawings.

1. Drawing No. SF-7403 Changeroom - Alt. #4
2. Drawing No. S-15190 Gen. Arrangement-Ground Floor
3. Drawing No. S-15191 Gen. Arrangement-2nd & 3rd Floor
4. Drawing No. 244-1540 Instrumentation-Calciner
5. Drawing No. 244-1542 Instrumentation-Scrubber
6. Drawing No. S-15192 Sectional Elevations
7. Drawing No. S-15193 Exhaust Details

Plates 1-5 represent simplified drawings of the current calciner, new calciner and scrubber system, and location of the new calciner in the A plant section of the mill.

## 2.2 Environmental Aspects

### 2.2.1 Stack Emissions

Based upon the May 30th 40 CFR190 NUS report submitted to your department, an effort has been made in the following table to determine emission rate comparisons in curies per year for the current operation, the proposed operation with a twenty-five inch pressure drop, and the proposed operation with a fifty inch pressure drop. These emission control scenarios correspond to the 67% and 83% reduction scenarios presented in the NUS report. NUS reduction scenarios were based upon a known 0.24 pounds per hour emission with a theoretical addition of 0.10 pounds per hour coming from the building itself, which would be controlled in the new design by the building ventilation system.

#### RADIOACTIVE STACK PARTICULATE EMISSIONS

##### YELLOWCAKE STACKS - Curies/year

<u>Isotope</u>	<u>Current Operation</u>	<u>Proposed Op. with 25" Press. Drop</u>	<u>Proposed Op. with 50" Press. Drop</u>
U-Nat.	1.608	8.04 E-01	4.02 E-01
Th-230	8.51 E-03	4.26 E-03	2.13 E-03
Ra-226	3.45 E-04	1.73 E-04	8.63 E-05
Pb-210	4.00 E-03	2.00 E-03	1.00 E-03

As shown in drawing No. S-15192, the scrubber system is designed so that if fan mechanical failure occurred, a change-over to a backup fan would not be time consuming or difficult. The system has been designed with the intention that if the twenty-five inch pressure drop across the venturi does not prove adequate to meet 40 CFR 190 regulations, a second fan in series can be installed to boost the drop to fifty inches. The electrical and foundation work needed for the third fan are to be installed pending the outcome of stack emission studies with the twenty-five inch pressure drop. The second fan could be utilized in series with the first during any necessary period needed for delivery of the third fan, if deemed necessary.

Ducted air temperature and pressure are to be monitored through instrumentation at the fan inlet, as shown in drawing No. 244-1542. High temperature and low pressure alarms will be connected to these monitors. Calciner shutdown is controlled through manual operator response to these alarms.

Emission and scrubber efficiency monitoring will begin within two weeks of the startup of this calciner, and will consist of the following:

1. Six Emission Stack Tests/Runs,
2. Three of which will consist of two simultaneous monitoring tests of both scrubber inlet conditions and emission conditions.

Particulate mass determination results would be summarized in report form, and available for review within two weeks of the last run. Radioactive emission rates, by isotope, would tentatively be available within forty-five days of the last run.

40 CFR 190 related radiological doses due to the yellowcake stacks for existing, and both control scenarios are discussed in the May 30th NUS report.

#### 2.2.2. NPDES Discharges

The installation of the new calciner and horizontal vacuum belt filter will not alter the chemical composition or quantity of flows of the industrial process waste-water discharge or of any liquid waste retained for evaporation. Chemical additions and water balances will not be significantly affected.

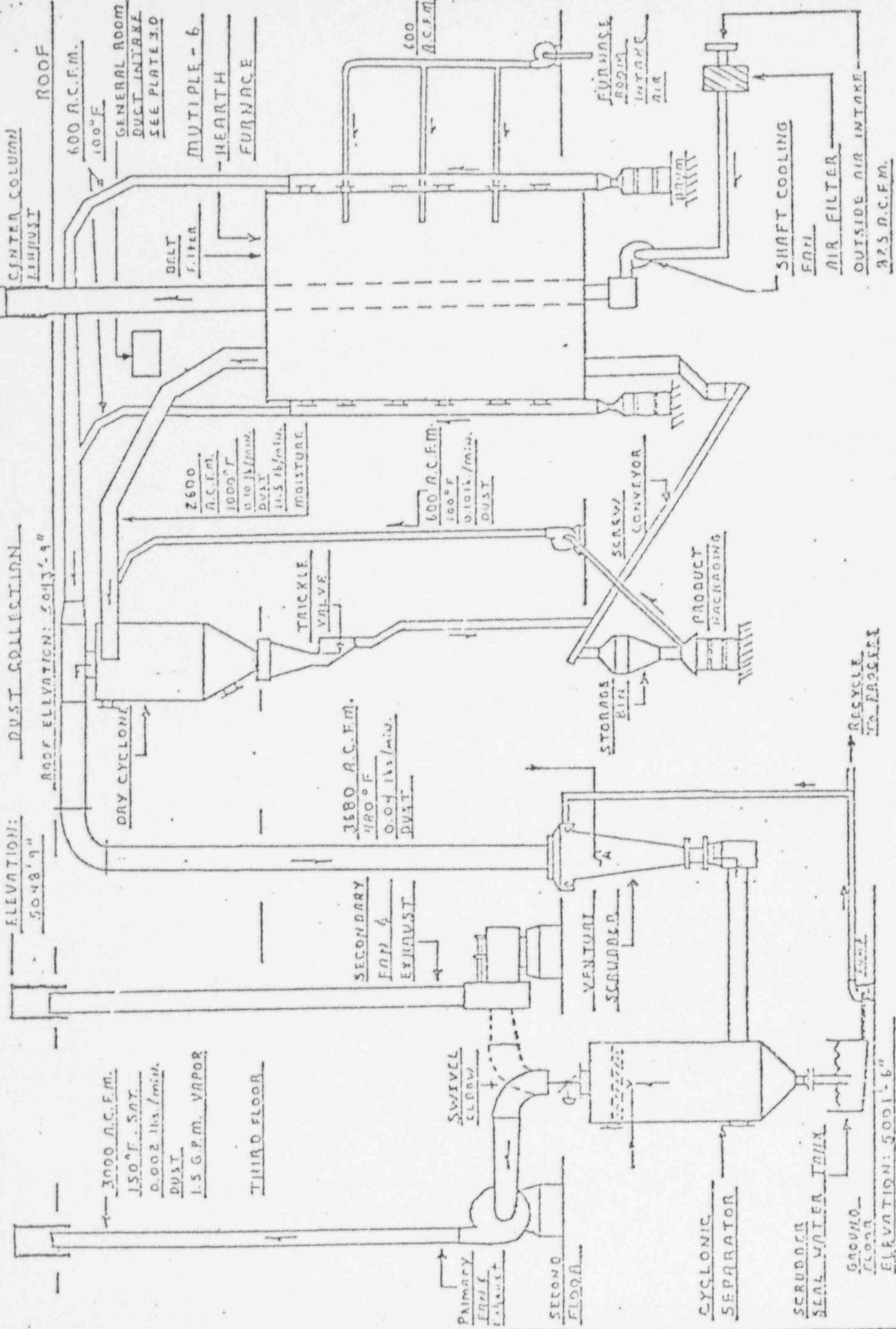
#### 2.2.3. Flood Plain

Based upon the 1978 Dames & Moore Environmental Report for Uravan, at the section of the San Miguel Canyon where the calciner will be located, the maximum elevation for a Probable Maximum Flood is estimated to be 5000 feet. Determination of this is shown on Plate 6.0. The base elevation of the yellowcake calciner is 5000 feet ten inches for the barreling room floor, and 5001 feet six inches for the calciner room floor. The base of the calciner is at 5009 feet eight inches.



NOT TO SCALE

NOT TO SCALE



DUST COLLECTION

ROOF ELEVATION: 5017'-9"

3000 N.C.F.M.  
150°F. SAT.  
0.002 lbs./min.  
DUST  
1.5 G.P.M. VAPOR

THIRD FLOOR

SECONDARY  
FARM &  
EXHAUST

72281/VS

BOOK 1  
SECOND

VENTURE  
SCOUTS

CYCLONIC  
SEPARATOR

SCRUDER  
SEAL WATER TAIL

6 NOV 1967

ELEVATION: 5001'-6"

DRY CYCLONE

3680 A.C.F.M.  
1180 °F  
0.04 lbs/min.  
PVIT

TRICKLE	YOLVER
---------	--------

2600  
A.C.F.M.  
1000' F  
0.10 lb/lb  
DUST  
11.5 lb/lb  
MOISTURE

600' R.C.F.M.  
100°F  
0.1016/min.  
DUST

STORAGE

RECEIVED

<u>PRODUCT</u>	<u>PACKAGING</u>
100% Pure White Paper	50 lb. Bag
80# Bright White Paper	40 lb. Bag
60# Yellow Paper	25 lb. Bag
40# Green Paper	15 lb. Bag
20# Blue Paper	10 lb. Bag
10# Red Paper	5 lb. Bag
5# Orange Paper	2.5 lb. Bag
2.5# Purple Paper	1.25 lb. Bag
1.25# Silver Paper	0.625 lb. Bag
0.625# Gold Paper	0.3125 lb. Bag
0.3125# Black Paper	0.15625 lb. Bag
0.15625# Grey Paper	0.078125 lb. Bag
0.078125# Brown Paper	0.0390625 lb. Bag
0.0390625# Pink Paper	0.01953125 lb. Bag
0.01953125# Light Blue Paper	0.009765625 lb. Bag
0.009765625# Very Light Blue Paper	0.0048828125 lb. Bag
0.0048828125# Off-White Paper	0.00244140625 lb. Bag
0.00244140625# Cream Paper	0.001220703125 lb. Bag
0.001220703125# Ivory Paper	0.0006103515625 lb. Bag
0.0006103515625# Pearl Paper	0.00030517578125 lb. Bag
0.00030517578125# Shell Paper	0.000152587890625 lb. Bag
0.000152587890625# Opal Paper	0.0000762939453125 lb. Bag
0.0000762939453125# Moonstone Paper	0.00003814697265625 lb. Bag
0.00003814697265625# Starlight Paper	0.000019073486328125 lb. Bag
0.000019073486328125# Aurora Paper	0.0000095367431640625 lb. Bag
0.0000095367431640625# Twilight Paper	0.00000476837158203125 lb. Bag
0.00000476837158203125# Dusk Paper	0.000002384185791015625 lb. Bag
0.000002384185791015625# Dawn Paper	0.0000011920928955078125 lb. Bag
0.0000011920928955078125# Sunrise Paper	0.00000059604644775390625 lb. Bag
0.00000059604644775390625# Sunset Paper	0.000000298023223876953125 lb. Bag
0.000000298023223876953125# Midnight Paper	0.0000001490116119384765625 lb. Bag
0.0000001490116119384765625# Indigo Paper	0.00000007450580596923828125 lb. Bag
0.00000007450580596923828125# Violet Paper	0.000000037252902984619140625 lb. Bag
0.000000037252902984619140625# Ultraviolet Paper	0.0000000186264514923095703125 lb. Bag
0.0000000186264514923095703125# X-Ray Paper	0.00000000931322574615478515625 lb. Bag
0.00000000931322574615478515625# Gamma Paper	0.000000004656612873077392578125 lb. Bag
0.000000004656612873077392578125# Delta Paper	0.0000000023283064365386962890625 lb. Bag
0.0000000023283064365386962890625# Epsilon Paper	0.00000000116415321826934814453125 lb. Bag
0.00000000116415321826934814453125# Zeta Paper	0.000000000582076609134674072265625 lb. Bag
0.000000000582076609134674072265625# Eta Paper	0.0000000002910383045673370361328125 lb. Bag
0.0000000002910383045673370361328125# Theta Paper	0.00000000014551915228366851806640625 lb. Bag
0.00000000014551915228366851806640625# Iota Paper	0.000000000072759576141834259033203125 lb. Bag
0.000000000072759576141834259033203125# Kappa Paper	0.0000000000363797880709171295166015625 lb. Bag
0.0000000000363797880709171295166015625# Lambda Paper	0.00000000001818989403545856475830078125 lb. Bag
0.00000000001818989403545856475830078125# Mu Paper	0.000000000009094947017729282379150390625 lb. Bag
0.000000000009094947017729282379150390625# Nu Paper	0.0000000000045474735088646411895751953125 lb. Bag
0.0000000000045474735088646411895751953125# Xi Paper	0.00000000000227373675443232059478759765625 lb. Bag
0.00000000000227373675443232059478759765625# Omicron Paper	0.000000000001136868377216160297393798828125 lb. Bag
0.000000000001136868377216160297393798828125# Pi Paper	0.0000000000005684341886080801486968994140625 lb. Bag
0.0000000000005684341886080801486968994140625# Rho Paper	0.00000000000028421709430404007434844970703125 lb. Bag
0.00000000000028421709430404007434844970703125# Sigma Paper	0.000000000000142108547152020037174224853515625 lb. Bag
0.000000000000142108547152020037174224853515625# Tau Paper	0.0000000000000710542735760100185871124267578125 lb. Bag
0.0000000000000710542735760100185871124267578125# Upsilon Paper	0.00000000000003552713678800500929355621337890625 lb. Bag
0.00000000000003552713678800500929355621337890625# Phi Paper	0.000000000000017763568394002500461778106689453125 lb. Bag
0.000000000000017763568394002500461778106689453125# Chi Paper	0.0000000000000088817841970012502308890533447265625 lb. Bag
0.00000000000000888178419700	

FINANCE  
ROOM  
STAFF  
FILE

### SHAFT COOLING

AIR FILTER

OUTSIDE AIR INTAKE

27.5 N.C.F.M.

RECYCLE  
TO PAPER

PLAYE 1.0

UNION CARBIDE CORPORATION

1480 D. S. F. m.

0.040 lb./min.

30 P.S.I.

1 min. ca. hr.

0.10%

MILL W. MAKEUP

OVERFLOW

150 GAL.

SCRUBBER SEAL  
TANK

0.10 %

0.05 %

THICKENER

1.5 G.P.M.

EMERGENCY M.W.

FLOWMETER

0.10%

0.10%

PLATE: 2.0

UNION CARBIDE CORP.  
URAVAN, COLORADO

PROPOSED Y.C. DRYER BLDG.  
AIR VENTILATION EMISSION

SCRUBBER

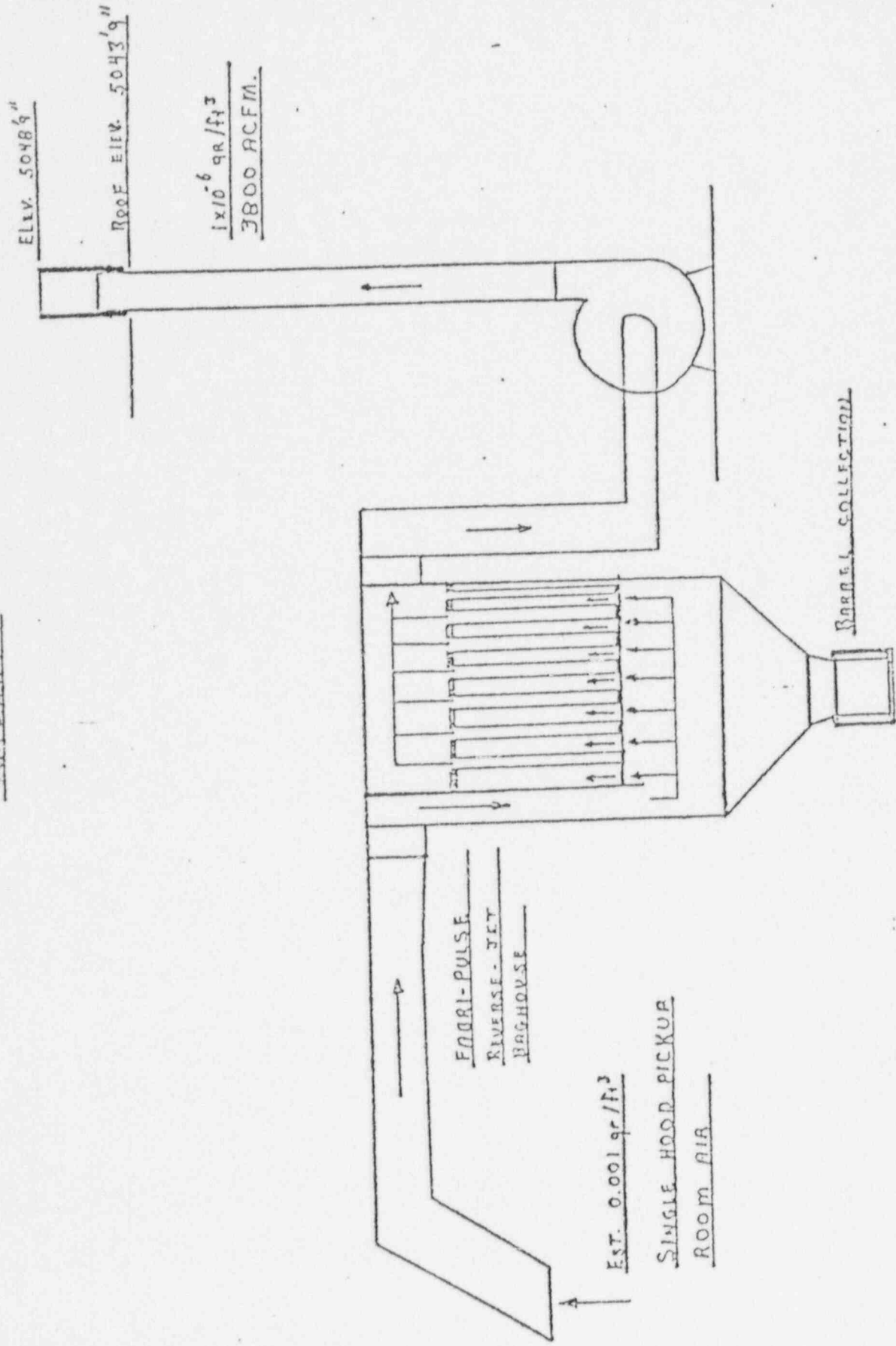


PLATE 3.0

NOT TO SCALE

UNION CARBIDE CORP.  
URAVAN, COLO.

# CURRENT URAVAN YELLOWCAKE CALCINER

SCHEMATIC

CENTER COLUMN  
EXHAUST

3330 A.C.F.M.  
122° F. SAT.  
0.0035 lbs/min.  
DUST

EMERGENCY EXHAUST  
STACK

Roof

THREE TIER  
PACKED  
TOWER

FOURTH FLOOR

6500 A.C.F.M.  
518° F.  
0.7" H<sub>2</sub>O S.P.

THIRD FLOOR

TEN HEARTH  
ROTARY FURNACE

SECOND FLOOR

600 A.C.F.M.

SHAFT COOLING FAN

OUTSIDE AIR  
INTAKE  
825 A.C.F.M.

FIRST FLOOR

PRODUCT PKG.

Product Slurry Drier Feed

DEMISTER

4.7" H<sub>2</sub>O  
STATIC PRESS.

MAKE-UP  
WATER

UNDERFLOW  
RECYCLED

NOT TO SCALE

UNION CARBIDE CORP.

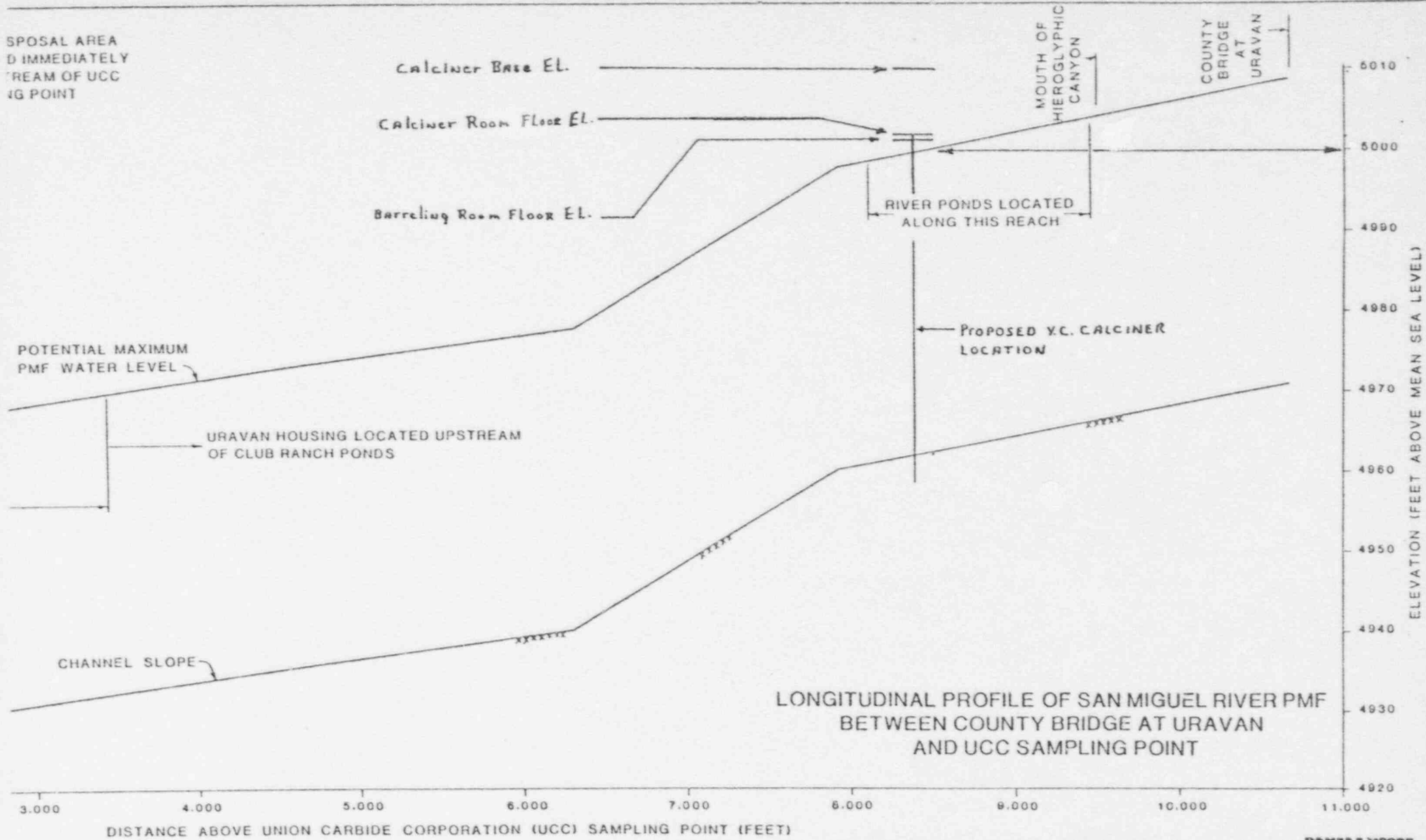
URAVAN, COLO.

PLATE 4.0





WASTEWATER DISPOSAL AREA  
DOWNSTREAM IMMEDIATELY  
UPSTREAM OF UCC  
SAMPLING POINT



DAMES MOORE  
PLATE 2.6-8

UNION CARBIDE CORPORATION  
URAPAN, CO.

PLATE 6.0

## 2.3 Health Physics

The following is a discussion by area of health physics related changes with the proposed yellowcake calciner.

2.3.1. The yellowcake calciner building is designed to be a total wash down facility such that yellowcake buildup on walls and floors can be sprayed and cleaned with water. The current facility does not allow for this type of cleaning system. The proposed facility would be washed down daily with the liquor produced entering floor sumps and returned to the precipitation circuit.

The access doors to the building, and isolated rooms within, are equipped with pneumatic door closures to help maintain an interior negative room pressure as induced by the room ventilation system. Room air dust pickup points are to be located in the vicinity of the top of the calciner. These points are connected to a fabric collector and fan located on the third floor of the building. This collector is of the reverse jet pulse type to minimize maintenance personnel exposure to airborne uranium dust.

The calciner itself is equipped with a double door access arrangement for each hearth whereby negative pressure can be maintained around the seals of each door to prevent movement of uranium dust into the operators environment. This system consists of a channel of air, moving upward to the scrubber system, contained inside a metal trough attached over the calciner access doors. The trough is ducted at the top to the main calciner ventilation exhaust system and at the bottom to a collection drum. Opposite each calciner door, the trough has a similar access door which, when opened, allows the operator to clean the drops and rotary rakes of the calciner, a necessary task. The negative pressure between the doors forces the lighter dust particulates to become entrained in the air flow to the main ventilation duct work while the heavier particulates, not entrained, fall to the collection drum. This reduces the migration of dust particulates to the operators breathing zone, thereby reducing his exposure to uranium.

The current calciner is a single door arrangement which increases dust exposure levels by not having a system to pick up door seal leaks or generated dust from the maintenance operations.

2.3.2 Dewatering of yellowcake by means of the current plate and frame filter presses allows for uncontrollable employee and clothing exposure to moist yellowcake which, if personal hygiene is not maintained, can lead to excessive uranium burdens to the body through the ingestion pathway.

The proposed calciner is equipped with a horizontal belt vacuum filter which drastically reduces potential for employee handling of wet yellowcake. This is essentially in the transport of moist cake from the dewatering equipment to the calciner. Currently, each plate of the filter press is manually scraped by the operator into a hopper. The hopper is then dumped into a repulper where the cake is pumped to the calciner. The proposed system has the dewatered cake falling a short distance off a belt filter into a hopper. The base of the hopper contains an enclosed screw conveyor which moves the cake horizontally to the calciner, and dumps it into the calciner. There is essentially no employee involvement in the transfer of the cake.

2.3.3. Product barreling of the yellowcake produces, during the barrel changing operation, a major source of employee exposure to uranium dust. The current system has a barrel sitting on top of a moveable dolly in a concrete pit, which moves the barrel away from the loading hood. The barrel is then lifted out of the pit by an overhead pulley, and is placed on weighing scales. The movement of the open container of cake generates dust in the vicinity of the employees breathing zone. The proposed system consists of a storage bin to contain the daily production. This bin is emptied daily into product drums mounted on a roller conveyor system. The barrels fit inside a dust pickup hood equipped with two plenums that maintain a negative pressure around the rim of the barrel. Dust generated during the filling operation is vented at 600 cfm. to the main scrubber duct. Movement of open filled barrels is along the horizontal roller system, which will produce less dust than the

present overhead pulley system. Filling operations, occurring at set daily periods, allow for closer and more consistent monitoring of employee breathing zones for uranium dust.

2.3.4. Along with the proposed calciner and horizontal belt filter is the intended installation of a changeroom facility for yellowcake operator personnel. This changeroom facility is to be constructed on the current site of the present calciner or pressroom. The changeroom consists of separate areas for "clean" personnel and "dirty personnel", for both sexes. The dirty area is equipped with a lunch bench, restrooms, bootwash, respirator and paper suit cleaning and storage. Personnel leaving the "dirty" section for the "clean" section pass through a "dirty" locker room, a shower facility, and then a "clean" locker room. Personnel will be required to shower prior to exiting the yellowcake compound area. The lunch facility area will be monitored weekly for removable and fixed alpha. The entire facility can be washed down by hoses. Shower and floor drains return solutions to the yellowcake circuit. Personnel will be equipped with clothing that will remain within the "dirty" side of the changeroom when they leave. The same requirements apply to maintenance personnel.

2.3.5 Monitoring, in respect to health physics, will continue as noted in the 1980 operational monitoring program with changes made as deemed necessary to facilitate maintaining the best possible employee monitoring coverage.

Reference No. 2

NAME: Terry N. Washburn

POSITION: Plant Superintendent

EFFECTIVE DATE: August 1, 1980

EDUCATION: New Mexico State University  
B. Sci. in Mechanical Engineering - 1962

EMPLOYMENT HISTORY: 1962-1965

Humble Oil & Refining  
Production Engineer

1965-1967

Union Carbide Corporation/  
Uravan, Colorado  
Plant Engineer

1967-1973

Union Carbide Corporation/  
Uravan, Colorado  
Maintenance Superintendent

2/1973-6/1973

Union Carbide Corporation/  
Uravan, Colorado  
"B" Plant Superintendent

1973-1980

Union Carbide Corporation/  
Hot Springs, Arkansas  
Vanadium Milling Facility  
Maintenance Superintendent &  
Department Head



## Supplement To Attachment B

### New Yellow Cake Calciner Description

#### 1.0 Introduction

Attachment B of the request for the Minor Health and Safety Amendment submitted to Mr. A. J. Hazle by Mr. R. K. Jones on July 11, 1980 describes the process design features of the new system. This supplement outlines the operational procedures that will be used to minimize employee exposure.

#### 2.0 Alarm and Shut-Off Systems Relating to Personnel Exposure

The emissions from the calciner, product barreling station, and calciner drop plenums are controlled by the venturi scrubber system; the work area atmosphere in the dryer enclosure and packing area is maintained by a separate ventilation system. The alarm point on the venturi scrubber can be set for a range of pressure drops. The features of these systems are as follows:

<u>Event</u>	<u>Response</u>
Pressure loss on the venturi or room ventilation system	Alarms will sound at the barreling station, first floor, second floor of the dryer, and packing area. Light alarm in the filter room and in the Plant 5 control room.

Loss of the emission control units will also stop the feed to the dryer and place the burners on low fire.

Other actions are at the discretion of the operator.

#### 3.0 Cleanup of Spilled Yellow Cake

A vacuum system for cleaning up spills will be installed. The air discharge from the system will pass through an absolute filter (less than one micron particle size) prior to discharge.

#### 4.0 Start-Up Procedures

Repirators will be required in all areas until acceptable airborne concentrations in the working areas are established by field measurement. The exhaust stacks from the operation would be sampled 8 times during the first month of operation, and then monthly for the rest of 1981.

#### 5.0 Change Room Facilities

The new facilities will be built as personnel become available during the six-month shutdown in 1981.

WM-34

PDR

COLORADO DEPARTMENT OF HEALTH  
Division or Section of Radiation & Hazardous Wastes

INTER-OFFICE COMMUNICATION

TO : Union Carbide Uravan File

DATE : January 14, 1981

FROM: Ken Weaver

SUBJECT: Yellowcake calciner authorization

By telcon January 14, 1981 (0930) notified Terry Washburn, Uravan Plant Superintendent of the Department's January 13, 1981 letter provisionally authorizing operation of the yellowcake calciner.

Washburn mentioned a question raised by MSHA about hazards from using natural gas without further protection's but believed this would be resolved.

RLEW/ldb

Ken LK Weaver 1-19-81  
Signature

10067