



UNITED STATES  
NUCLEAR REGULATORY COMMISSION  
WASHINGTON, D. C. 20555

July 27, 1983

- ERM  
- file

Docket No. 50-289

MEMORANDUM FOR: H. Denton T. Speis  
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D. Eisenhut R. Mattson S. Varga  
R. Purple H. Thompson D. Vassallo  
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F. Miraglia C. Heltemes

THRU: John F. Stolz, Chief, Operating Reactors Branch #4,  
Division of Licensing

FROM: James Van Vliet, Project Manager  
Operating Reactors Branch #4, Division of Licensing

SUBJECT: DAILY HIGHLIGHT

TMI-1 Steam Generator Repair Program

GPU Nuclear has recently completed an analysis predicting that steam generator tube thermally induced tensile loads tend to be smaller than previous analyses have indicated. In addition, GPU Nuclear has also observed a loss of initial tensile prestress in a few hundred tubes during the course of the kinetic expansion in adjacent tubes as a result of separation in the defective area of these tubes within the upper part of the tubesheet. These tubes were subsequently kinetically sealed to the tubesheet below the defective area to restore tube integrity.

GPU Nuclear is evaluating the effects of reduced tube tension and loss of prestress on through-wall crack leakage monitoring sensitivity. GPU Nuclear presently expects to submit its evaluation and findings the week of August 8, 1983. This new information will need to be evaluated as part of the staff's Safety Evaluation and will likely delay its issuance by about three weeks.

*James Van Vliet*  
James Van Vliet, Project Manager  
Operating Reactors Branch #4, DL

cc:  
JStolz  
JVan Vliet  
ORB#4 File

8506140287 850125  
PDR FOIA  
DETJENB4-897 PDR

## Inter-Office Memorandum

Date August 3, 1983



Subject Technical Review of Calc. 1101X-5450-014

To N. G. Trikouros, Location  
Manager - Safety Analysis & Plant Control

A technical review has been performed on the subject calculation. The governing equations are given in the calculation and also in a prior calculation 1101X-5450-010. The equations were digitally simulated using CSMP and are given in data sets N1564.ADV4.DATA and N1564.ADV.DATA.

A review of the equations and assumptions given in the subject calculation indicates that they are reasonable. The prior calculation, 1101X-5450-010, has already been reviewed (see Ref 1).

Following are pertinent comments for the two computer programs.

## A. N1564.ADV4.DATA

1. A review of this program indicates that the equations are coded as written in the calculations, except as noted in A.4 below. A random check was made on the value of constants, and none were found incorrect.
2. The MACRO HEM is essentially developed from the prior calculation.
3. This program uses a fixed time step. To check if this time step is sufficiently small, the reviewer halved the step size. The resulting integrated mass flow rate through the ADV was within 1% at the end of the run (10,000 sec); TAVG was within 3%; the reactor system pressure was within 4%; and the pressures of the secondary side were within 13%.
4. The algorithm for controlling the ADV (page 7 of subject calculation) is, in practice, impractical since it may occur too often for an operator to handle. Further, the code logic states the switching algorithm is not to be performed if TAVE is greater than 550°F; this is not stated in the calculations.

Changing the time step in A.3 above changed the switching times, and was the primary cause for the different results. Nonetheless, the algorithm appears to be adequate for this study in determining the cooldown rate and integrated mass flow rate.

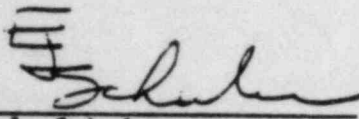
B. N1564.ADV.DATA

1. A review indicates that the equations are coded as written in the calculation. All constants were checked; small variances were found, and they were less than 4%.
2. The fixed time step was replaced by a variable time step for a check. A comparison of results indicate that they are almost identical.

C. Functions and Subroutines Appended to Above Two Programs.

Both programs use FORTRAN functions and subroutines; these are appended to the main program. Most of them are used to calculate water and steam properties.

These functions and subroutines have not been reviewed by the undersigned.

  
E. J. Schuler,  
Engineer - SAPC

EJS/ar

cc: F. G. Broughton, Director - Systems Engineering  
L. C. Pwu, Engineer - SAPC

SUBJECT TMI-1 Cooldown Rate Using  
Atmospheric Dump Valves

CALC. NO. 1101X-5450-014  
SHEET NO. 1 OF 22  
DATE 7-20-83  
COMP. BY/DATE X C Pua / 7-20-83  
CHK'D. BY/DATE E Schuler  
3 AUG '83

## Problem Statement

During a steam generator tube rupture (SGTR) event, ~~with loss of offsite power (LOOP)~~ concern is the method of cooldown and the associated dose release. Procedure guideline require isolation of ~~the affected~~ OTSG's and control the cooldown rate by the Atmospheric Dump Valves (ADV) and/or Turbine bypass valves (TBV). A calculation is presented below on the rate of cooldown and integrated steam <sup>release</sup> ~~loss~~ to the atmosphere by using one ADV valve.

## Method

A Four-node, 2 loop CSMP model is presented in Figure 1. The steam generator secondary in either side is modeled as a saturated two-phase volume which is



SUBJECT .....

CALC. NO. 1101X-5450-014  
 SHEET NO. 2 OF 22  
 DATE 7-20-83  
 COMP. BY/DATE R.C.P.  
 CHK'D. BY/DATE 3 AUG 83

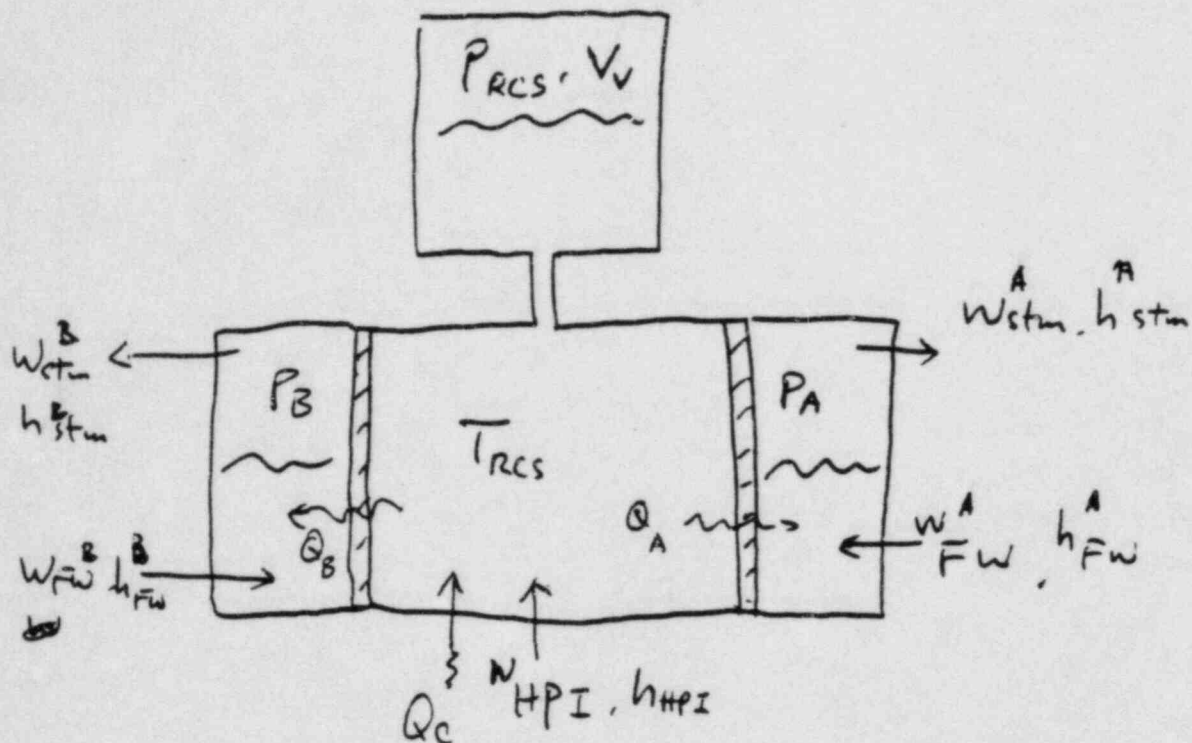


Figure 1 Two-Loop Four Node CSMP model

Similar to the pressurizer model of a calc # 110/X-5430-01

Since it is repeatedly used in both ~~sets~~ of the OTSG's, a MACRO in CSMP language is set up in the following format:

$$DXDT, DPDT, LSG, ALFA = HEM(X, P, WFW, HFW, WST, HST, QT, V)$$

where

$$DXDT = \frac{dx}{dt} = \text{rate of quality change in OTSG}$$

$$DPDT = \frac{dP}{dt} = \dots \text{ pressure } \dots$$

$$LSG = \text{Steam generator level}$$

$$ALFA = \alpha = \text{void fraction in the OTSG}$$

$$x = \text{steam quality}$$

$$P = \text{pressure}$$

$$WFW = \dot{W}_{FW} = \text{Feedwater flowrate}$$

$$HFW = h_{FW} = \text{enthalpy of feedwater}$$

$$WST = \text{steam flowrate}$$

$$HST = h_{st} = \text{steam } \text{flowrate} \text{ enthalpy}$$

( $h_g$ , i.e., specific enthalpy of saturated steam was used)

$$\begin{aligned}
 Q_T &= \text{heat removal by the OTSG} \\
 &= UA \Delta T \\
 &= UA (T_{\text{res}} - T_{\text{SG}})
 \end{aligned}$$

$$\begin{aligned}
 V &= \text{total volume of one OTSG} \\
 &= 3307 \text{ ft}^3
 \end{aligned}$$

At a given time the system's <sup>status</sup> ~~condition~~,  $x$  and  $P$  plus boundary conditions  $w_{\text{FW}}$ ,  $h_{\text{FW}}$ ,  $w_{\text{ST}}$ ,  $h_{\text{ST}}$  and  $Q_T$  are given to calculate the rate of change  $\dot{x}$  and  $\dot{P}$ . Then CSMP is used to solve  $x$  and  $P$  at the next time step.

Also,  $\alpha$ ,  $L_{\text{SG}}$  and  $x$  are interrelated by

$$M_T = \frac{V}{x \cdot v_g + (1-x) v_f} = \text{Total mass in OTSG}$$

$$M_F = M_T \cdot (1-x) = \text{fluid mass in OTSG}$$

$$\alpha = \frac{x v_g}{x v_g + (1-x) v_f}$$

$$L_{\text{SG}} = \frac{M_F \cdot v_f}{\text{SG cross section area}} \times 12 - 6 \quad \left( \begin{array}{l} \text{in inches there} \\ \text{is a 6" section} \\ \text{has no heat trans} \end{array} \right)$$

where S.G. x-s Area = 88.9 ft<sup>2</sup> (each)

On the primary side, the steam bubble and the liquid phase are treated separately.

Since in the depressurization process the steam bubble behaves very much ~~as~~ adiabatically, the adiabatic expansion law is used, i.e.

$$P_{RCS} V_v^{1.3} = \text{constant}$$

The liquid phase then expand or contract by the net heat input.

$$M_R C_p \frac{dT_{RCS}}{dt} = Q_{C_A} + Q_{RCP} - Q_T^A - Q_T^B$$

where

$M_R$  = total liquid mass in RCS  $= M_R(0) + \int_0^t \dot{m}_{in} dt$

$C_p$  = heat capacity of water

$T_{RCS}$  = RCS temp.

$Q_C$  = core heat (ANS Table is used)

$Q_{RCP}$  = RCP pump heat input

then

$$V_v = V_T - M_R \cdot V_L(T_{RCS}, P)$$



where  $V_T = \text{Total RCS volume (incl. PRZR)}$   
 $= 11500 \text{ ft}^3 \text{ (constant)}$

If there is RCP heat input.  $T_H$  and  $T_C$  is given in the following manner.

$$T_H = T_{RCS} + Q_T / 2 W_{RC} C_p$$

$$T_C = T_{RCS} - Q_T / 2 W_{RC} C_p$$

If the RCP are tripped, the RCS will be stagnated (no N.C. assumed) then an infinite  $W_{RC}$  should be input by the user (rather than zero) to result in  $T_{RC} = T_H = T_C$ .

Several Lag functions have to be introduced in the CSMP program to avoid ~~phi~~ infinite loops in the iteration. The results will be off by the lag time (3 second was chosen), but does not affect the general correctness.

HPZ is assumed to be initiated at 1615 psia RCS pressure and throttled back at subcool margin exceeding 120°F. (overcool criteria  $SCM = 100^\circ F$ )

ADV Discharge rate was chosen to be 93 lb/sec (23%)  
 at set opening pressure (1050 psia) and  
 decrease according to the square root of  
 the OTSG pressure.

Controlling the ADV is an operator action and  
 here is assumed that <sup>should</sup> ~~at~~ any time the cooldown  
 rate ~~should be less~~ <sup>becomes greater</sup> than 50°F/hr the operator  
 shall throttle the ADV area to 1/2.

### Calculation

The run attached using the following initial  
 and boundary condition.

$$Power = 2568 \text{ MWt}$$

$$T_{avg} = 579^\circ\text{F}$$

No RCP

$$L_{SG} (') = 120''$$

following trip A<sub>1</sub> <sup>OTSG</sup> controlled at 200".

using EFW. maximum flow rate ~~133 gpm~~  
 $= 133 \text{ lb/sec (950 gpm)}$

B is controlled at 30", TSV

Set at 1025 psia. TSV flow = 280 gpm

Program ADV.4. DATA is attached.

For long term cooling, a single volume  
 CSMP program is sufficient ( $t > 10,000 \text{ sec}$ )  
 Since the ADV is full open (not throttled)

Program AN. DITTO shall restart ADV & DITTO  
 at 10,000 sec. the OTSG pressure is 1346 psia.  
 the integrated steam loss to atmosphere  
 is  $4.412 \times 10^5 \text{ lbm}$ . Primary to secondary  
 $\Delta T$  is approximately zero. The secondary  
 ADV discharge rate is proportional to the square root  
 of OTSG pressure. i.e.

$$M C_p \frac{dT}{dt} = Q_c(t) - W_{st} \cdot (h_g(P) - h_{EFW})$$

where  $M = \text{RCS mass}$

$T = \text{RCS temp} \approx \text{OTSG Temp.}$

$P = T_{\text{sat}}$ .

The result is  $T$  cooled to  $275^\circ \text{F}$  in another  
 10,000 second.

SUBJECT

The results of the CSMP runs ADV4.DAT8  
and restart ADV.DAT8 for cool-down and  
ADV discharge are

<u>Time</u> <u>(hr)</u>	<u>Targ</u> <u>(°F)</u>	<u>Integrated Steam Discharge</u> <u>(lbm)</u>
0	579	0
1	444	$2.2 \times 10^5$
2	367	$3.6 \times 10^5$
3	331	$4.5 \times 10^5$
6	285	$6.3 \times 10^5$
16	225	$1.3 \times 10^6$



10 7 22

110/X-500

LCP

TITLE PROGRAM TO STUDY TMI-1 COOLDOWN USING ONE ADV ...  
ADV4.DATA CREATED FROM ADV2.A.DATA ON 6-3-83

- \* THROTTLED ADV TO COOLDOWN RATE OF 50 F/HR AT TEMP BELOW 550 F
- \* CLDN = COOLDOWN RATE (F/HR), ADV AREA WILL BE HALF IF EXCEEDING THIS
- \* TAVG-TSG FOR OTSG HEAT TRANSFER DURING TRANSIENT(NO LOG MEAN)
- \* TWO LOOP MODEL
- \* STEAMING A OTSG, B OTSG CONTROLLED AT 1025 PSIA AND 30 IN LEVEL
- \* A OTSG ADV STUCK OPEN, FLOW = 93 LB/SEC AT 1050 PSIA, SQRT(PRESS) DEP
- \* ADIABATIC PHZR MODEL
- \* VERY LARGE RCS LOOP FLOW = 1.E8(LB/SEC) ASSUMED (ALL RCP'S OFF)
- \* TO EQUATE TH AND TCI PUMP HEAT = 0
- \* USE MACRO TO CALCULATE DYNAMIC VARIABLES
- \* S.G. CROSS SECTION AREA = 88.9 FT\*\*2(PER OTSG)
- \* SIMPLE HOMOGENEOUS STEAM GENERATOR MODEL TO STUDY HEAT REMOVAL
- \* DECAY(TIME) = ANS DECAY HEAT TABLE
- \* ASME STEAM TABLE USED

MACRO DXT,DPDT,LSG,ALFA=HEM(X,P,WFW,HFW,WST,HST,QT,V)

VG=VGAS(P)

VF=VFLD(P)

HG=HVAP(P)

HF=HLIQ(P)

HGP=(HVAP(P+10.)-HVAP(P-10.))/20.

VGP=(VGAS(P+10.)-VGAS(P-10.))/20.

HFP=(HLIQ(P+10.)-HLIQ(P-10.))/20.

VFP=(VFLD(P+10.)-VFLD(P-10.))/20.

MT=V/(X\*VG+(1-X)\*VF)

MF=MT\*(1-X)

MM=X\*HG+(1-X)\*HF

ALFA=X\*VG/(X\*VG+(1-X)\*VF)

LSG=MF\*VF/88.9\*12-6

ΔMT=(VG-VF)

HMT=(X\*VGP+(1-X)\*VFP)

C=(WST-HFW)\*(X\*VG+(1-X)\*VF)

ΔHGH=HF

F=(HFW-HMT-WST\*(HST-HMT)\*QT)/MT

F=X\*HGP+(1-X)\*HFP-.1R5\*(X\*VG+(1-X)\*VF)

DXT=(C\*E-H\*F)/(A\*E-H\*0)

DPDT=(A\*F-C\*0)/(A\*E-H\*0)

ENDMAC

CONSTANT VRCS=10800., A0=1.32E5, POWER=2568., WRCS=1.E8,CLDN= 50

CONSTANT RCP=0., V=3307., HMF=400.,HEFW=60., WMFW=1458.,WEFW=137.

IVPRZ=900.

VPRZ=IVPRZ

P=930.

CDPS=-CLDN/3600

IP=P

Q=(RCP\*POWER)\*3.413E6/3600.

LSG=120.

DTLM=ITAVG-ITSG

DT=Q/1.34/WRCS

ITAVG=579.

U=Q/2/AREA/DTLM

AREA=(LSG\*6.)/12./52.\*40

ITC=ITAVG-DT/2

ITH=ITAVG+DT/2

TSG=ITSG

ITSG=535.85

IPRCS=2160.

VR=VL(ITAVG,IPRCS)

ALFA=1-MF\*VF/V  
 VG=VGAS(P)  
 IX=ALFA/VG/(ALFA/VG+(1.-ALFA)/VF)  
 TAVG=ITAVG

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MP=IMR

X1=IX

X2=IX

P1=P

P2=P

DYNAMIC

GRCS=(POWER\*DECAY(TIME)\*RCP)\*3.413E6/3600.

PROCEDURE WHPI=HPI(P RCS)

IF(P RCS.LT.1.15.) GO TO 78

WHPI=0.

GO TO 79

78 WHPI=PUMP(P RCS)\*2

IF(SCM.GT.120.) WHPI=0.

79 CONTINUE

ENDPROC

HST=HVP(P)

QT1=U\*AREA1\*DT1

QT2=U\*AREA2\*DT2

CP=SPHT(TAVG,P RCS)

THP=TAVG\*QT/W RCS/CP/2.

TC1P=TAVG\*QT1/W RCS/CP

TC2P=TAVG\*QT2/W RCS/CP

TH=REALPL(ITH,3.,THP)

TC1=REALPL(ITC,3.,TC1P)

TC2=REALPL(ITC,3.,TC2P)

VP=VL(TAVG,P RCS)

DT1=(TH+TC1)/2-TSG1

DT2=(TH+TC2)/2-TSG2

QT=QT1+QT2

UTDT=(GRCS-QT)/MR/CP

AREA1=(LSG1+6)/12\*40/52

AREA2=(LSG2+6)/12\*40/52

WST=930\*SURT(P1/1050)

PROCEDURE WFW1,HFW1,WST1 = EFW1(LSG1,TAVG,UTDT)

IF(TAVG.GT.550) GO TO 30

IF(UTDT.LT.CDPS) GO TO 40

30 WST1=WST

GO TO 50

40 WST1=WST/2.

50 CONTINUE

HFW1=HFW

IF(LSG1.GT.200.) GO TO 77

WFW1=HFW

GO TO 76

77 WFW1=0.

76 CONTINUE

ENDPROC

PROCEDURE WFW2,HFW2,WST2 = EFW2(P2,LSG2)

IF(P2.GT.1025) GO TO 15

WST2=0.

GO TO 16

15 WST2=280.

16 IF(LSG2.GT.30.) GO TO 17

WFW2=HFW

GO TO 18

17 WFW2=0.

18 CONTINUE

```

VPRZ=MR*VP=10000.
PP=IPRCS*(700/(11500.-MR*VP))*1.3
SCM=TSS=TH
* DUMMY VARIABLE TO AVOID VF BEING WIPED OUT BY TSS
TSS1=TSS
PRCS=REALPLT(IPRCS,3.0,PP)
DXDT1,DPDT1,LSG1,ALFA1=HEM(X1,P1,WFW1,HFW1,WST1,HST,QT1,V)
DXDT2,DPDT2,LSG2,ALFA2=HEM(X2,P2,WFW2,HFW2,WST2,HST,QT2,V)
MR=INTGRL(IMP,WHP1)
Zx1=INTGRL(IX,DXDT1)
Zx2=INTGRL(IX,DXDT2)
ZP1=INTGRL(IP,DPDT1)
ZP2=INTGRL(IP,DPDT2)
TAVG=INTGRL(ITAVG,DTDT)
PROCEDURE X1,TSG1,TSS,X2,TSG2=LIMIT(Zx1,Zx2,PRCS)
IF(Zx1.GF.1.0) Zx1=1.0
IF(ZP1.LT.15) ZP1=15.
IF(Zx2.LE.0.0.OR.Zx2.GE.1.) CALL FINISH
IF(LSG2.GT.300.0R.LSG2.LT..05) CALL FINISH
X1=Zx1
X2=Zx2
P1=ZP1
P2=ZP2
CALL TSAT(ZP1,TSGP1)
CALL TSAT(ZP2,TSGP2)
TSG1=TSGP1
TSG2=TSGP2
CALL TSAT(PRCS,TSS)
MST=INTGRL(0.,WADV)
WADV=WST1+WST2
ENDPRU
NOSORT
CALL DEBUG(2.0,T
* WRITE(21,99) TIME,TAVG,PRCS,LSG1,LSG2,WST1,MST,P1,P2
99 FORMAT(1X,10F9.1)
TERMINAL
METHOD RECT
TIMER FINTIM=10000,PRODEL=10, DELT=2., OUTDEL=20
PRINT TAVG,PRCS,VPRZ,P1,P2,LSG1,WST1,WST2,MST
PAGE XYPLOT
* OUTPUT TIME , P2(0,1200),P1(0,1200)
* OUTPUT TIME,WHP1
OUTPUT TIME,MST
OUTPUT TIME, PRCS
* OUTPUT TIME,TH(200.,600.),TC2(200.,600.),TSG2(200.,600.)
* OUTPUT TIME,TH(200.,600.),TC1(200.,600.),TSG1(200.,600.)
* OUTPUT TIME, VPRZ
* OUTPUT TIME,LSG1(0,300),LSG2(0,300)
OUTPUT TIME,WST1(0,200),WST2(0,200)
END
STOP
C FUNCTION OF HPI HEAD CURVE
FUNCTION PUMP(P)
DIMENSION PI(6),PM(6)
DATA PI/15.,615.,1015.,1515.,2015.,2415./
DATA PM/69.7,63.5,55.6,51.3,41.9,33.1/
CALL INTP(PI,PM,6,P,PP)
PUMP=PP
RETURN
END
C FUNCTION TO CALCULATE SUBCOOLED FLUID ENTHALPY
FUNCTION HFLD(T,P)
CALL ENTHAF(T,P,HL)
HFLD=HL

```



[illegible]



C3922.,4435.,4979.,5566./  
 IF(I8K.EQ.2)GO TO 20  
 CALL INTP(PRS,FLQ,13,P,YP)  
 MOODY=YP  
 RETURN  
 20 CALL INTP(PRS,POS,13,P,YP)  
 MOODY=YP  
 RETURN  
 END  
 FUNCTION DECAY(T)  
 DIMENSION TI(28),DI(28)  
 DATA TI/0.,1.,2.,4.,6.,8.,10.,20.,40.,60.,80.,100.,  
 C200.,400.,600.,800.,1000.,2000.,4000.,6000.,8000.,10000.,  
 C2.E4,4.E4,6.E4,8.E4,1.E5,2.E5/  
 DATA DI/.0675,.0625,.059,.0552,.0533,.0512,.05,  
 C.045,.0396,.0365,.0346,.0331,.0275,.0235,.0211,.0196,.0185,.0157,  
 C.0128,.0112,.0105,.00965,.00795,.00625,.00566,.00505,.00475,.004/  
 CALL INTP(TI,DI,27,T,DY)  
 DECAY=DY  
 RETURN  
 END

110/A-

5650-01X

14922

SUBROUTINE PSAT (DEGF, PSIA)

CALCULATES SATURATION PRESSURE GIVEN TEMPERATURE  
 IN DEGREES F IN RANGE 32 TO 662 DEGREES.

REF. - ASME STEAM TABLES - FOURTH EDITION  
 SECT. 5 (P. 17)

REAL\*8 DEGF, TREDU, PSIA, THETA, BETAT, BETAK

CONVERT TEMPERATURE TO REDUCED TEMP

THETA = TREDU (DEGF)

GET REDUCED SATURATION PRESS (BETA(K) = THE K FUNCTION)

BETA = BETAK (THETA)

CONVERT TO ABSOLUTE PRESSURE

$$PSIA = (BETA * 2.2120 * 7 * 0.025 * 0 * 0 * 0.2) / (9.806650 + 0 * 0.453592370 * 0)$$

BOUNDARY CHECKS

CALL HOUNDS (PSAT, 1, DEGF, PSIA, 1)

RETURN

END

SUBROUTINE TSAT (PIN, DEGF)

RETURNS SATURATION TEMPERATURE GIVEN A PRESSURE  
 IN PSIA IN THE RANGE 0 TO 2398.22.

USES A SIMPLE BISECTION METHOD TO CONVERGE  
 ON ON TSAT BY CALLING BETA (K).

REAL\*8 PIN, DEGF, TA, TR, TMID, PRESS, EPSLON, PMIN, PMAX,  
 BETA, BETAK, TREDU, PREDU

INTEGER ITER

TITLE PROGRAM TO COOLDOWN RATE BY USING ADV AT TMI  
ADV.DATA

110/X-5450 01,  
158 2

\* CONTINUATION OF TWO LOOP MODEL ADVA.DATA RUN

\* AT 10000 SEC TOTAL STEAM LOSS THROUGH TBV AND ADV IS 4.412E5 LBM  
CONSTANT POWER = 2568., V= 12000., DELAY=10000, HEFW=60

P=134.6

IP=P

IT=350

M=V\*50

CP=1.25

DYNAMIC

HST = HVAP(P)

WST = 93.\*SQRT(P/1050)

W=DECAY(TIME\*DELAY)\*POWER\*3.413E6/3600.=WST\*(HST-HEFW)

OTDT = Q/M/CP

ZT= INTGRL(IT,OTDT)

PROCEDURE P,T=LIMIT(ZT)

ZP=0

CALL PSAT(ZP,ZT)

IF(ZP.LT.20) CALL FINISH

P=ZP

T=ZT

ENOPRO

MST=INTGRL(4.4124E5,WST)

NOSORT

CALL DEBUG(2,0.)

TERMINAL

METHOD RECT

TIME= FINITIME=100000, PPDEL=100., DELT=10, OUTDEL=100.

PRINT TIME,T, WST,Q,P,MST

PAGE XYPLOT

LABEL TMI COOLDOWN USING ONE ADV

OUTPUT TIME,T

OUTPUT TIME,P

OUTPUT TIME,WST

OUTPUT TIME,Q

OUTPUT TIME,MST

END

STOP

C\* FUNCTION TO CALCULATE VAPOR ENTHALPY

FUNCTION HVAP(P)

U=ALOG(P)

IF(P.LE.450.)GO TO 2

IF(P.LE.2190.)GO TO 3

U=U-7.0

HVAP=(((((0.37170+16001\*U-0.91118126001)\*U-0.2444781002)\*U

-0.27217176002)\*U-0.44206896002)\*U-0.46351642002)\*U

+0.11876082004

RETURN

2 HVAP=(((((1-0.36740-04\*U-0.56620-03)\*U+0.435075980-02)\*U

-0.145350400-01)\*U+0.227759190-01)\*U

+0.8555091700)\*U+0.14228318002)\*U+0.11059625004

RETURN

3 HVAP=1.19251E3+6.416805E-2\*P-4.9871952E-5\*P\*\*2

+0.5502391E-8\*P\*\*3-9.3721615E-12\*P\*\*4

RETURN

END

C\* FUNCTION TO CALCULATE LIQUID ENTHALPY

# TMI-1 Cooldown Using One Atmosphere

Dump Valve

C.C. PWR 6-21-83

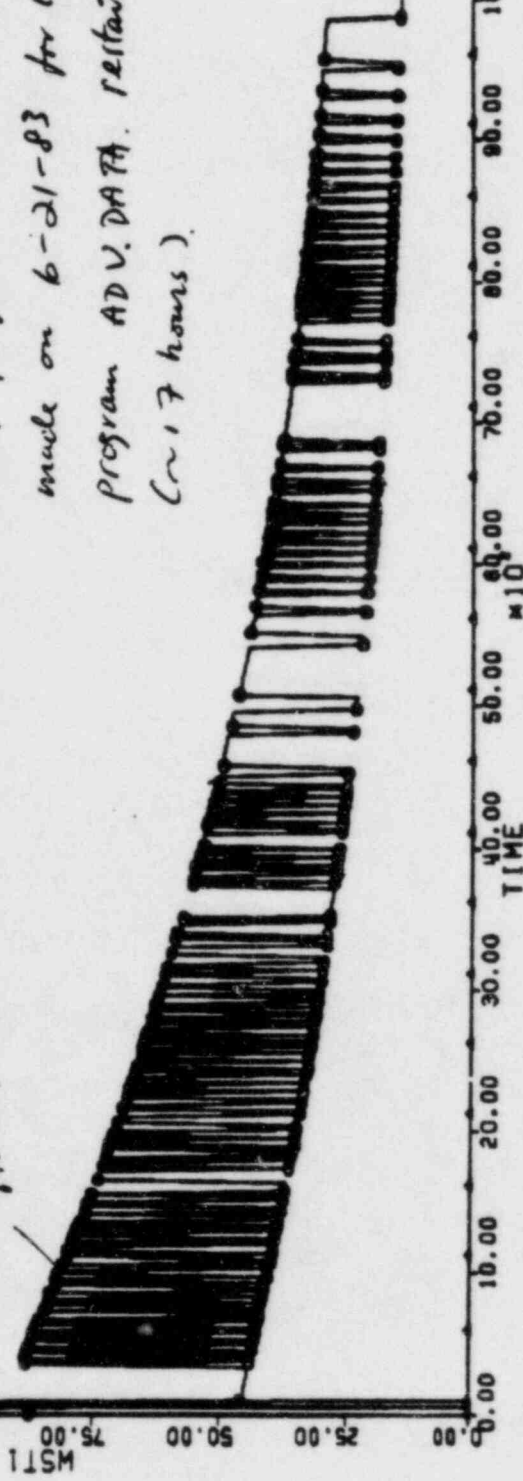
- ADV controlled to limit RCS Cooldown rate not exceeding 50°/hr instantaneously
- EFW throttled to maintain 50% Q146 operate range level

- 1.0 ANS Decayheat. No RCP heat input

- CSMP program ADV4.DAT runs #J111111 made on 6-21-83 for the first 1000 sec
- Program ADV.DAT. restart to 6000 sec (17 hours)

(L8/sec)  
1.1 TBV  
steamline  
(TBV Flow through 015B B)

ADV Flow through steamline A



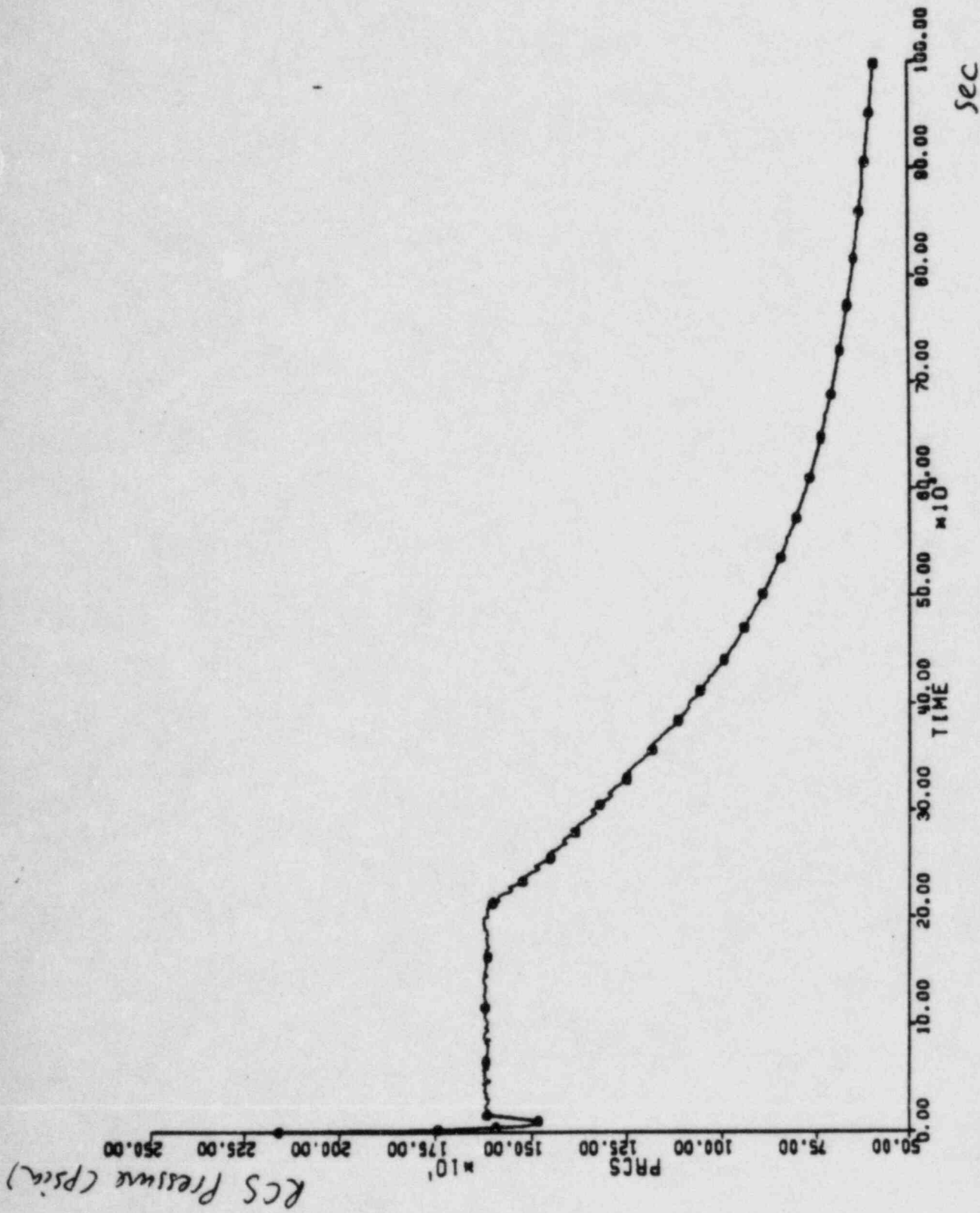
Seconds

Accumulated Steam Loss

Time (hr)	Mass (lbm)	RCS Temp (°F)
0	0	579
1	$2.2 \times 10^5$	464
2	$3.6 \times 10^5$	367
3	$4.5 \times 10^5$	331
4	$6.8 \times 10^5$	285

110/K-5252-014

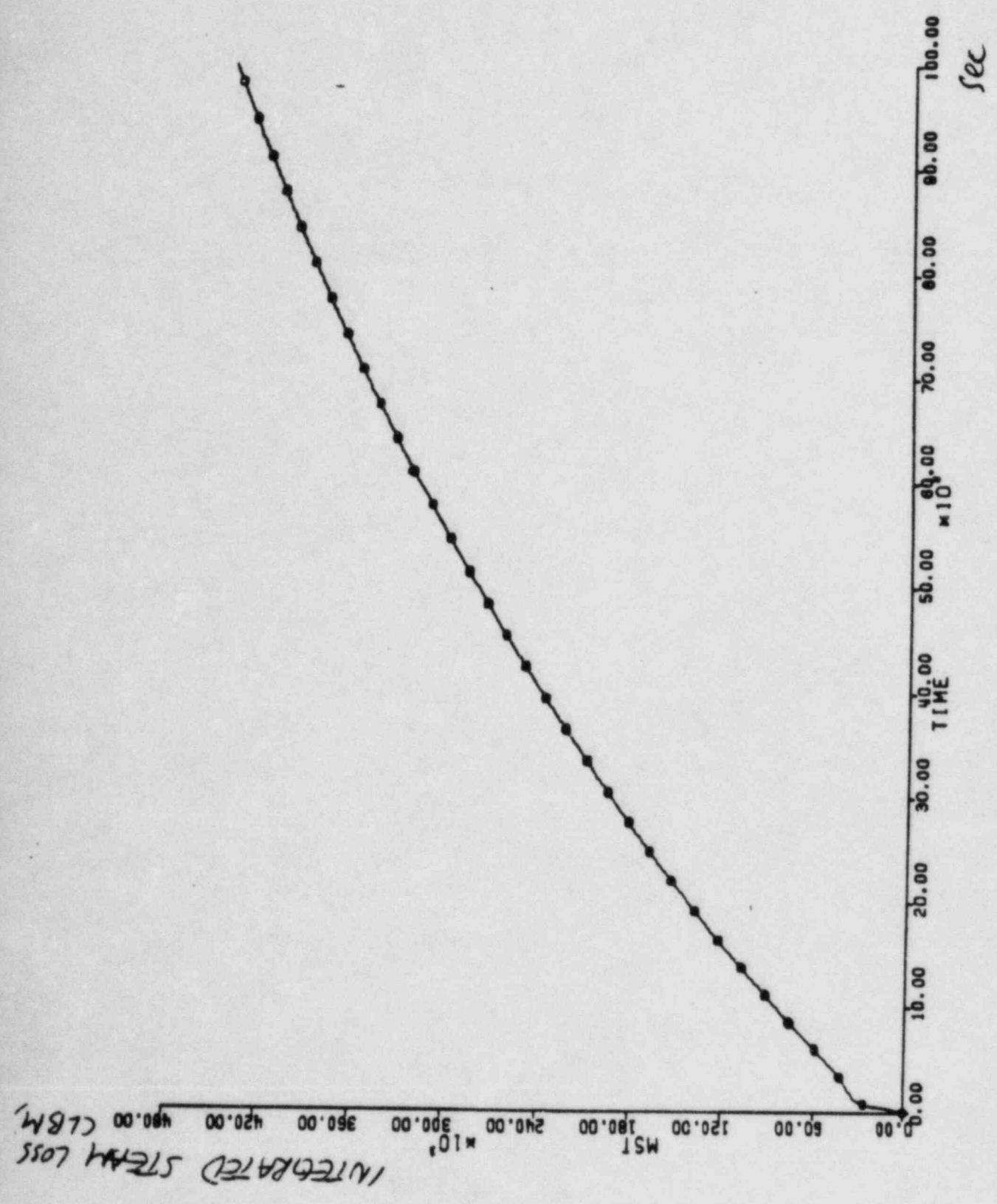
1707





110/x-5250-014

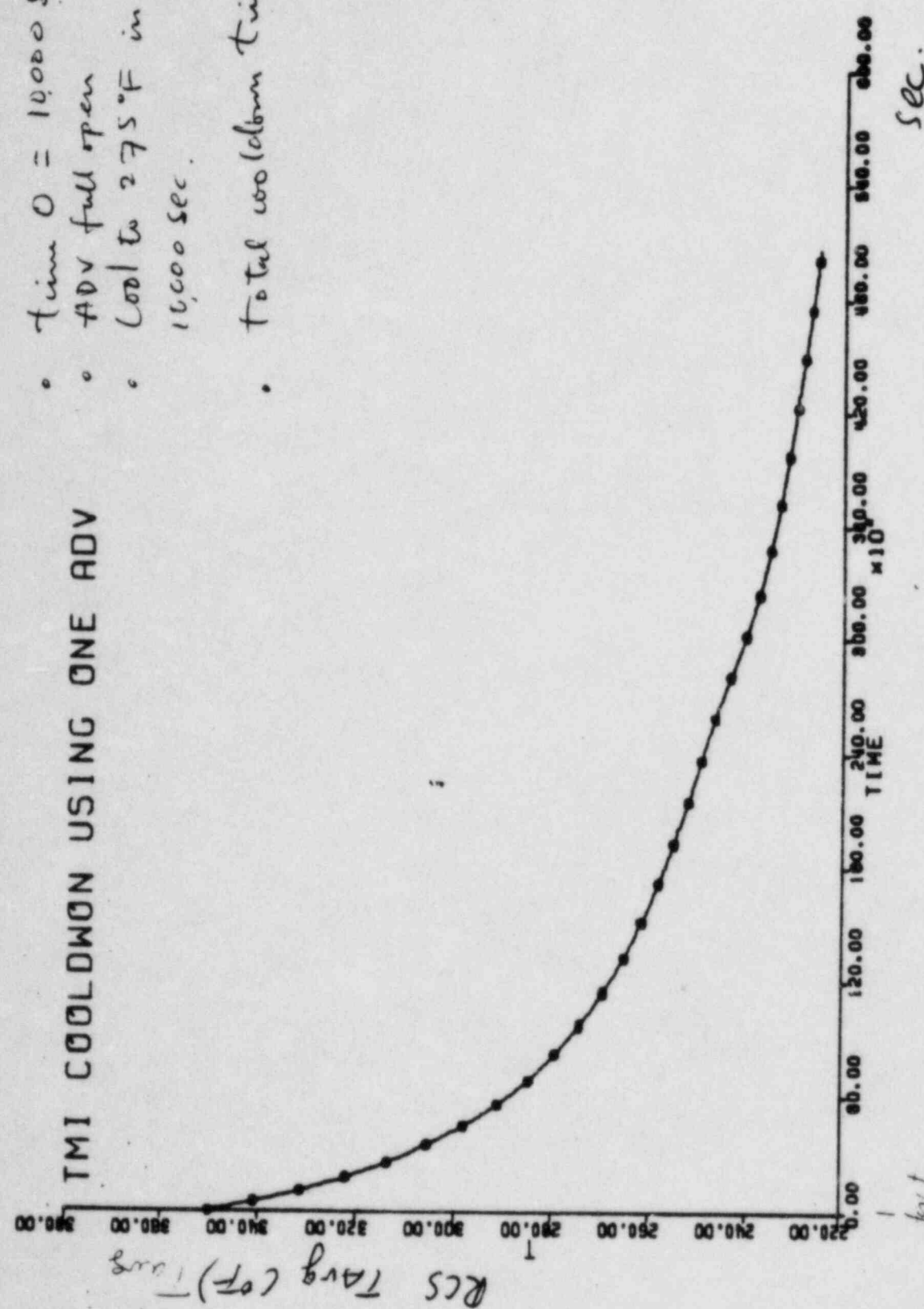
18 of 22



ADV DATA 6-4-13

TMI COOLDOWN USING ONE ADV

- Time 0 = 10000 Sec.
- ADV full open
- Cool to 275°F in another 10000 Sec.
- Total cooldown time  $\approx 6$  hr



110/x5250-014  
19 07 22

20 8 22

