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SUPPLEMENT TO THE JULY 1977 REPORT

PRESSURE MITIGATING SYSTEMS  
TRANSIENT ANALYSIS RESULTS

Prepared by

WESTINGHOUSE ELECTRIC CORPORATION

FOR

THE WESTINGHOUSE OWNERS GROUP ON

REACTOR COOLANT SYSTEM

OVERPRESSURIZATION

September 1977

775.000213

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59

DETERMINATION OF SETPOINT OVERSHOOT GIVEN SG

TUBE HEAT TRANSFER AREA AND RELIEF VALVE

SETPOINT WITHIN GENERIC ENVELOPE

REFERENCE

66

I. SUPPLEMENTARY LOFTRAN HEAT INPUT RESULTS

A. SETPOINT OVERSHOOT VARIATION WITH  
RELIEF VALVE OPENING TIME

Figure 1

# EFFECT OF RELIEF VALVE OPENING TIME ON RCS PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 6,000 CU.FT.

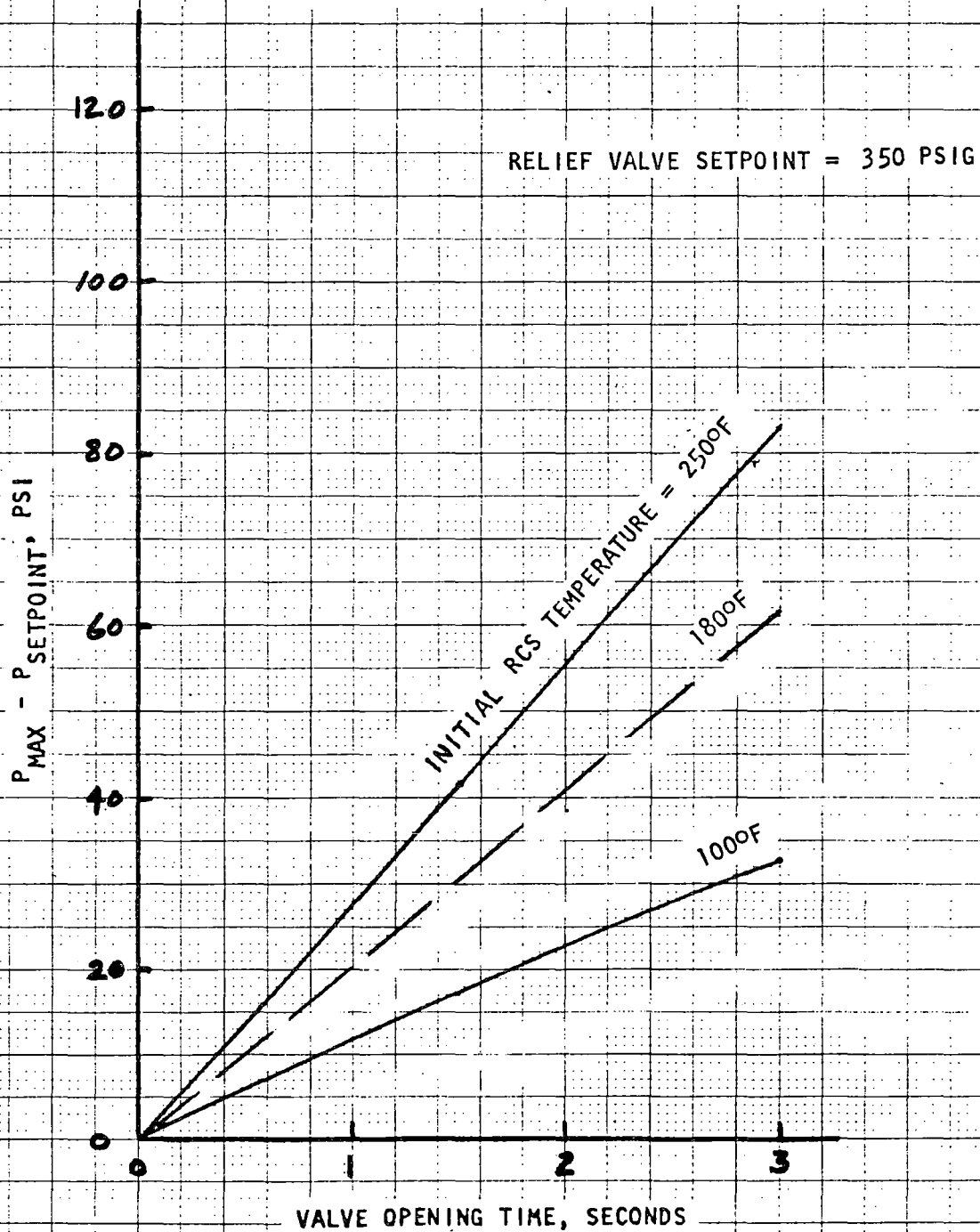
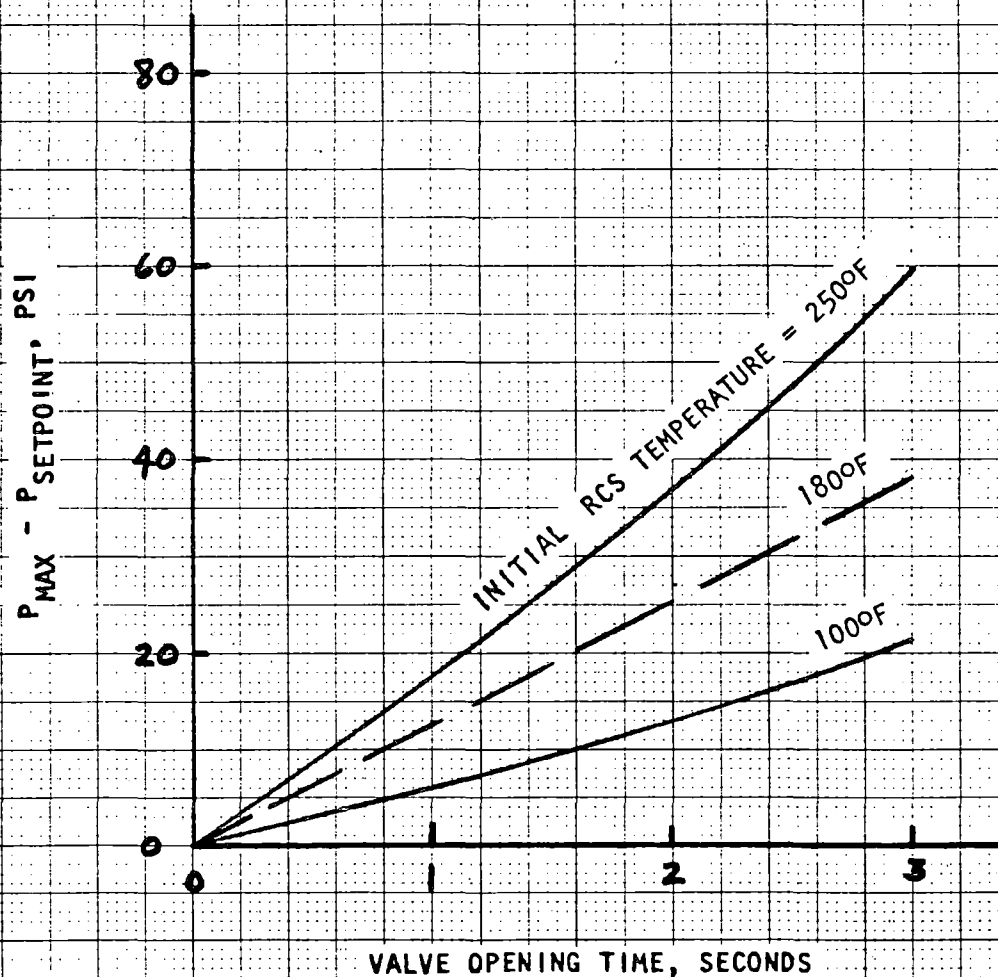


Figure 2

# EFFECT OF RELIEF VALVE OPENING TIME ON RCS PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 13000 CU.FT.

RELIEF VALVE SETPOINT = 350 PSIG



# EFFECT OF RELIEF VALVE OPENING TIME ON RCS PRESSURE OVERSHOOT

Figure 3

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 6,000 CU.FT.

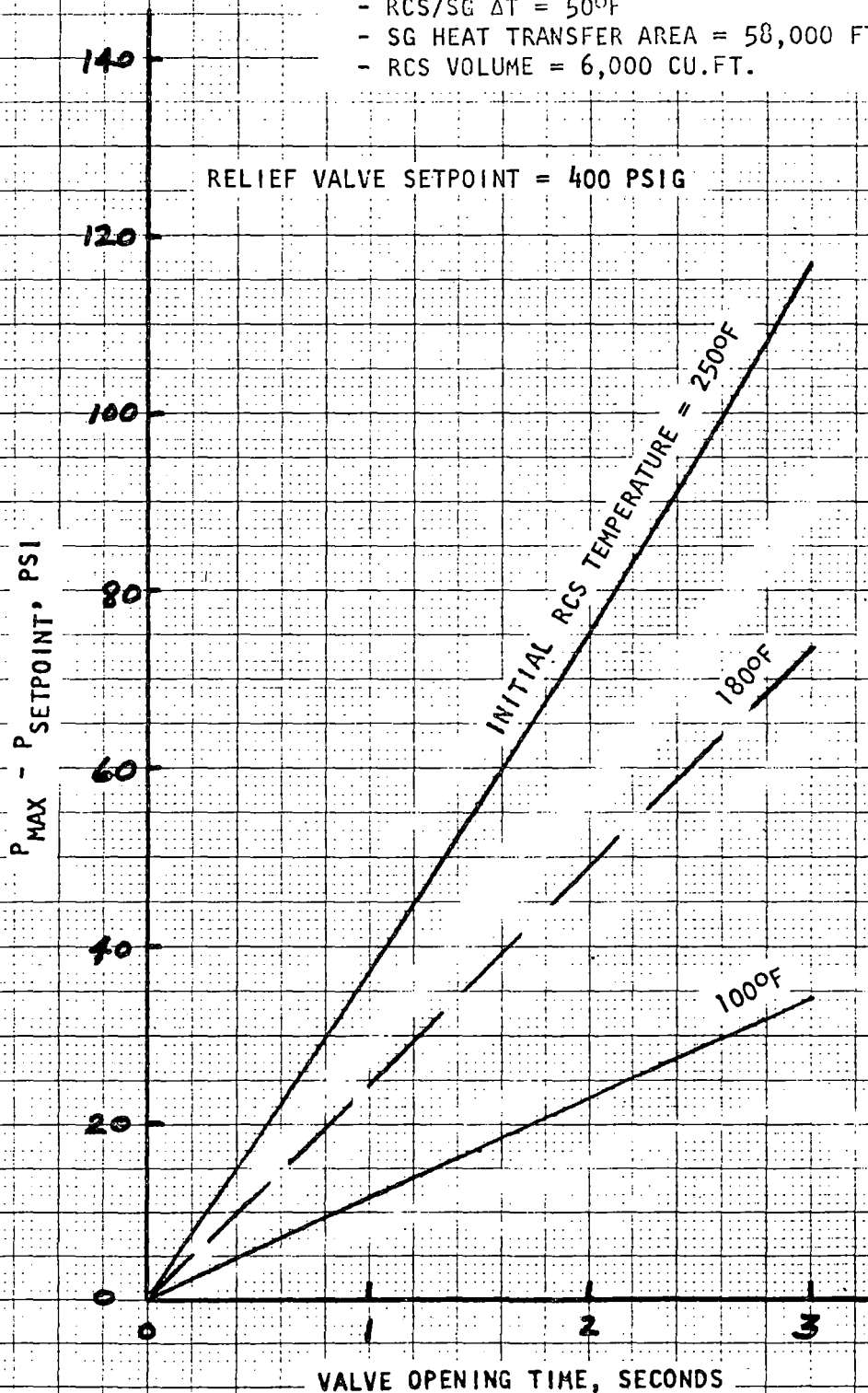


Figure 4

# EFFECT OF RELIEF VALVE OPENING TIME ON RCS PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 13000 CU. FT.

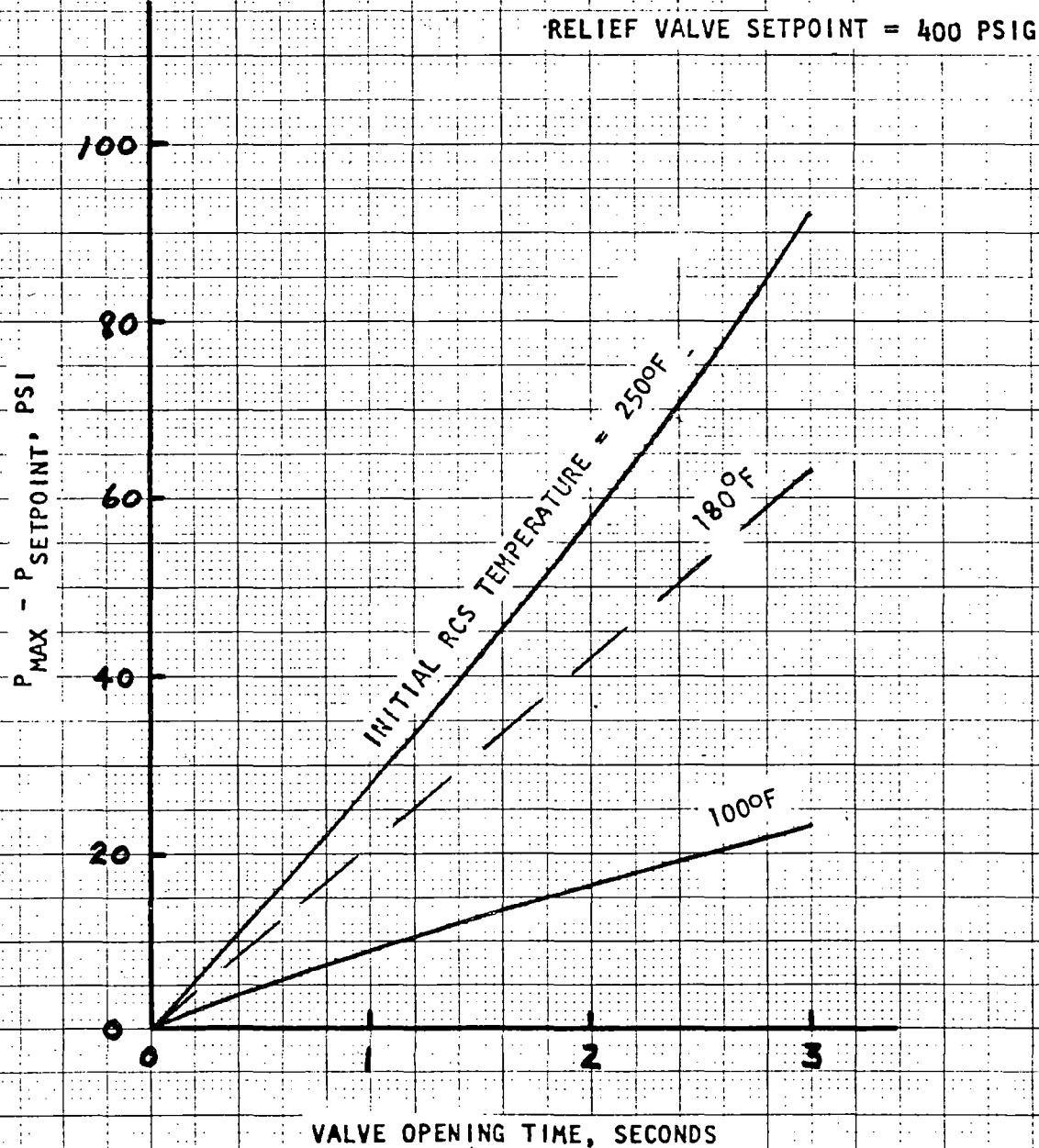
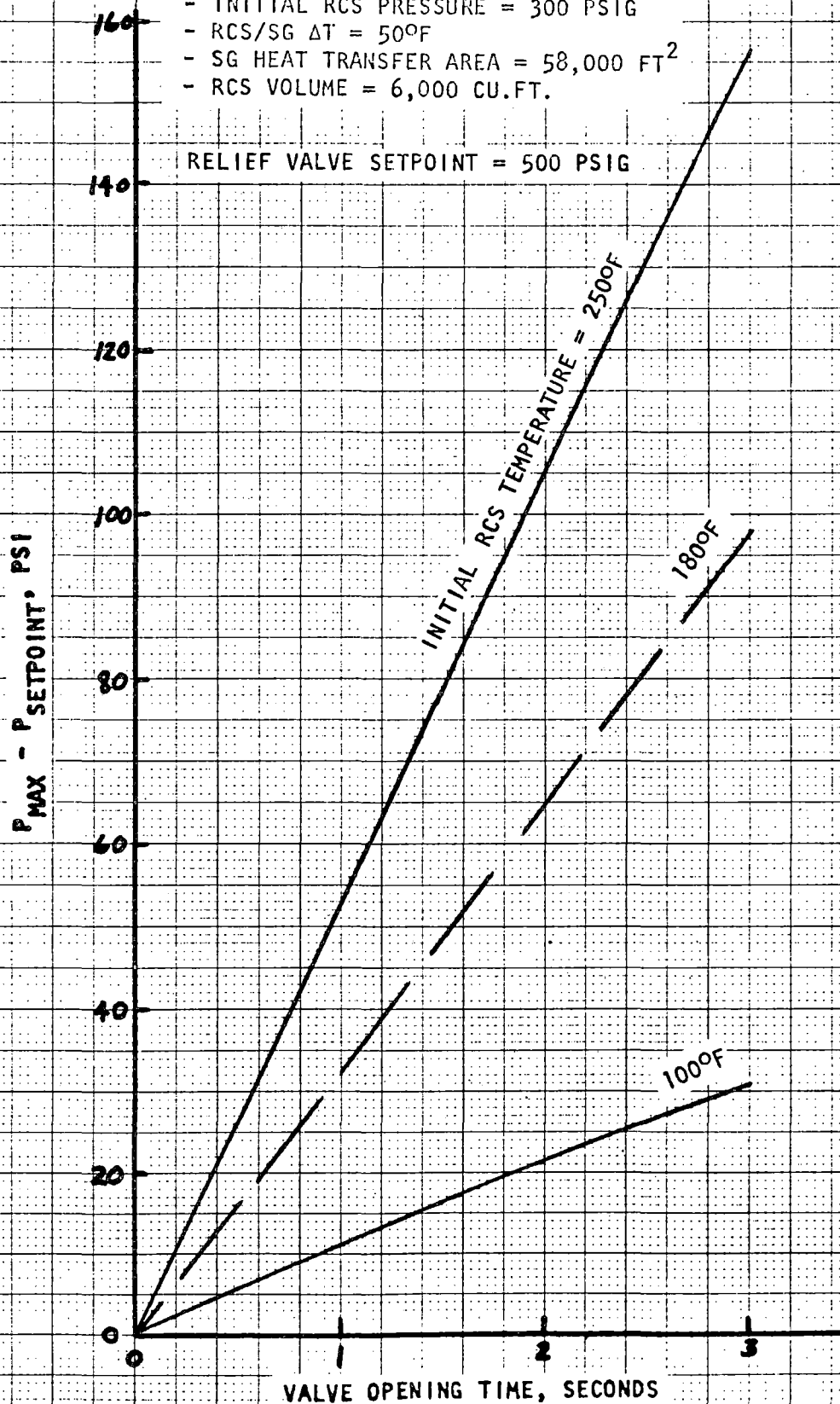


Figure 5

# EFFECT OF RELIEF VALVE OPENING TIME ON RCS PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 6,000 CU.FT.

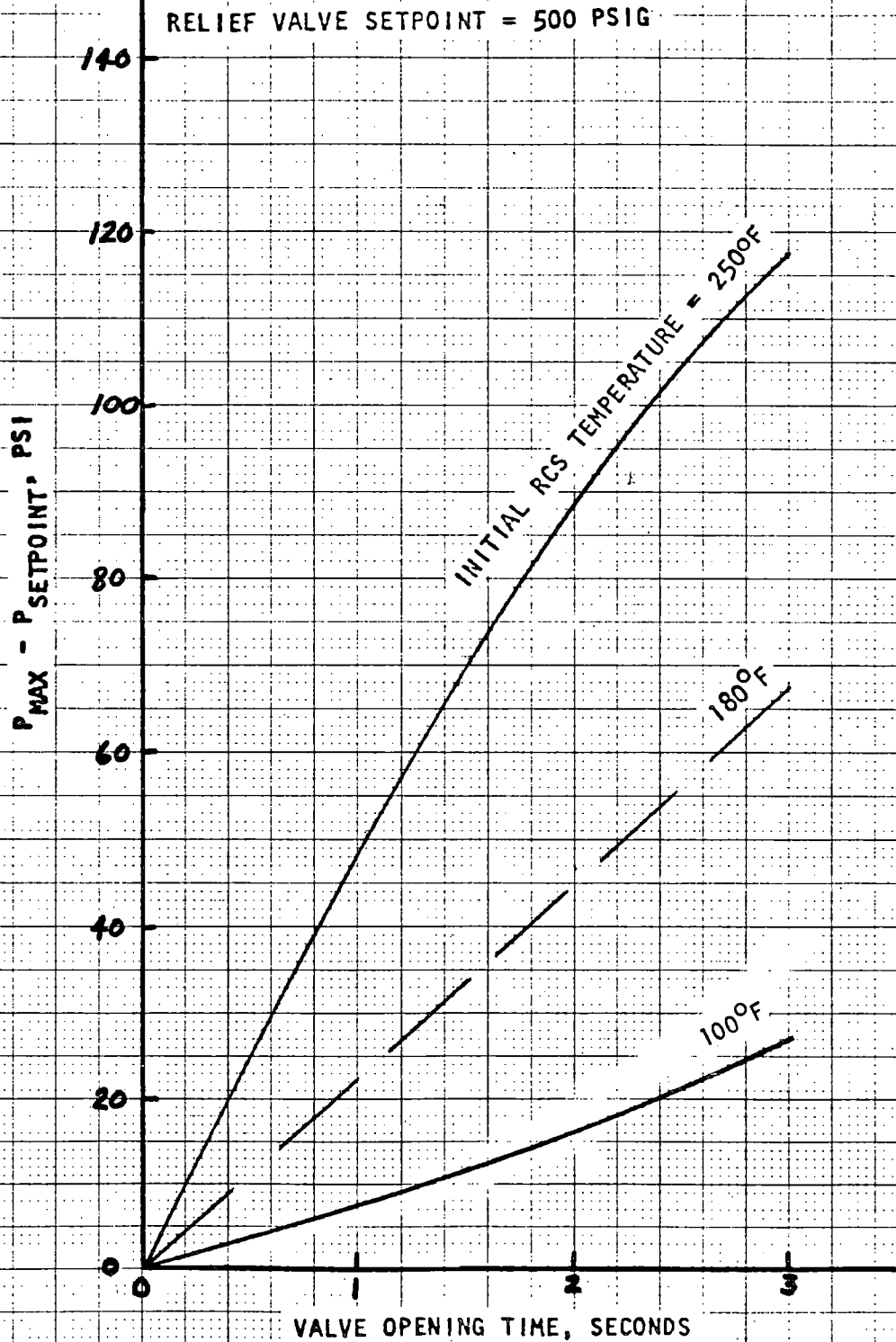
RELIEF VALVE SETPOINT = 500 PSIG



**EFFECT OF RELIEF VALVE  
OPENING TIME ON RCS  
PRESSURE OVERSHOOT**

Figure 6

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 13000 CU. FT.



B. SETPOINT OVERSHOOT VARIATION WITH  
RELIEF VALVE SETPOINT

Figure 7

# EFFECT OF RELIEF VALVE SETPOINT ON PRESSURE OVERSHOOT

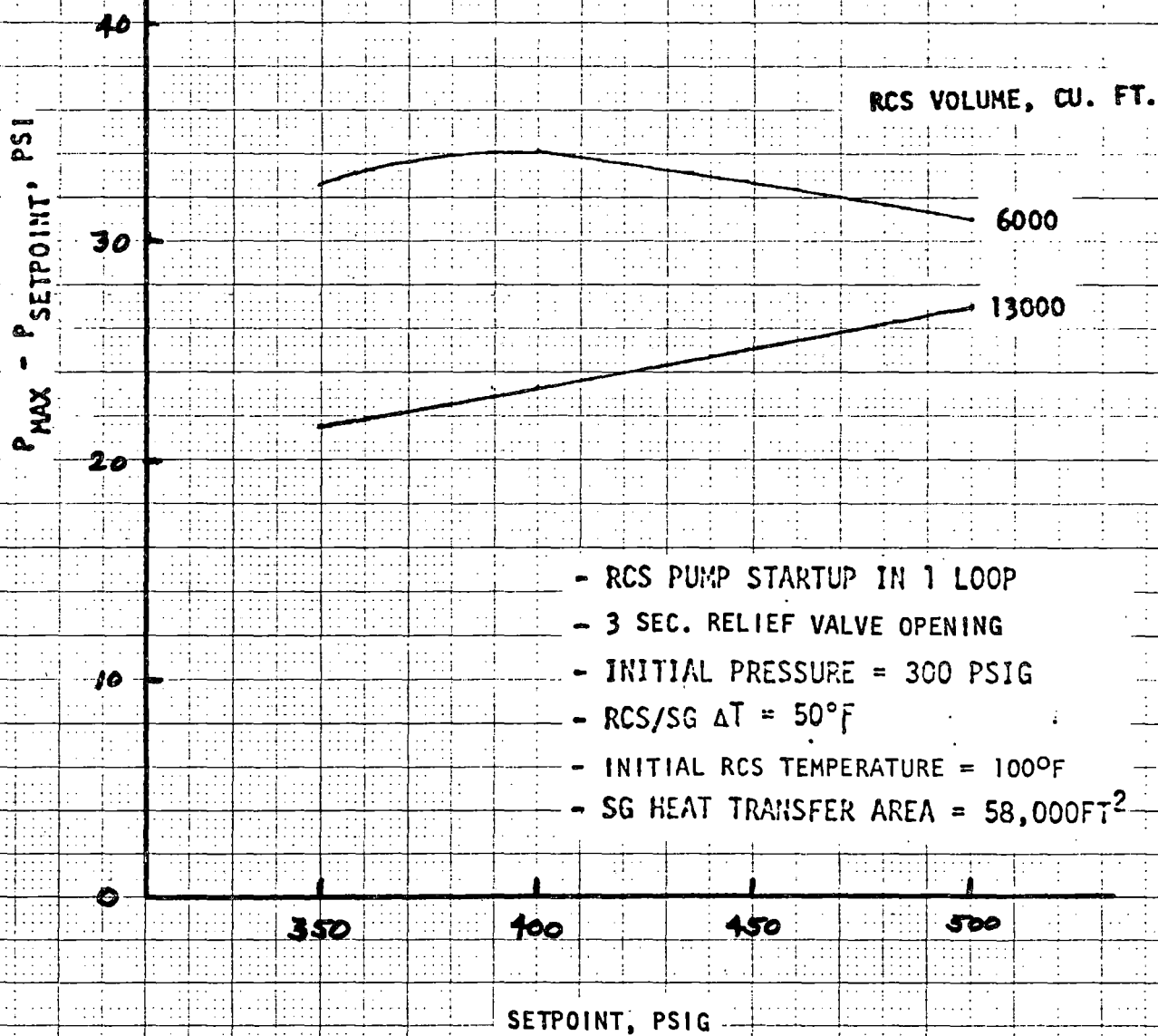


Figure 8

# EFFECT OF RELIEF VALVE SETPOINT ON PRESSURE OVERSHOOT

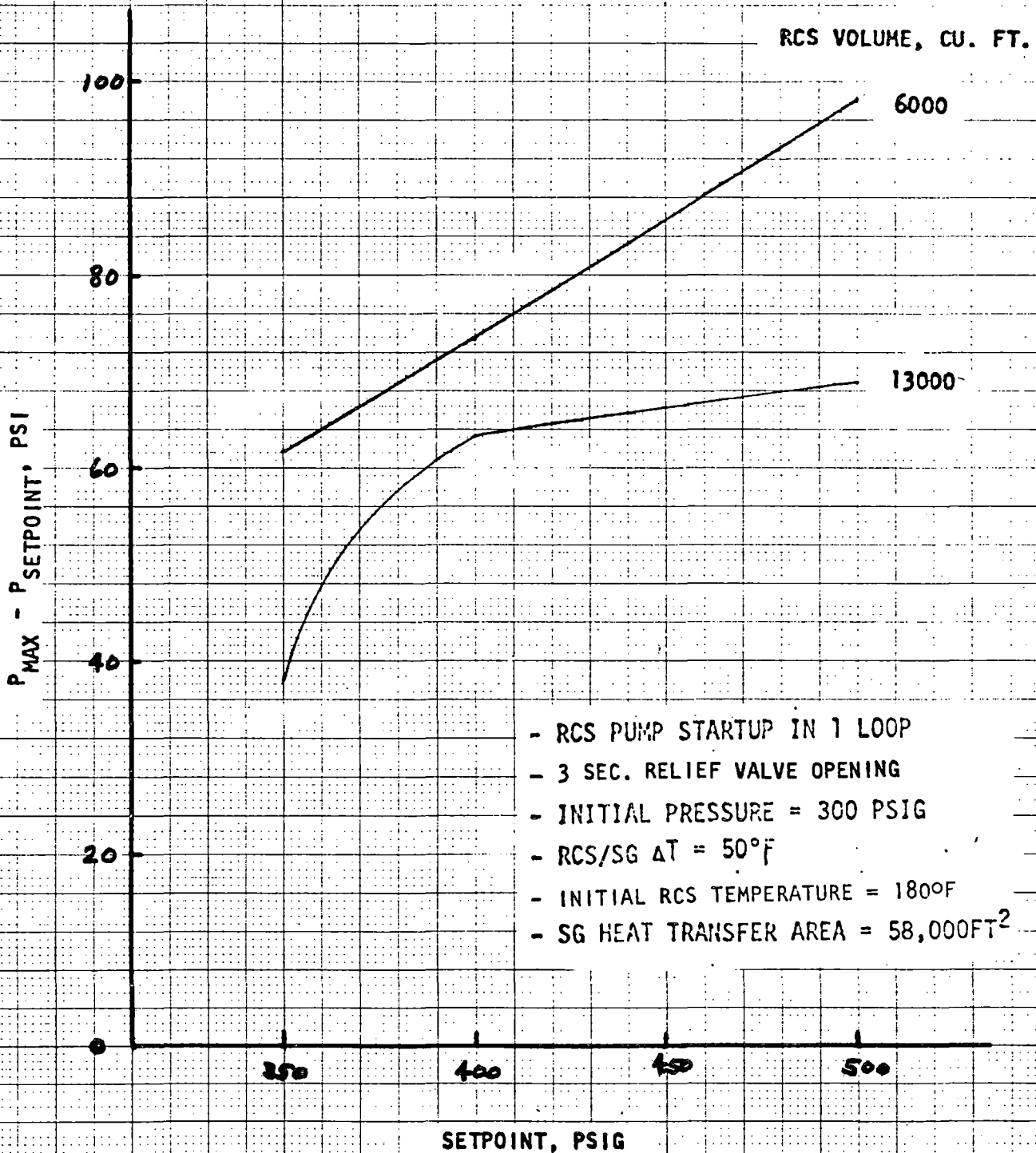


Figure 9

RCS VOLUME, CU. FT.

EFFECT OF RELIEF VALVE SETPOINT  
ON PRESSURE OVERSHOOT

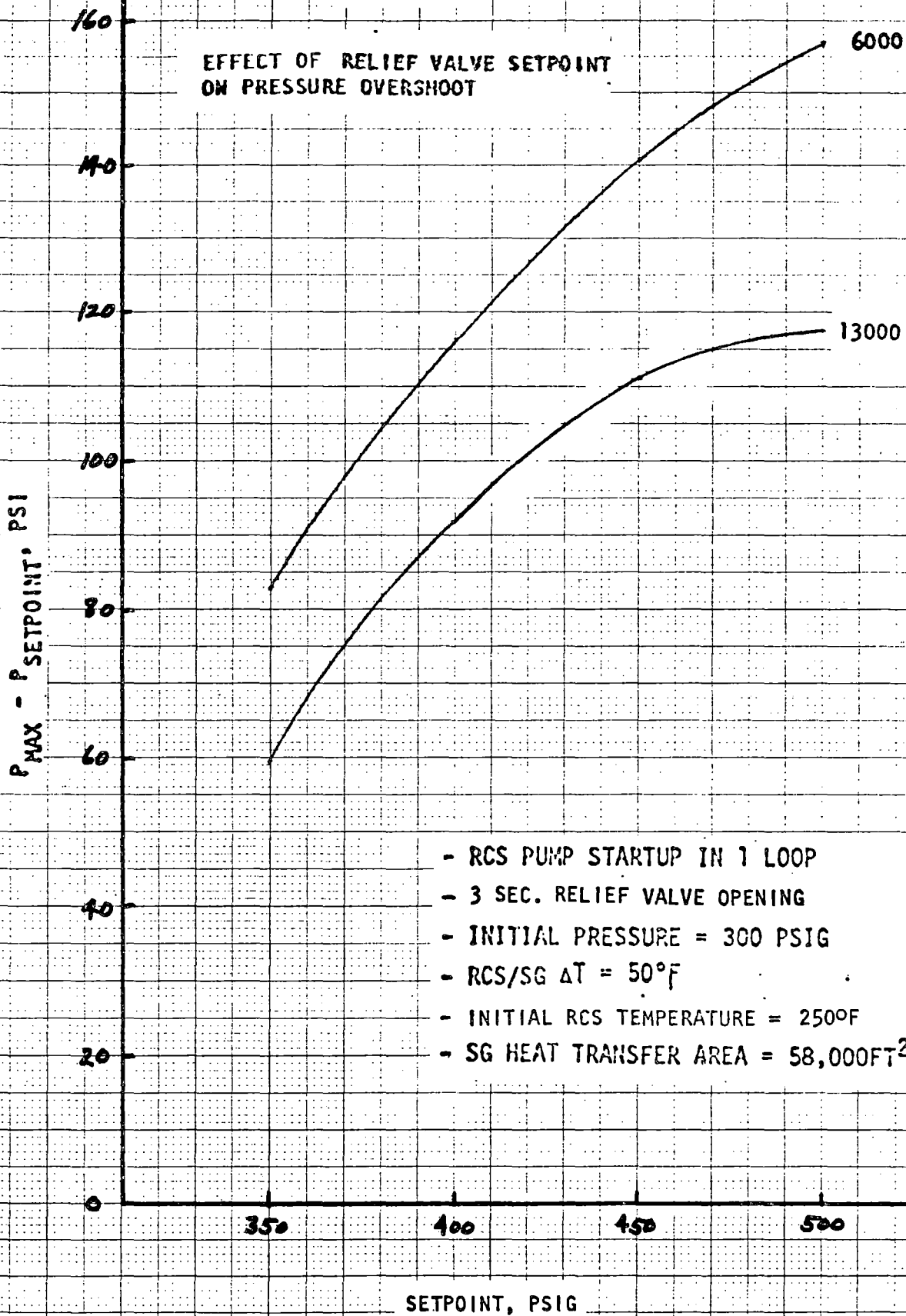


Figure 10

# EFFECT OF RELIEF VALVE SETPOINT ON PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- 1.5 SEC. RELIEF VALVE OPENING
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- INITIAL RCS TEMPERATURE =  $100^{\circ}F$
- SG HEAT TRANSFER AREA = 58,000FT<sup>2</sup>

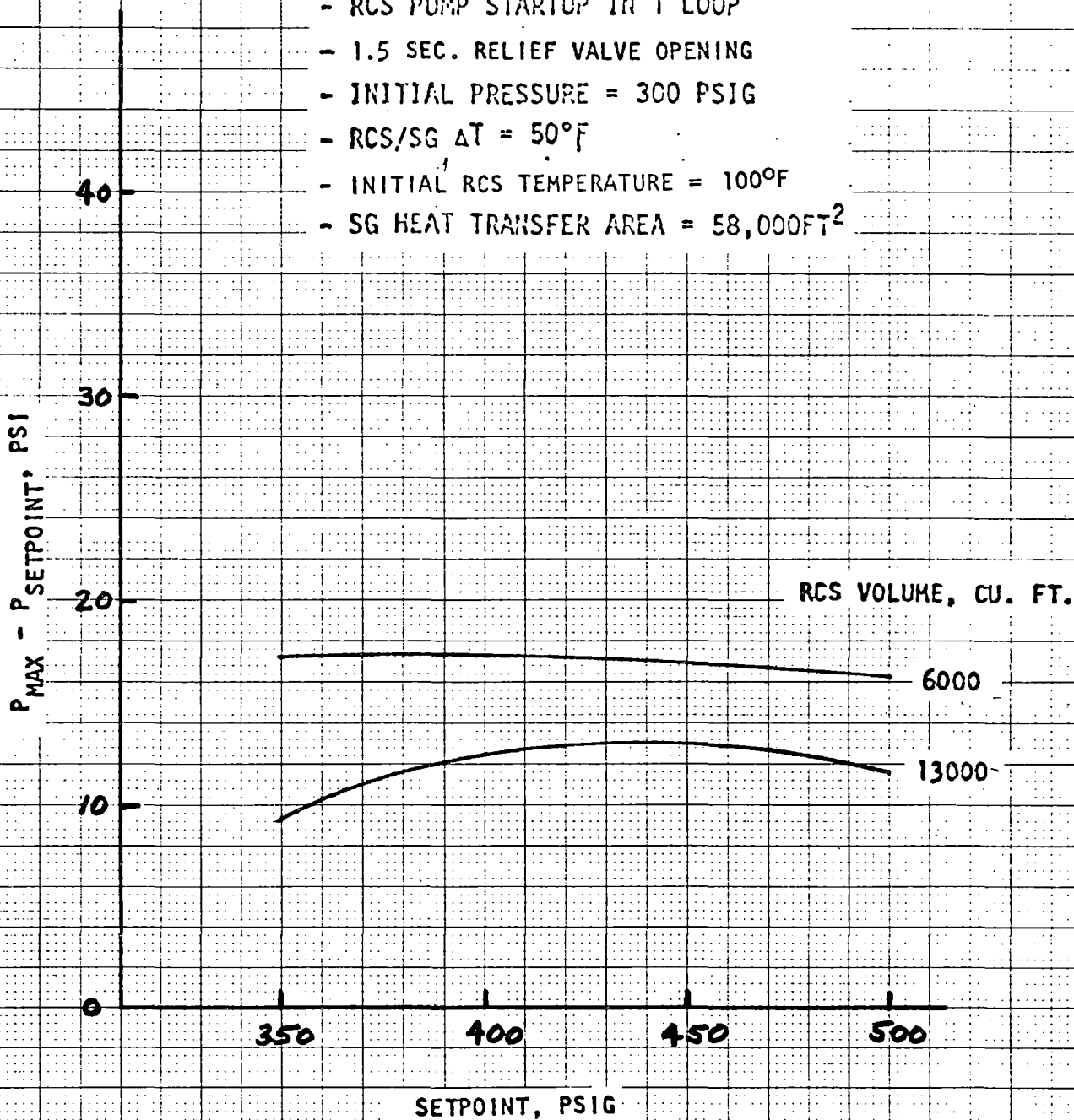
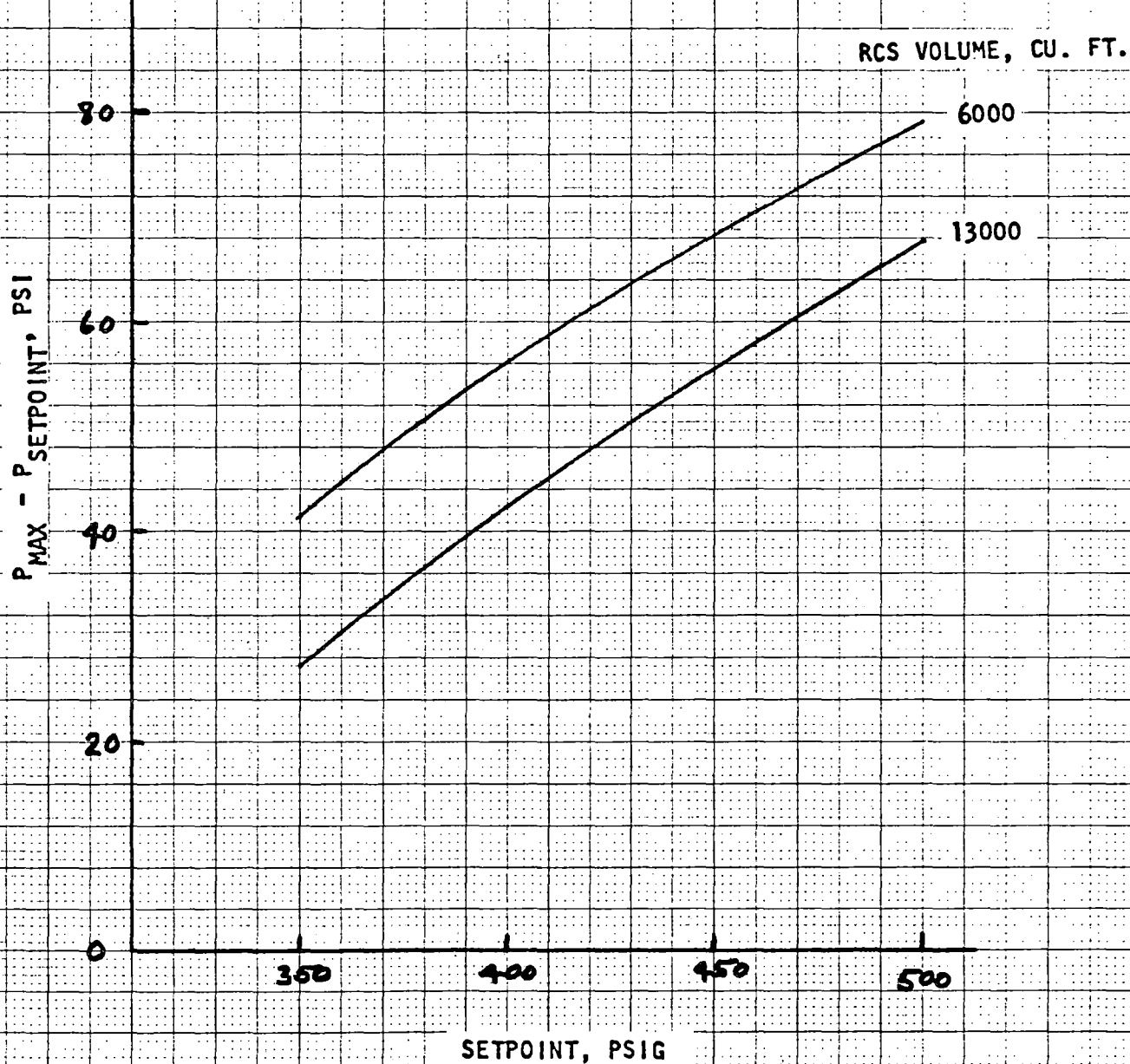


Figure 11

# EFFECT OF RELIEF VALVE SETPOINT ON PRESSURE OVERSHOOT

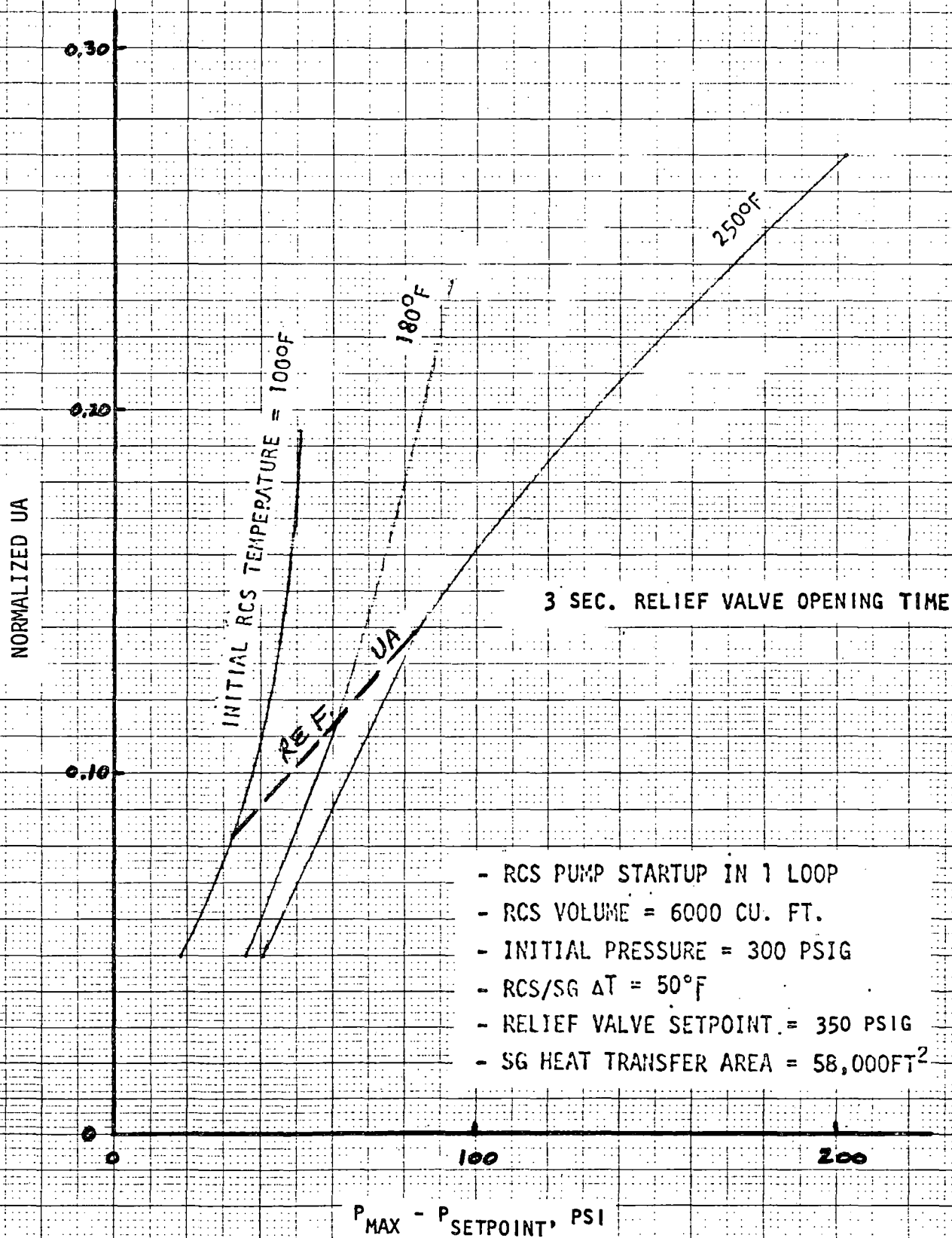
- RCS PUMP STARTUP IN 1 LOOP
- 1.5 SEC. RELIEF VALVE OPENING
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}F$
- INITIAL RCS TEMPERATURE =  $250^{\circ}F$
- SG HEAT TRANSFER AREA =  $58,000FT^2$



C. SETPOINT OVERSHOOT VARIATION WITH  
NORMALIZED STEAM GENERATOR UA

Figure 12

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT



# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

Figure 13

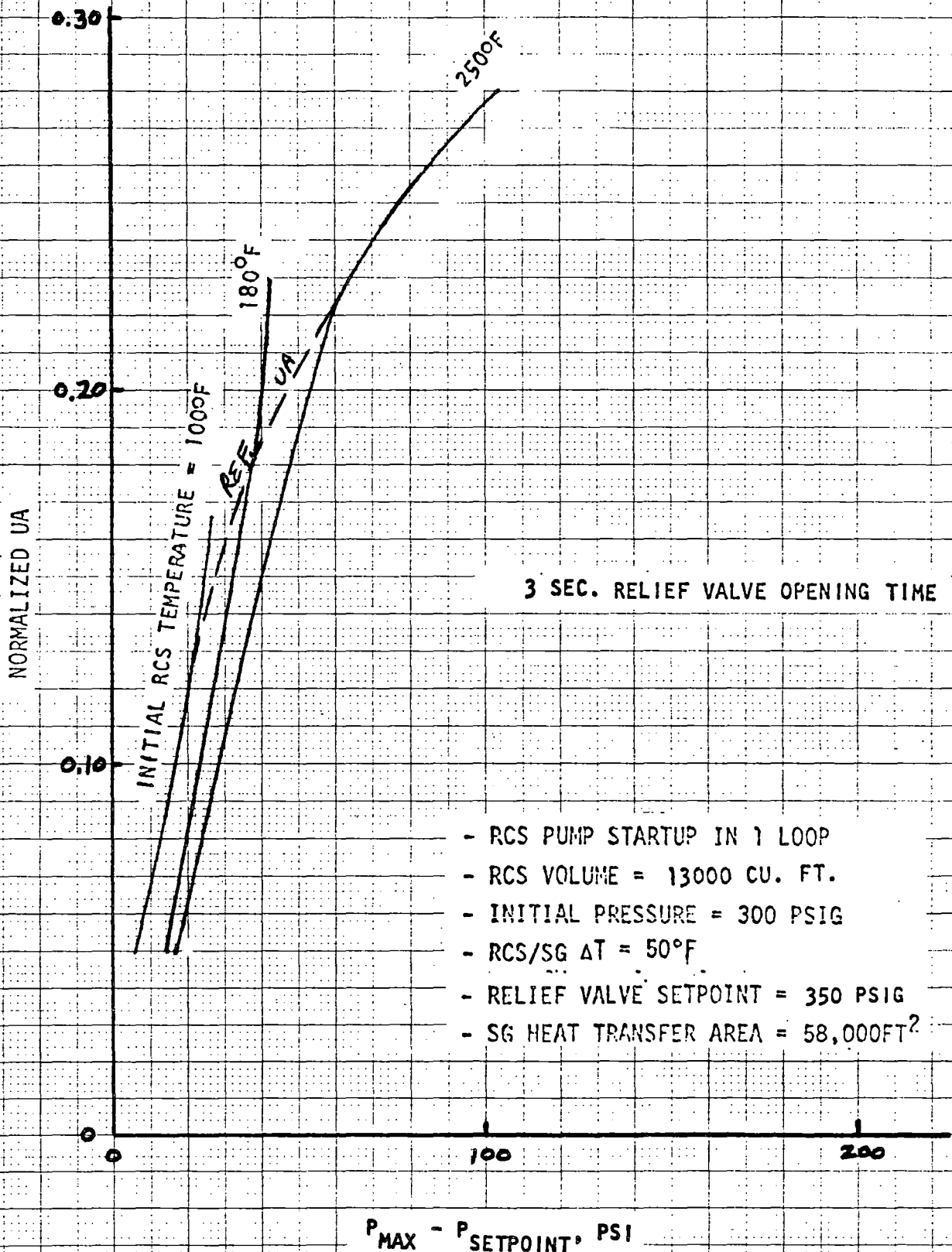
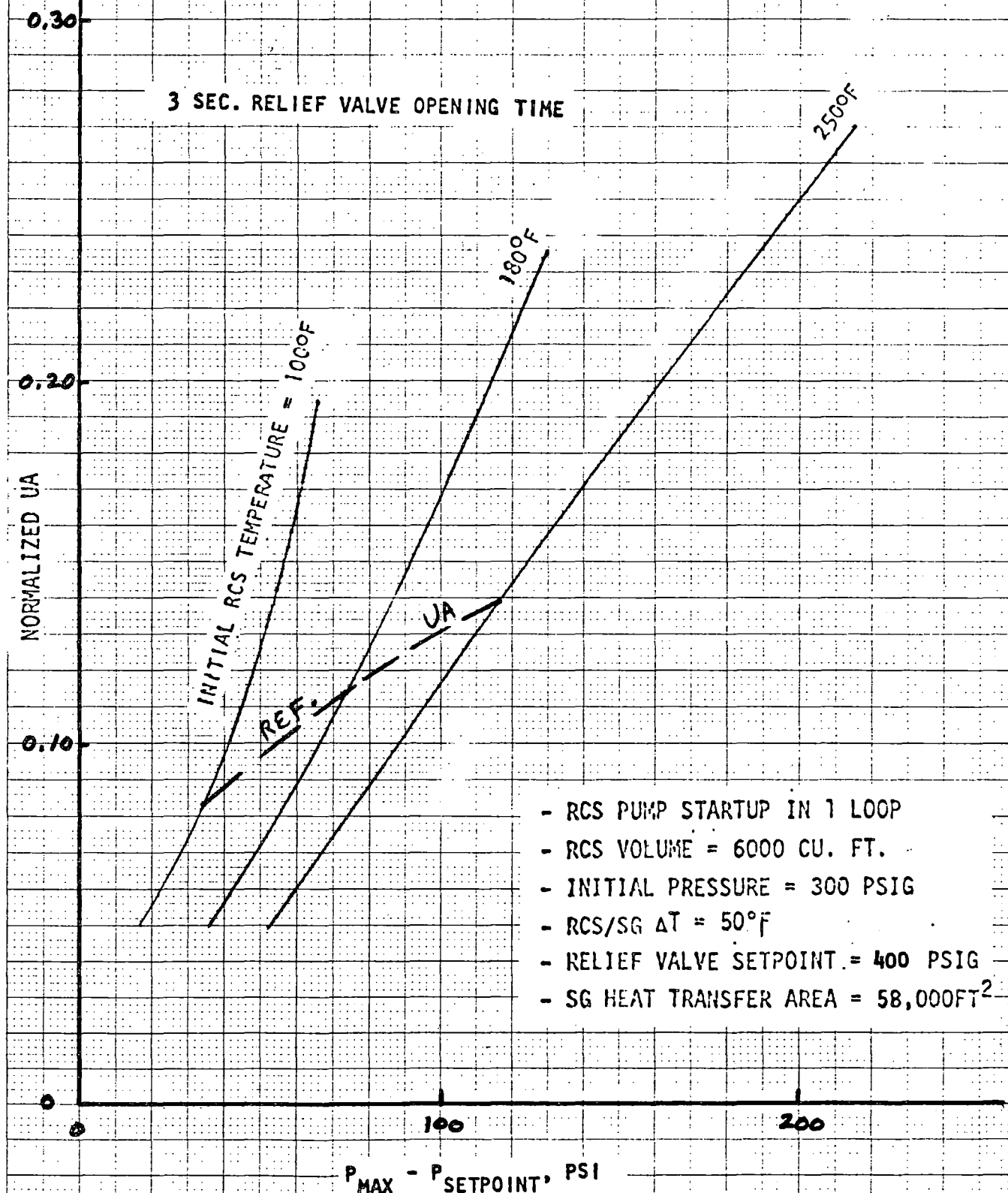


Figure 14

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT



# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

Figure 15

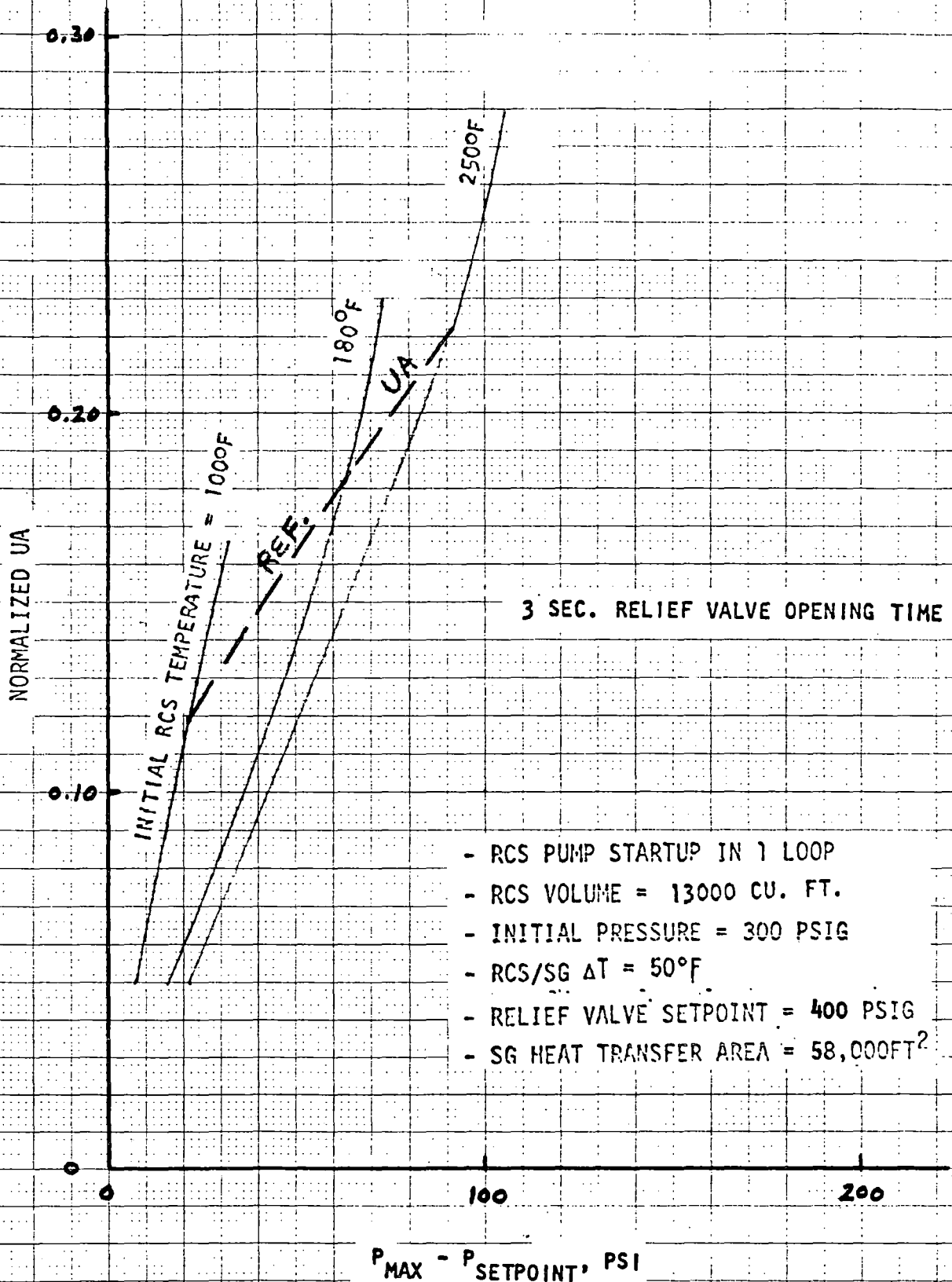


Figure 16

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

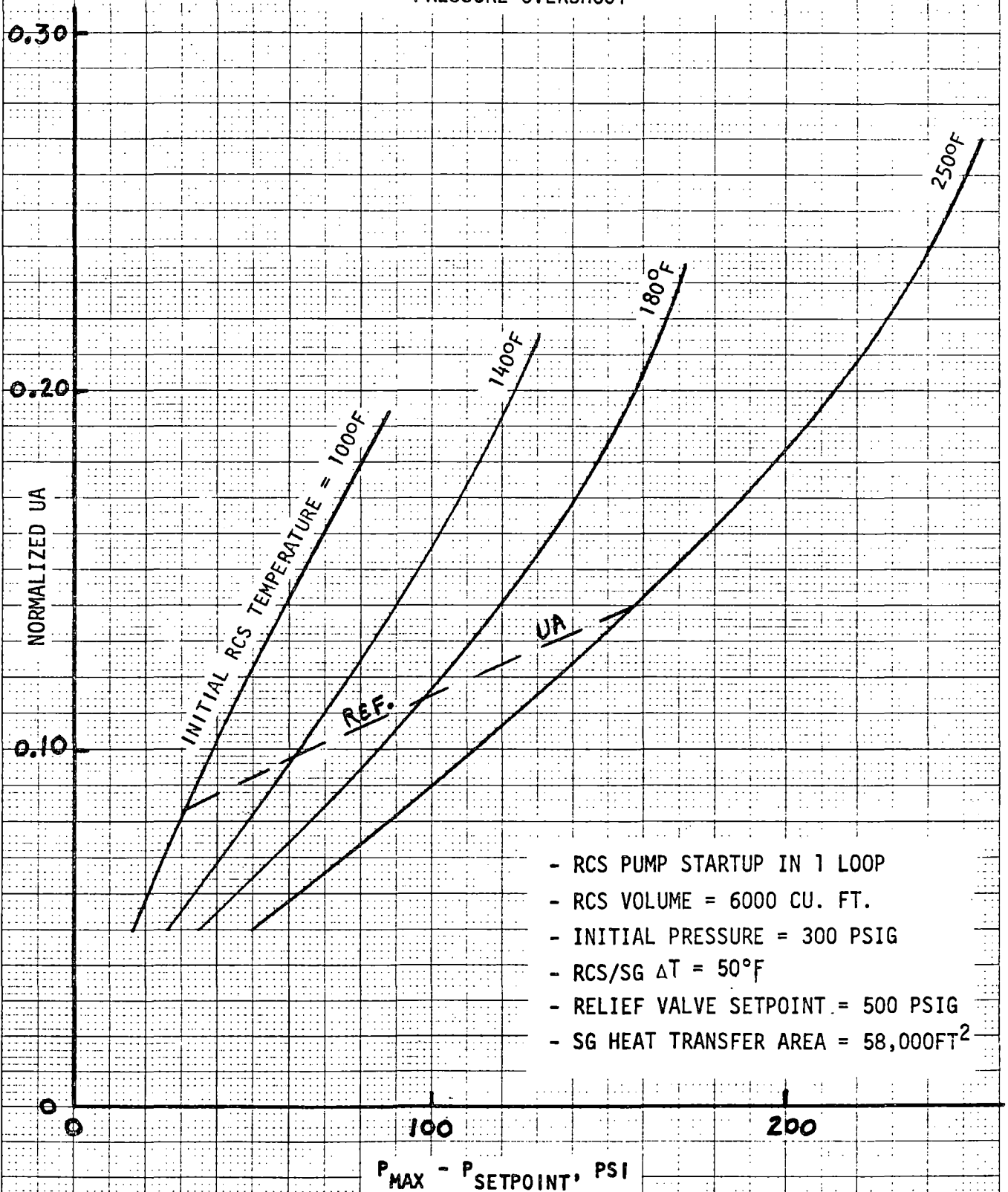


Figure 17

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

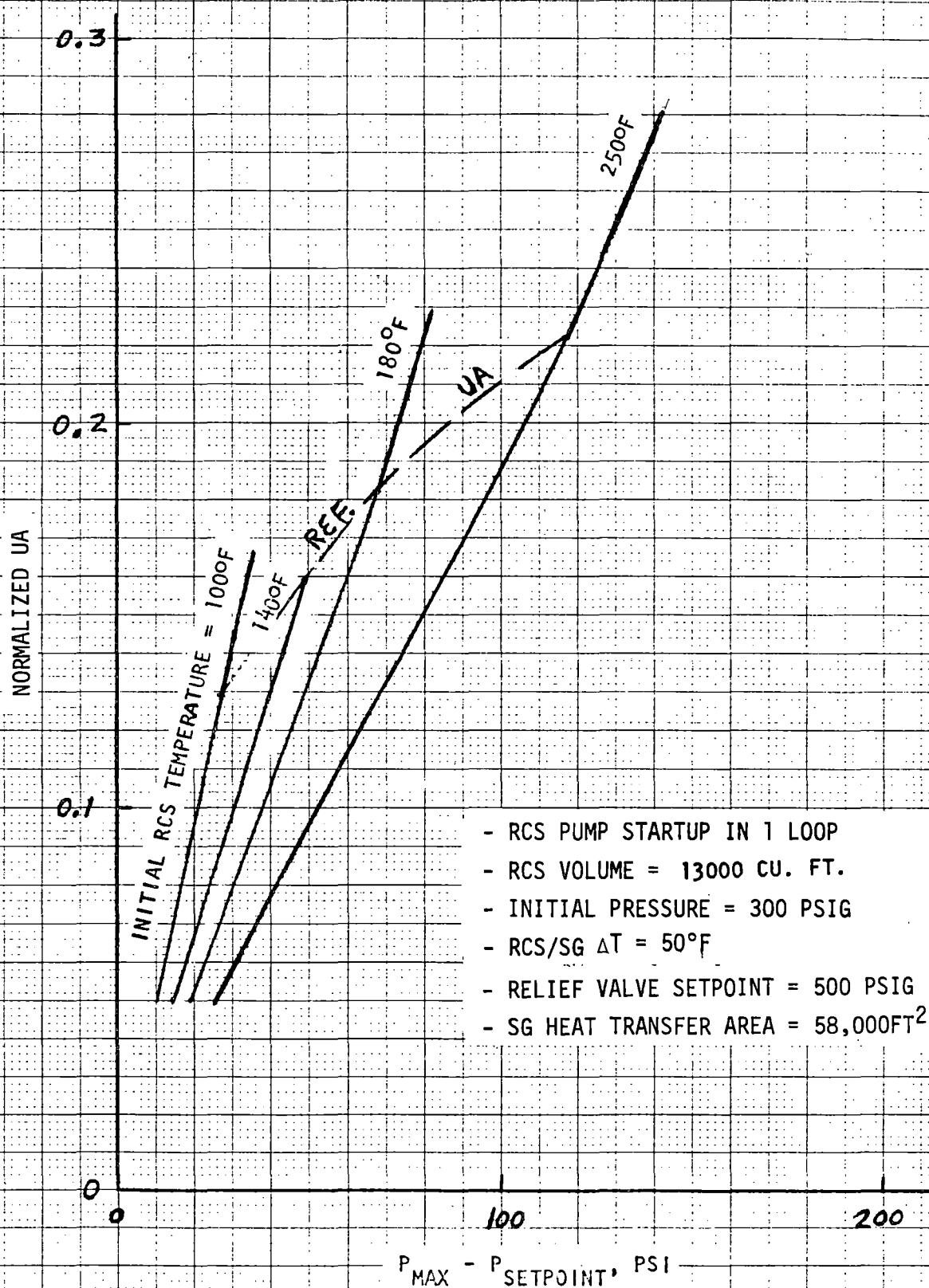
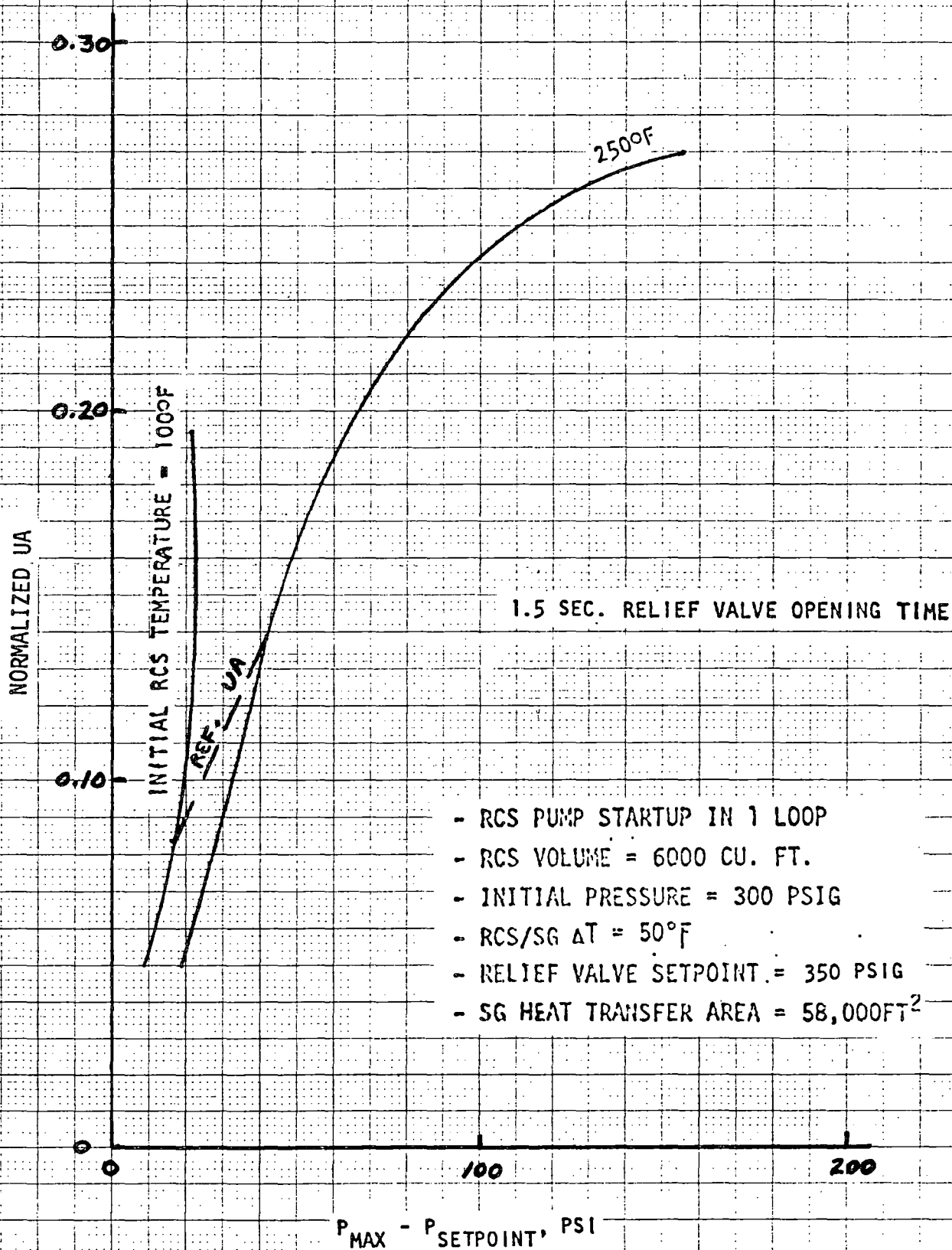


Figure 18

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT



- RCS PUMP STARTUP IN 1 LOOP
- RCS VOLUME = 6000 CU. FT.
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}\text{F}$
- RELIEF VALVE SETPOINT = 350 PSIG
- SG HEAT TRANSFER AREA = 58,000 $\text{FT}^2$

Figure 19

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

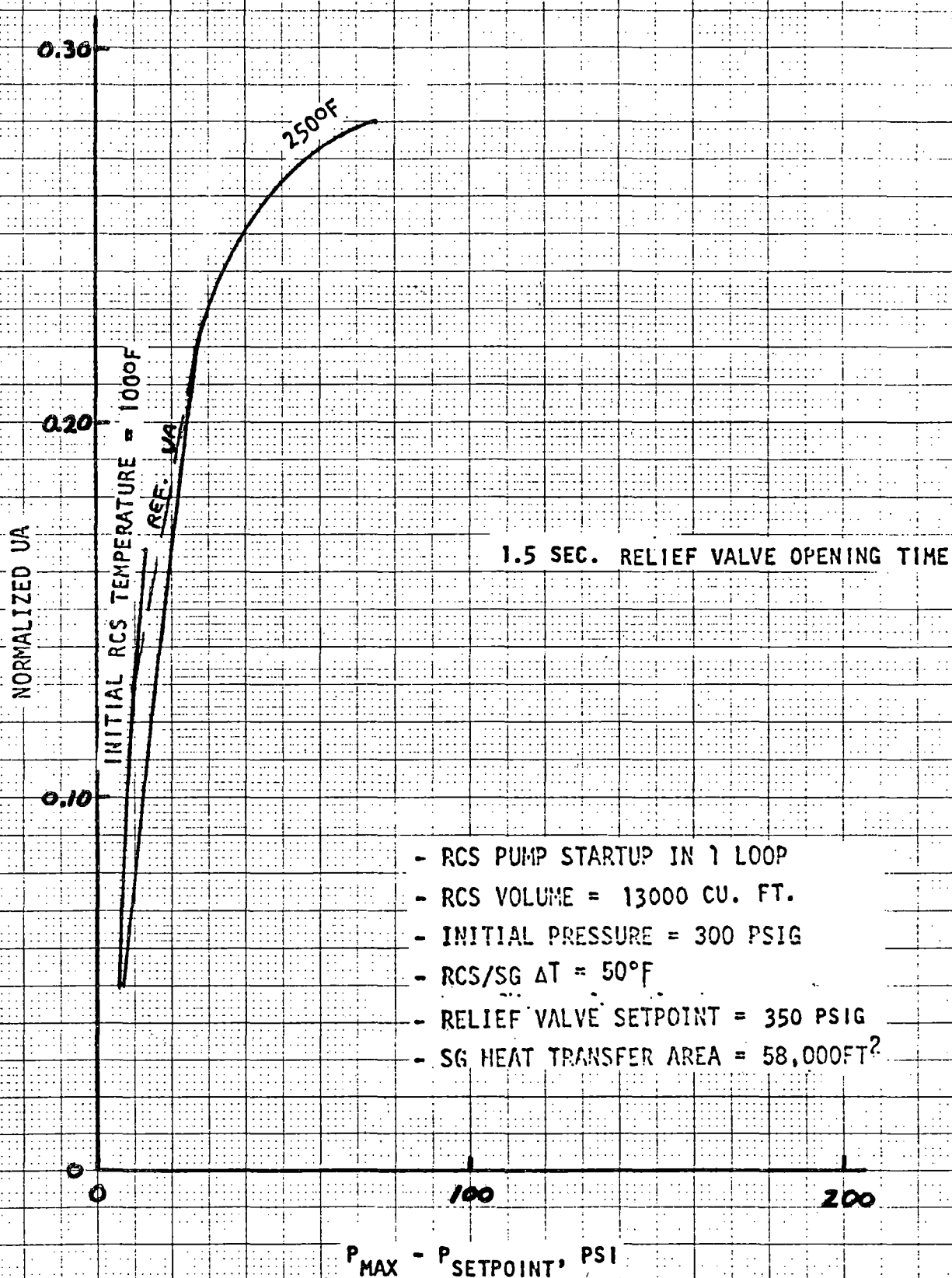


Figure 20

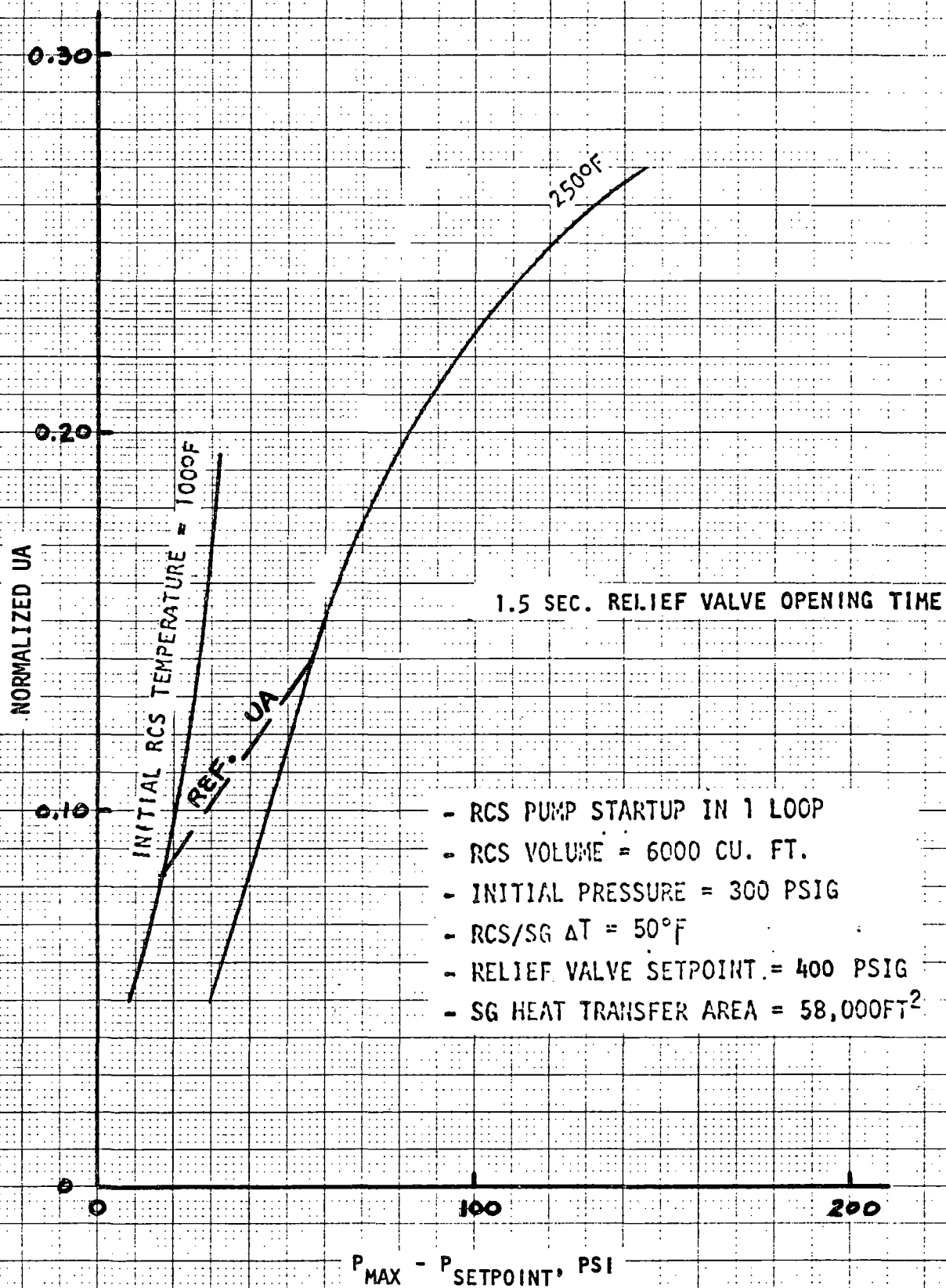
EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT

Figure 21

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

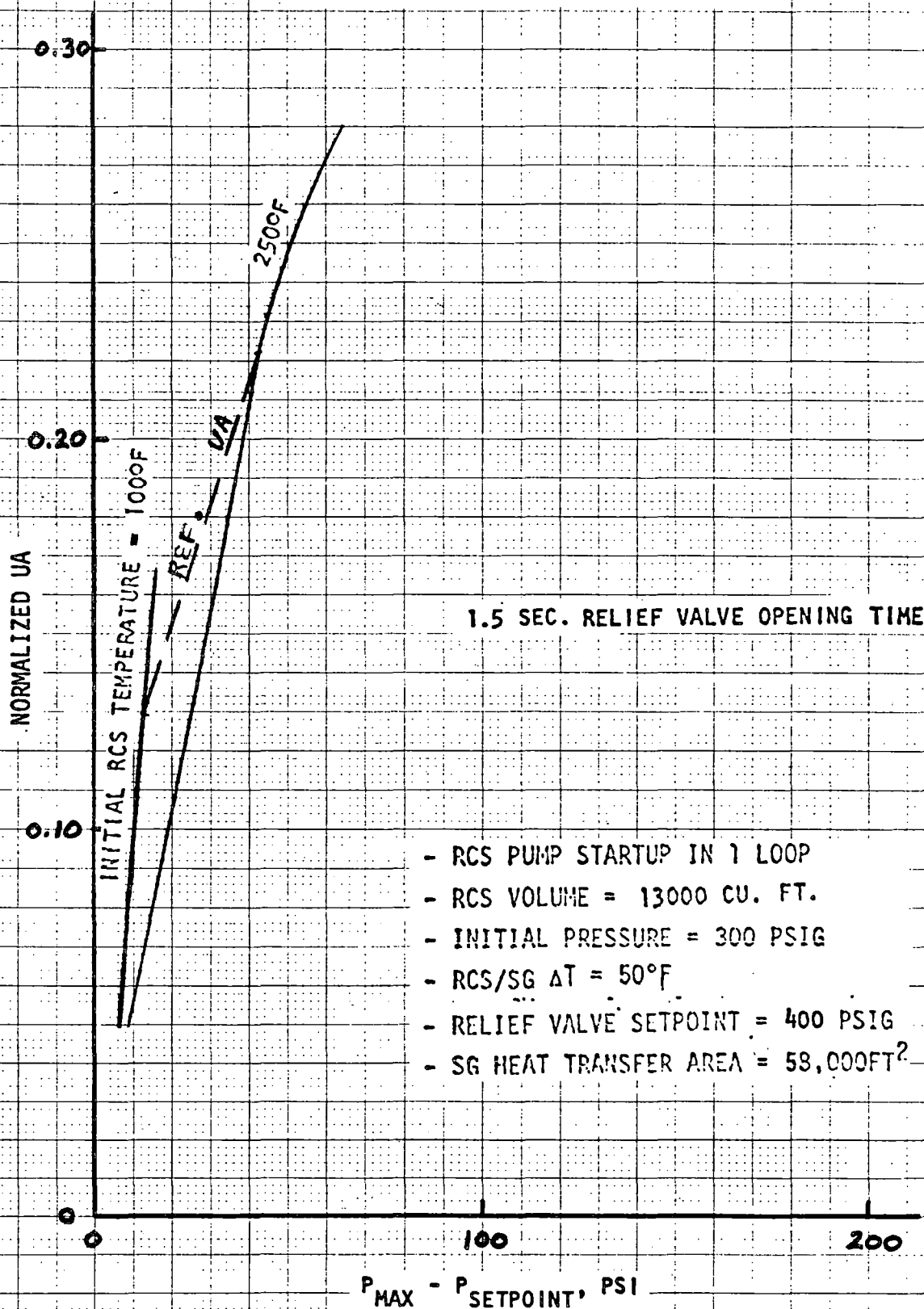


Figure 22

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT

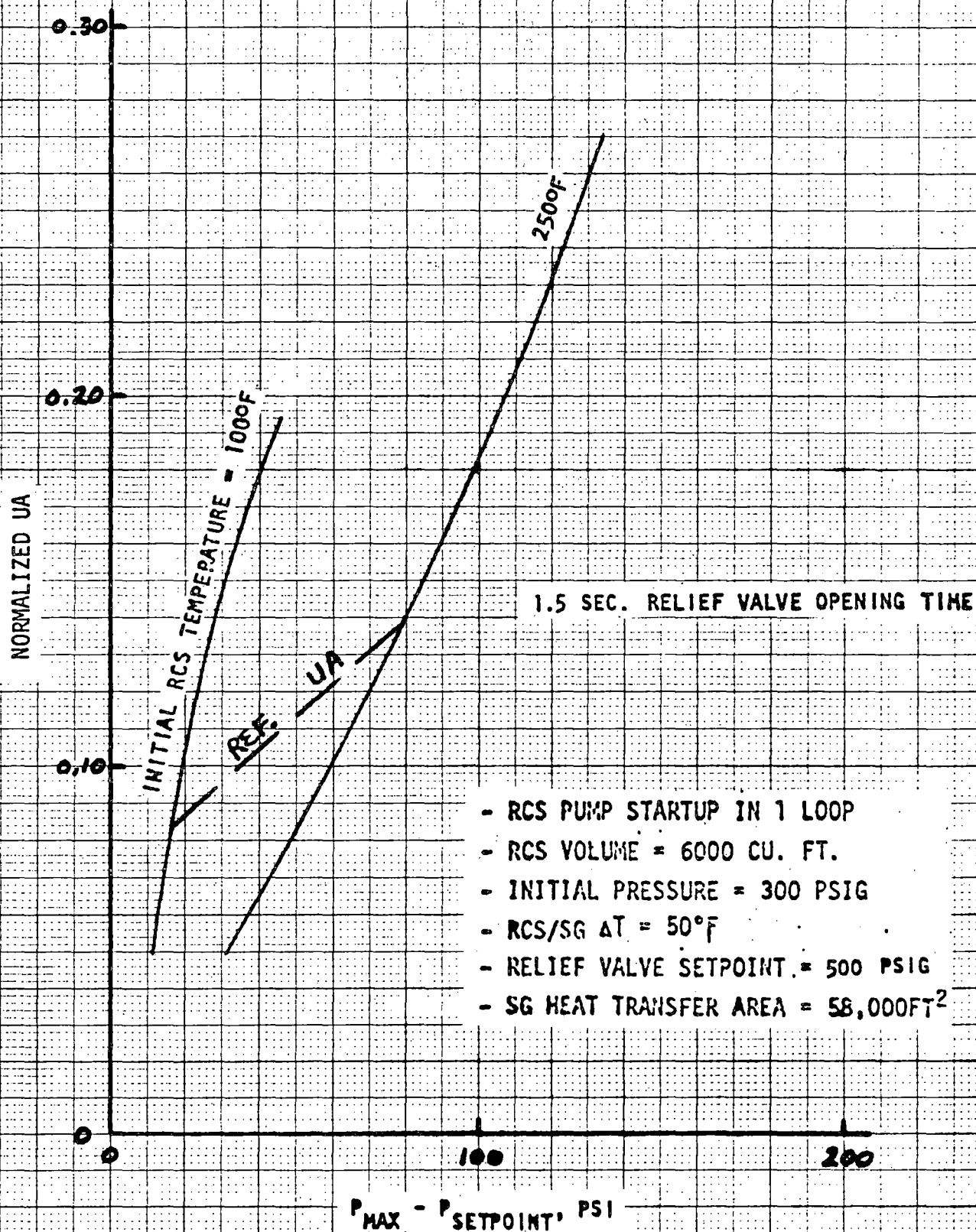
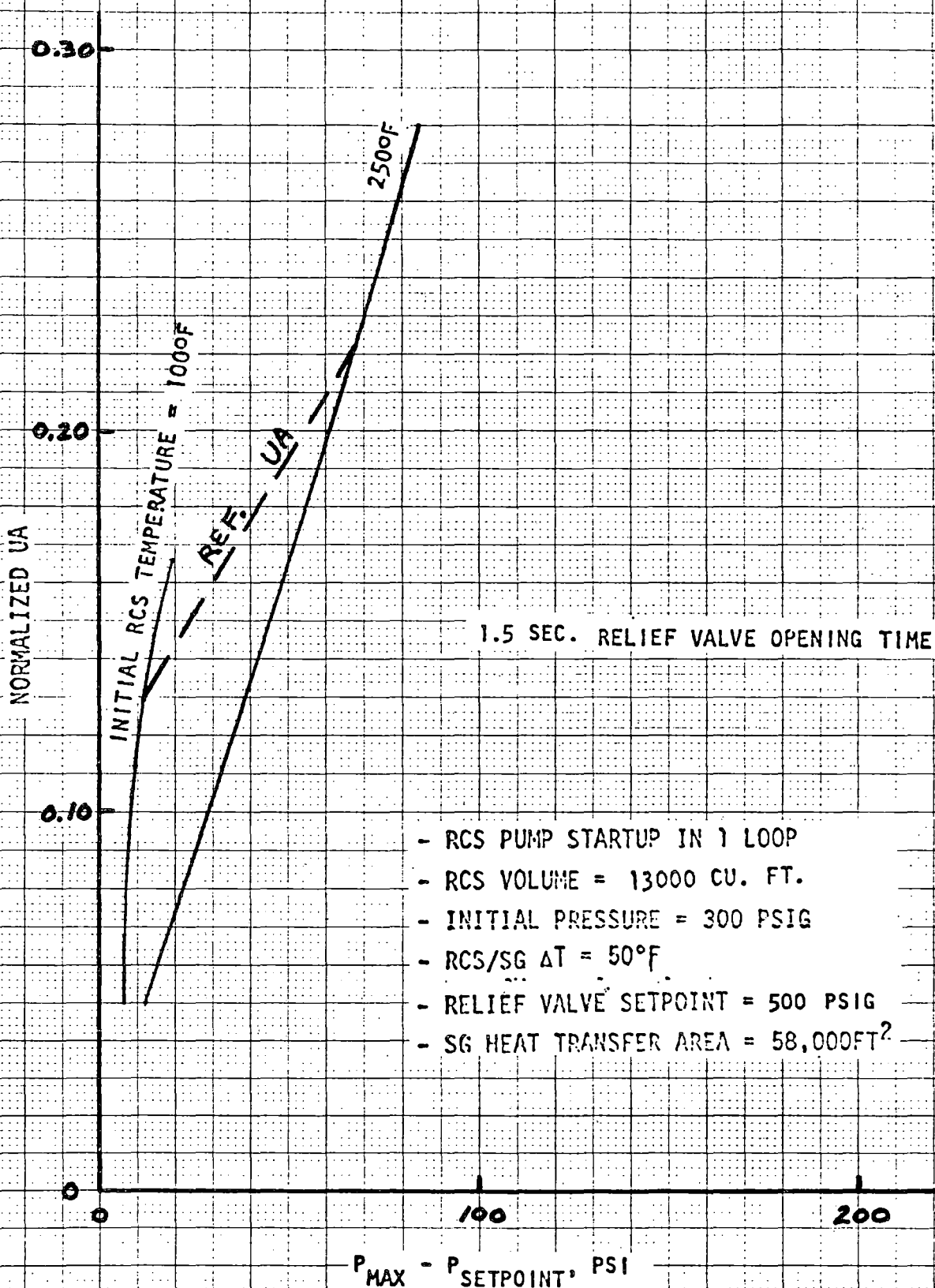


Figure 23

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT



D. SETPOINT OVERSHOOT VARIATION WITH  
REACTOR COOLANT SYSTEM TEMPERATURE

Figure 24

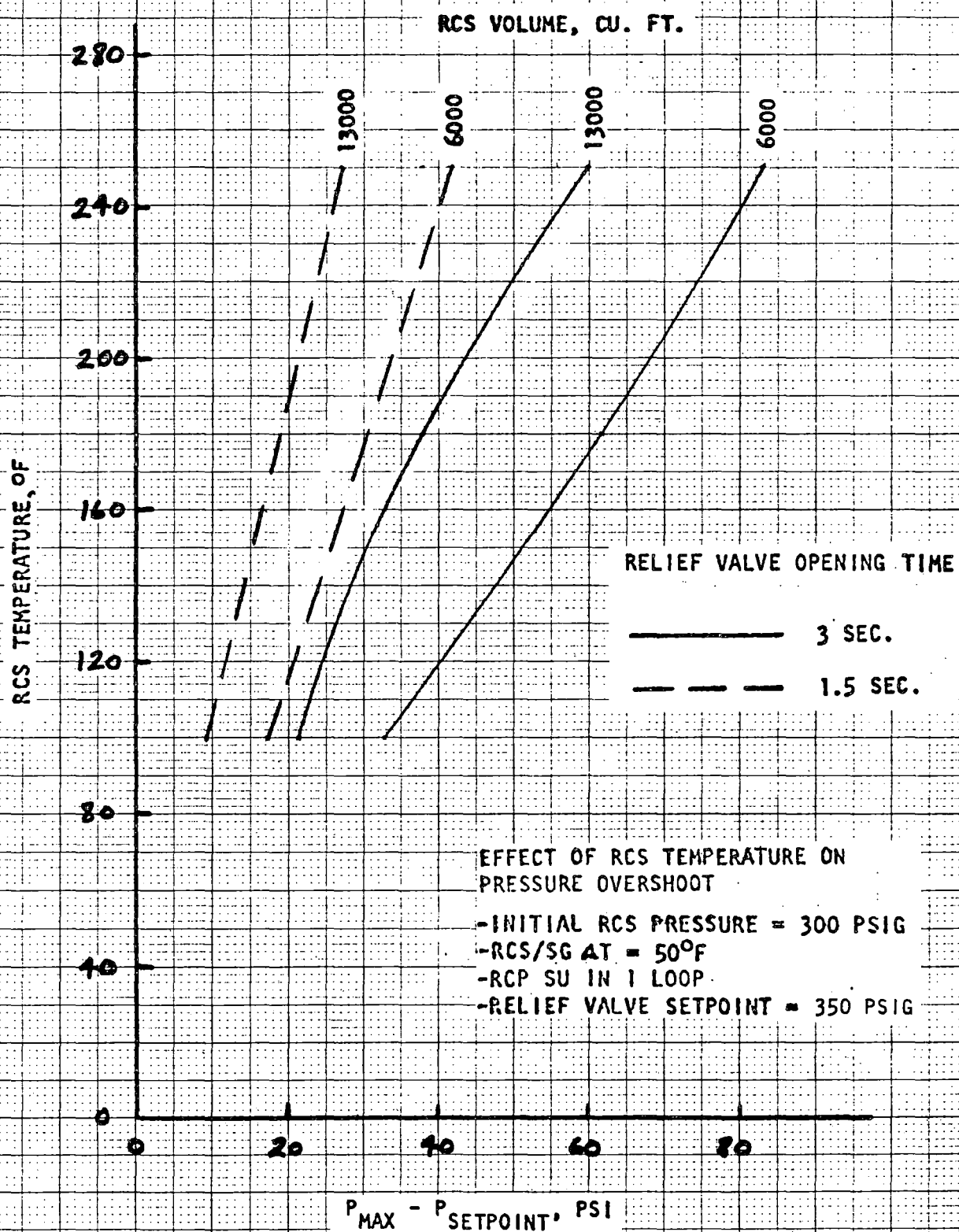


Figure 25

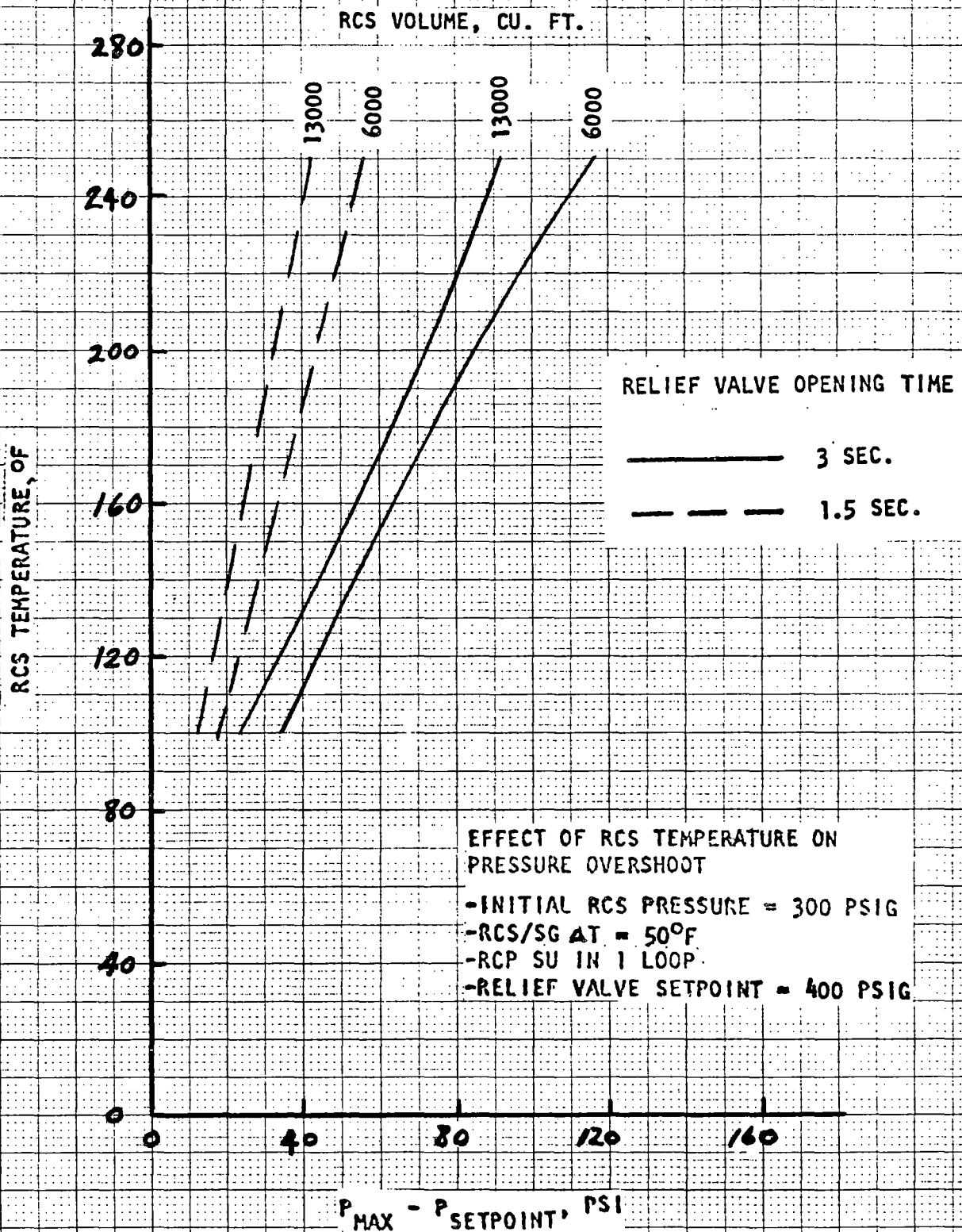
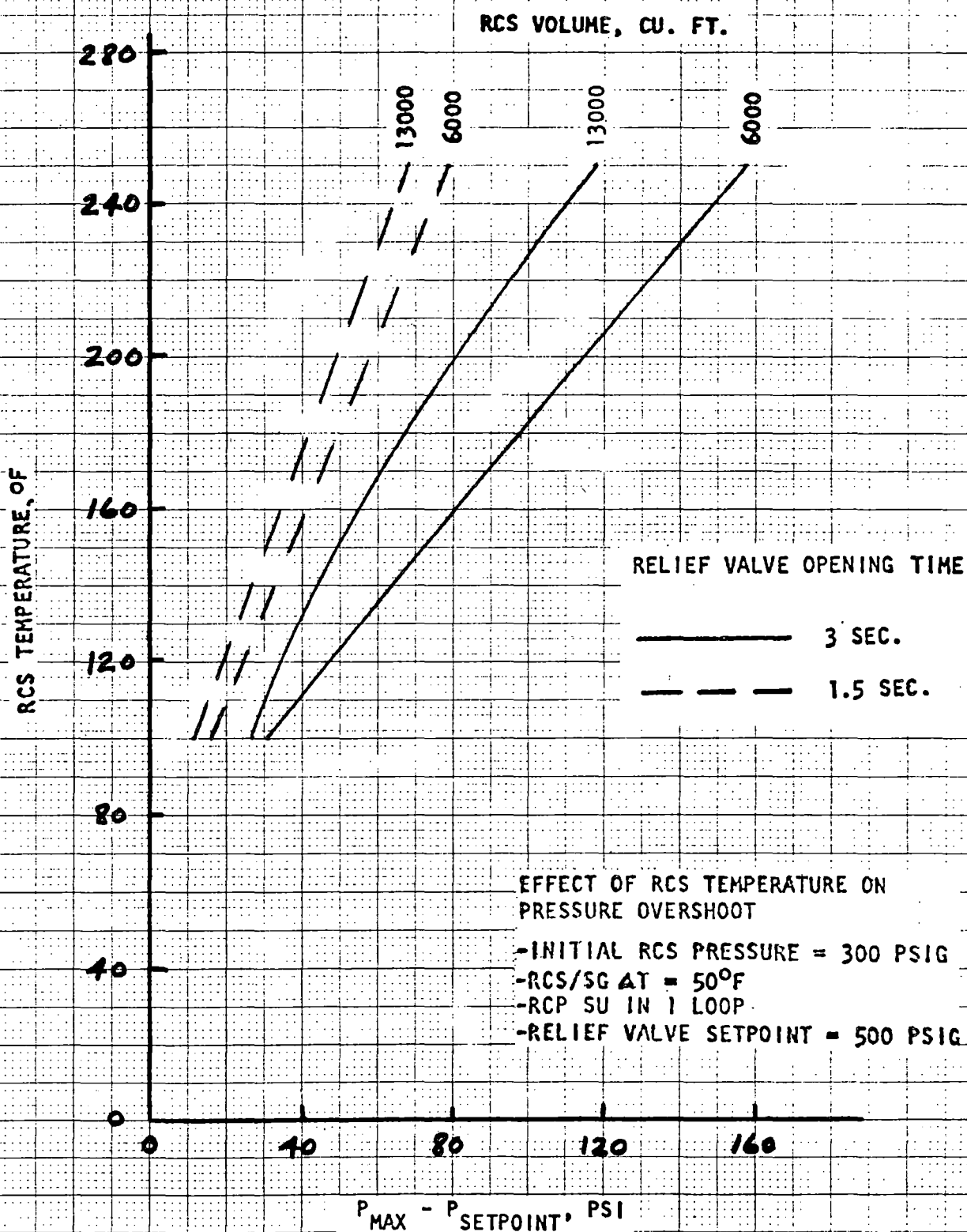


Figure 26



## II. INSTRUCTIONAL GUIDE FOR OVERSHOOT DETERMINATION

### A. General

The bounding envelope of LOFTRAN RCS Heat Input overpressurization generic results presented in Section I are not generally applicable to any specific plant of the W Owners Group on RCS Overpressurization. To determine a specific relief valve setpoint, a means of interpolating the setpoint overshoot from the generic envelope is required. Depending on the parameters to be interpolated and the correlation envelope available, separate procedures are required to perform the interpolation.

These procedures, similar in format except for the interpolated parameters and figure classification utilized, are developed for six typical heat input examples, listed below.

<u>Example</u>	<u>Parameters to be Interpolated Within Generic Data Envelope</u>	<u>Figure Classification Defining Generic Envelope Correlations</u>
1	Relief Valve Opening Time/ Relief Valve Setpoint	$(P_{MAX} \text{ vs. } P_{SETPOINT})^* \text{ vs. Valve Opening Time}$
2	Relief Valve Opening Time/ RCS Volume	$(P_{MAX} \text{ vs. } P_{SETPOINT}) \text{ vs. Valve Opening Time}$

---

\*Setpoint overshoot

- |   |   |   |
|---|---|---|
| 3 | Relief Valve Setpoint/<br>RCS Volume                    | ( $P_{MAX}$ vs. $P_{SETPOINT}$ ) vs.<br>Relief Valve Setpoint |
| 4 | UA(SG Heat Transfer Area)/<br>RCS Volume                | ( $P_{MAX}$ vs. $P_{SETPOINT}$ ) vs.<br>Normalized UA         |
| 5 | UA(SG Heat Transfer Area)/<br>Relief Valve Opening Time | ( $P_{MAX}$ vs. $P_{SETPOINT}$ ) vs.<br>Normalized UA         |
| 6 | UA(SG Heat Transfer Area)/<br>Relief Valve Setpoint     | ( $P_{MAX}$ vs. $P_{SETPOINT}$ ) vs.<br>Normalized UA         |

## B. Procedures

The procedures developed for the determination of setpoint overshoot are described below for six examples in which specific, typical operating plant parameters are used for interpolation within the operating plant generic data envelope. The results of the sequential application of each step in the procedure to these parameters is noted.

### C. Illustrative Examples

#### 1. ILLUSTRATIVE EXAMPLE 1: DETERMINATION OF SETPOINT OVERSHOOT GIVEN RELIEF VALVE SETPOINT AND RELIEF VALVE OPENING TIME WITHIN GENERIC ENVELOPE.

To determine setpoint overshoot for a specific relief valve setpoint ( $S$ ) and relief valve opening time ( $\Delta t$ ) within the generic envelope, the following interpolation procedure and Figures 1 and 3 of Section 1A are used.

# PARAMETERS FOR HEAT INPUT EXAMPLE 1

Initial RCS Pressure	300 psig
SG Heat Transfer Area	58,000 ft <sup>2</sup>
RCS Volume, V <sub>RCS</sub>	6,000 cu.ft.
Initial RCS Temperature, T <sub>RCS</sub>	250°F
RCS/SG ΔT	50°F
Relief Valve Opening Time, Δt	<u>2 sec.</u>
Relief Valve Setpoint, S	<u>375 psig</u>

<u>Step</u>	<u>Procedure</u>	<u>Example Application</u>
1	Using Figures C1 and C2 (V <sub>RCS</sub> = 6000 ft <sup>3</sup> ), determine the setpoint overshoots ΔP <sub>350</sub> and ΔP <sub>400</sub> with valve opening time (Δt) equal to 2 seconds and for the initial RCS temperature (T <sub>RCS</sub> ).	For T <sub>RCS</sub> = 250°F and Δt = 2 seconds, ΔP <sub>350</sub> = <u>55.5 psi</u> (Figure C1) and ΔP <sub>400</sub> = <u>75.5 psi</u> (Figure C2)
2	For the desired relief valve setpoint, linearly interpolate the setpoint overshoot, ΔP <sub>375</sub> , from ΔP <sub>350</sub> and ΔP <sub>400</sub> using the relationship:  $\Delta P_{375} = \Delta P_{350} + \frac{S-350}{400-350} (\Delta P_{400} - \Delta P_{350})$	For S = 375 psig (V <sub>RCS</sub> = 6000 ft <sup>3</sup> ), T <sub>RCS</sub> = 250°F and Δt = 2 seconds,  $\Delta P = 55.5 + \frac{375-350}{50} (75.5 - 55.5)$  <u>= 65.5 psi</u>

Figure C1

EFFECT OF RELIEF VALVE  
OPENING TIME ON RCS  
PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 6,000 CU.FT.

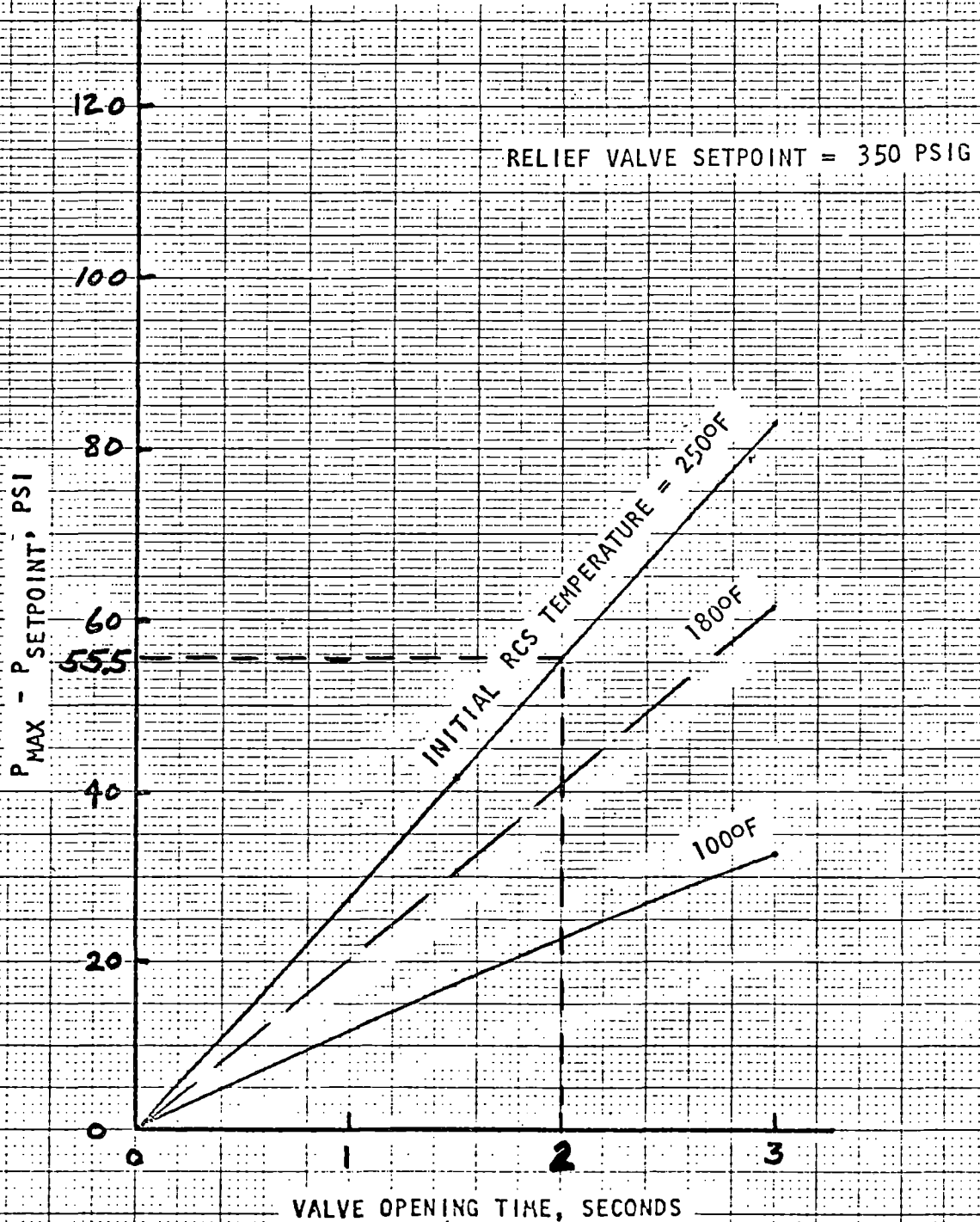
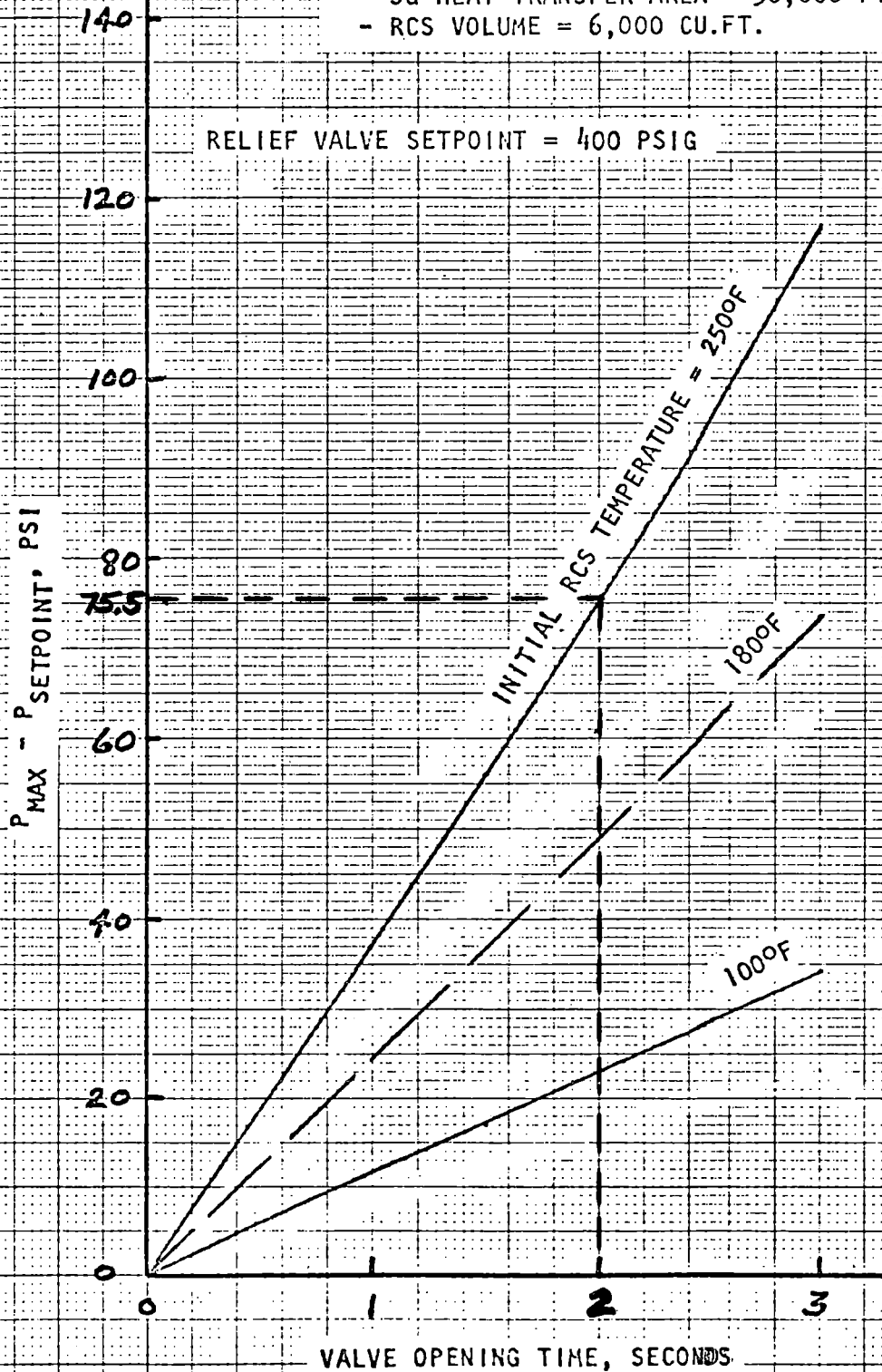


Figure C2

EFFECT OF RELIEF VALVE  
OPENING TIME ON RCS  
PRESSURE OVERTHROTT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^{\circ}\text{F}$
- SG HEAT TRANSFER AREA = 58,000  $\text{FT}^2$
- RCS VOLUME = 6,000  $\text{CU.FT.}$



2. ILLUSTRATIVE EXAMPLE 2: DETERMINATION OF SETPOINT  
OVERSHOOT GIVEN RCS VOLUME AND RELIEF VALVE OPENING  
TIME WITHIN GENERIC ENVELOPE

The following interpolation procedure is used to determine setpoint overshoot for a specified RCS volume ( $V_{RCS}$ ) and relief valve opening time ( $\Delta t$ ) within the generic envelope. By way of illustration, the following example heat input parameters, utilizing Figures 3 and 4 of Section 1.A are used:

PARAMETERS FOR HEAT INPUT EXAMPLE 2

Initial RCS Pressure	300 psig
SG Heat Transfer Area	58,000 ft <sup>2</sup>
RCS Volume, $V_{RCS}$	<u>10,000 cu.ft.</u>
Initial RCS Temperature, $T_{RCS}$	250°F
RCS/SG $\Delta T$	50°F
Relief Valve Setpoint, S	400 psig
Relief Valve Opening Time, $\Delta t$	<u>2 sec.</u>

StepProcedureExample Application

- 1 Using Figures C3 and C4  
(S = 400 psig), determine the  
setpoint overshoots  $\Delta P_{6K}$  and  
 $\Delta P_{13K}$  with valve opening time  
( $\Delta t$ ) equal to 2 seconds and  
for the initial RCS temperature  
( $T_{RCS}$ ).

For  $T_{RCS} = 250^{\circ}\text{F}$  and  
 $\Delta t = 2$  seconds,  
 $\Delta P_{6K} = \underline{75.5 \text{ psi}}$   
(Figure C3) and  $\Delta P_{13K} =$   
57.5 psi (Figure C4).

- 2 For the desired RCS volume,  
linearly interpolate the set-  
point overshoot,  $\Delta P_{10K}$ , from  
 $\Delta P_{6K}$  and  $\Delta P_{13K}$  using the  
relationship:

$$\Delta P_{10K} = \Delta P_{6K}$$

$$- \frac{V_{RCS} - 6000}{13,000 - 6,000} (\Delta P_{6K} - \Delta P_{13K})$$

For  $V_{RCS} = 10,000$  cu.ft.  
(S = 400 psig),  
 $T_{RCS} = 250^{\circ}\text{F}$  and  $\Delta t = 2$  seconds,

$$\Delta P = 75.5$$

$$- \frac{10,000 - 6000}{7000} (75.5 - 57.5)$$

$$= \underline{65.2 \text{ psi}}$$

Figure C3

EFFECT OF RELIEF VALVE  
OPENING TIME ON RCS  
PRESSURE OVERSHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ F$
- SG HEAT TRANSFER AREA = 58,000  $FT^2$
- RCS VOLUME = 6,000 CU.FT.

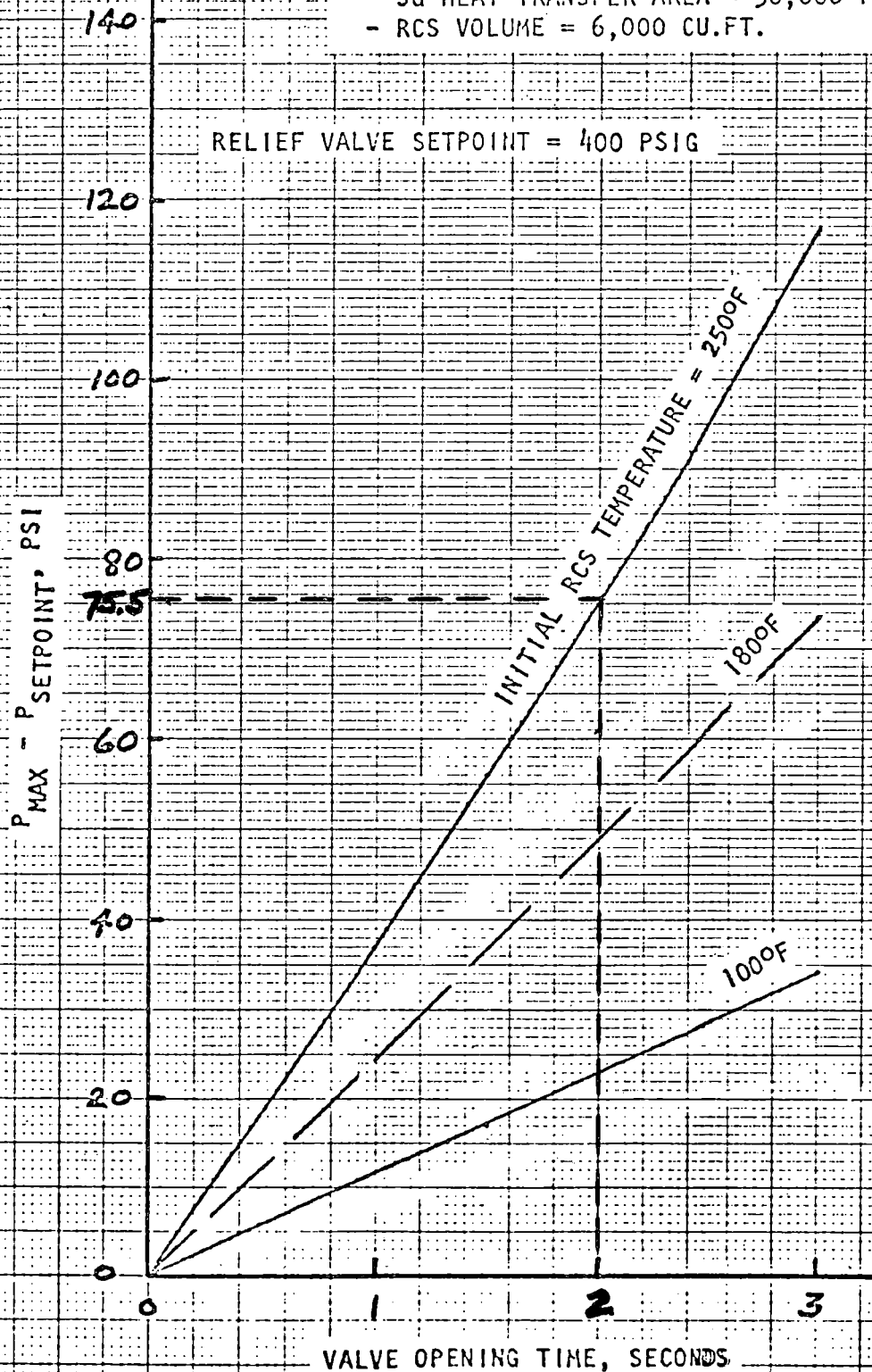
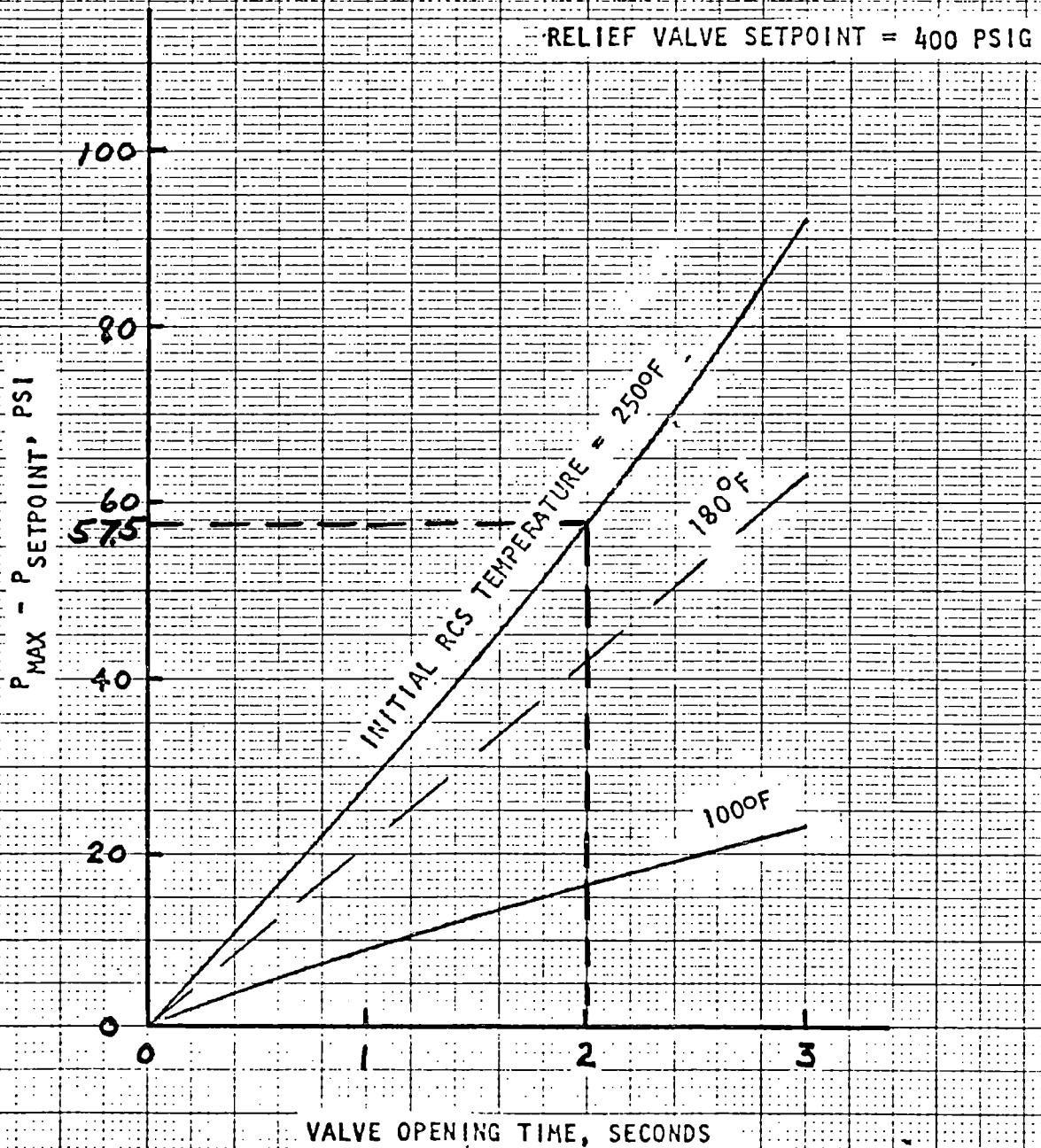


Figure C4

EFFECT OF RELIEF VALVE  
OPENING TIME ON RCS  
PRESSURE OVERTHOOT

- RCS PUMP STARTUP IN 1 LOOP
- LINEAR RELIEF VALVE
- VALVE DELAY = 20% OF OPENING TIME
- INITIAL RCS PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ\text{F}$
- SG HEAT TRANSFER AREA = 58,000  $\text{FT}^2$
- RCS VOLUME = 13000 CU. FT.



3. ILLUSTRATIVE EXAMPLE 3: DETERMINATION  
OF SETPOINT OVERSHOOT GIVEN RELIEF VALVE  
SETPOINT AND RCS VOLUME WITHIN GENERIC ENVELOPE

The following interpolative procedure is used to determine setpoint overshoot for a given relief valve setpoint(s) and RCS volume ( $V_{RCS}$ ) within the generic envelope. By way of illustration, the following example heat input parameters, utilizing Figure 9 of Section 1A are specified:

PARAMETERS FOR HEAT INPUT EXAMPLE 3

Initial RCS Pressure	300 psig
SG Heat Transfer Area	58,000 ft <sup>2</sup>
RCS Volume, $V_{RCS}$	<u>10,000 cu.ft.</u>
Initial RCS Temperature, $T_{RCS}$	250°F
RCS/SG $\Delta T$	50°F
Relief Valve Setpoint, S	<u>375 psig</u>
Relief Valve Opening Time, $\Delta t$	3 sec.

StepProcedureExample Application

- 1 For relief valve setpoint(s) equal to 375 psig ( t = 3 seconds), determine the setpoint overshoots  $P_{6K}$  and  $P_{13K}$  for the initial RCS temperature ( $T_{RCS}$ ).

For  $T_{RCS} = 250^{\circ}\text{F}$ ,  
 $P_{6K} = \underline{101.3 \text{ psi}}$   
and  $P_{13K} = \underline{78.5 \text{ psi}}$   
from Figure C5.

- 2 For the desired RCS volume, linearly interpolate the setpoint overshoot,  $P_{10K}$ , from  $P_{6K}$  and  $P_{13K}$  using the relationship:

For  $V_{RCS} = 10,000 \text{ cu.ft.}$   
( t = 3 seconds), and  
 $T_{RCS} = 250^{\circ}\text{F}$ ,

$$P_{10K} = P_{6K} - \frac{V_{RCS} - 6000}{13,000 - 6,000} (P_{6K} - P_{13K})$$

$$\begin{aligned} P &= 101.3 \\ &- \frac{10,000 - 6,000}{7000} (101.3 - 78.5) \\ &= \underline{88.3 \text{ psi}} \end{aligned}$$

Figure C5

EFFECT OF RELIEF VALVE SETPOINT  
ON PRESSURE OVERSHOOTP<sub>MAX</sub> - P<sub>SETPOINT</sub>, PSI101.3  
10080  
78.5

60

40

20

160

140

120

6000

13000

350

375

400

450

500

SETPOINT, PSIG

- RCS PUMP STARTUP IN 1 LOOP
- 3 SEC. RELIEF VALVE OPENING
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ F$
- INITIAL RCS TEMPERATURE =  $250^\circ F$
- SG HEAT TRANSFER AREA = 58,000FT<sup>2</sup>

4. ILLUSTRATIVE EXAMPLE 4: DETERMINATION OF  
SETPOINT OVERSHOOT GIVEN SG TUBE HEAT TRANSFER  
AREA AND RCS VOLUME WITHIN GENERIC ENVELOPE

For SG tube heat transfer area different from  $58,000 \text{ ft}^2$ , the determination of setpoint overshoot is made using a slightly modified version of the Heat Input Instructional Guide for Setpoint/Overshoot Determination prescribed in Chapter 4 of the July 1977 Report (Reference 1) and Figures 12 through 23 of Section IA (figures depicting setpoint overshoot variation with normalized steam generator UA). Setpoint overshoots may be obtained for 1.5 sec and 3 sec relief valve opening times ( $t$ ); for relief valve setpoints ( $S$ ) equal to 350 psig, 400 psig and 500 psig; and for RCS volumes ( $V_{\text{RCS}}$ ) equal to 6000 cu.ft. and 13,000 cu.ft. Setpoint overshoot may also be obtained for  $t$ ,  $S$  and  $V_{\text{RCS}}$  values within these envelopes, depending on the combination of Figures 12 through 23 of Section IA selected. Illustrative Example 4 and subsequent examples will illustrate this interpolative procedure for interpolating  $t$ ,  $S$  and  $V_{\text{RCS}}$ .

Illustration of the use of the modified interpolative procedure of Chapter 4 of Reference 1 is provided below for the determination of setpoint overshoot for a specified SG tube heat transfer

area and RCS volume within the generic envelope (Illustrative Example 4). Figures 12 and 13 of Section 1A are used in the procedure for the following example heat input parameters:

PARAMETERS FOR HEAT INPUT EXAMPLE 4

Initial RCS Pressure	300 psig
SG Heat Transfer Area	<u>29,000 ft<sup>2</sup></u>
RCS Volume, $V_{RCS}$	<u>10,000 cu.ft.</u>
Initial RCS Temperature, $T_{RCS}$	250°F
RCS/SG $\Delta T$	50°F
Relief Valve Setpoint, S	350 psig
Relief Valve Opening Time, t	3 sec.

Applying the heat input procedure:

<u>Step</u>	<u>Procedure</u>	<u>Example Application</u>
1	For both the 6000 ft <sup>3</sup> and 13,000 ft <sup>3</sup> RCS volumes (S = 350 psig), obtain the reference normalized UA ( $UA_{6K}$ and $UA_{13K}$ ) at the initial RCS temperature ( $T_{RCS}$ ) and relief valve setpoint (S), using Figures C6 and C7.	For $T_{RCS} = 250^{\circ}\text{F}$ and $S = 350$ psig, $UA_{6K} = \underline{0.139}$ (Figure C6) and $UA_{13K} = \underline{0.222}$ (Figure C7).
2	Determine what fraction, f, of 58,000 ft <sup>2</sup> constitutes the actual steam generator heat transfer area.	$29,000 \text{ ft}^2 / 58,000 \text{ ft}^2 = \underline{0.5}$

Figure C6

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT

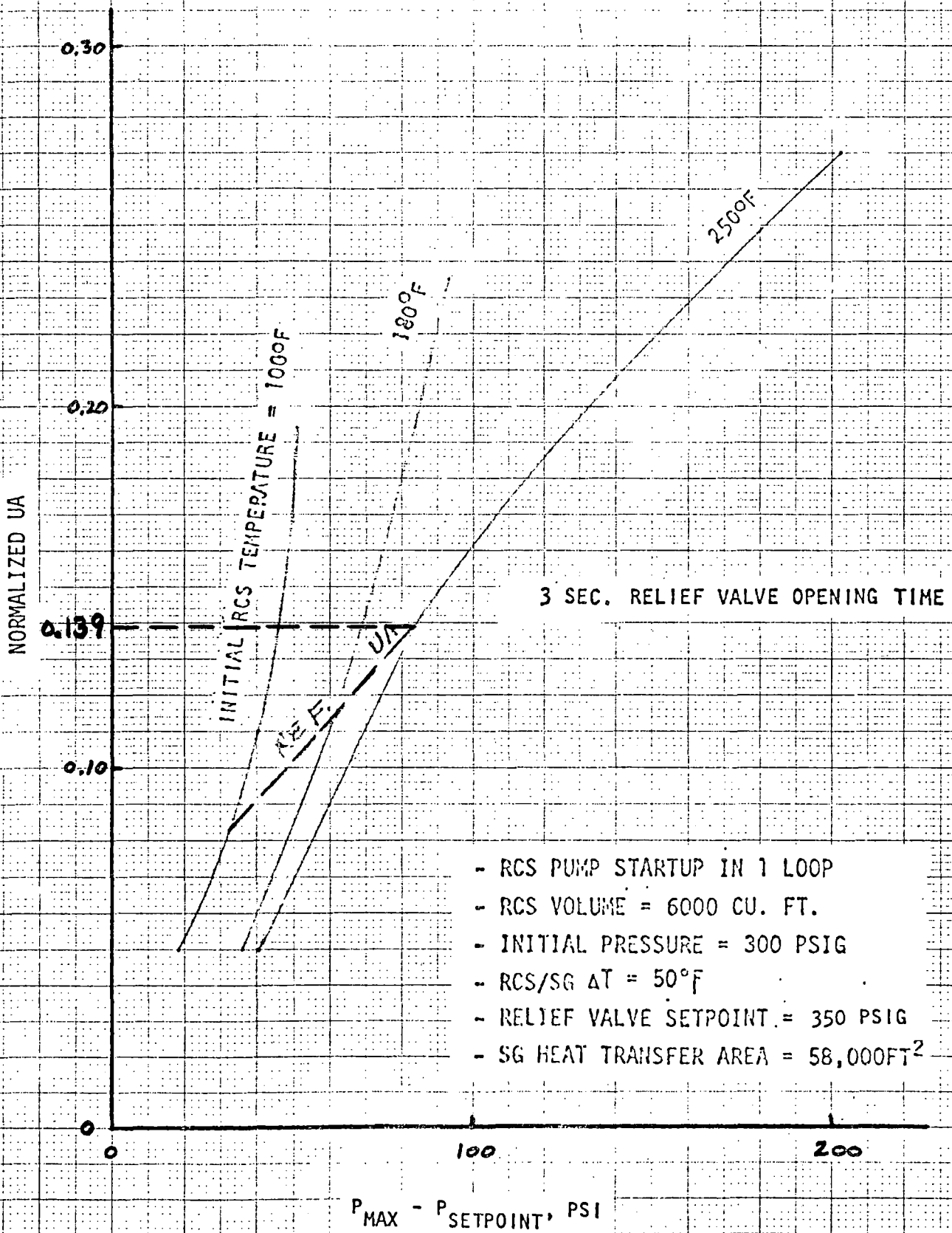
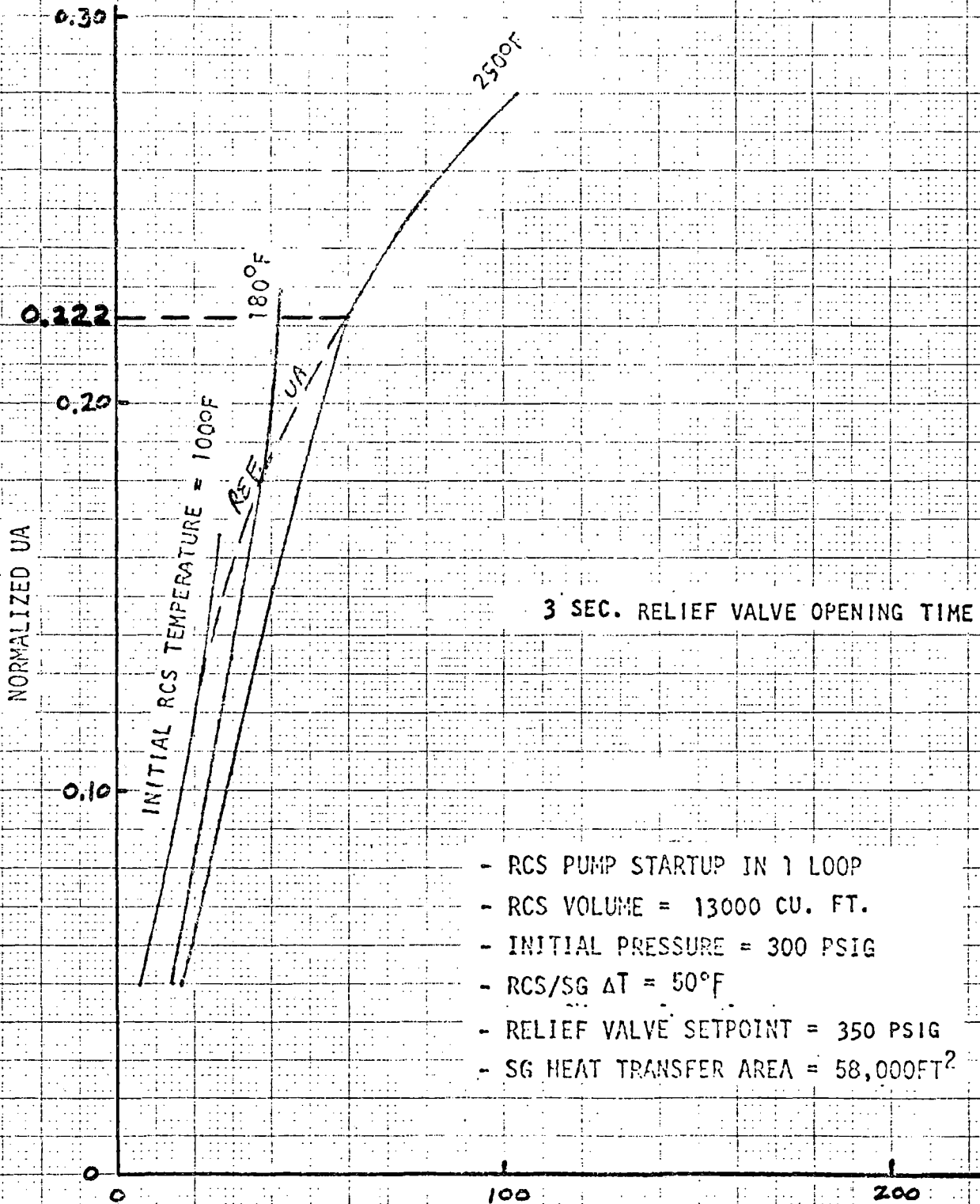


Figure C7

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



$P_{MAX} - P_{SETPOINT}, PSI$

StepProcedureExample Application

- 3 Multiply both  $UA_{6K}$  and  $UA_{13K}$  (from Step 1) by  $f$  (from Step 2) to obtain new normalized  $UA'_{6K}$  and  $UA'_{13K}$  values.
- 4 For the same isotherm,  $T_{RCS}$ , and for  $UA'_{6K}$  and  $UA'_{13K}$ , obtain new setpoint overshoots  $P'_{6K}$  and  $P'_{13K}$  for the 6000  $ft^3$  and 13,000  $ft^3$  volumes from Figures C8 and C9.
- 5 For the actual volume,  $V_{RCS}$ , linearly interpolate the setpoint overshoot,  $P'_{VRCS}$ , for the new steam generator UA from the relationship:

$$P'_{VRCS} = P'_{6K}$$

$$- \frac{V_{RCS} - 6000}{7000} (P'_{6K} - P'_{13K})$$

$$UA'_{6K} = 0.139 * 0.5 = \underline{0.0695} \text{ and}$$

$$UA'_{13K} = 0.222 * 0.5 = \underline{0.111}.$$

From Figure C8, for  $T_{RCS} = 250^{\circ}F$ ,  $S = 350$  psig and  $UA'_{6K} = 0.0695$ ,  $P'_{6K} = \underline{50 \text{ psi}}$ . From Figure C9 for  $T_{RCS} = 250^{\circ}F$ ,  $S = 350$  psig and  $UA'_{13K} = 0.111$ ,  $P'_{13K} = \underline{31 \text{ psi}}$ .

For  $V_{RCS} = 10,000$  cu.ft.,  $P'_{6K} = 50$  psi and  $P'_{13K} = 31$  psi,

$$P'_{10K} = 50$$

$$- \frac{10,000 - 6000}{7000} (50 - 31)$$

$$= \underline{39.2 \text{ psi}}$$

Figure C8

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT

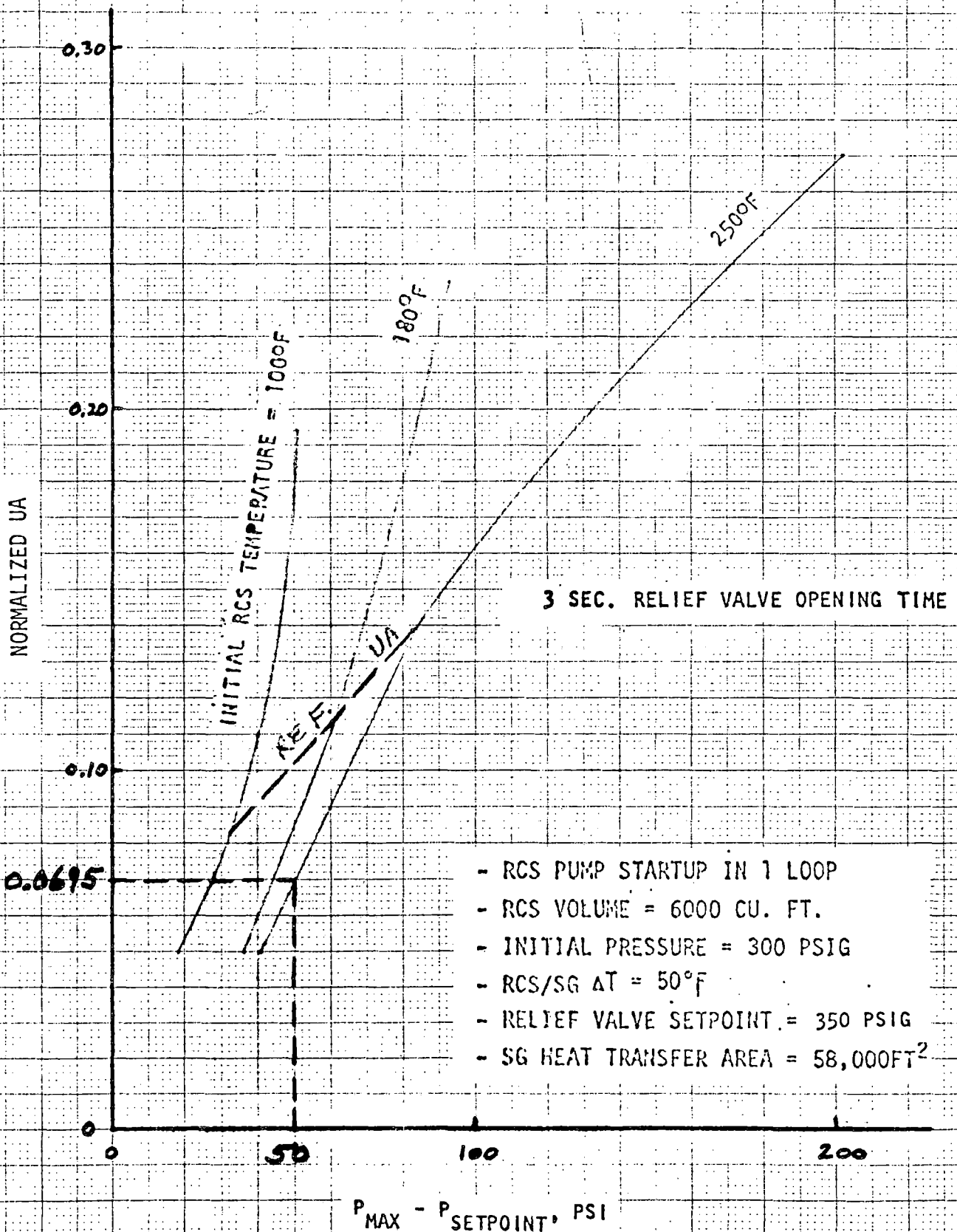
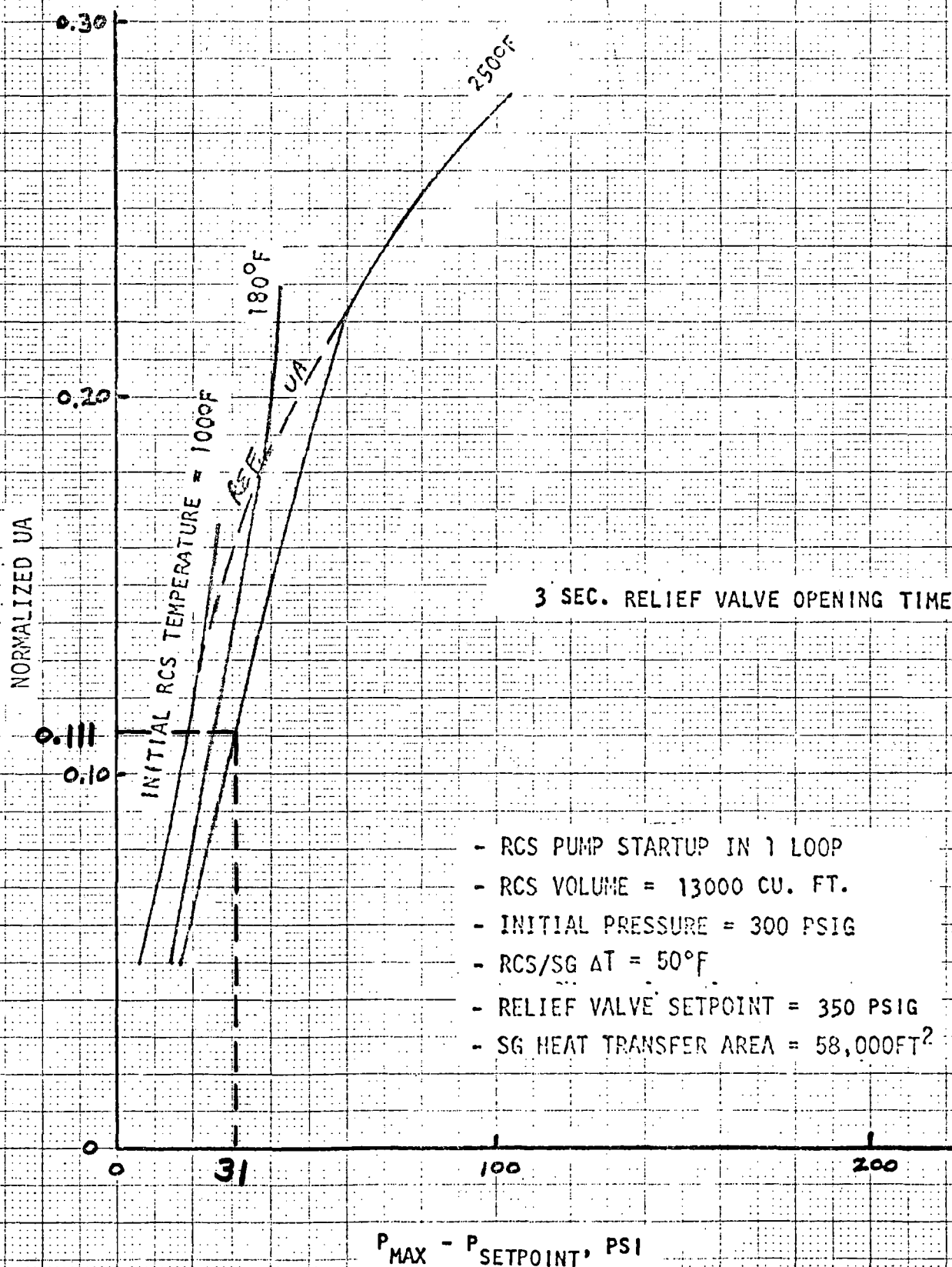


Figure C9

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



5. ILLUSTRATIVE EXAMPLE 5: DETERMINATION OF SETPOINT  
OVERSHOOT GIVEN SG TUBE HEAT TRANSFER AREA AND RELIEF  
VALVE OPENING TIME WITHIN GENERIC ENVELOPE.

The interpolative procedure of Example 5 (modified procedure of Reference 1, Chapter 4) is applied below for the determination of setpoint overshoot for a specified SG tube heat transfer area and relief valve opening time within the generic envelope. Figures 12 and 18 of Section 1A are used in the procedure for the following example heat input parameters:

PARAMETERS FOR HEAT INPUT EXAMPLE 5

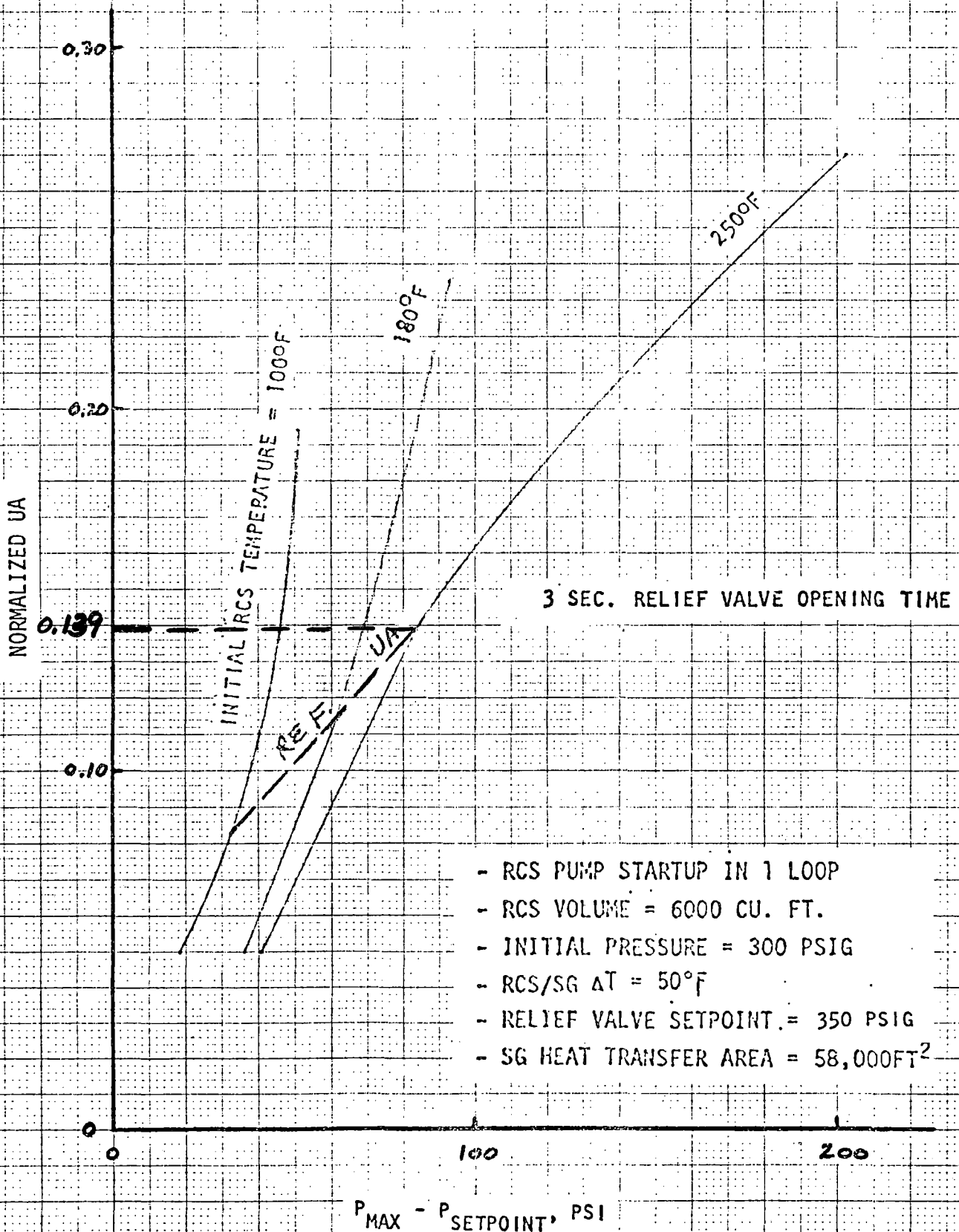
Initial RCS Pressure	300 psig
SG Heat Transfer Area	<u>29,000 ft<sup>2</sup></u>
RCS Volume, $V_{RCS}$	6,000 cu.ft.
Initial RCS Temperature, $T_{RCS}$	250°F
RCS/SG $\Delta T$	50°F
Relief Valve Setpoint, S	350 psig
Relief Valve Opening Time, t	<u>2 sec.</u>

Applying the heat input procedure:

<u>Step</u>	<u>Procedure</u>	<u>Example Application</u>
1	For both the 3 second and 1.5 second relief valve opening times, obtain the reference normalized UA ( $UA_3$ and $UA_{1.5}$ ) for the initial RCS temperature ( $T_{RCS}$ ) and relief valve setpoint (S), using Figures C10 and C11.	For $T_{RCS} = 250^{\circ}\text{F}$ and $S = 350$ psig, $UA_3 = UA_{1.5} = \underline{0.139}$ from Figures C10 and C11. ( $V_{RCS} = 6000$ cu.ft.)
2	Determine what fraction, f, of 58,000 $\text{ft}^2$ constitutes the actual steam generator heat transfer area.	$29,000 \text{ ft}^2 / 58,000 \text{ ft}^2 = \underline{0.5}$
3	Multiply both $UA_3$ and $UA_{1.5}$ (from step 1) by f (from Step 2) to obtain new normalized $UA_3^1$ and $UA_{1.5}^1$ valves.	$UA_3^1 = UA_{1.5}^1 = 0.139 * 0.5$ $= \underline{0.0695}$

Figure C10

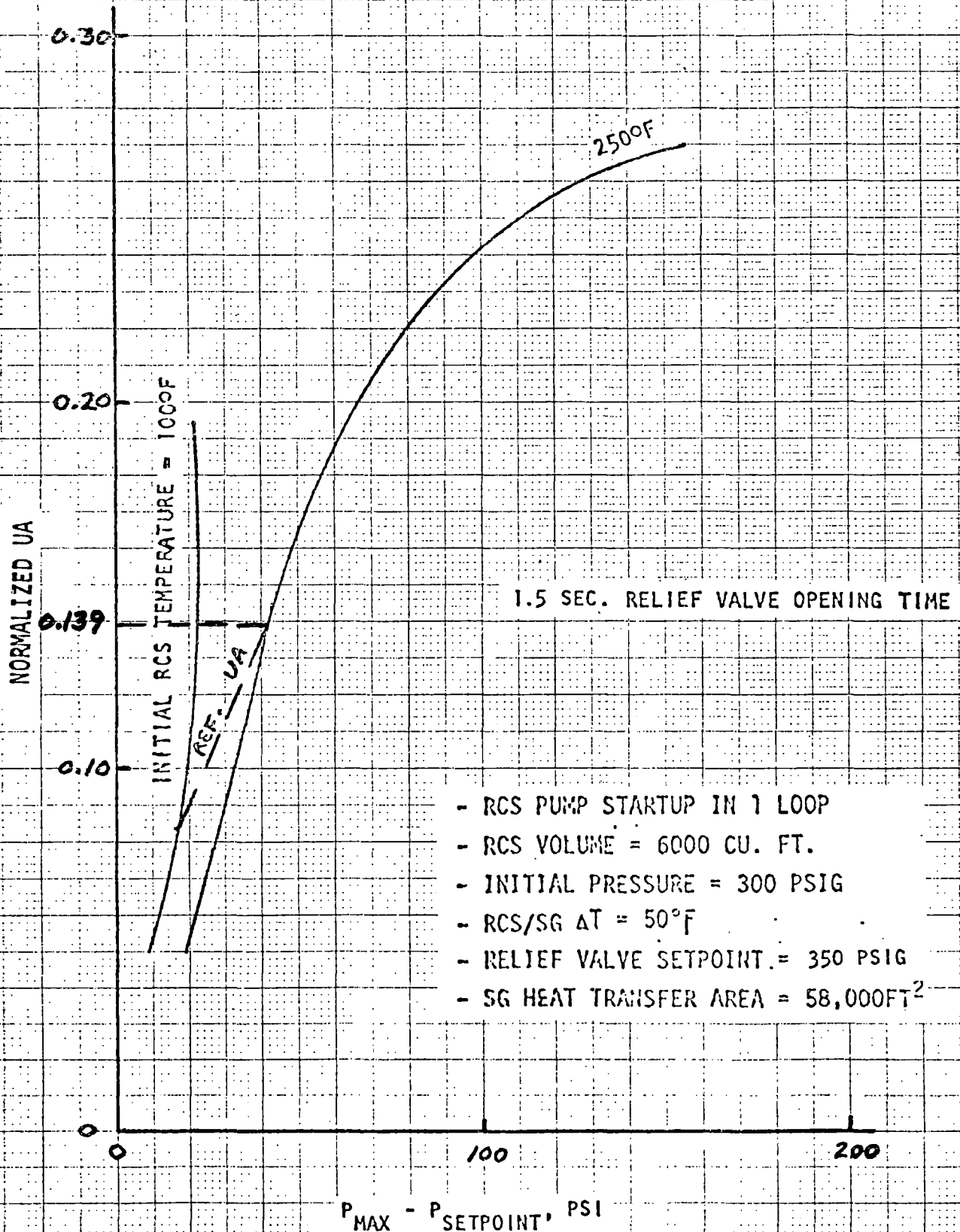
EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



- RCS PUMP STARTUP IN 1 LOOP
- RCS VOLUME = 6000 CU. FT.
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ\text{F}$
- RELIEF VALVE SETPOINT = 350 PSIG
- SG HEAT TRANSFER AREA = 58,000FT<sup>2</sup>

Figure C11

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



- RCS PUMP STARTUP IN 1 LOOP
- RCS VOLUME = 6000 CU. FT.
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ F$
- RELIEF VALVE SETPOINT = 350 PSIG
- SG HEAT TRANSFER AREA = 58,000FT<sup>2</sup>

StepProcedureExample Application

- 4 For the same isotherm,  $T_{RCS}$ , and for  $UA_3^1$  and  $UA_{1.5}^1$  obtain new setpoint overshoots  $\Delta P_3^1$  and  $P_{1.5}^1$  for the 3 second and 1.5 second relief valve opening times, using Figures C12 and C13.

- 5 For the actual relief valve opening time,  $t$ , linearly interpolate the setpoint overshoot,  $P_t^1$ , for the new steam generator UA from the relationship:

$$P_{\Delta t}^1 = P_{1.5}^1 + \frac{t - 1.5}{3 - 1.5} (P_3^1 - P_{1.5}^1)$$

From Figure C12, for  $T_{RCS} = 250^\circ\text{F}$ ,  $S = 350$  psig and  $UA_3^1 = 0.0695$ ,  $P_3^1 = \underline{50 \text{ psi}}$ . From Figure C13, for  $T_{RCS} = 250^\circ\text{F}$ ,  $S = 350$  psig and  $UA_{1.5}^1 = 0.0695$ ,  $P_{1.5}^1 = \underline{25 \text{ psi}}$ .

For,  $t = 2$  seconds,

$$P_3^1 = 50 \text{ psi and } P_{1.5}^1 = 25 \text{ psi,}$$

$$P_2^1 = 25 + \frac{2 - 1.5}{3 - 1.5} (50 - 25) = \underline{33.4 \text{ psi}}$$

Figure C12

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT

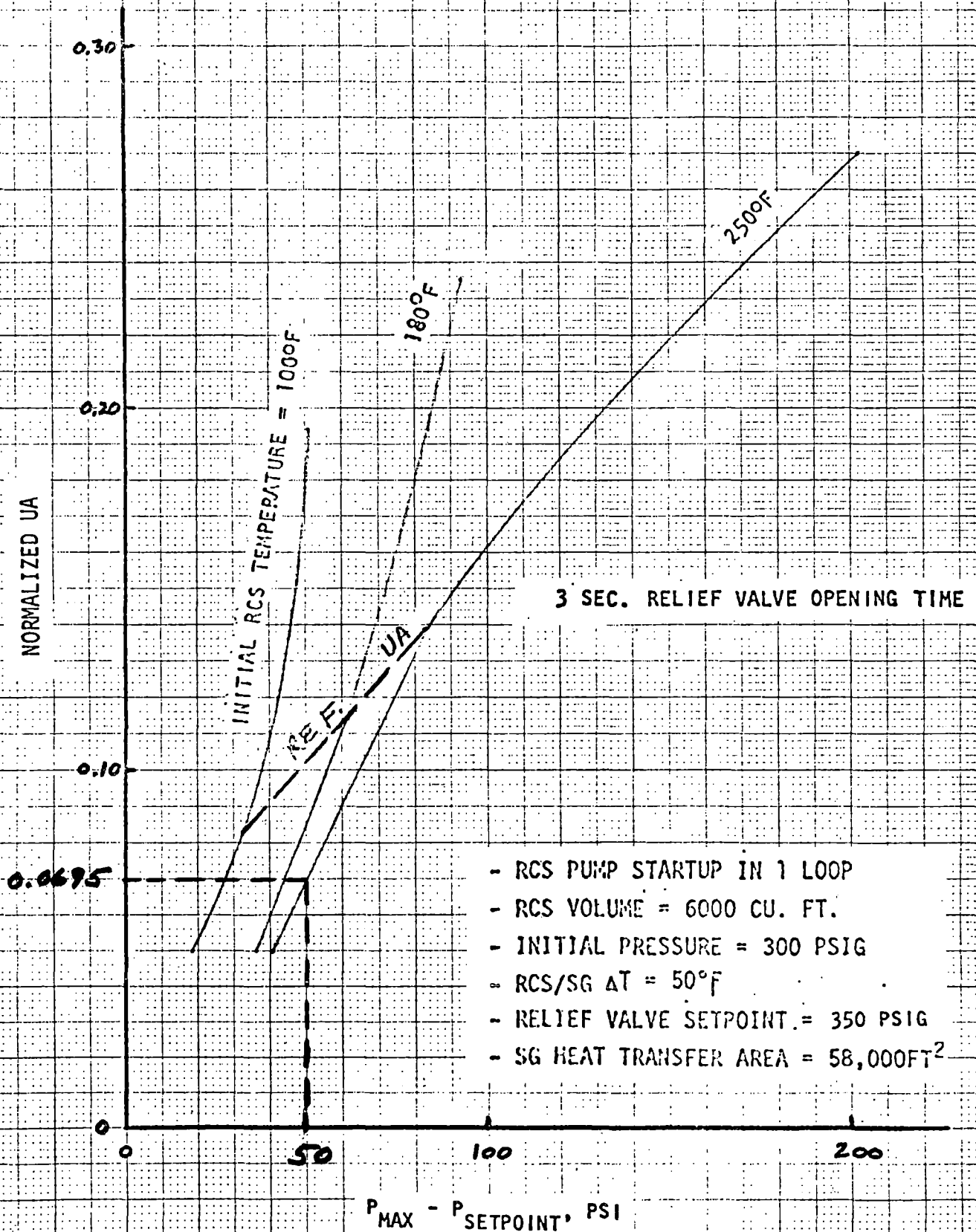
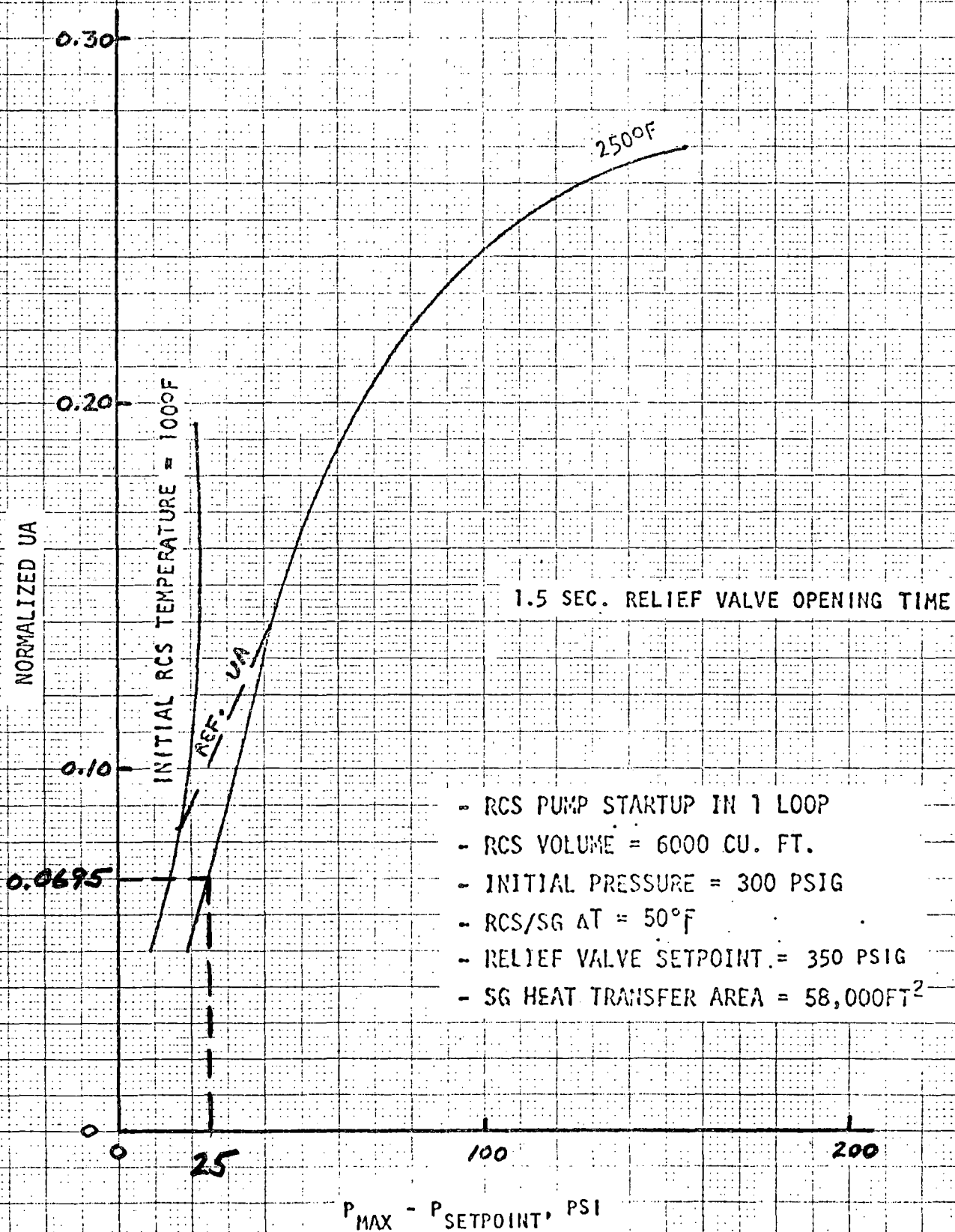


Figure C13  
EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



6. ILLUSTRATIVE EXAMPLE 6: DETERMINATION OF SETPOINT  
OVERSHOOT GIVEN SG TUBE HEAT TRANSFER AREA AND  
RELIEF VALVE SETPOINT WITHIN GENERIC ENVELOPE.

The interpolative procedure of Example 6 (modified procedure of Reference 1, Chapter 4) is applied below for the determination of setpoint overshoot for a specified SG tube heat transfer area and relief valve setpoint within the generic envelope. Figures 12 and 14 of Section 1A are used in the procedure for the following example heat input parameters:

PARAMETERS FOR HEAT INPUT EXAMPLE 6

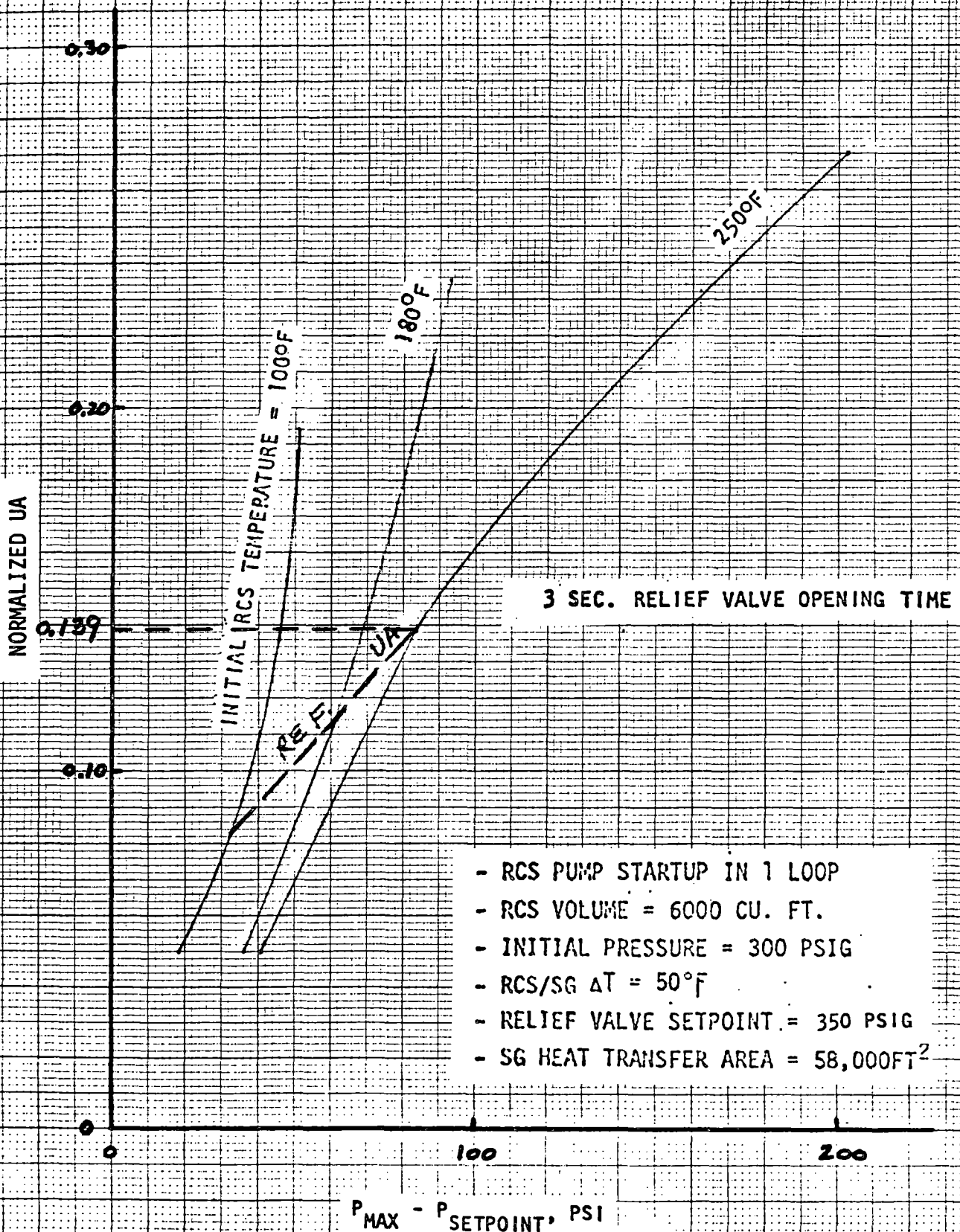
Initial RCS Pressure	300 psig
SG Heat Transfer Area	<u>29,000 ft<sup>2</sup></u>
RCS Volume, $V_{RCS}$	6,000 cu.ft.
Initial RCS Temperature, $T_{RCS}$	250°F
RCS/SG $\Delta T$	50°F
Relief Valve Setpoint, $S$	<u>375 psig</u>
Relief Valve Opening Time, $t$	3 sec.

Applying the heat input procedure:

<u>Step</u>	<u>Procedure</u>	<u>Example Application</u>
1	For both the 350 psig and 400 psig relief valve setpoints, obtain the reference normalized UA ( $UA_{350}$ and $UA_{400}$ ) for the initial RCS temperature ( $T_{RCS}$ ) and relief valve opening time ( $t$ ), using Figures C14 and C15.	For $T_{RCS} = 250^{\circ}\text{F}$ and $t = 3$ seconds, $UA_{350} = UA_{400} = \underline{0.139}$ from Figures C14 and C15.  ( $V_{RCS} = 6000 \text{ cu.ft.}$ )
2	Determine what fraction, $f$ , of $58,000 \text{ ft}^2$ constitutes the actual steam generator heat transfer area.	$29,000 \text{ ft}^2 / 58,000 \text{ ft}^2 = \underline{0.5}$
3	Multiply both $UA_{350}$ and $UA_{400}$ (from Step 1) by $f$ (from Step 2) to obtain new normalized $UA_{350}^1$ and $UA_{400}^1$ values.	$UA_{350}^1 = UA_{400}^1 = 0.139 * 0.5 = \underline{0.0695}$

Figure C14

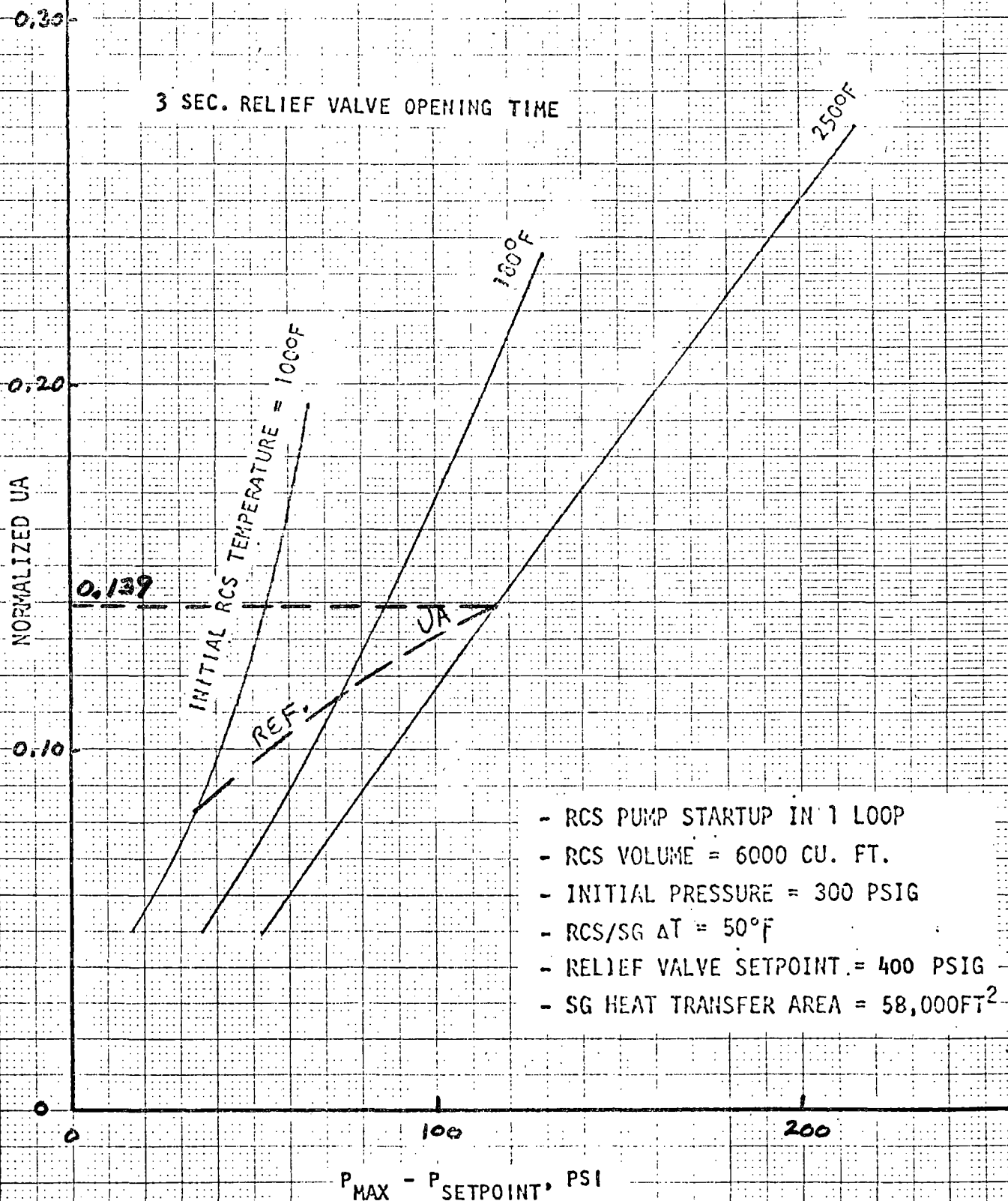
# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERSHOOT



- RCS PUMP STARTUP IN 1 LOOP
- RCS VOLUME = 6000 CU. FT.
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ F$
- RELIEF VALVE SETPOINT = 350 PSIG
- SG HEAT TRANSFER AREA = 58,000FT<sup>2</sup>

Figure C15

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



- RCS PUMP STARTUP IN 1 LOOP
- RCS VOLUME = 6000 CU. FT.
- INITIAL PRESSURE = 300 PSIG
- RCS/SG  $\Delta T = 50^\circ F$
- RELIEF VALVE SETPOINT = 400 PSIG
- SG HEAT TRANSFER AREA = 58,000FT<sup>2</sup>

StepProcedureExample Application

- 4 For the same isotherm,  $T_{RCS}$ , and for  $UA_{350}^I$  and  $UA_{400}^I$  obtain new setpoint overshoots,  $\Delta P_{350}^I$  and  $\Delta P_{400}^I$  for the 350 psig and 400 psig relief valve setpoints, using Figures C16 and C17.
- 5 For the actual relief valve setpoint,  $S$ , linearly interpolate the setpoint overshoot,  $\Delta P_S^I$ , for the new steam generator UA from the relationship:

$$\Delta P_S^I = \Delta P_{350}^I + \frac{S - 350}{400 - 350} (\Delta P_{400}^I - \Delta P_{350}^I)$$

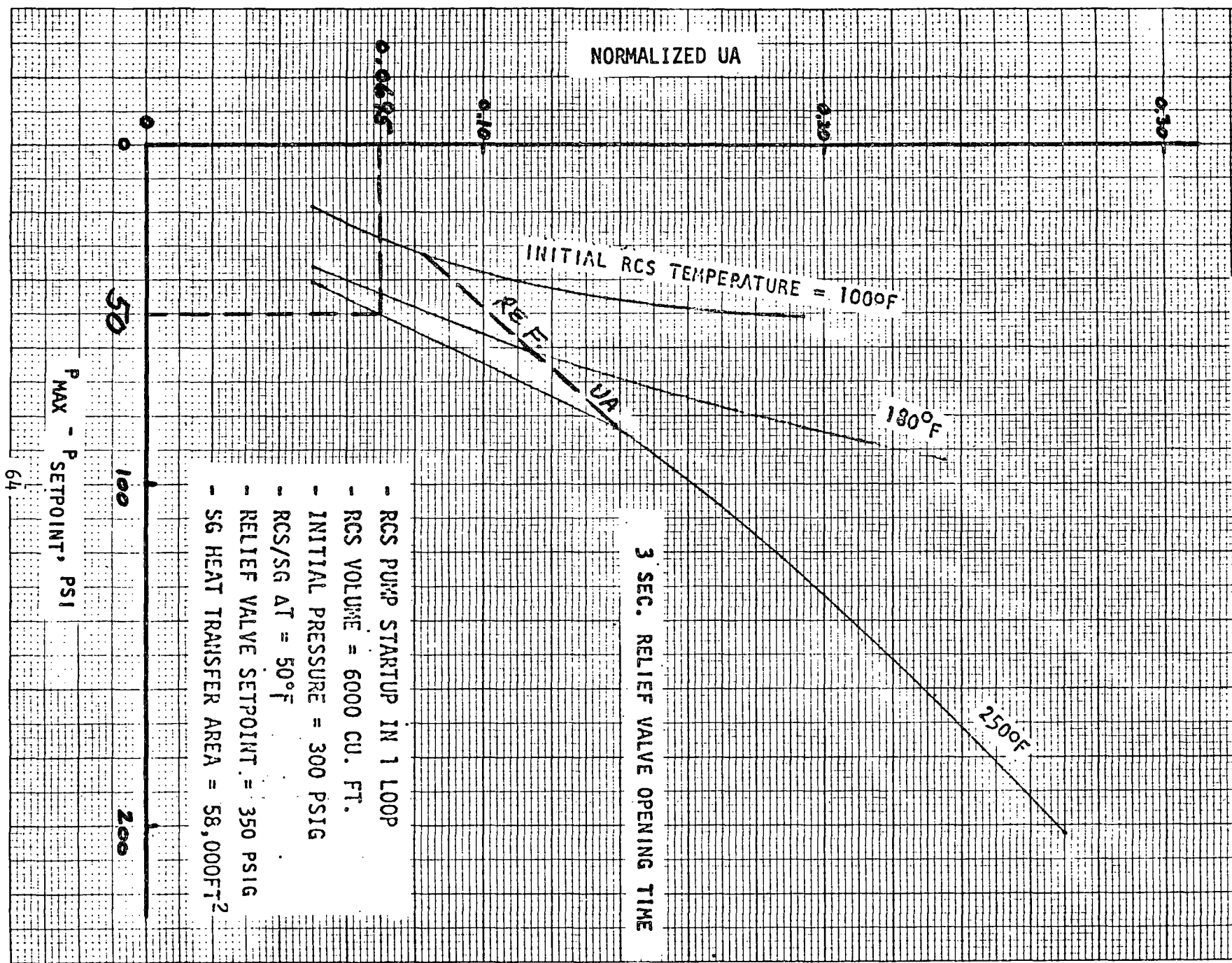
From Figure C16, for  $T_{RCS} = 250^\circ\text{F}$ ,  $t = 3$  seconds and  $UA_{350}^I = 0.0695$ ,  $\Delta P_{350}^I = 50$  psi. From Figure C17, for  $T_{RCS} = 250^\circ\text{F}$ ,  $t = 3$  seconds and  $UA_{400}^I = 0.0695$ ,  $\Delta P_{400}^I = 66$  psi.

For  $S = 375$  psig,  $\Delta P_{350}^I = 50$  psi and  $\Delta P_{400}^I = 66$  psi,

$$\begin{aligned} \Delta P_{375}^I &= 50 \\ &+ \frac{375 - 350}{400 - 350} (66 - 50) \\ &= 58 \text{ psi} \end{aligned}$$

Figure C16

# EFFECT OF STEAM GENERATOR UA ON PRESSURE OVERTHOOT



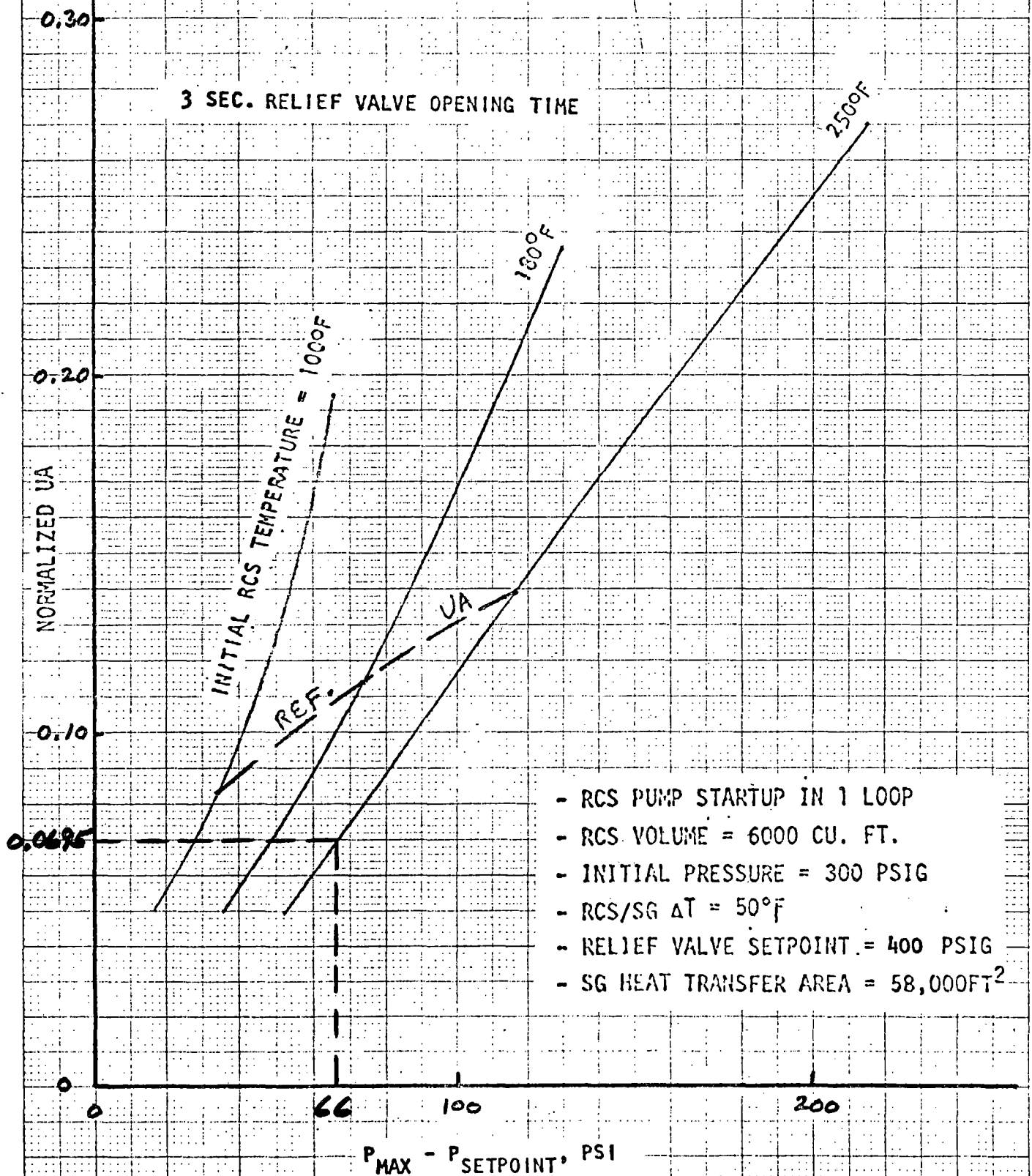
3 SEC. RELIEF VALVE OPENING TIME

- RCS PUMP STARTUP IN 1 LOOP
- RCS VOLUME = 6000 CU. FT.
- INITIAL PRESSURE = 300 PSIG
- RCS/SG ΔT = 50°F
- RELIEF VALVE SETPOINT = 350 PSIG
- SG HEAT TRANSFER AREA = 58,000 FT<sup>2</sup>

P<sub>MAX</sub> - P<sub>SETPOINT</sub>, PSI

Figure C17

EFFECT OF STEAM GENERATOR UA ON  
PRESSURE OVERSHOOT



## REFERENCE

1. "Pressure Mitigating Systems Transient Analysis Results," July 1977.  
(Westinghouse Report on RCS Solid Water Overpressurization prepared  
for the W Owners Group on RCS Overpressurization.)

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