

DRAFT

INDIAN POINT 3  
COMPONENT COOLING SYSTEM

A. SUMMARY

A.1 INTRODUCTION

The component cooling system (CCS) is evaluated for its ability to perform its heat removal function during the recirculation phase of all LOCAs and during all transient events. The primary function of the system following an accident is to remove residual and sensible heat from residual heat removal (RHR) heat exchangers, RHR pumps, safety injection pumps, charging pumps, and supply water to the auxiliary component cooling pumps for recirculation pump cooling.

The analysis is carried out under the following conditions:

- The system was operating in the normal mode of cooling prior to the LOCA or transient.
- No operator action to recover the system following failure or to correct deficiencies in the system are considered in this analysis for the first hour following an initiating event.
- System success is: one of three pumps starts and operates for 24 hours; and one heat exchanger continues to operate for 24 hours.

A.2 RESULTS

Table 1 summarizes the results obtained for the component cooling system analysis. Two cases of electric power are presented: "No Loss of Offsite Power" and "Loss of Offsite Power." Three boundary conditions for each electric power case are analyzed: power at all 480V buses, loss of power at a single bus, and loss of power at two 480V buses.

The analysis has revealed the following dominant contributors to failure of the CCS to supply a sufficient amount of cooled water to time  $t = 24$  hours:

- |  | <u>Mean</u>          |
|--|----------------------|
| • Case 1 - No Loss of Offsite Power.                   |                      |
| - Power at all 480V buses                              |                      |
| • Passive valve failure (service water supply) (95.5%) | $1.0 \times 10^{-7}$ |
| - Power at two 480V buses                              |                      |
| • Failure of the two operable pump trains (94%)        | $1.6 \times 10^{-6}$ |
| - Power at one 480V bus                                |                      |
| • Failure of the operable pump train (99.9%)           | $8.3 \times 10^{-5}$ |

- Case 2 - Loss of offsite power Mean
  - Power at all 480V buses
    - Random failures in the pump trains (63%)  $1.9 \times 10^{-7}$
    - Passive valve failure (service water supply)  $1.0 \times 10^{-7}$   
(31%)
  - Power at two 480V buses
    - Failure of the two operable pump trains  $3.0 \times 10^{-5}$   
(99.7%)
  - Power at one 480V bus
    - Failure of the operable pump train (99.9%)  $1.5 \times 10^{-3}$

No comparison is made to WASH-1400 results as there is no comparable system analysis in WASH-1400.

### A.3 CONCLUSIONS

The component cooling system is required to support plant operations and will be operating at the time of the initiating event. For this reason, this system is unusual in relation to the plant standby emergency systems in that the dominant contributors to system failure, with power available to all pumps, are passive valve and pipe failures.

## B. SYSTEM DESCRIPTION

### B.1 SYSTEM FUNCTION

The CCS is one of three subsystems of the auxiliary coolant system (ACS) of Indian Point 3. It is a closed loop cooling system which is designed to remove residual and sensible heat from various primary plant components during power operations, shutdown operation, and under accident and transient conditions. The system also provides a barrier between the primary plant and the environment to prevent radioactive releases to the environment.

A block diagram and a simplified system piping arrangement are presented in Figures 1 and 2. Success of the system is defined as: one of three CCS pumps operating initially, followed by a second pump as power is available; and one of two CCS heat exchangers operating supplying postaccident loads.

### B.2 BASIC DESCRIPTION

The CCS consists of: Three pumps, two CCS heat exchangers which are cooled by service water, two CCS surge tanks, and two supply and return headers. Table 2 presents the normal and emergency flows required to the CCS and the number of pumps and heat exchangers required during various plant conditions.

The CCS pumps are horizontal, centrifugal pumps rated at 3,600 gpm at 150 psi. During normal plant operation, two of the three pumps are required to supply the necessary flow for plant cooling loads. During accident conditions, one of three pumps is required at the start of the recirculation phase to supply the necessary flow for the plant emergency cooling loads followed by a second pump as power becomes available.

The three CCS pumps are always lined up to the common pump discharge header and pump return header. The pump discharge header cross-tie valves and the pump suction header cross-tie valves are normally open during power operation. Both CCS heat exchangers are fed from the common pump discharge header. Low discharge pressure on either heat exchanger supply header (which indicates insufficient capacity) is annunciated on the ACS panel in the control room and starts the third CCS pump.

Each CCS pump requires a minimum flow of 500 gpm for the removal of pump heat. A low flow in the CCS supply header of 1,500 gpm is alarmed in the control room at the ACS panel.

The CCS pumps are supplied from the following 480V switchgear buses:

- Pump No. 31, Bus No. 5A
- Pump No. 32, Bus No. 2A
- Pump No. 33, Bus No. 6A

Each of these 480V switchgear buses is supplied by separate emergency diesel generators.

The CCS surge tanks are located in the primary auxiliary building (PAB) and have a normal working volume of 1,000 gallons. The surge tanks accommodate changes in operating volume of the CCS due to changes in operating temperature. The free volume of each tank is sufficient to accommodate an in-leakage from a rupture of a reactor coolant pump thermal barrier cooling coil for three minutes. Makeup to the tanks for system leakage is normally provided by the flash evaporator through a manual valve. The primary water storage tank is the alternate makeup supply for the surge tanks. The surge tanks are normally vented to atmosphere; however, high radiation detected at the CCS return headers causes automatic closing of the vent valves. Relief valves on the surge tanks discharge to the waste holdup tank to provide pressure relief when the normal vents are closed. The high radiation condition is alarmed in the control room. Surge tank levels are indicated and alarmed in the control room.

The two CCS heat exchangers are shell and tube-type heat exchangers which are cooled by the service water system. The heat exchangers are designed to remove  $3.14 \times 10^7$  Btu/hr at a shell side  $\Delta T$  of 12°F with 5,320 gpm CCS flow and a tube side  $\Delta T$  of 7°F with 9,100 gpm service water flow. Both heat exchangers are lined up on the component cooling side and the service water side. After recirculation has started, service water is lined up to both heat exchangers and the component cooling loops are split into two distinct subsystems. During accident conditions, only one heat exchanger is required for heat removal. The heat exchanger outlet temperature is monitored and alarmed in the control room as is header return temperature.

The CCS is basically two distinct systems from the heat exchangers back to the CCS pumps. The necessary cooling lines are branched off of these main supply and return headers. Most of the components cooled by the CCS receive flow during all plant conditions; the exceptions are discussed in the following:

- Reactor coolant pump cooling. Two series, motor-operated, isolation valves are provided for the reactor coolant pump supply line, the reactor coolant pump motor cooling return line, and the thermal barrier return line. These valves are automatically closed upon receipt of a containment isolation phase B signal. Each valve in a single line receives power from a separate 480V MCC (either 36A or 36B) which in turn receives power from the vital switchgear buses. FCV-625 in the return line from the reactor coolant pump thermal barriers also closes on a high flow condition in this return line. This high flow condition is indicative of a thermal barrier cooling coil failure. Closure of FCV-625 limits the amount of in-leakage from this failure.



- Excess letdown heat exchanger cooling. The supply line to this heat exchanger contains two, series, air-operated, normally open valves. These valves are designed to fail closed on loss of power or loss of air. These valves receive a containment isolation phase A automatic close signal. The return line from this heat exchanger contains two series, air-operated valves. One of the valves is normally closed. In all other respects, the operation of these valves is the same as the supply valves.
- Residual heat removal heat exchanger cooling. Each RHR heat exchanger receives component cooling water from a separate CCS supply header. Each RHR heat exchanger has a normally closed motoroperated valve located in the CCS outlet line. These valves receive an automatic open signal from the engineered safeguards actuation system.

The three safety injection pumps receive flow during all plant conditions. Two safety injection pumps are supplied from one CCS supply header; the third safety injection pump is supplied from the other CCS supply header. Each pump drives an attached circulating pump which is capable of supplying the cooling requirements for the safety injection pump using the water contained in the CCS supply headers. The CCS outlets of the three safety injection pumps are monitored for flow and alarmed in the control room on low flow.

The two RHR pumps also receive flow during all plant conditions, one from each supply header. Flow from these pumps is indicated locally and alarmed in the control room on low flow.

There are four auxiliary component cooling pumps which are used to supply component cooling water to the engineered safeguards system recirculation pumps. Two pumps supply a single recirculation pump from a single CCS supply header. These pumps are included in the low pressure recirculation system analysis and, therefore, are excluded from this analysis.

### 8.3 SYSTEM OPERATION DURING EMERGENCY CONDITIONS

As stated previously, two of the three CCS pumps are required to be in operation to support plant power operation and both CCS heat exchangers will be in operation (receiving service water). The following paragraphs discuss the response of this system to various emergency conditions.

- Unit Trip, No Blackout and No Safety Injection. When the unit trips and no blackout or safety injection occurs, the system will remain in operation as it was before the event since all power requirements will have transferred from the unit auxiliary transformer to the station auxiliary transformer, and the CCS pumps will continue to operate.

- Unit Trip, With Blackout and No Safety Injection. When this condition occurs, all CCS pumps are tripped. Electrical power is reestablished using the emergency diesel generators. CCS pumps are automatically started by this event as a function of energized (live) 480V buses.

The CCS pump is started for this condition to protect the reactor coolant pumps (RCP) lower radial bearing and seal package since the charging pumps will have tripped and RCP seal and lower radial bearing water will be derived from hot reactor coolant system (RCS) water. The component cooling water will cool this hot RCS water as it passes by the thermal barrier heat exchanger.

- Unit Trip, With Blackout and With Safety Injection. When this condition occurs, all CCS pumps are tripped. Electrical power is reestablished using the emergency diesel generators. The following events will occur in the component cooling loop:
  - Valves 822A and 822B (RHR heat exchangers) are opened.
  - The auxiliary component cooling pumps are started to protect the motors of the recirculation pumps from the containment accident atmosphere.
  - The shaft driven circulating pumps will be running when the safety injection pumps run and will supply cooling services for these pumps.

These events occur automatically as a result of the engineered safeguards sequence signal. When the injection phase safeguards is completed and the recirculation phase is entered into, two CCS pumps or one CCS pump are started by recirculation phase switches RS-2 and RS-5. RS-2 will start one pump; RS-5 another pump if all four 480V buses are energized and a second service water pump is running. Positioning RS-2 to the "On" position will start pump 33; if it failed to start, pump 32 would be started; and if pump 32 failed to start, pump 31 would be started. This action is independent of the supporting service water system pumps. Positioning switch RS-5 to "On" will (providing power is available and two of the selected recirculation phase service water pumps are running) start pump 32. If pump 32 fails to start or is running, pump 31 is started.

- Unit Trip, No Blackout With Safety Injection. If there is a safety injection signal and the unit trips with no blackout, the CCS pumps which were running will continue running and the standby pump will start.

#### B.4 SUPPORT SYSTEMS

Successful operation of the CCS requires operation of the service water system and the electric power system. All three CCS pumps receive power from the 480V switchgear buses supplied by the emergency diesel generators. Both CCS heat exchangers receive service water from the conventional service water header.

## B.5 INSTRUMENTATION AND CONTROLS

Control of the CCS pumps is accomplished by the plant operator from the ACS panel in the control room.

The control switch for each pump breaker is located at the ACS panel in the control room; status light indications are above each switch. As each pump breaker control circuit is identical, only the circuit for pump no. 31 will be discussed.

The control switch has four positions (spring-return to Auto).

- Pull-out. The pump is disabled from starting by any automatic start signal. With the switch in this position, the "Safeguards Equipment Locked Open" alarm will be annunciated on the safeguards panel in the control room.
- Stop. The pump breaker is tripped open.
- Auto. The pump will be started for any one of the following conditions:
  - Low discharge header pressure during normal operation.
  - Timed start on a "Unit Trip with Blackout or No SI" condition.
  - Timed start on a "SI and No Blackout" condition.
  - Automatic start during SI and blackout when shifting from the injection phase to the recirculation phase.

NOTE: The operator must make the switchover, automatic starting is a result of recirculation phase switches RS-2 and RS-5 being turned to "On" by the operator.

- Start. The pump will be started.

While the pump is running it can be tripped by:

- Placing the control switch to the Stop or Pull-out position
- Undervoltage on the associated 480V switchgear bus
- Blackout and SI conditions
- Overload.

All motor-operated or air-operated valves used for containment isolation are operated from the containment isolation panel in the control room. The RHR heat exchanger outlet motor-operated valves are operated from the ACS panel in the control room.

Automatic operation of the CCS in response to emergency conditions has been discussed in the preceding paragraphs. The standby CCS pump will start automatically in response to a low header pressure from either

supply header (sensed at the heat exchanger inlet) or in response to a safety injection signal.

During system operation, header pressure, supply and return temperature, header flow, and individual component flows are monitored in the control room. Abnormal system conditions are alarmed in the control room on the ACS panel.

#### B.6 TECHNICAL SPECIFICATIONS

The plant technical specifications require that the reactor not be brought above the cold shutdown condition unless:

- Two CCS water pumps together with their associated piping and valves are operable. This condition may be modified to allow one of the two operable pumps to be out of service provided it is restored to an operable status within 24 hours.
- Two CCS heat exchangers and associated piping and valves are operable. One CCS heat exchanger or other passive component may be out of service for a period not to exceed 48 hours provided the system still operates at design accident capability.
- Two auxiliary component cooling pumps, one per each recirculation pump, together with their associated piping and valves are operable.
- Two auxiliary component cooling pumps serving the same recirculation pump may be out of service, provided at least one is restored to an operable status within 24 hours and at least one auxiliary component cooling pump serving the other recirculation pump is demonstrated to be operable.
- If the CCS is not restored to meet the above requirements within the times specified, then:
  - If the reactor is critical, it shall be brought to the hot shutdown condition utilizing normal operating procedures. The shutdown shall start no later than at the end of the specified time period.
  - If the reactor is subcritical, the reactor coolant system temperature and pressure shall not be increased more than 25°F and 100 psi, respectively, over existing values.
  - In either case, if the requirements for operable components are not satisfied within an additional 48 hours, the reactor shall be brought to the cold shutdown condition utilizing normal operating procedures. The shutdown shall start no later than the end of the 48-hour period.



## B.7 TESTING AND MAINTENANCE

1. Automatic starting of the CCS pumps and the auxiliary component cooling pumps in response to recirculation switchover is performed every refueling cycle.

Periodic testing of the CCS pumps is required by ASME Section XI. The required frequency of testing is monthly during normal plant operation. ASME Section XI also requires monthly testing of the auxiliary component cooling pumps. Pump operability is checked annually using 3PT-A9. In addition to the annual operability check, plant operating procedures require a weekly shift of operating CCS pumps.

Routine monitoring of the CCS is performed by the plant operators to determine system status.

2. Periodic maintenance is performed as required on the components of the CCS system. This maintenance includes such items as lubrication, inspection, and adjustment.
3. Contribution of Maintenance.

A review of plant work permits revealed two maintenance actions on CCS pumps in 4-1/2 years of plant operation. (This excludes cold shutdown periods.) Using the data from the work permits, we obtain for the probability of pump unavailability due to maintenance the following distribution:

Mean:  $1.84 \times 10^{-2}$

Unavailability of a component cooling pump due to maintenance

Variance:  $1.64 \times 10^{-4}$ .

Upon completion of pump maintenance, testing is performed to determine pump operability and to ensure correct system lineup. At the completion of this testing, the pump is returned to its normal lineup (auto or running).

## B.8 OPERATOR INTERACTION WITH THE COMPONENT COOLING SYSTEM

As this system is required to support normal plant operation, most operator errors that affect system operation will be annunciated or indicated in the control room within a short period of time after their occurrence. These actions include placing the standby pump switch in the "Pull-Out" position, or mispositioning manual or power operated valves. These errors do not contribute to system unavailability on demand during accident conditions.

Operator error after maintenance is precluded by the testing that is performed at the completion of the maintenance and the requirements imposed on system operability.



Operator error during the shift from injection phase to recirculation phase of LOCA events is possible and is discussed in the recirculation system description.

Operator error during the splitting of the CCS and service water system is discussed in Section D.5 of this analysis.

#### B.9 COMMON CAUSE ANALYSIS

Table 3 represents a listing of the components included in the component cooling system analysis, their failure mode, their location, and their susceptibility to various causes of common cause failure. The contribution of common cause failures to system failure is presented in Section D.6.

## C. SYSTEM FAULT TREE MODELING AND RESULTS

### C.1 EVENT TREES

In the event trees, the CCS is included with failure of the recirculation phase events.

### C.2 SYSTEM FAULT TREES

Figure 3 presents the fault tree developed for the Indian Point 3 CCS. The top event, "No or Insufficient Flow (NOIF) from the Component Cooling Water System", may be further defined as flow delivered to the supply headers that is less than the capacity of one component cooling pump.

### C.3 FAULT TREE CODING

Table 3 is a list of basic events, their failure modes, the corresponding codes, and the failure rates associated with these events.

### C.4 MINIMAL CUTSETS

The minimal cutsets for the CCS are identified in Table 4.

The single event cutsets, block F of Figure 1, consist of piping failures which result in system failure and failures in the service water supply to the CCS heat exchangers. The piping failure effects table, (Table 5) presents the results of the analysis of piping failures on the CCS.

The two event cutsets, blocks D and E of Figure 1, consist of failures in the two heat exchanger trains, failures in the supply and return headers, and failures of the two surge tanks. Block D consists of the following basic events:

- TXV34--C: Service water inlet valve, SWN-34, transfers closed
- TXV36--C: Service water outlet valve, SWN-36, transfers closed
- UXV759AC: Heat exchanger 31 inlet valve, 759A, transfers closed
- UXV765AC: Heat exchanger 31 outlet valve, 765A, transfers closed
- UHE0031L: Heat exchanger 31 loss of cooling capability (rupture, plugging, etc.)
- UTK0031L: CC surge tank 31 leak or rupture.

Block E consists of the following basic events:

- TXV34-1C: Service water inlet valve, SWN-34-1, transfers closed
- TXV36-1C: Service water outlet valve, SWN-36-1, transfers closed
- UXV759BC: Heat exchanger 32 inlet valve, 759B, transfers closed
- UXV765BC: Heat exchanger 32 outlet valve, 765B, transfers closed
- TXV33--C: Service water crossover valve, SWN-33, transfers closed

- TXV33-1C: Service water crossover valve, SWN-33-1, transfers closed
- UHE0032L: Heat exchanger 32 loss of cooling capability (rupture, plugging, etc.)
- UTK0032L: CC surge tank 32 leak or rupture.

Blocks A, B, and C of Figure 1 identify the components that comprise the three event cutsets. Block A consists of the following basic events:

- JBS-35AD: No power at switchgear bus 5A
- 4BS-331D: No control power at switchgear bus 5A
- UXV760AC: Pump 31 suction valve, 760A, transfers closed
- UXV762AC: Pump 31 discharge valve, 762C, transfers closed
- UCV761AQ: Pump 31 discharge check valve, 761A, transfers closed/fails to open
- UPM0031S: Pump 31 fails mechanically; start or run
- UM00031S: Motor for pump 31 fails
- UCC0031F: Control circuit for pump 31 fails.

Block B consists of the following basic events:

- JBS-32AD: No power at switchgear bus 2A
- 4BS-333D: No control power at switchgear bus 2A
- UXV760BC: Pump 32 suction valve, 760B, transfers closed
- UXV762BC: Pump 32 discharge valve, 762B, transfers closed
- UCV761BQ: Pump 32 discharge check valve, 761B, transfers closed/fails to open
- UPM0032S: Pump 32 fails mechanically; start or run
- UM00032S: Motor for pump 32 fails
- UCC0032F: Control circuit for pump 32 fails.

Block C consists of the following basic events:

- JBS-33AD: No power at switchgear bus 6A
- 4BS-333D: No control power at switchgear bus 6A
- UXV760CC: Pump 33 suction valve, 760C, transfers closed
- UXV762CC: Pump 33 discharge valve, 762C, transfers closed
- UCV761CQ: Pump 33 discharge check valve, 761C, transfers closed/fails to open
- UPM0033S: Pump 33 fails mechanically; start or run
- UM00033S: Motor for pump 33 fails
- UCC0033F: Control circuit for pump 33 fails.

D. QUANTIFICATION BOUNDARY CONDITION, OFFSITE POWER AVAILABLE

D.1 QUANTIFICATION OF SINGLE FAILURES (BLOCK F) (HARDWARE)

The single event failures consist of piping failures which fail the entire CC system, no flow from the conventional service water header, and service water valve SWN-31 transferring closed.

- No flow from the conventional service water header. This failure results in plant shutdown and is detected upon occurrence. This event is quantified at the event tree level and is shown here only for completeness.
- Pipe failures. Table 5 identifies the pipe sections whose failure results in CCS failure. The mean and variance for failure in a single section of pipe is:

Mean:  $8.60 \times 10^{-10}$

Probability of failure per  
hour per section

Variance:  $6.00 \times 10^{-17}$ .

We have determined 17 major sections of CCS piping whose failure results in system failure. This results in the following piping contribution to failure:

Mean:  $1.46 \times 10^{-8}$

Probability of failure per  
hour

Variance:  $1.24 \times 10^{-13}$ .

- SWN-31 transfers closed. This valve is normally open and the failure of interest transfers closed. This failure mode results in a loss of service water flow to the CCS heat exchangers which causes high temperature alarms on the CCS heat exchanger outlet. Recovery from this failure during normal plant operation consists of transferring the service water supply to the CCS heat exchangers to the other service water header. The mean and variance for this event are:

Mean:  $9.15 \times 10^{-8}$

Probability of failure per  
hour

Variance:  $1.01 \times 10^{-4}$ .

The single event contribution to system failure per hour is now:

$Q_{\text{Block F}} = \text{piping} + \text{valve}$

$= 1.06 \times 10^{-7}$

$\text{Variance}_{\text{Block F}} = 1.53 \times 10^{-14}$ .

The failures described above require immediate plant shutdown if they occur during plant operation. For this reason, single failures prior to the initiating event are not considered in this analysis.

The single failures which affect this analysis are those which occur after the initiating event. The time period of interest is the first 24 hours after the initiating event. After the first hour following an initiating event, the CCS is split by procedure into two separate and distinct subsystems. Operator error during this split is discussed in Section D.5 of this analysis. After the split, there are no single failures which can fail the CCS. For these reasons, the single event failure contributions to system failure are those failures which occur during the first hour after an initiating event. The probability of system failure due to single event failures is described by the following mean and variance:

Mean:  $1.06 \times 10^{-7}$

Variance:  $1.53 \times 10^{-14}$ .

#### D.2 QUANTIFICATION OF TWO EVENT CUTSETS (BLOCKS D AND E) (HARDWARE)

As stated in Section C.4, the two event cutset contributions to failure consist of failures in blocks D and E of Figure 1. For block D we have:

Manual valve (service water) (2)  
(failure per hour)

Mean:  $9.15 \times 10^{-8}$

Variance:  $1.01 \times 10^{-14}$

Manual valve (CCW) (2)  
(failure per hour)

Mean:  $9.15 \times 10^{-8}$

Variance:  $1.01 \times 10^{-14}$

Heat exchanger  
(failure per hour)

Mean:  $9.73 \times 10^{-7}$

Variance:  $3.34 \times 10^{-12}$

Surge tank (leak or rupture)  
(failure per hour)  
(same as pipe rupture)

Mean:  $8.60 \times 10^{-10}$

Variance:  $6.00 \times 10^{-17}$ .



The probability of failure for block D is now:

$$\begin{aligned}\text{Mean (D):} & \quad 4 \alpha_{\text{valve}} + \alpha_{\text{heat exchanger}} + \alpha_{\text{tank}} \\ & = 1.34 \times 10^{-6}\end{aligned}$$

$$\text{Variance (D): } 2.84 \times 10^{-12}.$$

For block E, we have two additional service water valves in the supply line. This results in the following distribution for the probability of failure of block E:

$$\text{Mean: } 1.52 \times 10^{-6}$$

$$\text{Variance: } 3.01 \times 10^{-12}.$$

The failures described above are failures per hour, and we are interested in failures on demand. Note that failures in either component cooling train which occur during plant operation are immediately detectable. Operator action would then be taken to determine the cause, and repairs would be initiated. These failures are included in the maintenance contribution to system failure. Given that the system was operating prior to the initiating event, the failures that affect this system are those failures which occur from the time of the initiating event to time  $t = 24$  hours after the initiating event. Approximately 1 hour after the initiating event, the operator is directed, by procedure, to split the CCS and the service water system into two distinct subsystems. This results in a change in the components in blocks D and E. Block D now consists of:

- TXV34--C
- TXV36--C
- UXV759AC
- UXV765AC
- UHE0031L
- UTK0031L
- TXV32--C
- Nine sections of CCS piping (including pump suction and discharge cross-ties).

Block E consists of:

- TXV34-1C
- TXV36-1C
- UXV759C
- UXV765BC
- UHE0032L
- UTX0032L
- TXV31--C
- Seven sections of CCS piping.

NOTE: After the split, CCS pumps 31 and 32 will be supplying heat exchanger 31 and CCS pump 33 will be supplying heat exchanger 32. The CCS heat exchanger cross-tie will be isolated.

The following equation defines probability of system failure due to random failures in blocks D and E:

$$Q = [(4V3 + V2 + V1) (6V3 + V2 + V1)] \\ + 1 - (4V3 + V2 + V1) (6V3 + V2 + V1) \\ \times [23(5V3 + V2 + V1 + 9V4)] \times [23(5V3 + V2 + V1 + 7V4)]$$

where

V1 = Probability of surge tank failure

V2 = Probability of heat exchanger failure

V3 = Probability of a manual valve transferring closed

V4 = Probability of a single pipe section failure

Using the above equation, the probability of system failure due to random two event failures is:

Mean:  $3.52 \times 10^{-9}$

Variance:  $2.91 \times 10^{-16}$ .

### D.3 QUANTIFICATION OF THREE EVENT CUTSETS (BLOCKS A, B, C) (HARDWARE FAILURES)

As stated in Section C.4, the three event cutset contribution to system failure on demand consists of random failures in the pump trains, blocks A, B, and C of Figure 1. For block A we have:

- Pump (including motor and controls)

- Failure to start (on demand)

Mean:  $1.36 \times 10^{-3}$

Variance:  $1.22 \times 10^{-6}$ .

- Failure to run (per hour)

Mean:  $3.26 \times 10^{-6}$

Variance:  $2.47 \times 10^{-11}$ .

- Manual valve
  - Transfers closed (per hour)
    - Mean:  $9.15 \times 10^{-8}$
    - Variance:  $1.01 \times 10^{-14}$ .
- Check valve
  - Fails to open (on demand)
    - Mean:  $6.91 \times 10^{-5}$
    - Variance:  $1.03 \times 10^{-8}$ .

Blocks B and C consist of similar components. With a safety injection signal and no loss of offsite power, the CCS pumps which were running continue to run. The probability of failure per hour of a running CCS pump train is described by the following distribution (made up of pump failure to continue running and manual valves transferring closed):

Mean:  $3.44 \times 10^{-6}$   
 Variance:  $2.13 \times 10^{-11}$ .

For a time,  $t = 24$  hours, we have the following distribution for failure of an operating pump train:

Mean:  $8.26 \times 10^{-5}$   
 Variance:  $1.23 \times 10^{-8}$ .

With a loss of offsite power, the CCS pumps are started as a result of the operator action which occurs when entering the recirculation phase of the accident (with the diesel generators available). The probability of failure to start on demand of a previously operating CCS pump train is made up of: Pump failure to start on demand; check valve failure to open on demand; and the transferring closed of either the pump suction valve or discharge valve during the period of time that the pump is idle. For a time,  $t \leq$  one hour, the probability of failure of a single manual valve is:

Mean:  $9.15 \times 10^{-8}$   
 Variance:  $1.01 \times 10^{-14}$ .

For a single previously operating pump train, the probability of failure on demand is described by the following distribution:

Mean:  $1.43 \times 10^{-3}$   
 Variance:  $1.13 \times 10^{-6}$ .

Given a successful start, the CCS pump must operate for 24 hours. The total probability of failure (start and operate for 24 hours) for a single previously operating CCS pump train is now:

Mean:  $1.51 \times 10^{-3}$

Variance:  $1.03 \times 10^{-6}$ .

During plant operation, one CCS pump train is normally in standby. Pump failure to start on demand and check valve failure to open on demand remain as previously defined; however, the manual valves' contribution to pump train failure on demand must be developed. Plant procedures require routine shifting of the CCS pumps weekly. The fault detection time for this event is taken as one-half of the test interval (84 hours). This results in the following distribution for failure of a single manual valve in the standby pump train:

Mean:  $7.69 \times 10^{-6}$

Variance:  $6.74 \times 10^{-11}$ .

The failure of the standby pump train to start on demand is now described by the following mean and variance:

Mean:  $1.44 \times 10^{-3}$

Variance:  $1.13 \times 10^{-6}$ .

Given a successful start, the pump must continue to run for 24 hours, which results in a total failure probability for the standby pump of:

Mean:  $1.53 \times 10^{-3}$

Variance:  $1.03 \times 10^{-6}$ .

The following expression defines the probability of failure for the CCS pumps with differing probabilities for the status of the standby pump.

$$Q_{\text{pumps}} = P(1S) \left[ \binom{2}{2} P(OP)^2 \times P(STBY) \right] + 3P(OS) \left[ \binom{2}{2} P(OP)^2 \right]$$

where:

$P(1S)$  = Probability of having one pump in standby which equals  $1 - (\text{probability of maintenance of a single CCS pump})$ .

$P(OS)$  = Probability of having one CCS pump undergoing maintenance.

$P(OP)$  = Probability of failure of a running (or previously running) pump (to  $t = 24$  hours).

$P(STBY)$  = Probability of failure of the standby pump (to  $t = 24$  hours).

For the pump contribution to system failure, with no loss of offsite power and power available at all 480V switchgear buses, we have the following distribution:

Mean:  $9.15 \times 10^{-10}$

Variance:  $7.99 \times 10^{-16}$ .

For the pump contribution to system failure, with a loss of offsite power and power available at all 480V switchgear buses, we have the following distribution:

Mean:  $1.87 \times 10^{-7}$

Variance:  $1.21 \times 10^{-13}$ .

#### D.4 QUANTIFICATION OF TEST AND MAINTENANCE

##### D.4.1 Test Contribution

Testing of the CCS consists of starting the standby CCS pump monthly to satisfy ASME Section XI requirements and the weekly pump shift to satisfy plant operating requirements.

No system lineup changes are required for this testing. Therefore, no contribution of system failure on demand is assigned because of testing.

##### D.4.2 Maintenance Contribution

The maintenance contribution to system failure is included with the quantification of the pump trains' effect on system failure.

#### D.5 QUANTIFICATION OF HUMAN INTERACTION

The operator error of failing to switch from injection to recirculation is presented in the recirculation system analysis and is not quantified here.

With sufficient electric power, and after the shift to recirculation has been successfully completed, the operator is required by plant procedures to shift the CCS and service water system lineups. This shift results in splitting the CCS and the service water system into distinct subsystems. After the shift, pumps 31 or 32 of the CCS will be supplying a single header, and pump 33 will be supplying the other header. Each CCS heat exchanger will be receiving water from a separate service water header.

No probability for system failure due to operator errors in this shift are assigned for the following reasons:

- In order to start the shift, plant conditions must be stable, with sufficient electric power available and the shift to recirculation successfully completed. Conditions in the control room by this time



will be approaching the conditions in the control room during normal plant operations.

- The procedure details by valve number, the sequence of steps that must be performed to complete the shift. Verification of each significant change is monitored by monitoring the system conditions; major errors will be immediately detected and corrected.
- If problems are encountered, the shift is not made and the system remains or is returned to the normal lineup.

#### D.6 QUANTIFICATION OF COMMON CAUSE

Although there are many similar components sharing common locations in the CCS, a large portion of these components are not highly susceptible to common cause failure mechanisms because they perform a passive function. These items include manual valves, check valves, tanks, heat exchangers, and piping. The active components of the system, the CCS pumps, and various motor-operated valves are more likely candidates for common cause failure and are discussed below. External events such as earthquakes, flooding, etc., are discussed elsewhere in this report.

- a. Fire. The three CCS pumps share a common room in the primary auxiliary building at elevation 68'. The "Review of the Indian Point Station Fire Protection Program" described this area as having a low fire loading and postulated no fires which could affect all three CCS pumps.
- b. Moisture. Located in the vicinity of the CCS pumps are the CCS heat exchangers, the CCS surge tank, and the piping and valves for alignment and isolation of this equipment. Leakage (spray) from these components is detectable during plant operation and would be corrected upon occurrence prior to damage occurring. This common cause failure is not quantified for the above reason.
- c. Grit. During plant operation, no grit producing activities occur. During plant shutdown, these activities are protected against by plant procedures. This mechanism for common cause failure is not quantified for this analysis.
- d. Other causes - Other common cause susceptibilities, such as manufacturer, test and maintenance procedures, etc., are possible contributors to common cause failure of the CCS pumps. However, the plant test program, maintenance program, and technical specifications combine to (1) aid in discovery of pump problems and (2) limit the effects of common cause failures. No quantification is performed for these causes of failure.

NOTE: The CCS pump breakers are susceptible to the common cause failure mechanisms of fire, moisture and grit due to their common location in the switchgear room. Quantification and discussion of these effects are presented in the event tree analysis as these effects would be felt throughout the plant.

## D.7 SYSTEM FAILURE QUANTIFICATION

The failure frequency per demand for the CCS is made up of the following contributors: single event, double event, and triple event random hardware failures; test and maintenance in conjunction with random hardware failures; human error contribution to failure; and common cause contribution to failure.

The probability of failure of the CCS, given no loss of offsite power, to time ( $t = 24$  hours) is characterized by the following mean and variance:

$$Q_{\text{system}}: \alpha_{\text{singles}} + \alpha_{\text{doubles}} + \alpha_{\text{triples}} + \alpha_{\text{T\&M}} \\ \alpha_{\text{operator error}} + \alpha_{\text{common cause}}$$

$$1.11 \times 10^{-7}$$

$$\text{Variance: } 1.54 \times 10^{-14}$$

With a loss of offsite power, we have the following distribution for failure of the CCS to operate to time,  $t = 24$  hours:

$$Q_{\text{system}}: 2.97 \times 10^{-7}$$

$$\text{Variance: } 1.34 \times 10^{-13}$$

E. QUANTIFICATION BOUNDARY CONDITION, LOSS OF ONSITE POWER BUS(ES)

1. Loss of a single 480V bus

- a. No loss of offsite power. The following equation defines the probability of failure for the CCS pumps given a loss of a single 480V switchgear bus supply:

$$Q_{\text{pumps}} = P(1S) [P(OP) \times P(STBY)] + P(OS) [P(OP)]$$

where the terms of the equation remain as defined in Section D.3. For conservatism, the failed 480V switchgear bus is defined as a bus supplying a running CCS pump. The pump train contribution to system failure under the conditions defined above is:

$$\text{Mean: } 1.64 \times 10^{-6}$$

$$\text{Variance: } 5.72 \times 10^{-12}.$$

The probability of system failure under these conditions is:

$$Q_{\text{system:}} 1.75 \times 10^{-6}$$

$$\text{Variance: } 5.72 \times 10^{-12}.$$

- b. Loss of offsite power. The equation defined above is also applicable for this case. The pump train contribution to system failure under these conditions is:

$$\text{Mean: } 3.01 \times 10^{-5}$$

$$\text{Variance: } 8.38 \times 10^{-10}.$$

The probability of system failure is now:

$$Q_{\text{system:}} 3.02 \times 10^{-5}$$

$$\text{Variance: } 8.37 \times 10^{-10}.$$

2. Loss of two 480V buses

- a. No loss of offsite power. Under these conditions, the contribution to system failure of the CCS pumps is the value determined for a single CCS pump. From Section D.3, the value for an operating pump to time  $t = 24$  hours is:

$$\text{Mean: } 8.26 \times 10^{-5}$$

$$\text{Variance: } 1.23 \times 10^{-8}$$

This results in the following probability of system failure under these conditions:

$Q_{\text{system}}: 8.27 \times 10^{-5}$

Variance:  $1.22 \times 10^{-8}$ .

- b. Loss of offsite power. Under this condition, the contribution to system failure of the CCS pumps is the value determined for a single, previously operating, CCS pump. From Section D.3, this value is:

Mean:  $1.51 \times 10^{-3}$

Variance:  $1.03 \times 10^{-6}$

which results in a system probability of failure of:

$Q_{\text{system}}: 1.51 \times 10^{-3}$

Variance:  $1.03 \times 10^{-6}$ .

TABLE 1

SUMMARY OF RESULTS--COMPONENT COOLING SYSTEM ANALYSIS

Case 1--No Loss Of Offsite Power

	Mean	Variance	5th Percentile	95th Percentile	Median	ASH-1400
Boundary Condition Power at All Buses						
Singles	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.0 \times 10^{-8}$	$2.6 \times 10^{-7}$	$6.6 \times 10^{-8}$	No Comparable Analysis
Heat Exchangers	$3.5 \times 10^{-9}$	$2.9 \times 10^{-16}$	$6.3 \times 10^{-11}$	$1.1 \times 10^{-8}$	$8.1 \times 10^{-10}$	
Pump Trains	$9.1 \times 10^{-10}$	$8.0 \times 10^{-18}$	$4.1 \times 10^{-12}$	$3.3 \times 10^{-9}$	$1.2 \times 10^{-10}$	
Test and Maintenance	-	(with pump trains)				
Operator Error	-					
Common Cause	-					
Other	-					
System	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.2 \times 10^{-8}$	$2.6 \times 10^{-7}$	$7.6 \times 10^{-8}$	
Boundary Condition Power at Two Buses						
Singles	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.0 \times 10^{-8}$	$2.6 \times 10^{-7}$	$6.6 \times 10^{-8}$	No Comparable Analysis
Heat Exchangers	$3.5 \times 10^{-9}$	$2.9 \times 10^{-16}$	$6.3 \times 10^{-11}$	$1.1 \times 10^{-8}$	$8.1 \times 10^{-10}$	
Pump Trains	$1.5 \times 10^{-6}$	$5.7 \times 10^{-12}$	$1.4 \times 10^{-7}$	$4.7 \times 10^{-6}$	$2.6 \times 10^{-7}$	
Test and Maintenance	-	(with pump trains)				
Operator Error	-					
Common Cause	-					
Other	-					
System	$1.3 \times 10^{-6}$	$5.7 \times 10^{-12}$	$2.4 \times 10^{-7}$	$4.8 \times 10^{-6}$	$1.0 \times 10^{-6}$	
Boundary Condition Power at One Bus						
Singles	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.0 \times 10^{-8}$	$2.6 \times 10^{-7}$	$6.6 \times 10^{-8}$	No Comparable Analysis
Heat Exchangers	$3.5 \times 10^{-9}$	$2.9 \times 10^{-16}$	$6.3 \times 10^{-11}$	$1.1 \times 10^{-8}$	$8.1 \times 10^{-10}$	
Pump Trains	$8.3 \times 10^{-5}$	$1.2 \times 10^{-8}$	$1.2 \times 10^{-5}$	$2.0 \times 10^{-4}$	$4.5 \times 10^{-5}$	
Test and Maintenance	-	(with pump trains)				
Operator Error	-					
Common Cause	-					
Other	-					
System	$8.3 \times 10^{-5}$	$1.2 \times 10^{-8}$	$1.1 \times 10^{-5}$	$2.4 \times 10^{-4}$	$4.7 \times 10^{-5}$	



TABLE 1 (continued)

SUMMARY OF RESULTS--COMPONENT COOLING SYSTEM ANALYSIS

Case 2--Loss Of Offsite Power

	Mean	Variance	5th Percentile	95th Percentile	Median	W-1400
Boundary Condition Power at All Buses						
Singles	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.0 \times 10^{-8}$	$2.5 \times 10^{-7}$	$6.6 \times 10^{-8}$	No Comparable Analysis
Heat Exchangers	$3.5 \times 10^{-9}$	$2.9 \times 10^{-16}$	$6.3 \times 10^{-11}$	$1.1 \times 10^{-8}$	$8.1 \times 10^{-10}$	
Pump Trains	$1.9 \times 10^{-7}$	$1.2 \times 10^{-13}$	$7.0 \times 10^{-9}$	$6.0 \times 10^{-7}$	$7.0 \times 10^{-8}$	
Test and Maintenance	-	(with pump trains)				
Operator Error	-					
Common Cause	-					
Other	-					
System	$3.0 \times 10^{-7}$	$1.3 \times 10^{-13}$	$5.4 \times 10^{-8}$	$7.8 \times 10^{-7}$	$1.9 \times 10^{-7}$	
Boundary Condition Power at Two Buses						
Singles	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.0 \times 10^{-8}$	$2.5 \times 10^{-7}$	$5.5 \times 10^{-8}$	No Comparable Analysis
Heat Exchangers	$3.5 \times 10^{-9}$	$2.9 \times 10^{-16}$	$6.3 \times 10^{-11}$	$1.1 \times 10^{-8}$	$8.1 \times 10^{-10}$	
Pump Trains	$3.0 \times 10^{-5}$	$8.4 \times 10^{-10}$	$5.1 \times 10^{-6}$	$7.3 \times 10^{-5}$	$2.0 \times 10^{-5}$	
Test and Maintenance	-	(with pump trains)				
Operator Error	-					
Common Cause	-					
Other	-					
System	$3.0 \times 10^{-5}$	$8.4 \times 10^{-10}$	$5.3 \times 10^{-6}$	$7.4 \times 10^{-5}$	$2.0 \times 10^{-5}$	
Boundary Condition Power at One Bus						
Singles	$1.1 \times 10^{-7}$	$1.5 \times 10^{-14}$	$2.0 \times 10^{-8}$	$2.5 \times 10^{-7}$	$6.6 \times 10^{-8}$	No Comparable Analysis
Heat Exchangers	$3.5 \times 10^{-9}$	$2.9 \times 10^{-16}$	$6.3 \times 10^{-11}$	$1.1 \times 10^{-8}$	$8.1 \times 10^{-10}$	
Pump Trains	$1.5 \times 10^{-3}$	$1.0 \times 10^{-6}$	$4.3 \times 10^{-4}$	$3.5 \times 10^{-3}$	$1.2 \times 10^{-3}$	
Test and Maintenance	-	(with pump trains)				
Operator Error	-					
Common Cause	-					
Other	-					
System	$1.5 \times 10^{-3}$	$1.0 \times 10^{-6}$	$4.3 \times 10^{-4}$	$3.4 \times 10^{-3}$	$1.2 \times 10^{-3}$	

TABLE 2

## REQUIRED CCS FLOWS FOR PLANT CONDITIONS

Components Cooled	Normal Operation Flow (gpm)		Shutdown Flow (gpm)		Accident Conditions Flow (gpm)	
	Component	Total	Component	Total	Component	Total
1. High Head Safety Injection Pumps	15/pump	45	15/pump	45	15/pump	45
2. Residual Heat Removal Pumps	15/pump	30	15/pump	30	15/pump	30
3. Residual Heat Exchanger	-	-	-	4000	-	4000
4. Recirculation Pumps	-	-	-	-	40/pump	80
5. Spent Fuel Pit Heat	2000	2000	2000	2000	-	-
6. Reactor Coolant Pumps						
a. Upper Motor Bearing Heat Exchanger	150/pump	600	-	-	-	-
b. Lower Motor Bearing Heat Exchanger	5/pump	20	-	-	-	-
c. Pump Thermal Barrier	25/pump	100	-	-	-	-
7. Letdown Heat Exchanger		1000		-		-
8. Seal Water Heat Exchanger		200		-		-
9. Primary Makeup Water Heat Exchanger		400		-		-
10. Boric Acid Regeneration System		815		-		-
11. Waste Evaporation System		155		-		-
12. Charging Pumps	90	270	-	-	-	-
13. Excess Letdown Heat Exchanger		230		-		-
14. Reactor Vessel Support Blocks		50		-		-
15. Miscellaneous Sample Heat Exchangers		168		-		-
		6,100		6,075		4,155
	Two of Three Pumps One of Two Heat Exchangers		Two of Three Pumps One of Two Heat Exchangers		Two of Three Pumps One of Two Heat Exchangers	

TABLE 3

## BASIC EVENT DATA COMPONENT COOLING - INDIAN POINT 3

Event Description and Failure Mode	Fault Tree Coding	Failure Data				Common Cause Data			Comments
		Mean	H/D	Variance	MITR	Reference No.*	Location	Susceptibility	
No Power at Switchgear Bus 2A	JBS-32AD	-	-	-	-	-	Control Bldg. El 15'	V, I, H, M	See EP Analysis
No Power at Switchgear Bus 5A	JBS-35AD	-	-	-	-	-	Control Bldg. El 15'	"	See EP Analysis
No Power at Switchgear Bus 6A	JBS-36AD	-	-	-	-	-	Control Bldg. El 15'	"	See EP Analysis
No Control Power at Switchgear Bus 2A	4BS-333D	-	-	-	-	-	Control Bldg. El 15'	"	See EP Analysis
No Control Power at Switchgear Bus 5A	4BS-331D	-	-	-	-	-	Control Bldg. El 15'	"	See EP Analysis
No Control Power at Switchgear Bus 6A	4BS-332D	-	-	-	-	-	Control Bldg. El 15'	"	See EP Analysis
No Flow from Service Water Supply Header (Conventional)	TSW2NOFL	-	-	-	-	-	NA	-	See EP Analysis
CC Pump 31 Does Not Start	UPM0031S	$1.36 \times 10^{-3}$	D	$1.22 \times 10^{-6}$	-	11	PAB El 41'	V, H, I	See SW Analysis
Does Not Continue Running		$3.26 \times 10^{-6}$	H	$2.47 \times 10^{-11}$	In Text	15			
CC Pump 32 Does Not Start	UPM0032S	$1.36 \times 10^{-3}$	D	$1.22 \times 10^{-6}$	-	11	PAB El 41'	V, H, I	
Does Not Continue Running		$3.26 \times 10^{-6}$	H	$2.47 \times 10^{-11}$	In Text	15			
CC Pump 33 Does Not Start	UPM0033S	$1.36 \times 10^{-3}$	D	$1.22 \times 10^{-6}$	-	11	PAB El 41'	V, H, I	
Does Not Continue Running		$3.26 \times 10^{-6}$	H	$2.47 \times 10^{-11}$	In Text	15			
CC Pump 31 Motor, Does Not Start/Run	UM00031N	-	-	-	-	-	Same as Pump	V, I, H, M	With Pump
CC Pump 32 Motor, Does Not Start/Run	UM00032N	-	-	-	-	-	Same as Pump	V, I, H, M	With Pump
CC Pump 33 Motor, Does Not Start/Run	UM00033N	-	-	-	-	-	Same as Pump	V, I, H, M	With Pump

\*Reference number refers to item numbers in the plant failure data section of this report.

TABLE 3 (continued)

## BASIC EVENT DATA COMPONENT COOLING - INDIAN POINT 3

Event Description and Failure Mode	Fault Tree Coding	Failure Data					Common Cause Data		Comments
		Mean	H/D	Variance	MTTR	Reference No.*	Location	Susceptibility	
Pump 31 Discharge Valve, Transfers Closed	UXV762AC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Pump Discharge	1	
Pump 32 Discharge Valve, Transfers Closed	UXV762BC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Pump Discharge	1	
Pump 33 Discharge Valve, Transfers Closed	UXV762CC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Pump Discharge	1	
Heat Exchanger 31 Inlet Valve, Transfers Closed	UXV759AC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Near Heat Exchanger	1	
Heat Exchanger 32 Inlet Valve, Transfers Closed	UXV759BC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Near Heat Exchanger	1	
Heat Exchanger 31 Outlet Valve, Transfers Closed	UXV765AC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Near Heat Exchanger	1	
Heat Exchanger 32 Outlet Valve, Transfers Closed	UXV765BC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Near Heat Exchanger	1	
SW Inlet to Heat Exch. 31, Transfers Closed	FXV034AC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	PAB Near Heat Exchanger	1	
SW Inlet to Heat Exch. 32, Transfers Closed	FXV034BC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	PAB Near Heat Exchanger	1	
SW Outlet from Heat Exchanger 31, Transfers Closed	FXV035AC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	PAB Near Heat Exchanger	1	
SW Outlet from Heat Exchanger 32, Transfers Closed	FXV035BC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	PAB Near Heat Exchanger	1	

\*Reference number refers to item numbers in the plant failure data section of this report.

TABLE 3 (continued)

## BASIC EVENT DATA COMPONENT COOLING - INDIAN POINT 3

Event Description and Failure Mode	Fault Tree Coding	Failure Data					Common Cause Data		Comments
		Mean	H/D	Variance	MEIR	Reference No.*	Location	Susceptibility	
CC Pump 31 Breaker, Does Not Close/Transfers Open	UCB0031X	-	-	-	-	-	Switchgear Bus 5A	V, I, H, M	With Pump
CC Pump 32 Breaker, Does Not Close/Transfers Open	UCB0032X	-	-	-	-	-	Switchgear Bus 2A	V, I, H, M	With Pump
CC Pump 33 Breaker, Does Not Close/Transfers Open	UCB0033X	-	-	-	-	-	Switchgear Bus 6A	V, I, H, M	With Pump
CC Surge Tank 31 Leak or Rupture	UTK0031L	$8.60 \times 10^{-10}$	H	$6.00 \times 10^{-17}$	In Text	48	PAB E1 01*	I	
CC Surge Tank 32 Leak or Rupture	UIE0031L	$8.60 \times 10^{-10}$	H	$6.00 \times 10^{-17}$	In Text	48	PAB E1 01*	I	
CC Heat Exchanger 31, Loss of Cooling Capability (Leak/Rupture)	UIE0031L	$9.73 \times 10^{-7}$	H	$3.34 \times 10^{-12}$	In Text	24	PAB E1 55 to 01*	I	
CC Heat Exchanger 32, Loss of Cooling Capability (Leak/Rupture)	UIE0032L	$9.73 \times 10^{-7}$	H	$3.34 \times 10^{-12}$	In Text	24	PAB E1 55 to 01*	I	
Pump 31 Suction Valve, Transfers Closed	UXV760AC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Pump Suction	I	
Pump 32 Suction Valve, Transfers Closed	UXV760BC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Pump Suction	I	
Pump 33 Suction Valve, Transfers Closed	UXV760CC	$9.15 \times 10^{-8}$	H	$1.01 \times 10^{-14}$	In Text	1	Pump Suction	I	
Pump 31 Discharge Check Valve, Fails to Open	UCV761AQ	$6.91 \times 10^{-5}$	D	$1.03 \times 10^{-8}$	-	3	Pump Discharge	I	
Pump 32 Discharge Check Valve, Fails to Open	UCV761BQ	$6.91 \times 10^{-5}$	D	$1.03 \times 10^{-8}$	-	3	Pump Discharge	I	
Pump 33 Discharge Check Valve, Fails to Open	UCV761CQ	$6.91 \times 10^{-5}$	D	$1.03 \times 10^{-8}$	-	3	Pump Discharge	I	

\*Reference number refers to item numbers in the plant failure data section of this report.



TABLE 3 (continued)

## BASIC EVENT DATA COMPONENT COOLING - INDIAN POINT 3

Event Description and Failure Mode	Fault Tree Coding	Failure Data				Causation Cause Data			Comments
		Mean	H/D	Variance	MITR	Reference No. *	Location	Susceptibility	
Su Supply Valve, 31, Transfers Closed	TXV31--C	9.15 x 10 <sup>-8</sup>	II	1.01 x 10 <sup>-14</sup>	In Text	1	Pipe Tunnel	1	
Su Supply Valve, 32, Transfers Closed	TXV32--C	9.15 x 10 <sup>-8</sup>	II	1.01 x 10 <sup>-14</sup>	In Text	1	Pipe Tunnel	1	
Su Supply Valve, 33, Transfers Closed	TXV33--C	9.15 x 10 <sup>-8</sup>	II	1.01 x 10 <sup>-14</sup>	In Text	1	Pipe Tunnel	1	
Su Supply Valve, 34, Transfers Closed	TXV33-1C	9.15 x 10 <sup>-8</sup>	II	1.01 x 10 <sup>-14</sup>	In Text	1	Pipe Tunnel	1	
CC Pipe Failure	UPPFAILS	8.60 x 10 <sup>-10</sup>	II	6.00 x 10 <sup>-17</sup>	See Text	48	Various	1	

\*Reference number refers to Item numbers in the plant failure data section of this report.

TABLE 4

MINIMAL CUTSETS FOR PHASE 1

# COMPONENT COOLING WATER SYSTEM INDIAN POINT 3 MINIMAL CUTSETS (Sheet 1 of 4)

TITLE: COMPONENT COOLING WATER SYSTEM INDIAN POINT 3

CUT SETS WITH 1 BASIC EVENTS.

1. 11. 21. 31.

CUT SETS WITH 2 BASIC EVENTS.

21	11	01E0031L	01E0032L	21	0XV759AC	0XV759BC	31	01G31L	0XV759BC	41	0XV765AC	0XV759BC
11	01	1XV0342L	0XV759BC	21	1XV035AC	0XV759BC	71	0XV759AC	0HE0032L	21	0HE0031L	0HE0032L
11	01	0XV765AC	0HE0032L	101	1XV034AC	0HE0032L	111	1XV035AC	0HE0032L	121	0XV759AC	0XV765BC
11	01	0HE0031L	0XV765BC	141	0XV765AC	0XV765BC	151	1XV034AC	0XV765BC	161	1XV035AC	0XV765BC
21	11	1XV759AC	1XV034BC	181	0HE0031L	1XV034BC	191	0XV765AC	1XV034BC	201	1XV034AC	1XV034BC
21	11	1XV759AC	1XV034BC	221	0XV759AC	1XV035BC	231	0HE0031L	1XV035BC	241	0XV765AC	1XV034BC
21	11	1XV034AC	1XV035BC	261	1XV035AC	1XV035BC	271	1XV33--C	0XV759BC	281	1XV33--C	0XV759BC
21	11	1XV33--C	0HE0032L	301	1XV33--C	0HE0032L	311	1XV33--C	0XV765BC	321	1XV33--C	0XV765BC
21	11	1XV33--C	1XV034BC	341	1XV33--C	1XV034BC	351	1XV33--C	1XV035BC	361	1XV33--C	1XV035BC
41	11	4BS-333C	4BS-333C	381	4BS-333C	4BS-333C	391	0XV766AC	4BS-333C	401	0M00C31S	4BS-333C
421	11	0XV762AC	4BS-333C	421	0PP0031S	4BS-333C	431	0CV761AC	4BS-333C	441	0CC0C31F	4BS-333C

CUT SETS WITH 3 BASIC EVENTS.

11	11	0XV762AC	0XV762AC	21	0PP0031S	0XV762BC	0XV762AC	31	0CV761CQ	0XV762BC	0XV762AC
11	11	0XV762BC	0XV762AC	51	0XV762BC	0PP0032S	0XV762AC	61	0PP0C31S	0PP0C32S	0XV762AC
11	11	0PP0C32S	0XV762AC	61	0CC0C31F	0PP0C32S	0XV762AC	91	0XV762CC	0CV761BC	0XV762AC
11	11	0PP0C32S	0CV761BC	111	0CV761CQ	0CV761BC	0XV762AC	121	0CC0C32F	0CV761BC	0XV762AC
11	11	0XV762CC	0CC0C32F	141	0PP0C31S	0CC0C32F	0XV762AC	151	0CV761CQ	0CC0C32F	0XV762AC
11	11	0CC0C32F	0XV762AC	171	0XV762CC	0XV762BC	0PP0C31S	181	0PP0C31S	0XV762BC	0PP0C31S
11	11	0CV761BC	0XV762BC	201	0CC0C31F	0XV762BC	0PP0C31S	211	0XV762CC	0PP0C32S	0PP0C31S
11	11	0PP0C32S	0PP0C31S	231	0CV761CQ	0PP0C32S	0PP0C31S	241	0CC0C32F	0PP0C32S	0PP0C31S
11	11	0XV762CC	0CV761CQ	261	0PP0C31S	0CV761CQ	0PP0C31S	271	0CV761CQ	0CV761BC	0PP0C31S
11	11	0CC0C31F	0CV761BC	291	0XV762CC	0CC0C32F	0PP0C31S	301	0PP0C31S	0CC0C32F	0PP0C31S
11	11	0XV762CC	0CC0C32F	321	0CC0C31F	0CC0C32F	0PP0C31S	331	0XV762CC	0XV762BC	0CV761AC
11	11	0PP0C32S	0CV761AC	351	0CV761CQ	0XV762BC	0CV761AC	361	0CC0C32F	0XV762BC	0CV761AC
11	11	0XV762CC	0PP0C32S	381	0PP0C31S	0PP0C32S	0CV761AC	391	0CV761CQ	0PP0C32S	0CV761AC
11	11	0CC0C32F	0PP0C32S	411	0XV762CC	0CV761BC	0CV761AC	421	0PP0C31S	0CV761BC	0CV761AC
11	11	0CV761CQ	0CV761AC	441	0CC0C31F	0CV761BC	0CV761AC	451	0XV762CC	0CC0C32F	0CV761AC
11	11	0PP0C31S	0CC0C32F	471	0CV761CQ	0CC0C32F	0CV761AC	481	0CC0C31F	0CC0C32F	0CV761AC

TABLE 4 (continued)

COMPONENT COOLING WATER SYSTEM INDIAN POINT 3 MINIMAL CUTSETS  
(Sheet 2 of 4)

TABLE 4 (continued)

TABLE 4 (continued)

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1001	1001	UCV7610C	UCV7620C	UCC0031F	501	UPM0033S	UCV7620C	UCC0031F	511	UCV7610C	UCV7620C	UCC0031F
1002	1002	UCV7610C	UCV7620C	UCC0031F	511	UCV7620C	UPM0032S	UCC0031F	541	UPM0033S	UPM0032S	UCC0031F
1003	1003	UCV7610C	UPM0032S	UCC0031F	561	UCC0031F	UPM0032S	UCC0031F	571	UCV7620C	UCV7610C	UCC0031F
1004	1004	UPM0033S	UCV7610C	UCC0031F	591	UCV7610C	UCV7610C	UCC0031F	601	UCC0031F	UCV7610C	UCC0031F
1005	1005	UCV7620C	UCC0031F	UCC0031F	621	UPM0033S	UCC0032F	UCC0031F	631	UCV7610C	UCC0032F	UCC0031F
1006	1006	UCC0031F	UCC0032F	UCC0031F	651	UCV7620C	UCV7620C	J05-3540	661	UPM0033S	UCV7620C	J05-3540
1007	1007	UCV7610C	UCV7620C	J05-3540	681	UCC0031F	UCV7620C	J05-3540	691	UCV7620C	UPM0032S	J05-3540
1008	1008	UPM0033S	UPM0032S	J05-3540	711	UCV7610C	UPM0032S	J05-3540	721	UCC0031F	UPM0032S	J05-3540
1009	1009	UCV7620C	UCV7610C	J05-3540	741	UPM0033S	UCV7610C	J05-3540	751	UCV7610C	UCV7610C	J05-3540
1010	1010	UCC0031F	UCV7610C	J05-3540	771	UCV7620C	UCC0032F	J05-3540	781	UPM0033S	UCC0032F	J05-3540
1011	1011	UCV7610C	UCC0032F	J05-3540	801	UCC0031F	UCC0032F	J05-3540	811	UCV7620C	UCV7620C	J05-3540
1012	1012	UPM0033S	UCV7620C	J05-3540	831	UCV7610C	UCV7620C	J05-3540	841	UCC0031F	UCV7620C	J05-3540
1013	1013	UCV7620C	UPM0032S	J05-3540	861	UPM0033S	UPM0032S	J05-3540	871	UCV7610C	UPM0032S	J05-3540
1014	1014	UCV7610C	UPM0032S	J05-3540	891	UCV7620C	UCV7610C	J05-3540	901	UPM0033S	UCV7610C	J05-3540
1015	1015	UCV7610C	UCV7610C	J05-3540	921	UCC0031F	UCV7610C	J05-3540	931	UCV7620C	UCC0032F	J05-3540
1016	1016	UPM0033S	UCC0032F	J05-3540	951	UCV7610C	UCC0032F	J05-3540	961	UCC0031F	UCC0032F	J05-3540
1017	1017	UCV7620C	UCV7620C	UCV7604C	981	UPM0033S	UCV7620C	UCV7604C	991	UCV7610C	UCV7620C	UCV7604C
1018	1018	UCC0031F	UCV7620C	UCV7604C	1011	UCV7620C	UPM0032S	UCV7604C	1021	UPM0033S	UPM0032S	UCV7604C
1019	1019	UCV7610C	UPM0032S	UCV7604C	1041	UCC0031F	UPM0032S	UCV7604C	1051	UCV7620C	UCV7610C	UCV7604C
1020	1020	UPM0033S	UCV7610C	UCV7604C	1071	UCV7610C	UCV7610C	UCV7604C	1081	UCC0031F	UCV7610C	UCV7604C
1021	1021	UCV7610C	UCC0032F	UCV7604C	1101	UPM0033S	UCC0032F	UCV7604C	1111	UCV7610C	UCC0032F	UCV7604C
1022	1022	UCC0031F	UCC0032F	UCV7604C	1121	UCV7620C	UCV7620C	UPM0031S	1141	UPM0033S	UCV7620C	UPM0031S
1023	1023	UCV7610C	UCV7620C	UPM0031S	1161	UCC0031F	UCV7620C	UPM0031S	1171	UCV7620C	UPM0032S	UPM0031S
1024	1024	UPM0033S	UPM0032S	UPM0031S	1191	UCV7610C	UPM0032S	UPM0031S	1201	UCC0031F	UPM0032S	UPM0031S
1025	1025	UCV7620C	UCV7610C	UPM0031S	1221	UPM0033S	UCV7610C	UPM0031S	1231	UCV7610C	UCV7610C	UPM0031S
1026	1026	UCC0031F	UCV7610C	UPM0031S	1251	UCV7620C	UCC0032F	UPM0031S	1261	UPM0033S	UCC0032F	UPM0031S
1027	1027	UCV7620C	UCC0032F	UPM0031S	1281	UCC0031F	UCC0032F	UPM0031S	1291	UCV7620C	J05-3540	J05-3540
1028	1028	UPM0033S	J05-3540	J05-3540	1311	UCV7610C	J05-3540	J05-3540	1321	UCC0031F	J05-3540	J05-3540
1029	1029	UCV7620C	J05-3540	J05-3540	1341	UPM0033S	J05-3540	J05-3540	1351	UCV7610C	J05-3540	J05-3540
1030	1030	UCC0031F	J05-3540	J05-3540	1371	UCV7620C	UCV7604C	J05-3540	1381	UPM0033S	UCV7604C	J05-3540
1031	1031	UCV7610C	UCV7604C	J05-3540	1401	UCC0031F	UCV7604C	J05-3540	1411	UCV7620C	UPM0031S	J05-3540
1032	1032	UPM0033S	UPM0031S	J05-3540	1431	UCV7610C	UPM0031S	J05-3540	1441	UCC0031F	UPM0031S	J05-3540
1033	1033	UCV7610C	J05-3540	UCV7600C	1461	UPM0033S	J05-3540	UCV7600C	1471	UCV7610C	J05-3540	UCV7600C
1034	1034	UCC0031F	J05-3540	UCV7600C	1491	UCV7620C	J05-3540	UCV7600C	1501	UPM0033S	J05-3540	UCV7600C
1035	1035	UCV7610C	J05-3540	UCV7600C	1521	UCC0031F	J05-3540	UCV7600C	1531	UCV7620C	UCV7604C	UCV7600C
1036	1036	UPM0033S	UCV7604C	UCV7600C	1551	UCV7610C	UCV7604C	UCV7600C	1561	UCC0031F	UCV7604C	UCV7600C
1037	1037	UCV7620C	UPM0031S	UCV7600C	1581	UPM0033S	UPM0031S	UCV7600C	1591	UCV7610C	UPM0031S	UCV7600C
1038	1038	UCV7610C	UCC0031S	UCV7600C	1611	UCV7620C	J05-3540	UPM0032S	1621	UPM0033S	J05-3540	UPM0032S
1039	1039	UCV7610C	J05-3540	UCC0032S	1641	UCC0031F	J05-3540	UPM0032S	1651	UCV7620C	J05-3540	UPM0032S
1040	1040	UPM0033S	J05-3540	UPM0032S	1671	UCV7610C	J05-3540	UPM0032S	1681	UCC0031F	J05-3540	UPM0032S
1041	1041	UCV7620C	UCV7604C	UPM0032S	1701	UPM0033S	UCV7604C	UPM0032S	1711	UCV7610C	UCV7604C	UPM0032S
1042	1042	UCC0031F	UCV7604C	UPM0032S	1721	UCV7620C	UPM0031S	UPM0032S	1741	UPM0033S	UPM0031S	UPM0032S
1043	1043	UCV7610C	UPM0031S	UPM0032S	1771	UCC0031F	UPM0031S	UPM0032S	1781	J05-3540	J05-3540	J05-3540
1044	1044	J05-3540	J05-3540	J05-3540	1791	UCV7604C	J05-3540	J05-3540	1801	UPM0031S	J05-3540	J05-3540
1045	1045	J05-3540	J05-3540	J05-3540	1821	J05-3540	UCV7600C	J05-3540	1831	UCV7604C	UCV7600C	J05-3540
1046	1046	UCV7600C	UCV7600C	J05-3540	1851	J05-3540	UPM0032S	J05-3540	1861	J05-3540	UPM0032S	J05-3540

TABLE 4 (continued)

COMPONENT COOLING WATER SYSTEM INDIAN POINT 3

COMPONENT COOLING WATER SYSTEM INDIAN POINT 3 MINIMAL CUTSETS  
(Sheet 3 of 4)

TITLE: COMPONENT COOLING WATER SYSTEM INDIAN POINT 3

CUT SETS WITH 3-FAULT CUTSETS

1841	1841	485-3310	J85-3240	UXV760CC	1911	UXV760AC	J85-3240	UXV760CC	1921	UM000315	J85-3240	UXV760CC
1842	1842	485-3310	UXV760CC	UXV760CC	1941	485-3310	UXV760CC	UXV760CC	1951	UXV760AC	UXV760CC	UXV760CC
1843	1843	485-3310	UXV760CC	UXV760CC	1971	J85-3540	UM000325	UXV760CC	1981	485-3310	UM000325	UXV760CC
1844	1844	UXV760CC	UM000325	UXV760CC	2001	UM000315	UM000325	UXV760CC	2011	J85-3540	J85-3240	UM000315
1845	1845	485-3310	J85-3240	UM000315	2031	UXV760AC	J85-3240	UM000315	2041	UM000315	J85-3240	UM000315
1846	1846	J85-3310	UXV760CC	UM000315	2061	485-3310	UXV760CC	UM000315	2071	UXV760AC	UXV760CC	UM000315
1847	1847	UM000315	UXV760CC	UM000315	2091	J85-3540	UM000325	UM000315	2101	485-3310	UM000325	UM000315
1848	1848	UXV760CC	UM000325	UM000315	2121	UM000315	UM000325	UM000315	2131	UXV762CC	J85-3540	J85-3340
1849	1849	UXV762CC	J85-3540	J85-3340	2151	UCV761CC	J85-3540	J85-3340	2161	UCC0032F	J85-3540	J85-3340
1850	1850	UXV762CC	485-3310	J85-3340	2181	UPM00325	485-3310	J85-3340	2191	UCV761CC	485-3310	J85-3340
1851	1851	UCC0032F	485-3310	J85-3340	2211	UXV762CC	UXV760AC	J85-3340	2221	UPM00325	UXV760AC	J85-3340
1852	1852	UCV761CC	UXV760AC	J85-3340	2241	UCC0032F	UXV760AC	J85-3340	2251	UXV762CC	UM000315	J85-3340
1853	1853	UPM00325	UXV760AC	J85-3340	2271	UCV761CC	UM000315	J85-3340	2281	UCC0032F	UM000315	J85-3340
1854	1854	UXV760CC	J85-3540	UXV760CC	2301	UPM00325	J85-3540	UXV760CC	2311	UCV761CC	J85-3540	UXV760CC
1855	1855	UCC0032F	J85-3540	UXV760CC	2331	UXV762CC	485-3310	UXV760CC	2341	UPM00325	485-3310	UXV760CC
1856	1856	UXV761CC	485-3310	UXV760CC	2361	UCC0032F	485-3310	UXV760CC	2371	UXV762CC	UXV760AC	UXV760CC
1857	1857	UPM00325	UXV760AC	UXV760CC	2391	UCV761CC	UXV760AC	UXV760CC	2401	UCC0032F	UXV760AC	UXV760CC
1858	1858	UXV760CC	UM000315	UXV760CC	2421	UPM00325	UM000315	UXV760CC	2431	UCV761CC	UM000315	UXV760CC
1859	1859	UCC0032F	UXV760CC	UXV760CC	2451	UXV762CC	J85-3540	UM000315	2461	UPM00325	J85-3540	UM000315
1860	1860	UXV761CC	J85-3540	UM000315	2481	UCC0032F	J85-3540	UM000315	2491	UXV762CC	485-3310	UM000315
1861	1861	UPM00325	485-3310	UM000315	2511	UCV761CC	485-3310	UM000315	2521	UCC0032F	485-3310	UM000315
1862	1862	UXV761CC	UXV760AC	UM000315	2541	UPM00325	UXV760AC	UM000315	2551	UCV761CC	UXV760AC	UM000315
1863	1863	UCC0032F	UXV760AC	UM000315	2571	UXV762CC	UPM00315	UM000315	2581	UPM00325	UM000315	UM000315
1864	1864	UCV761CC	UM000315	UM000315	2601	UCC0032F	UM000315	UM000315	2611	UXV762CC	UXV762AC	J85-3240
1865	1865	UPM00315	UXV762CC	J85-3240	2631	UCV761CC	UXV762CC	J85-3240	2641	UCC0032F	UXV762AC	J85-3240
1866	1866	UXV761CC	UPM00315	J85-3240	2661	UPM00315	UPM00315	J85-3240	2671	UCV761CC	UPM00315	J85-3240
1867	1867	UCC0032F	UPM00315	J85-3240	2691	UXV762CC	UCV761CC	J85-3240	2701	UPM00315	UCV761CC	J85-3240
1868	1868	UXV761CC	UCV761CC	J85-3240	2721	UCC0032F	UCV761CC	J85-3240	2731	UXV762CC	UCC0031F	J85-3240
1869	1869	UPM00315	UCC0031F	J85-3240	2751	UCV761CC	UCC0031F	J85-3240	2761	UCC0032F	UCC0031F	J85-3240
1870	1870	UXV762CC	UXV762CC	UXV760CC	2781	UPM00315	UXV762CC	UXV760CC	2791	UCV761CC	UXV762CC	UXV760CC
1871	1871	UCC0031F	UXV762CC	UXV760CC	2811	UXV762CC	UPM00315	UXV760CC	2821	UPM00315	UPM00315	UXV760CC
1872	1872	UXV761CC	UPM00315	UXV760CC	2841	UCC0031F	UPM00315	UXV760CC	2851	UXV762CC	UCV761CC	UXV760CC
1873	1873	UPM00315	UCV761CC	UXV760CC	2871	UCV761CC	UCV761CC	UXV760CC	2881	UCC0031F	UCV761CC	UXV760CC
1874	1874	UXV760CC	UCC0031F	UXV760CC	2901	UPM00315	UCC0031F	UXV760CC	2911	UCV761CC	UCC0031F	UXV760CC
1875	1875	UCC0031F	UCC0031F	UXV760CC	2931	UXV762CC	UXV762CC	UM000325	2941	UPM00315	UXV762CC	UM000325
1876	1876	UXV761CC	UXV762CC	UM000325	2961	UCC0031F	UXV762CC	UM000325	2971	UXV762CC	UPM00315	UM000325
1877	1877	UCV761CC	UPM00315	UM000325	2991	UCV761CC	UPM00315	UM000325	3001	UCC0031F	UPM00315	UM000325
1878	1878	UXV762CC	UCV761CC	UM000325	3021	UPM00315	UCV761CC	UM000325	3031	UCV761CC	UCV761CC	UM000325
1879	1879	UCC0032F	UCV761CC	UM000325	3051	UXV762CC	UCC0031F	UM000325	3061	UPM00315	UCC0031F	UM000325
1880	1880	UXV761CC	UCC0031F	UM000325	3091	UCC0031F	UCC0031F	UM000325	3091	UXV762CC	J85-3240	J85-3340
1881	1881	UPM00315	J85-3240	J85-3340	3111	UCV761CC	J85-3240	J85-3340	3121	UCC0031F	J85-3240	J85-3340
1882	1882	UXV762CC	UXV760CC	J85-3340	3141	UPM00315	UXV760CC	J85-3340	3151	UCV761CC	UXV760CC	J85-3340
1883	1883	UCC0031F	UXV760CC	J85-3340	3171	UXV762CC	UM000325	J85-3340	3181	UPM00315	UM000325	J85-3340
1884	1884	UXV761CC	UM000325	J85-3340	3201	UCC0031F	UM000325	J85-3340	3211	UXV762CC	J85-3240	UXV760CC
1885	1885	UCC0031F	J85-3240	UXV760CC	3231	UCV761CC	J85-3240	UXV760CC	3241	UCC0031F	J85-3240	UXV760CC
1886	1886	UXV761CC	UXV760CC	UXV760CC	3261	UPM00315	UXV760CC	UXV760CC	3271	UCV761CC	UXV760CC	UXV760CC
1887	1887	UCC0031F	UXV760CC	UXV760CC	3291	UXV762CC	UM000325	UXV760CC	3301	UPM00315	UM000325	UXV760CC



TABLE 4 (continued)

TABLE 1. *Phylogenetic relationships of the 10 studied species*

TABLE 1. AERIAL COLLING WATER SYSTEM (INDIAN POINT)

COMPONENT COOLING WATER SYSTEM INDIAN POINT 3 MINIMAL CUTSETS  
(Sheet 4 of 4)

001 8:15, 1990 0 2942 19415.

[illegible]



TABLE 5

SYSTEM EFFECTS OF PIPE FAILURE - INDIAN POINT 3 COMPONENT COOLING SYSTEM

Pipe Section	Diameter (Inches)	System Failure	Potential for Other Systems Impact	Comments
1. #199 CC Pump Discharge Header to Heat Exchanger 31	14	Yes	Systems Cooled by CC System Fail	May split the system and recover one half of system. (Operator action)
2. #211 CC Pump Discharge Header to Heat Exchanger 32	14	Yes	Systems Cooled by CC System Fail	Same As 1 Above
3. #209 CC Pumps Discharge Cross-Tie Header	14	Yes	Systems Cooled by CC System Fail	Same As 1 Above
35 4. #53 CC Heat Exchangers Cross-Tie Header	12	Yes	Systems Cooled by CC System Fail	Same As 1 Above
5. #53 Supply Header from Heat Exchanger 31 (Three Sections)	16 14 12	Yes	Systems Cooled by CC System Fail	Same As 1 Above
6. #53A Supply Header from Heat Exchanger 32 (Three Sections)	16 14 12		Systems Cooled by CC System Fail	Same As 1 Above
7. #52 Return Header from RIHR Heat Exchanger 31 (Three Sections)	12 14 16	Yes	Systems Cooled by CC System Fail	Same As 1 Above
8. #52 Return Header from RIHR Heat Exchanger 32 (Three Sections)	12 14 16	Yes	Systems Cooled by CC System Fail	Same As 1 Above
9. #197 CC Pumps Suction Cross-Tie Header	12	Yes	Systems Cooled by CC	Same As 1 Above

TABLE 6

INDIAN POINT 3 COMPONENT COOLING SYSTEM - CAUSE TABLE

Basic Events	Failure Data				System Effect	Failure Data (t = 24 hours)	
	Hourly		Demand			Mean	Variance
	Mean	Variance	Mean	Variance			
CASE 1 BOUNDARY CONDITION: POWER AT ALL BUSES							
1. Single Events							
a. Manual Valve	$9.15 \times 10^{-8}$	$1.01 \times 10^{-14}$	-	-			
b. Service Water Supply Fails*	-	-	-	-			
c. Piping Failure (17)	$1.46 \times 10^{-8}$	$1.24 \times 10^{-13}$	-	-			
TOTAL	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$			System Failure	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$
2. Heat Exchanger Trains							
a. Train D	$1.34 \times 10^{-6}$	$.84 \times 10^{-12}$	-	-			
b. Train E	$1.52 \times 10^{-6}$	$3.01 \times 10^{-12}$	-	-			
TOTAL					System Failure	$3.52 \times 10^{-9}$	$2.91 \times 10^{-16}$
3. Pump Trains							
a. Operating Pump	$3.44 \times 10^{-6}$	$2.13 \times 10^{-11}$	-	-			
b. Standby Pump	-	-	$1.44 \times 10^{-3}$	$1.13 \times 10^{-6}$			
c. Previously Operating Pump	-	-	$1.43 \times 10^{-3}$	$1.13 \times 10^{-6}$			
TOTAL					System Failure	$9.15 \times 10^{-10}$	$7.99 \times 10^{-18}$
4. Test and Maintenance		(with pump trains)					
5. Human Error	-						
6. Common Cause	-						
7. Other	-						
SYSTEM TOTAL						$1.11 \times 10^{-7}$	$1.54 \times 10^{-14}$

\* Service water shown for completeness only, quantified at the event tree level.

TABLE 6 (continued)

## INDIAN POINT 3 COMPONENT COOLING SYSTEM - CAUSE TABLE

Basic Events	Failure Data				System Effect	Failure Data (t = 24 hours)	
	Hourly		Demand			Mean	Variance
	Mean	Variance	Mean	Variance			
CASE 1 BOUNDARY CONDITION: POWER AT TWO BUSES							
1. Single Events							
a. Manual Valve	$9.15 \times 10^{-8}$	$1.01 \times 10^{-14}$	-	-			
b. Service Water Supply Failure*	$1.46 \times 10^{-8}$	$1.24 \times 10^{-13}$	-	-			
c. Piping Failure (17)	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$			System Failure	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$
TOTAL							
2. Heat Exchanger Trains							
a. Train D	$1.34 \times 10^{-6}$	$2.84 \times 10^{-12}$	-	-			
b. Train E	$1.52 \times 10^{-6}$	$3.01 \times 10^{-12}$	-	-	System Failure	$3.52 \times 10^{-9}$	$2.91 \times 10^{-16}$
TOTAL							
3. Pump Trains							
a. Operating Pump	$3.44 \times 10^{-6}$	$2.13 \times 10^{-11}$	-	-			
b. Standby Pump	-	-	$1.44 \times 10^{-3}$	$1.13 \times 10^{-6}$			
c. Previously Operating Pump	-	-	$1.43 \times 10^{-3}$	$1.13 \times 10^{-6}$	System Failure	$1.64 \times 10^{-6}$	$5.72 \times 10^{-12}$
TOTAL							
4. Test and Maintenance							
5. Human Error	-						
6. Common Cause	-						
7. Other	-						
SYSTEM TOTAL						$1.75 \times 10^{-6}$	$5.72 \times 10^{-12}$

\* Service water shown for completeness only, quantified at the event tree level.

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TABLE 6 (continued)

## INDIAN POINT 3 COMPONENT COOLING SYSTEM - CAUSE TABLE

Basic Events	Failure Data			System Effect	Failure Data (t x 24 hours)	
	Hourly		Demand		Mean	Variance
	Mean	Variance				
CASE 1 BOUNDARY CONDITION: Pump is AT ONE BUS						
1. Single Events						
a. Manual Valve	$9.15 \times 10^{-8}$	$1.01 \times 10^{-14}$	-			
b. Service Water Supply Falls*	$1.46 \times 10^{-8}$	$1.24 \times 10^{-13}$	-			
c. Piping Failure (17)	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$	-			
TOTAL				System Failure	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$
2. Heat Exchanger Trains						
a. Train D	$1.34 \times 10^{-6}$	$2.84 \times 10^{-12}$	-			
b. Train E	$1.52 \times 10^{-6}$	$3.01 \times 10^{-12}$	-			
TOTAL				System Failure	$3.52 \times 10^{-9}$	$2.91 \times 10^{-16}$
3. Pump Trains						
a. Operating Pump	$3.44 \times 10^{-6}$	$2.13 \times 10^{-11}$	-			
b. Standby Pump	-	-	$1.44 \times 10^{-3}$			$1.13 \times 10^{-6}$
c. Previously Operating Pump	-	-	$1.43 \times 10^{-3}$			$1.13 \times 10^{-6}$
TOTAL						
4. Test and Maintenance						
5. Human Error	-	-				
6. Common Cause	-	-				
7. Other	-	-				
SYSTEM TOTAL					$8.27 \times 10^{-5}$	$1.22 \times 10^{-8}$

\* Service water shown for completeness only, quantified at the event tree level.

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TABLE 6 (continued)

INDIAN POINT 3 COMPONENT COOLING SYSTEM - CAUSE TABLE

Basic Events	Failure Data				System Effect	Failure Data (t = 24 hours)	
	Hourly		Demand			Mean	Variance
	Mean	Variance	Mean	Variance			
CASE 2 BOUNDARY CONDITION: POWER AT ALL BUSES							
1. Single Events							
a. Manual Valve	9.15 x 10-8	1.01 x 10-14	-	-			
b. Service Water Supply Calls*	-	-	-	-			
c. Piping Failure (17)	1.46 x 10-8	1.24 x 10-13	-	-			
TOTAL	1.06 x 10-7	1.53 x 10-14			System Failure	1.06 x 10-7	1.53 x 10-14
2. Heat Exchanger Trains							
a. Train D	1.34 x 10-6	2.04 x 10-12	-	-			
b. Train E	1.52 x 10-6	3.01 x 10-12	-	-			
TOTAL					System Failure	3.52 x 10-9	2.91 x 10-16
3. Pump Trains							
a. Operating Pump	3.44 x 10-6	2.13 x 10-11	-	-			
b. Standby Pump	-	-	1.44 x 10-3	1.13 x 10-6			
c. Previously Operating Pump	-	-	1.43 x 10-3	1.13 x 10-6			
TOTAL					System Failure	1.87 x 10-7	1.21 x 10-13
4. Test and Maintenance							
5. Human Error	-						
6. Common Cause	-						
7. Other	-						
SYSTEM TOTAL						2.97 x 10-7	1.34 x 10-13

\* Service water shown for completeness only, quantified at the event tree level.

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TABLE 6 (continued)

## INDIAN POINT 3 COMPONENT COOLING SYSTEM - CAUSE TABLE

Basic Events	Failure Data				System Effect	Failure Data (t = 24 hours)	
	Hourly		Demand			Mean	Variance
	Mean	Variance	Mean	Variance			
CASE 2							
BOUNDARY CONDITION:							
POWER AT TWO BUSES							
1. Single Events							
a. Manual Valve	$9.15 \times 10^{-8}$	$1.01 \times 10^{-14}$	-	-			
b. Service Water Supply Falls*	-	-	-	-			
c. Piping Failure (17)	$1.46 \times 10^{-8}$	$1.24 \times 10^{-13}$	-	-			
TOTAL	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$			System Failure	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$
2. Heat Exchanger Trains							
a. Train D	$1.34 \times 10^{-6}$	$2.84 \times 10^{-12}$	-	-			
b. Train E	$1.52 \times 10^{-6}$	$3.01 \times 10^{-12}$	-	-			
TOTAL					System Failure	$3.51 \times 10^{-9}$	$2.91 \times 10^{-16}$
3. Pump Trains							
a. Operating Pump	$3.44 \times 10^{-6}$	$2.13 \times 10^{-11}$	-	-			
b. Standby Pump	-	-	$1.44 \times 10^{-3}$	$1.13 \times 10^{-6}$			
c. Previously Operating Pump	-	-	$1.43 \times 10^{-3}$	$1.13 \times 10^{-6}$			
TOTAL					System Failure	$3.01 \times 10^{-5}$	$8.34 \times 10^{-10}$
4. Test and Maintenance		(with pump trains)					
5. Human Error	-						
6. Common Cause	-						
7. Other	-						
SYSTEM TOTAL						$3.02 \times 10^{-5}$	$8.37 \times 10^{-10}$

\* Service water shown for completeness only, quantified at the event tree level.

TABLE 6 (continued)

## INDIAN POINT 3 COMPONENT COOLING SYSTEM - CAUSE TABLE

Basic Events	Failure Data				System Effect	Failure Data (t = 24 hours)	
	Hourly		Demand			Mean	Variance
	Mean	Variance	Mean	Variance			
CASE 2							
BOUNDARY CONDITION:							
POWER AT ONE BUS							
1. Single Events							
a. Manual Valve	$9.15 \times 10^{-8}$	$1.01 \times 10^{-14}$	-	-			
b. Service Water Supply Fails*	-	-	-	-			
c. Piping Failure (17)	$1.46 \times 10^{-8}$	$1.24 \times 10^{-13}$	-	-			
TOTAL	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$			System Failure	$1.06 \times 10^{-7}$	$1.53 \times 10^{-14}$
2. Heat Exchanger Trains							
a. Train D	$1.34 \times 10^{-6}$	$2.04 \times 10^{-12}$	-	-			
b. Train E	$1.52 \times 10^{-6}$	$3.01 \times 10^{-12}$	-	-			
TOTAL					System Failure	$3.52 \times 10^{-9}$	$2.91 \times 10^{-16}$
3. Pump Trains							
a. Operating Pump	$3.44 \times 10^{-6}$	$2.13 \times 10^{-11}$	-	-			
b. Standby Pump	-	-	$1.44 \times 10^{-3}$	$1.13 \times 10^{-6}$			
c. Previously Operating Pump	-	-	$1.43 \times 10^{-3}$	$1.13 \times 10^{-6}$			
TOTAL					System Failure	$1.51 \times 10^{-3}$	$1.03 \times 10^{-6}$
4. Test and Maintenance		(with pump trains)					
5. Human Error	-						
6. Common Cause	-						
7. Other	-						
SYSTEM TOTAL						$1.51 \times 10^{-3}$	$1.03 \times 10^{-6}$

\* Service water shown for completeness only, quantified at the event tree level.

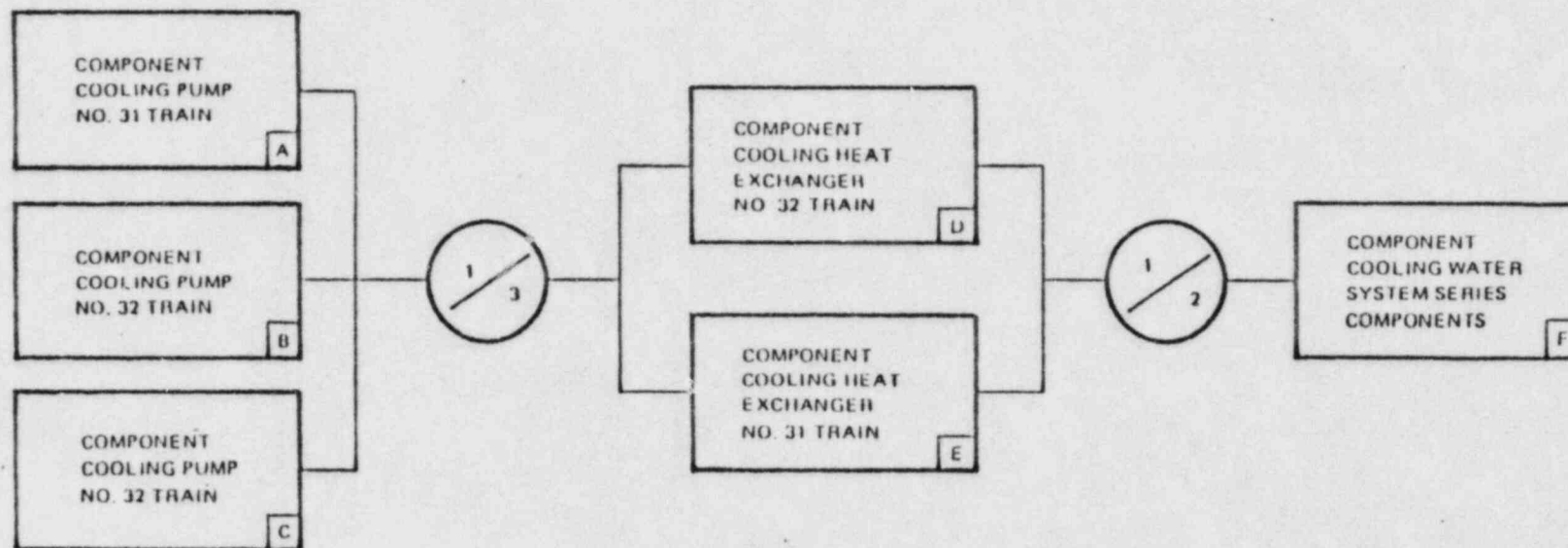


Figure 1. Indian Point 3 Component Cooling Water System Block Diagram

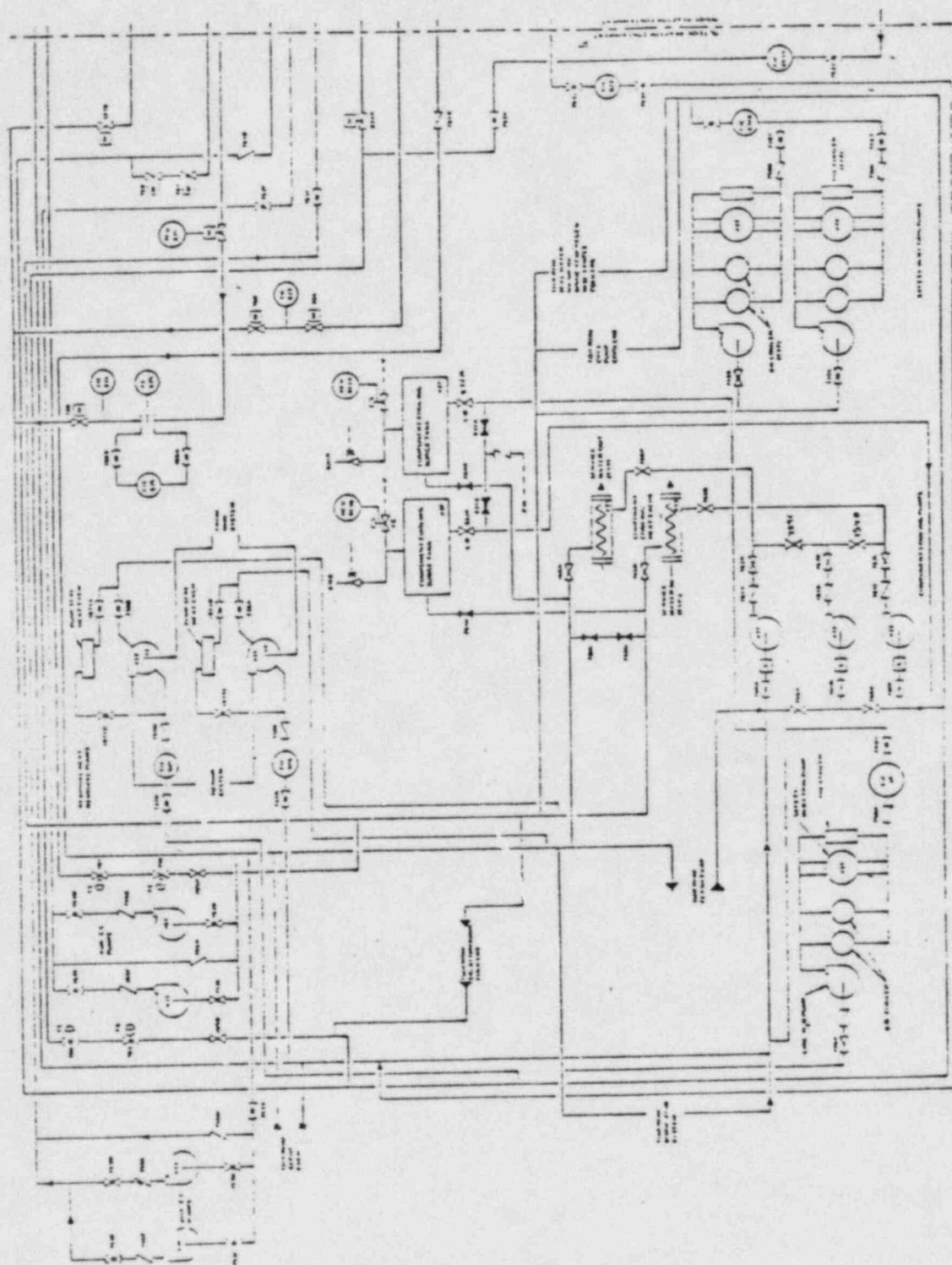


Figure 2. Simplified Schematic of Component Cooling System  
(Sheet 1 of 2)

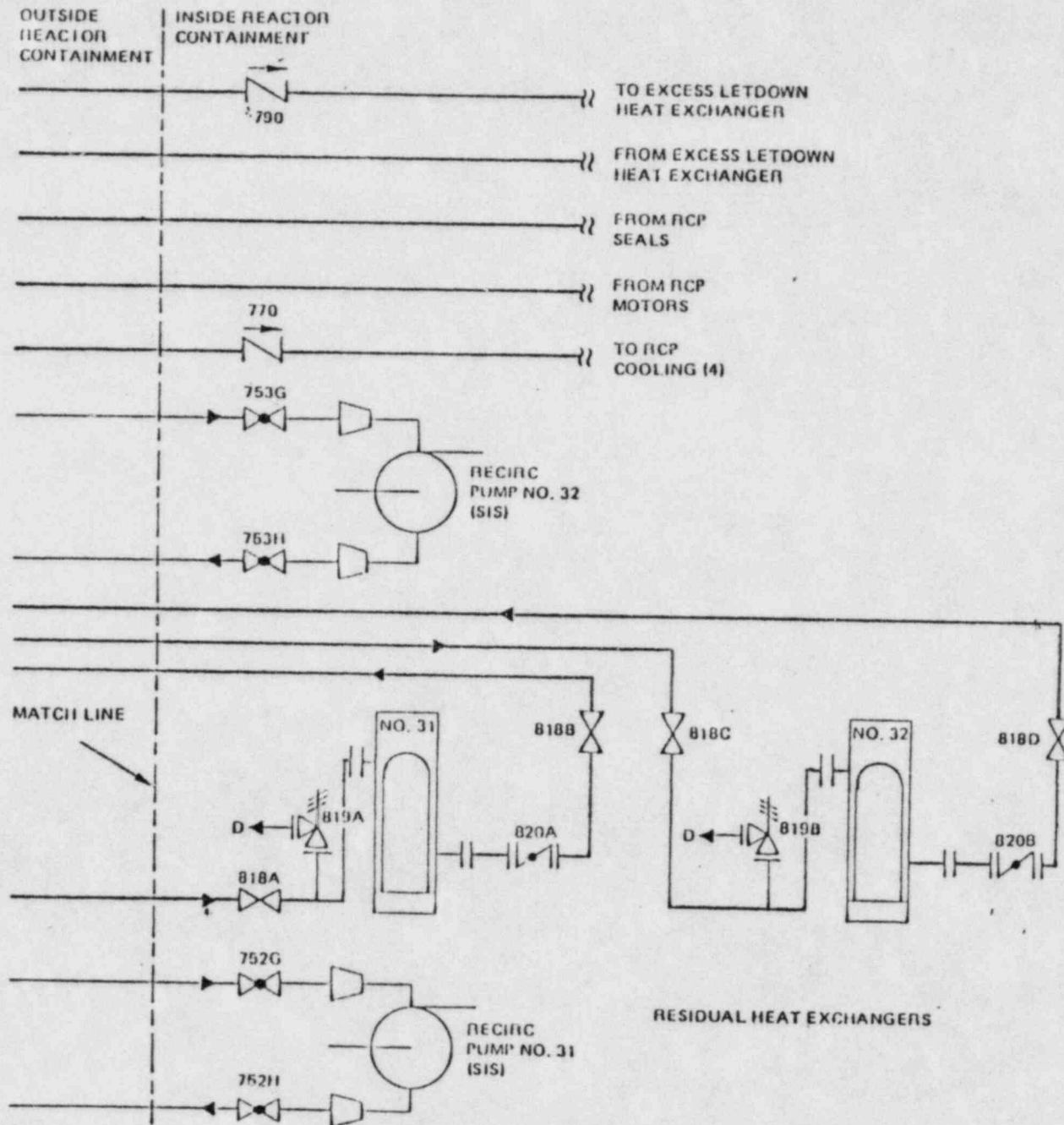


Figure 2. (Sheet 2 of 2)



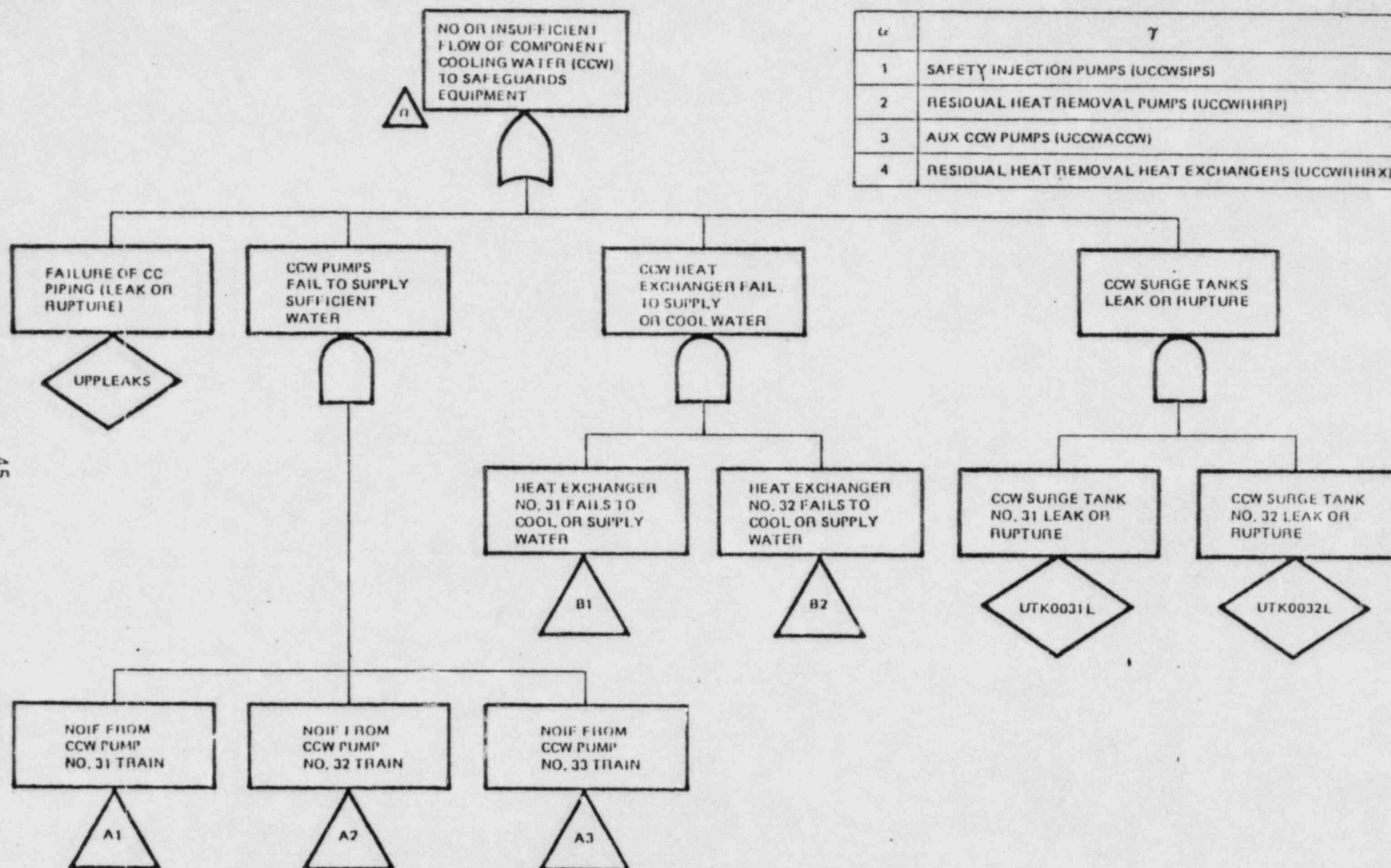


Figure 3. Indian Point 3 Component Cooling System Fault Tree  
(Sheet 1 of 4)

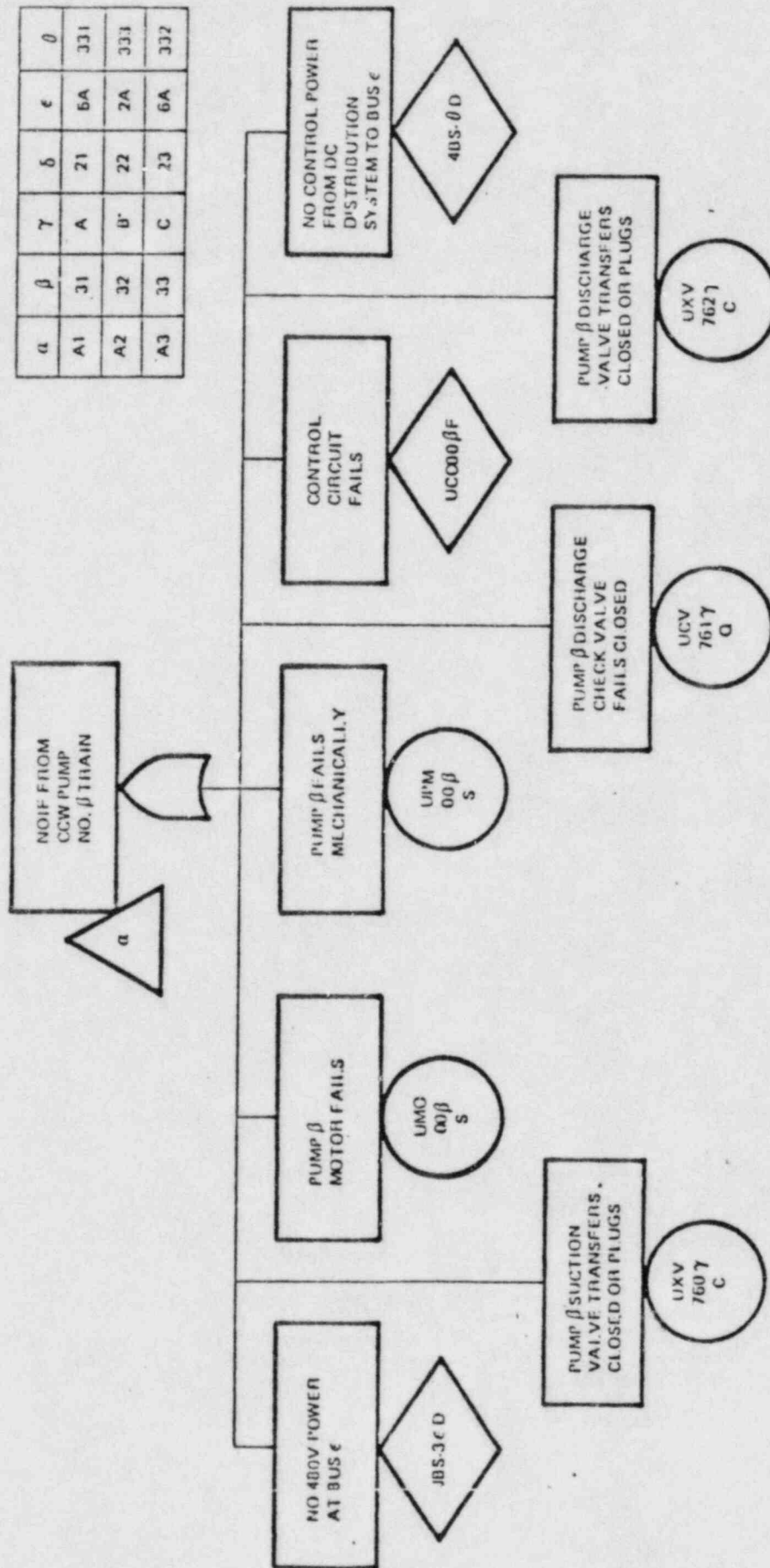


Figure 3. (Sheet 2 of 4)

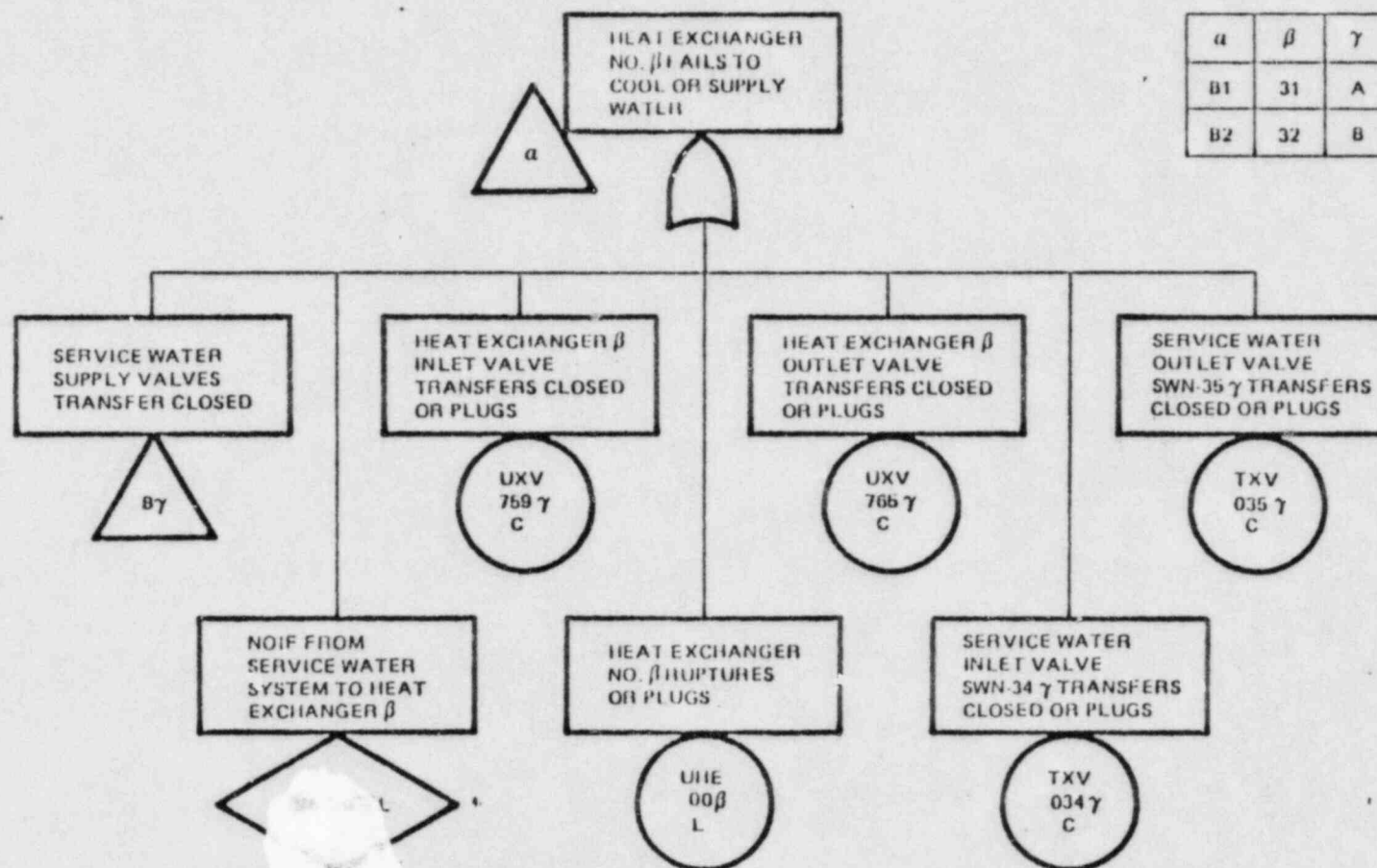


Figure 3. (Sheet 3 of 4)

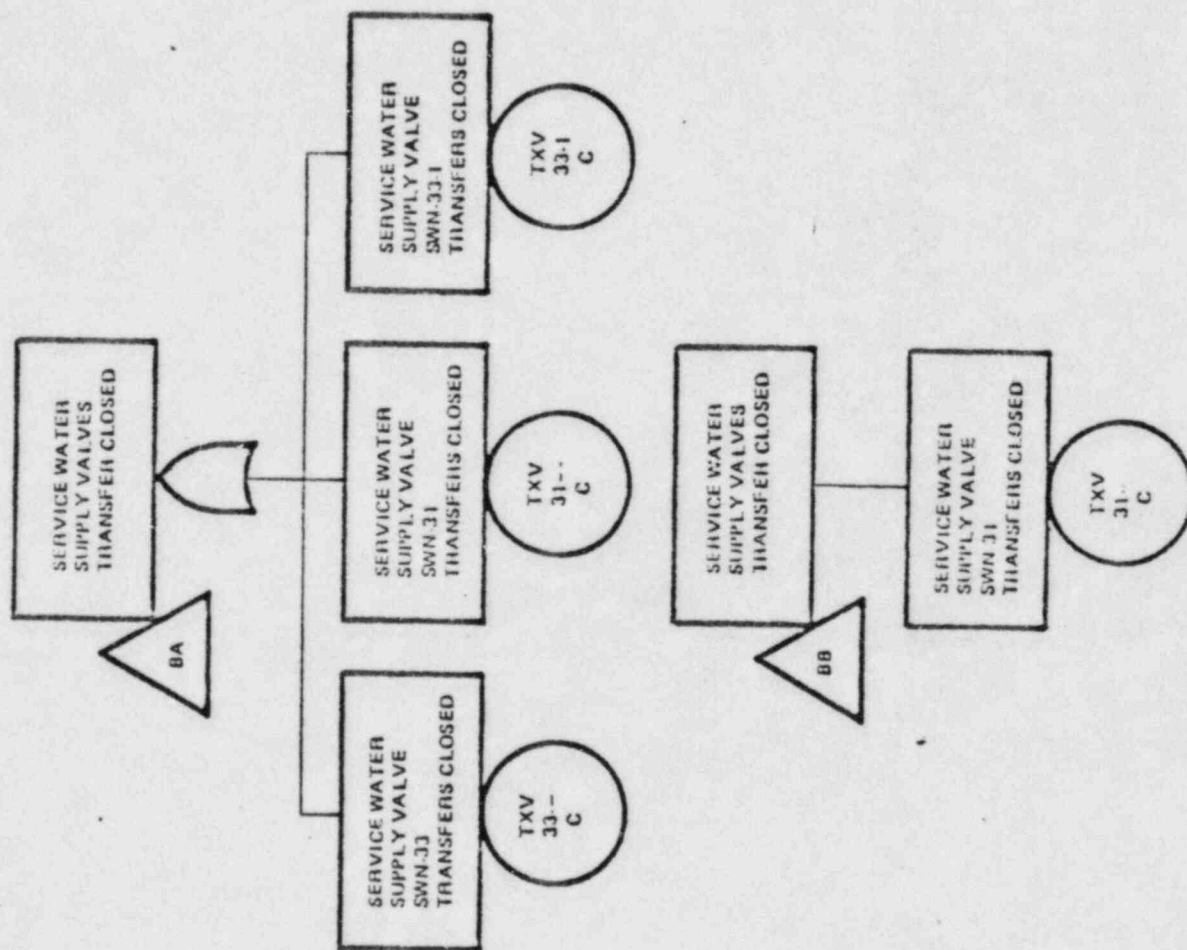


Figure 3. (Sheet 4 of 4)