

REGULATORY INFORMATION DISTRIBUTION SYSTEM (RIDS)

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 FACIL: 50-261 H. B. Robinson Plant, Unit 2, Carolina Power and Light 05000261
 AUTH. NAME: AUTHOR AFFILIATION
 ZIMMERMAN, S.R. Carolina Power & Light Co.
 RECIP. NAME: RECIPIENT AFFILIATION
 VARGA, S.A. Operating Reactors Branch 1

SUBJECT: Provides results of verification of calculations to verify pressure buildup & max temp addition resulting in pipe penetration area after pipe rupture. Info closes out temp profiles in SER open item.

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NOTES:

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Carolina Power & Light Company

MAY 30 1984

SERIAL: NLS-84-218

Director of Nuclear Reactor Regulation
Attention: Mr. Steven A. Varga, Chief
Operating Reactors Branch No. 1
Division of Licensing
United States Nuclear Regulatory Commission
Washington, DC 20555

H. B. ROBINSON STEAM ELECTRIC PLANT, UNIT NO. 2
DOCKET NO. 50-261/LICENSE NO. DPR-23
ENVIRONMENTAL QUALIFICATION OF ELECTRICAL EQUIPMENT

Dear Mr. Varga:

BACKGROUND

Carolina Power & Light Company (CP&L) has been discussing the issue of High Energy Line Break Outside of Containment as it relates to environmental qualification (EQ) of electrical equipment at the H. B. Robinson Steam Electric Plant Unit No. 2 (HBR2) with your staff. This issue is also listed as an open item in your Safety Evaluation Report (SER) concerning EQ for HBR2 dated January 5, 1983. Page 5 of your SER discusses the acceptability of temperature profiles outside containment.

Carolina Power & Light Company submitted the document, "Postulated Pipe Failure Analysis Outside of Containment" by Westinghouse, dated November 9, 1973, for your review. Your staff requested additional information concerning the assumptions used in this report (Attachment 1). However, due to the fact that the analysis is over 10 years old, no additional information regarding the analysis can be located. Your staff then requested that we perform a sample calculation to verify the results of the report. The purpose of this letter is to provide you with the results of our verification, including a summary of our assumptions, as committed in our letter dated March 2, 1984.

DETAILS

As agreed upon with members of your staff, CP&L conducted calculations to verify the pressure buildup (0.2 psi) and maximum temperature addition (2.4°F) resulting in the pipe penetration area after a pipe rupture, as discussed on page 45 of the aforementioned Westinghouse report. The calculations were completed by CP&L using the CONTEMPT-LT28 computer code, and the results are attached (Attachment 2). The responses to your questions are also included in Attachment 2 for this sample calculation.

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The CONTEMPT calculations result in a pressure buildup of 0.3 psi and a maximum temperature of 206.6°F. It is clear that the pressure buildup is in agreement with the original analysis. The maximum temperature results, however, appear to indicate a typographical error in the original analysis. When the corrected Westinghouse value is utilized, the maximum temperatures are also in good agreement. Westinghouse was contacted to review these results, and they concur that it was a typographical error; the maximum temperature should have been 214°F (versus 2.4°F). The remaining analyses within the Westinghouse document are still valid.

It should be noted that the corrected maximum temperature value will modify conclusions previously reached within the EQ program at HBR2. A harsh environment outside containment has now been identified. This modification will be discussed, both in scope and schedule, in our May 31, 1984 response to your request for additional information dated May 7, 1984.

CONCLUSION

The calculations performed by CP&L (attached) verify the results of the original analysis performed by Westinghouse. Carolina Power & Light Company considers that this submittal, along with our May 31, 1984 submittal, will close out the open item concerning temperature profiles outside containment on page 5 of your SER.

If you have any questions on this subject, please contact Mr. David Stadler at (919) 836-6737.

Yours very truly,



S. R. Zimmerman

Manager

Nuclear Licensing Section

ONH/ccc (0550NH)
Attachments

cc: Mr. J. P. O'Reilly (NRC-RII)
Mr. G. Requa (NRC)
Mr. Steve Weise (NRC-HBR)

PRESSURE AND TEMPERATURE PROFILES FOR PIPE BREAKS OUTSIDE CONTAINMENT

The following information is required for each pipe break analysis performed by the applicants.

1. With respect to the pipe to be broken, we need to know the:
 - a. Type of fluid (water or steam);
 - b. Temperature;
 - c. Pressure;
 - d. Source of the fluid;
 - e. Flow rate (or assumed flow rate) versus time; and
 - f. Enthalpy versus time
2. With respect to the compartments being analyzed:
 - a. Number of compartment analyzed;
 - b. For each compartment:
 - i. initial temperature
 - ii. initial pressure
 - iii. initial humidity
 - iv. floor area including floor space taken by equipment (square feet)
 - v. number of vents and vent areas (square feet) for each vent; and
 - vi. compartment wall height (feet) and
 - c. Simple compartment and interconnection diagram.
3. All assumptions used, including but not limited to the:
 - a. Orifice coefficient;
 - b. Fluid expansion factor; and
 - c. Heat transfer coefficient for heat through the walls
4. Utilities analysis results:
 - a. Temperature versus time curve (peak temperature specified);
 - b. Pressure versus time curve (peak pressure specified); and
 - c. Humidity versus time curve (peak humidity specified)

STEAM GENERATOR BLOWDOWN LINE RUPTURE

1. FLUID CONDITIONS (1)

a. TYPE OF FLUID: Water, flashing to steam
 b. TEMPERATURE: 450 F
 c. PRESSURE: 1000 psia
 d. SOURCE OF FLUID: Steam Generator Blowdown System
 e. FLOWRATE:

| TIME (sec) | FLOWRATE (lbm/sec) |
|------------|--------------------|
| 0 < t < 1 | 484.0 |
| 1 < t < 4 | 269.6 |
| 4 < t | 27.6 |

f. ENTHALPY:

| TIME (sec) | ENTHALPY (lbm/sec) |
|------------|--------------------|
| 0 < t < 1 | 258.7 |
| 1 < t < 4 | 289.1 |
| 4 < t | 555.4 |

2. COMPARTMENT CONDITIONS

a. NUMBER OF COMPARTMENTS: 1
 b.

| | |
|-------------------------|----------------------|
| i. INITIAL TEMPERATURE: | 104 F |
| ii. INITIAL PRESSURE: | 14.7 psia |
| iii. INITIAL HUMIDITY: | 70% |
| iv. FLOOR AREA: | 2200 ft ² |
| v. NUMBER OF VENTS: | 0 |
| vi. WALL HEIGHT: | 18.5 ft |

c. Compartment drawings attached

3. ASSUMPTIONS

a. ORIFICE COEFFICIENT: See note (2)
 b. FLUID EXPANSION FACTOR: See note (2)
 c. HEAT TRANSFER COEFFICIENT: Tagami-Uchida (3) (4)
 d. AIR ADDITION RATE: 1750 CFM
 e. LEAKAGE RATE: $Q=k(\Delta P)$ (5)

4. RESULTS

Temperature, pressure, and humidity vs time curves are attached

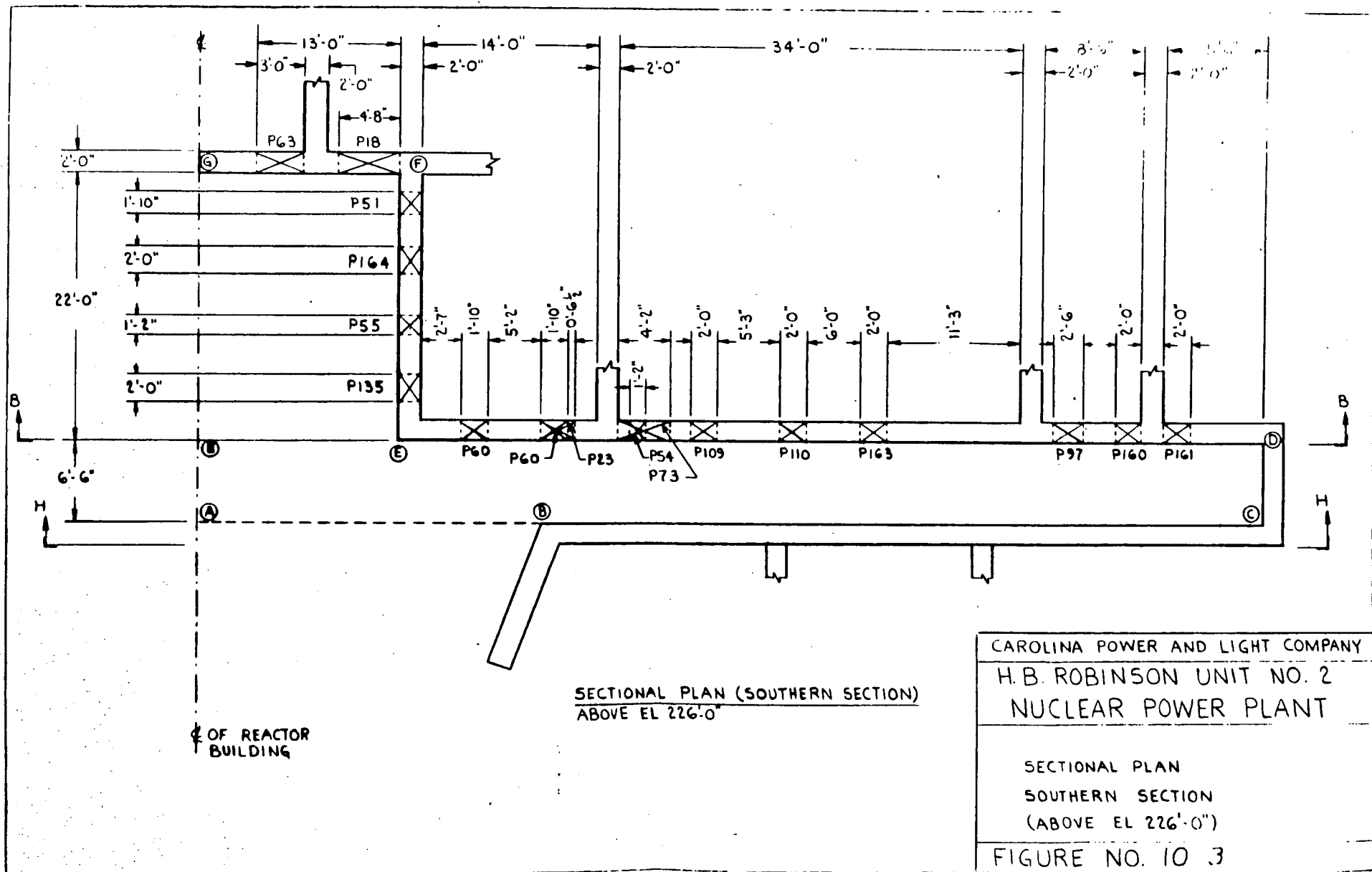
5. NOTES

- (1) Primary fluid conditions were not modeled. Mass and energy added to the compartment was calculated directly from the blowdown enthalpy and flowrate.
- (2) Data for the blowdown rate was taken directly from the 1973 Westinghouse report. The orifice coefficient and fluid expansion factor used was not specified.
- (3) Heat conduction structures included the painted concrete walls and pool of liquid on the floor. All pipes were assumed insulated and therefore neither added nor removed heat.

- (4) The change from the Tagami to the Uchida heat transfer model occurred at 4 seconds.
- (5) The leakage rate from the penetration gallery to the auxiliary building varies with the pressure differential between the two compartments. It is assumed that the air flow geometry does not change and the leakage coefficient, k , is a constant. A value for k was determined that resulted in a leakage rate during normal conditions equal to the air addition rate.

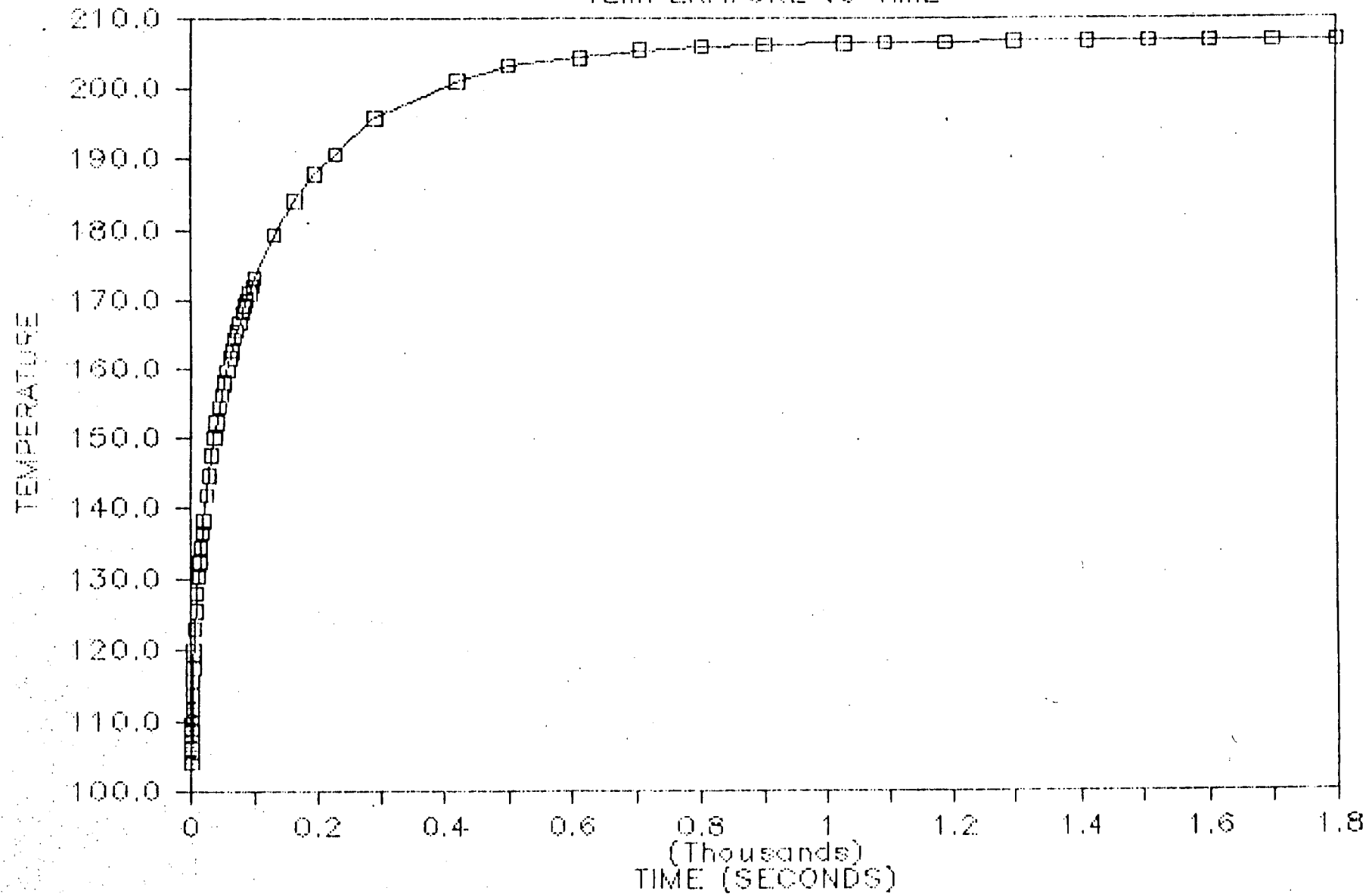


FIGURE NO. 101



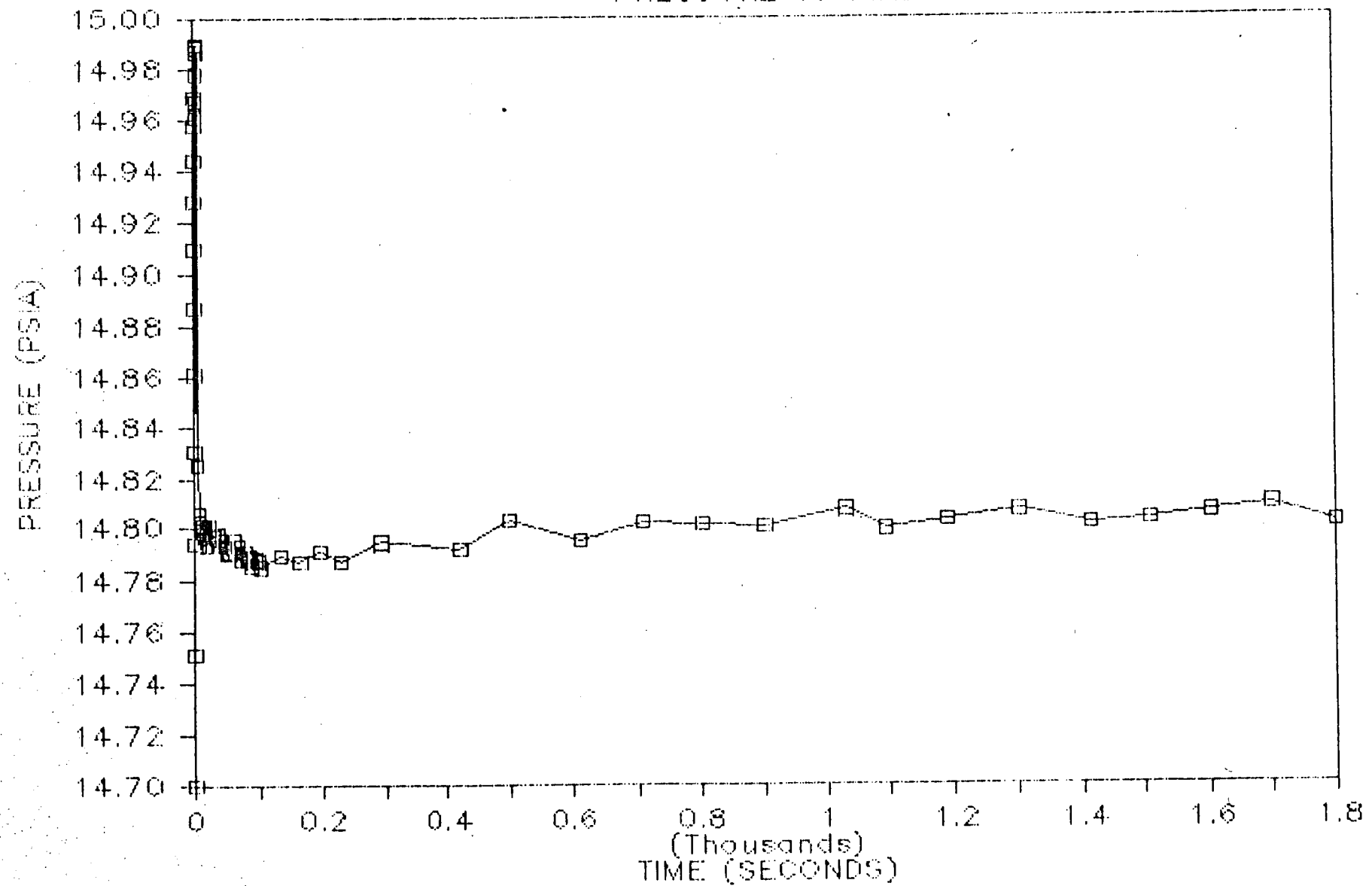
S.G. BLOWDOWN LINE RUPTURE

TEMPERATURE vs TIME



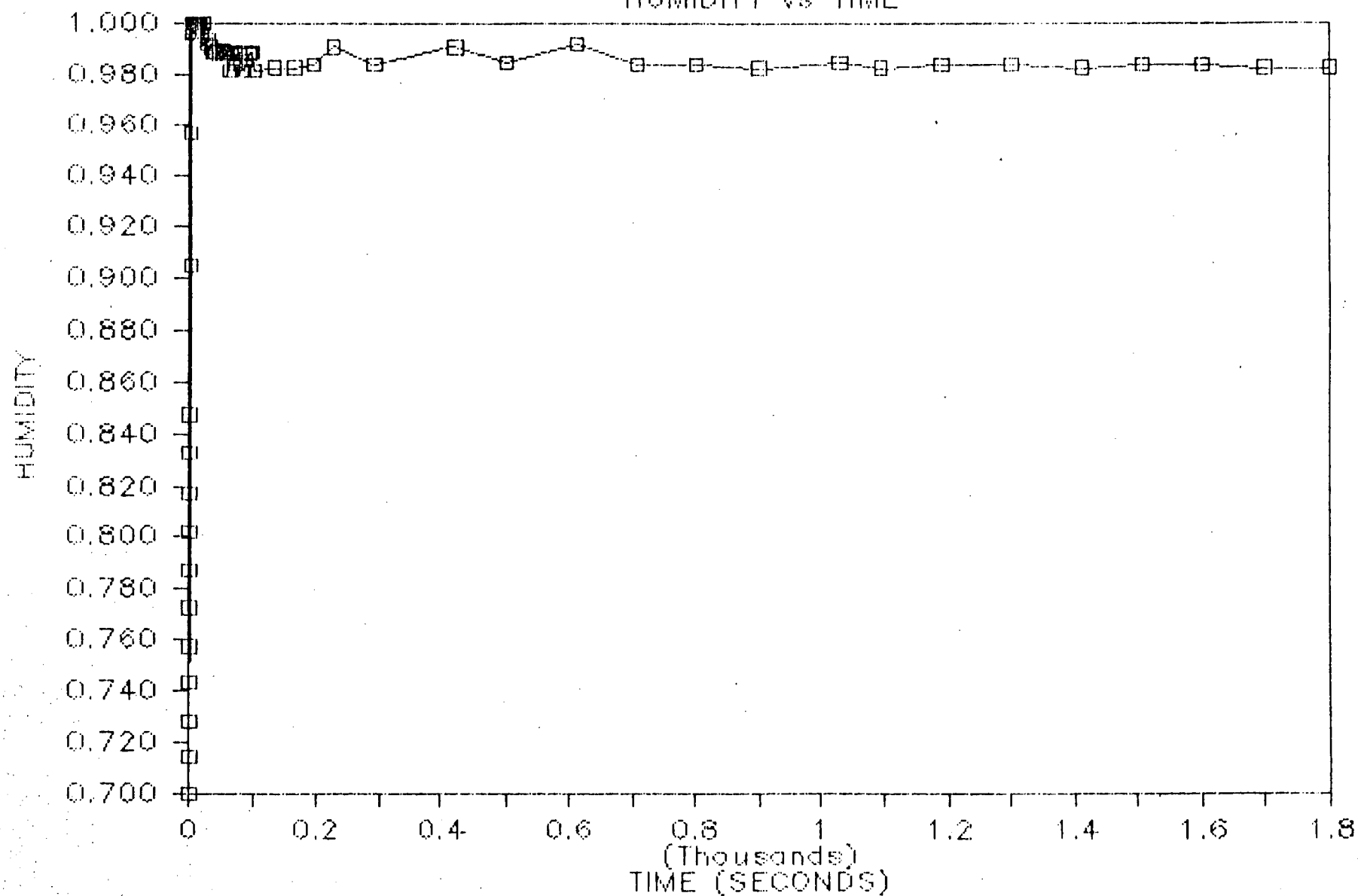
S.G. BLOWDOWN LINE RUPTURE

PRESSURE vs TIME



S.G. BLOWDOWN LINE RUPTURE

HUMIDITY vs TIME



LISTING OF INPUT DATA FOR CASE 1

| | |
|----|---|
| 1 | =CONTEMPT TEST RUN |
| 2 | 11000 BRITISH |
| 3 | 11001 0.333 6 0 95.0 14.7 0.5 104.0 0.0 0.0 0.0 0.0 0.0 1.0 0.0 |
| 4 | 10031 40700.0 0.0 104.0 104.0 14.7 0.7 108.0 1.0 1.0 1.0 |
| 5 | 9000 SEC |
| 6 | 9001 1.0 0.1 10 1 4.0 0.1 40 4 20.0 0.2 80 10 100.0 0.4 200 10 |
| 7 | 9002 1200.0 0.4 2750 50 |
| 8 | 300 SEC LBM/SEC BTU/LBM |
| 9 | 301 0.0 484.0 258.7 1.0 484.0 258.7 |
| 10 | 302 1.1 269.6 289.07 4.0 269.6 289.07 |
| 11 | 303 4.2 27.6 555.4 1.0E9 27.6 555.4 |
| 12 | 901 0.0 7455.0 104.0 0.333 7455.0 104.0 |
| 13 | 30301 0.0 0.0001 1.17E7 0.005 1.17E7 100.0 1.17E7 |
| 14 | 101000 '1.5 FT THICK CONCRETE WALLS' |
| 15 | 101001 30 3 0 0.0 1.0 0.0 5285.0 3 0 |
| 16 | 101101 2 0.001 24 1.001 3 1.5001 |
| 17 | 101201 1 2 2 |
| 18 | 101300 0 0.0 |
| 19 | 101400 53 2 0 0 0 0.00111 2.0 2.0 |
| 20 | 102000 '2 FT THICK CONCRETE WALLS' |
| 21 | 102001 33 3 0 0.0 1.0 0.0 3404.0 3 0 |
| 22 | 102101 2 0.001 24 1.001 6 2.001 |
| 23 | 102201 1 2 2 |
| 24 | 102300 0 0.0 |
| 25 | 102400 53 2 0 0 0 0.00111 2.0 2.0 |
| 26 | 103000 '3 FT THICK CONCRETE WALLS' |
| 27 | 103001 39 3 0 0.0 1.0 0.0 365.0 3 0 |
| 28 | 103101 2 0.001 24 1.001 12 3.001 |
| 29 | 103201 1 2 2 |
| 30 | 103300 0 0.0 |
| 31 | 103400 53 2 0 0 0 0.00111 2.0 2.0 |
| 32 | 104000 '3.5 FT CONCRETE WALLS' |
| 33 | 104001 42 3 0 0.0 1.0 0.0 544.0 3 0 |
| 34 | 104101 2 0.001 24 1.001 15 3.501 |
| 35 | 104201 1 2 2 |
| 36 | 104300 0 0.0 |
| 37 | 104400 53 2 0 0 0 0.00111 2.0 2.0 |
| 38 | 105000 '4 FT THICK CONCRETE WALLS' |
| 39 | 105001 45 3 0 0.0 1.0 0.0 352.0 3 0 |
| 40 | 105101 2 0.001 24 1.001 18 4.001 |
| 41 | 105201 1 2 2 |
| 42 | 105300 0 0.0 |
| 43 | 105400 53 2 0 0 0 0.00111 2.0 2.0 |
| 44 | 106000 '4.5 FT THICK CONCRETE FLOOR' |
| 45 | 106001 55 1 0 0.0 1.0 0.0 2200.0 3 0 |
| 46 | 106101 54 4.5 |
| 47 | 106201 2 |
| 48 | 106300 0 0.0 |
| 49 | 106400 3 3 0 0 |
| 50 | 410001 0.21 18.84 0.55 29.40 |
| 51 | |

BRITI UNITS USED FOR INPUT AND OUTPUT WHERE UNITS ARE UNSPECIFIED.

PROBLEM END TIME= 3.330000E-01 HRS NO. HEAT STRUCTURES= 6 PRESSURE SUPPRESSION OPT.= 0
OUTSIDE AIR TEMPERATURE = 9.500000E+01 F PRESSURE = 1.470000E+01 PSIA HUMIDITY = 5.000000E-01
CONSTANT TEMP. FOR HEAT SLABS= 1.040000D+02 F STEP WATER TO DRY WELL = 0. LBM, WITH STEP ENERGY = 0. BTU
PRIMARY SYSTEM END-OF-BLOWDOWN WATER CONTENT = 0. LBM, WITH ENERGY = 0. BTU
CALCULATE EVAPORATION OR CONDENSATION RATE BETWEEN ATMOSPHERE AND POOL DURING BLOWDOWN.

SPRAY-ECC HEAT EXCHANGER, NO. 1
TYPE = 0 HEAT TRANSFER AREA = 0. OVERALL H.T. COEFF. = 0. COOLANT INLET TEMP. = 0.
INLET MASS FLOW = 0.
PRESSURE FOR SPRAY ON AND OFF = 0. 0.

SPRAY-ECC HEAT EXCHANGER, NO. 2
TYPE = 0 HEAT TRANSFER AREA = 0. OVERALL H.T. COEFF. = 0. COOLANT INLET TEMP. = 0.
INLET MASS FLOW = 0.
PRESSURE FOR SPRAY ON AND OFF = 0. 0.

COMP. = 3 VOL. = 4.070000D+04 LIQ. VOL = 0. VAPOR VOL = 4.070000D+04 HUMIDITY = .7000 TOTAL PRESSURE = 1.470000D+01
VAPOR TEMPERATURE = 1.040000D+02 LIQ. TEMP. = 1.040000D+02 SURF. AREA = 1.080000D+02
HEAT TRANS. MULT. = 1.000000D+00 MASS TRANS. MULT. = 1.000000D+00
DRYWELL PRESSURE FLASH MODEL SELECTED.

NORMAL COMPARTMENT LEAKAGE TABLE OF DELTA-PRESSURE AND COEFFICIENT -- FROM COMPARTMENT 3 TO 0
1.000000E-04 1.170000E+07 5.000000E-03 1.170000E+07
1.000000E+02 1.170000E+07

TABLE OF TIME, POWER DECAY
0. 0. 3.600000E+09 0.

TABLE OF TIME, METAL-WATER REACTION
0. 0. 3.600000E+09 0.

| TABLE OF TIME(SEC) | WATER ADDITION RATE(LBM/SEC) | AND ENTHALPY(BTU/LBM) |
|----------------------|--------------------------------|-------------------------|
| 0. | 4.840000D+02 | 2.587000D+02 |
| 1.100000D+00 | 2.696000D+02 | 2.890700D+02 |
| 4.200000D+00 | 2.760000D+01 | 5.554000D+02 |

PRIMARY VESSEL ENERGY INPUT, TIME, POWER MULT., M-W MULT.
0. 0. 0. 3.600000E+09 0. 0.

TOP REGION DIRECT ADDITION TABLE, TIME, WATER RATE, HEAT RATE
0. 0. 0. 1.000000E+06 0. 0.

LIQUID REGION DIRECT ADDITION TABLE, TIME, WATER RATE, HEAT RATE
0. 0. 0. 1.000000E+06 0. 0.

SUPER HEAT ADDITION TABLE, TIME, POW MULT., M-W MULT., FLOW RATE
0. 0. 0. 0.
1.000000E+06 0. 0. 0.

| SPRAY-ECC SYSTEM, NO. 1 | TIME | FLOW RATE | DR.W.EFF | PCT.DRY | PCT.WET | PCT.ECC | PCT.DWL | INP.DRY | INP.WET | OUT.TEMP. |
|-------------------------|------|-----------|----------|---------|---------|---------|---------|---------|---------|-----------|
| 0. | 0. | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0. |
| 1.000000E+06 | 0. | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0. |

SPRAY-ECC SYSTEM, NO. 2

| TIME | FLOW RATE | DR.W.EFF | PCT.DRY | PCT.WET | PCT.ECC | PCT.DWL | INP.DRY | INP.WET | OUT.TEMP. |
|--------------|-----------|----------|---------|---------|---------|---------|---------|---------|-----------|
| 0. | 0. | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0. |
| 1.000000E+06 | 0. | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0. |

ARBITRARY AIR ADDITION TABLE, TIME, AIR ADDED, TEMP.

| | | | | | |
|----|--------------|--------------|--------------|--------------|--------------|
| 0. | 7.455000E+03 | 1.040000E+02 | 3.330000E-01 | 7.455000E+03 | 1.040000E+02 |
|----|--------------|--------------|--------------|--------------|--------------|

OUTSIDE AIR CONDITIONS TABLE, TIME, TEMP., HEAT TRANSFER COEF. (24 HR. CYCLE)

| | | | | | |
|----|----|----|--------------|----|----|
| 0. | 0. | 0. | 2.400000E+01 | 0. | 0. |
|----|----|----|--------------|----|----|

TABLE OF TIME, TIME STEP (BOTH IN SEC), SLAB PRINT FREQUENCY, AND CONTAINMENT DATA PRINT FREQUENCY

| | | | | | | | |
|--------------|--------------|------|----|--------------|--------------|-----|----|
| 1.000000D+00 | 1.000000D-01 | 10 | 1 | 4.000000D+00 | 1.000000D-01 | 40 | 4 |
| 2.000000D+01 | 2.000000D-01 | 80 | 10 | 1.000000D+02 | 4.000000D-01 | 200 | 10 |
| 1.200000D+03 | 4.000000D-01 | 2750 | 50 | | | | |

HEAT STRUCTURE NO. 1 TRANSFER BETWEEN FOLLOWING COMPARTMENTS LEFT= 3 RIGHT= 0
 1.5 FT THICK CONCRETE WALLS

30 MESH POINTS 3 REGIONS RECTANGULAR GEOMETRY SOURCE FACTOR = 1.000000E+00 SURFACE FACTOR = 5.285000E+03
 DELAY = 0.

MESH POINT COORDINATES (* INDICATES REGION BOUNDARY)

| | | | | | | |
|--------------|---------------|---------------|--------------|--------------|---------------|--------------|
| 0. | 5.000000E-04 | 1.000000E-03* | 4.266667E-02 | 8.433333E-02 | 1.260000E-01 | 1.676667E-01 |
| 2.093333E-01 | 2.510000E-01 | 2.926667E-01 | 3.343333E-01 | 3.760000E-01 | 4.176667E-01 | 4.593333E-01 |
| 5.010000E-01 | 5.426667E-01 | 5.843333E-01 | 6.260000E-01 | 6.676667E-01 | 7.093333E-01 | 7.510000E-01 |
| 7.926667E-01 | 8.343333E-01 | 8.760000E-01 | 9.176667E-01 | 9.593333E-01 | 1.001000E+00* | 1.167367E+00 |
| 1.333733E+00 | 1.500100E+00* | | | | | |

COMPOSITION OVERLAY

1 2 2

SOURCE SPATIAL DEPENDENCE

| | | | | | | |
|----|----|----|----|----|----|----|
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |

INTEGRATED SPACIAL DEPENDENCE = 0.

BOUNDARY CONDITION CONTROL OPTIONS = 53, 2, 0, 0

LEFT BOUNDARY TAGAMI CONTROLS* TIME TO PEAK PRESSURE= 1.110E-03 HRS. 2ND H.T. OPTION= 2 2ND BULK TEMP. CONTROL= 2

HEAT STRUCTURE NO. 2 TRANSFER BETWEEN FOLLOWING COMPARTMENTS LEFT= 3 RIGHT= 0
 2 FT THICK CONCRETE WALLS

33 MESH POINTS 3 REGIONS RECTANGULAR GEOMETRY SOURCE FACTOR = 1.000000E+00 SURFACE FACTOR = 3.404000E+03
 DELAY = 0.

MESH POINT COORDINATES (* INDICATES REGION BOUNDARY)

| | | | | | | |
|--------------|--------------|---------------|--------------|---------------|---------------|--------------|
| 0. | 5.000000E-04 | 1.000000E-03* | 4.266667E-02 | 8.433333E-02 | 1.260000E-01 | 1.676667E-01 |
| 2.093333E-01 | 2.510000E-01 | 2.926667E-01 | 3.343333E-01 | 3.760000E-01 | 4.176667E-01 | 4.593333E-01 |
| 5.010000E-01 | 5.426667E-01 | 5.843333E-01 | 6.260000E-01 | 6.676667E-01 | 7.093333E-01 | 7.510000E-01 |
| 7.926667E-01 | 8.343333E-01 | 8.760000E-01 | 9.176667E-01 | 9.593333E-01 | 1.001000E+00* | 1.167667E+00 |
| 1.334333E+00 | 1.501000E+00 | 1.667667E+00 | 1.834333E+00 | 2.001000E+00* | | |

COMPOSITION OVERLAY

1 2 2

SOURCE SPATIAL DEPENDENCE

| | | | | | | |
|----|----|----|----|----|----|----|
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |

INTEGRATED SPACIAL DEPENDENCE = 0.

BOUNDARY CONDITION CONTROL OPTIONS = 53, 2, 0, 0

LEFT BOUNDARY TAGAMI CONTROLS* TIME TO PEAK PRESSURE= 1.110E-03 HRS. 2ND H.T. OPTION= 2 2ND BULK TEMP. CONTROL= 2

HEAT STRUCTURE NO. 3 TRANSFER BETWEEN FOLLOWING COMPARTMENTS LEFT= 3 RIGHT= 0
 3 FT THICK CONCRETE WALLS

39 MESH POINTS 3 REGIONS RECTANGULAR GEOMETRY SOURCE FACTOR = 1.000000E+00 SURFACE FACTOR = 3.650000E+02
 DELAY = 0.

MESH POINT COORDINATES (* INDICATES REGION BOUNDARY)

| | | | | | | |
|--------------|--------------|---------------|---------------|--------------|---------------|--------------|
| 0. | 5.000000E-04 | 1.000000E-03* | 4.266667E-02 | 8.433333E-02 | 1.260000E-01 | 1.676667E-01 |
| 2.093333E-01 | 2.510000E-01 | 2.926667E-01 | 3.343333E-01 | 3.760000E-01 | 4.176667E-01 | 4.593333E-01 |
| 5.010000E-01 | 5.426667E-01 | 5.843333E-01 | 6.260000E-01 | 6.676667E-01 | 7.093333E-01 | 7.510000E-01 |
| 7.926667E-01 | 8.343333E-01 | 8.760000E-01 | 9.176667E-01 | 9.593333E-01 | 1.001000E+00* | 1.167667E+00 |
| 1.334333E+00 | 1.501000E+00 | 1.667667E+00 | 1.834333E+00 | 2.001000E+00 | 2.167667E+00 | 2.334333E+00 |
| 2.501000E+00 | 2.667667E+00 | 2.834333E+00 | 3.001000E+00* | | | |

COMPOSITION OVERLAY

1 2 2

SOURCE SPATIAL DEPENDENCE

| | | | | | | |
|----|----|----|----|----|----|----|
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |

INTEGRATED SPACIAL DEPENDENCE = 0.

BOUNDARY CONDITION CONTROL OPTIONS = 53, 2, 0, 0

LEFT BOUNDARY TAGAMI CONTROLS* TIME TO PEAK PRESSURE= 1.110E-03 HRS. 2ND H.T. OPTION= 2 2ND BULK TEMP. CONTROL= 2

HEAT STRUCTURE NO. 4 TRANSFER BETWEEN FOLLOWING COMPARTMENTS LEFT= 3 RIGHT= 0
 3.5 FT CONCRETE WALLS

42 MESH POINTS 3 REGIONS RECTANGULAR GEOMETRY SOURCE FACTOR = 1.000000E+00 SURFACE FACTOR = 5.440000E+02
 DELAY = 0.

MESH POINT COORDINATES (* INDICATES REGION BOUNDARY)

| | | | | | | |
|--------------|--------------|---------------|--------------|--------------|---------------|---------------|
| 0. | 5.000000E-04 | 1.000000E-03* | 4.266667E-02 | 8.433333E-02 | 1.260000E-01 | 1.676667E-01 |
| 2.093333E-01 | 2.510000E-01 | 2.926667E-01 | 3.343333E-01 | 3.760000E-01 | 4.176667E-01 | 4.593333E-01 |
| 5.010000E-01 | 5.426667E-01 | 5.843333E-01 | 6.260000E-01 | 6.676667E-01 | 7.093333E-01 | 7.510000E-01 |
| 7.926667E-01 | 8.343333E-01 | 8.760000E-01 | 9.176667E-01 | 9.593333E-01 | 1.001000E+00* | 1.167667E+00 |
| 1.334333E+00 | 1.501000E+00 | 1.667667E+00 | 1.834333E+00 | 2.001000E+00 | 2.167667E+00 | 2.334333E+00 |
| 2.501000E+00 | 2.667667E+00 | 2.834333E+00 | 3.001000E+00 | 3.167667E+00 | 3.334333E+00 | 3.501000E+00* |

COMPOSITION OVERLAY

1 2 2

SOURCE SPATIAL DEPENDENCE

| | | | | | | |
|----|----|----|----|----|----|----|
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |

INTEGRATED SPACIAL DEPENDENCE = 0.

BOUNDARY CONDITION CONTROL OPTIONS = 53, 2, 0, 0

LEFT BOUNDARY TAGAMI CONTROLS* TIME TO PEAK PRESSURE= 1.110E-03 HRS. 2ND H.T. OPTION= 2 2ND BULK TEMP. CONTROL= 2

HEAT STRUCTURE NO. 5 TRANSFER BETWEEN FOLLOWING COMPARTMENTS LEFT= 3 RIGHT= 0
 4 FT THICK CONCRETE WALLS

45 MESH POINTS 3 REGIONS RECTANGULAR GEOMETRY SOURCE FACTOR = 1.000000E+00 SURFACE FACTOR = 3.520000E+02
 DELAY = 0.

MESH POINT COORDINATES (* INDICATES REGION BOUNDARY)

| | | | | | | |
|--------------|--------------|---------------|--------------|--------------|---------------|--------------|
| 0. | 5.000000E-04 | 1.000000E-03* | 4.266667E-02 | 8.433333E-02 | 1.260000E-01 | 1.676667E-01 |
| 2.093333E-01 | 2.510000E-01 | 2.926667E-01 | 3.343333E-01 | 3.760000E-01 | 4.176667E-01 | 4.593333E-01 |
| 5.010000E-01 | 5.426667E-01 | 5.843333E-01 | 6.260000E-01 | 6.676667E-01 | 7.093333E-01 | 7.510000E-01 |
| 7.926667E-01 | 8.343333E-01 | 8.760000E-01 | 9.176667E-01 | 9.593333E-01 | 1.001000E+00* | 1.167667E+00 |
| 1.334333E+00 | 1.501000E+00 | 1.667667E+00 | 1.834333E+00 | 2.001000E+00 | 2.167667E+00 | 2.334333E+00 |
| 2.501000E+00 | 2.667667E+00 | 2.834333E+00 | 3.001000E+00 | 3.167667E+00 | 3.334333E+00 | 3.501000E+00 |
| 3.667667E+00 | 3.834333E+00 | 4.001000E+00* | | | | |

COMPOSITION OVERLAY

1 2 2

SOURCE SPATIAL DEPENDENCE

| | | | | | | |
|----|----|----|----|----|----|----|
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |

INTEGRATED SPACIAL DEPENDENCE = 0.

BOUNDARY CONDITION CONTROL OPTIONS = 53, 2, 0, 0

LEFT BOUNDARY TAGAMI CONTROLS* TIME TO PEAK PRESSURE= 1.110E-03 HRS. 2ND H.T. OPTION= 2 2ND BULK TEMP. CONTROL= 2

HEAT STRUCTURE NO. 6 TRANSFER BETWEEN FOLLOWING COMPARTMENTS LEFT= 3 RIGHT= 0
4.5 FT THICK CONCRETE FLOOR

55 MESH POINTS 1 REGIONS RECTANGULAR GEOMETRY SOURCE FACTOR = 1.000000E+00 SURFACE FACTOR = 2.200000E+03
DELAY = 0.

MESH POINT COORDINATES (* INDICATES REGION BOUNDARY)

| | | | | | | |
|--------------|--------------|--------------|--------------|--------------|---------------|--------------|
| 0. | 8.333333E-02 | 1.666667E-01 | 2.500000E-01 | 3.333333E-01 | 4.166667E-01 | 5.000000E-01 |
| 5.833333E-01 | 6.666667E-01 | 7.500000E-01 | 8.333333E-01 | 9.166667E-01 | 1.000000E+00 | 1.083333E+00 |
| 1.166667E+00 | 1.250000E+00 | 1.333333E+00 | 1.416667E+00 | 1.500000E+00 | 1.583333E+00 | 1.666667E+00 |
| 1.750000E+00 | 1.833333E+00 | 1.916667E+00 | 2.000000E+00 | 2.083333E+00 | 2.166667E+00 | 2.250000E+00 |
| 2.333333E+00 | 2.416667E+00 | 2.500000E+00 | 2.583333E+00 | 2.666667E+00 | 2.750000E+00 | 2.833333E+00 |
| 2.916667E+00 | 3.000000E+00 | 3.083333E+00 | 3.166667E+00 | 3.250000E+00 | 3.333333E+00 | 3.416667E+00 |
| 3.500000E+00 | 3.583333E+00 | 3.666667E+00 | 3.750000E+00 | 3.833333E+00 | 3.916667E+00 | 4.000000E+00 |
| 4.083333E+00 | 4.166667E+00 | 4.250000E+00 | 4.333333E+00 | 4.416667E+00 | 4.500000E+00* | |

COMPOSITION OVERLAY

2

SOURCE SPATIAL DEPENDENCE

| | | | | | | |
|----|----|----|----|----|----|----|
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| 0. | 0. | 0. | 0. | 0. | 0. | 0. |

INTEGRATED SPACIAL DEPENDENCE = 0.

BOUNDARY CONDITION CONTROL OPTIONS = 3, 3, 0, 0

TABLES COMMON TO ALL HEAT SLABS

THERMAL CONDUCTIVITY AND VOLUMETRIC HEAT CAPACITY TABLE
COMPOSITION NO., THERMAL CONDUCTIVITY, HEAT CAPACITY

| | | |
|---|--------------|--------------|
| 1 | 2.100000E-01 | 1.884000E+01 |
| 2 | 5.500000E-01 | 2.940000E+01 |

THE FOLLOWING DEFINITIONS WILL BE USED AT TIMES FOR COMPARTMENT IDENTIFICATION

- 0 = OUTSIDE ATMOSPHERE
- 1 = PRIMARY SYSTEM
- 2 = WET WELL
- 3 = DRY WELL
- 4 = ANNULAR COMPARTMENT

HEAT STRUCTURE 1 BETWEEN COMPARTMENTS 3 AND 0 1.5 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 3.189605D-06 0. 0. OLIVID 0. 0.
LEFT FILM COEF. $h = 1.761102E-04$ BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.040000E+02 F
RIGHT FILM COEF. $h = 0$ BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 2 BETWEEN COMPARTMENTS 3 AND 0 2 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 2.050134D-06 0. 0. OLIVID 0. 0.
LEFT FILM COEF. $h = 1.761102E-04$ BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.040000E+02 F
RIGHT FILM COEF. $h = 0$ BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 3 BETWEEN COMPARTMENTS 3 AND 0 3 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 2.181142D-07 0. 0. OLIVID 0. 0.
LEFT FILM COEF. $h = 1.761102E-04$ BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.040000E+02 F
RIGHT FILM COEF. $h = 0$ BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 4 BETWEEN COMPARTMENTS 3 AND 0 3.5 FT CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 3.240864D-07 0. 0. OLIVID 0. 0.
LEFT FILM COEF. $h = 1.761102E-04$ BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.040000E+02 F
RIGHT FILM COEF. $h = 0$ BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02

HEAT STRUCTURE 5 BETWEEN COMPARTMENTS 3 AND 0 4 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 2.106894D-07 0. 0. OLIVID 0. 0.
LEFT FILM COEF. $h = 1.761102E-04$ BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.040000E+02 F

RIGHT FILM COEF $\alpha_H = 0$ BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 6 BETWEEN COMPARTMENTS 3 AND 0 4.5 FT THICK CONCRETE FLOOR

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|----------|---------------|----------------|-----------------|----------|---------------|
| 3 LIQUID | 9.306532D-07 | 0. | 0. | 0 LIQUID | 0. | 0. | 0. |

LEFT FILM COEF $\alpha_H = 4.000000E-01$ BTU/HR.FT².F FIRST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000E+02 F
RIGHT FILM COEF $\alpha_H = 0$ BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

***** TIME = 0. HR = 0. MIN = 0. SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE |
|--|------------------------|-------------|---------------------------|-------------|-------------------|------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.47000D+01 | 7.48758D-01 | 1.04000D+02 | 1.04000D+02 | 3.57491D+05 | 0. | 3.57491D+05 |
| <p>AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION (LB/S) TRANSFER COEFFICIENTS MASS HEAT</p> <p>3 2.72290D+03 9.10107D+01 0. 0. 9.10107D+01 7.00000D-01 0. 0. 0. 0.</p> <p>COMP. 3 LEAKAGE OUTFLOW- MASS= 0. LBM/HR ENERGY BTU/HR = 0. (NORMAL= 0. PENETRATION= 0.)</p> <p>STEP AND NET MASS LOSSES LBM STEP VAPOR= 0. STEP AIR= 0. NET VAPOR= 0. NET AIR= 0.</p> | | | | | | | |

***** TIME = 2.777778E-05 HR = 1.666667E-03 MIN = 1.000000E-01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE |
|--|------------------------|-------------|---------------------------|-------------|-------------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.47509D+01 | 7.82565D-01 | 1.04776D+02 | 2.12014D+02 | 3.61922D+05 | 8.01283D+03 | 3.69934D+05 |
| <p>AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION (LB/S) TRANSFER COEFFICIENTS MASS HEAT</p> <p>3 2.72248D+03 9.49064D+01 0. 4.44825D+01 1.39389D+02 7.14340D-01 0. 0. 0. 0.</p> <p>COMP. 3 LEAKAGE OUTFLOW- MASS= 2.3294D+04 LBM/HR ENERGY BTU/HR = 3.9107D+06 (NORMAL= 3.9107D+06 PENETRATION= 0.)</p> <p>STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.1797D-02 STEP AIR= 6.2527D-01 NET VAPOR= 2.1797D-02 NET AIR= 6.2527D-01</p> <p>TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 6.252663D-01 WATER VAPOR(LBM)= 2.179730D-02</p> | | | | | | | |

***** TIME = 5.555556E-05 HR = 3.333333E-03 MIN = 2.000000E-01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE |
|---|------------------------|-------------|---------------------------|-------------|-------------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.47940D+01 | 8.15278D-01 | 1.05507D+02 | 2.12094D+02 | 3.66162D+05 | 1.60345D+04 | 3.82197D+05 |
| <p>AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION (LB/S) TRANSFER COEFFICIENTS MASS HEAT</p> <p>3 2.72100D+03 9.87543D+01 0. 8.89741D+01 1.87728D+02 7.28360D-01 -4.86775D-04 1.57746D-06 8.15474D-09</p> <p>COMP. 3 LEAKAGE OUTFLOW- MASS= 6.3036D+04 LBM/HR ENERGY BTU/HR = 1.0645D+07 (NORMAL= 1.0645D+07 PENETRATION= 0.)</p> <p>STEP AND NET MASS LOSSES LBM STEP VAPOR= 6.0552D-02 STEP AIR= 1.6905D+00 NET VAPOR= 8.2349D-02 NET AIR= 2.3157D+00</p> <p>TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.315727D+00 WATER VAPOR(LBM)= 8.234911D-02</p> | | | | | | | |

***** TIME = 8.333333E-05 HR = 5.000000E-03 MIN = 3.000000E-01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE |
|---|------------------------|-------------|---------------------------|-------------|-------------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.48307D+01 | 8.47622D-01 | 1.06171D+02 | 2.12169D+02 | 3.70243D+05 | 2.40640D+04 | 3.94307D+05 |
| <p>AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION (LB/S) TRANSFER COEFFICIENTS MASS HEAT</p> <p>3 2.71864D+03 1.02560D+02 0. 1.33473D+02 2.36033D+02 7.42638D-01 -5.33460D-04 1.57594D-06 9.60000D-09</p> <p>COMP. 3 LEAKAGE OUTFLOW- MASS= 9.5838D+04 LBM/HR ENERGY BTU/HR = 1.6315D+07 (NORMAL= 1.6315D+07 PENETRATION= 0.)</p> <p>STEP AND NET MASS LOSSES LBM STEP VAPOR= 9.5338D-02 STEP AIR= 2.5668D+00 NET VAPOR= 1.7769D-01 NET AIR= 4.8826D+00</p> <p>TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.882562D+00 WATER VAPOR(LBM)= 1.776873D-01</p> | | | | | | | |

***** TIME = 1.111111E-04 HR = 6.666667E-03 MIN = 4.000000E-01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--|---|---------------------------|---------------------------|-------------------|---------------------|---------------------|-------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.48617D+01 | 8.79628D-01 | 1.06777D+02 | 2.12239D+02 | 3.74183D+05 | 3.21001D+04 | 4.06283D+05 | -4.46907D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R V A P O R -- A T M O S -- L I Q U I D | | M A S S (L B M) P O O L | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 2.71554D+03 | 1.06328D+02 0. | | 1.77977D+02 | 2.84306D+02 | 7.57156D-01 | -5.67496D-04 | 1.57461D-06 1.07401D-08 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 1.2367D+05 LBM/HR ENERGY BTU/HR = 2.1226D+07 (NORMAL= 2.1226D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.2743D-01 STEP AIR= 3.3079D+00 NET VAPOR= 3.0512D-01 NET AIR= 8.1905D+00 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 8.190477D+00 WATER VAPOR(LBM)= 3.051168D-01 | | | | | | | | |

***** TIME = 1.388889E-04 HR = 8.333333E-03 MIN = 5.000000E-01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|------------------------|----------------------|---------------------------|-----------------|---------------------|-------------|--------------|-----------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.48878D+01 | 9.11328D-01 | 1.07330D+02 | 2.12301D+02 | 3.78002D+05 | 4.01420D+04 | 4.18144D+05 | -4.03918D-04 |
| | AIR MASS | W A T E R | | M A S S | (L B M) | HUMIDITY | CONDENSATION | TRANSFER COEFFICIENTS |
| | (L B M) | VAPOR--ATMOS--LIQUID | | POOL | TOTAL | | (LB/S) | MASS |
| | | | | | | | | HEAT |
| 3 | 2.71181D+03 | 1.10062D+02 | 0. | 2.22487D+02 | 3.32549D+02 | 7.71899D-01 | -5.91822D-04 | 1.57343D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- | MASS= | 1.4720D+05 LBM/HR | ENERGY BTU/HR = | 2.5472D+07 (NORMAL= | 2.5472D+07 | PENETRATION= | 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.5698D-01 STEP AIR= 3.9320D+00 NET VAPOR= 4.6209D-01 NET AIR= 1.2122D+01 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.212244D+01 WATER VAPOR(LBM)= 4.620920D-01 | | | | | | | | |

***** TIME = 1.666667E-04 HR = 1.000000E-02 MIN = 6.000000E-01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--------------------------|--------------------------------|---------------------------|--------------------|-------------------|---------------------|---------------------|----------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.49098D+01 | 9.42747D-01 | 1.07835D+02 | 2.12358D+02 | 3.81713D+05 | 4.81885D+04 | 4.29902D+05 | -3.65058D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 2.70756D+03 | 1.13764D+02 0. | | 2.67001D+02 | 3.80765D+02 | 7.86863D-01 | -6.08672D-04 | 1.57234D-06 1.22802D-08 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 1.6701D+05 LBM/HR | | ENERGY BTU/HR = | 2.9133D+07 (NORMAL= | | 2.9133D+07 PENETRATION= 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.8414D-01 STEP AIR= 4.4550D+00 NET VAPOR= 6.4623D-01 NET AIR= 1.6577D+01 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.657745D+01 WATER VAPOR(LBM)= 6.462303D-01 | | | | | | | | |

***** TIME = 1.944444E-04 HR = 1.166667E-02 MIN = 7.000000E-01 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | CONVERGENCE |
|--|--|----------------------------|--|-----------------|-----------------|---------------------|-------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.49282D+01 | 9.73910D-01 | 1.08297D+02 | 2.12409D+02 | 3.85332D+05 | 5.62391D+04 | 4.41571D+05 |
| | TRANSFER COEFFICIENTS | | | | | | -3.29773D-04 |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | | MASS (LBM) POOL | HUMIDITY | CONDENSATION (LB/S) | MASS HEAT (BTU/S FT2 R) |
| 3 | 2.70288D+03 | 1.17437D+02 | | 0.3.11518D+02 | 4.28955D+02 | 8.02045D-01 | -6.19672D-04 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 1.8360D+05 LBM/HR | | ENERGY BTU/HR = 3.2283D+07 (NORMAL= 3.2283D+07 | | PENETRATION= 0. | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.0908D-01 STEP AIR= 4.8910D+00 NET VAPOR= 8.5531D-01 NET AIR= 2.1468D+01 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.146841D+01 WATER VAPOR(LBM)= 8.553144D-01 | | | | | | | |

***** TIME = 2.222222E-04 HR = 1.333333E-02 MIN = 8.000000E-01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|--------------|-------------------------|
| 3 | 1.49443D+01 | 1.00490D+00 | 1.08730D+02 | 2.12455D+02 | 3.88890D+05 | 6.42930D+04 | 4.53183D+05 | -2.41044D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT | | | | | | | | |
| 3 | 2.69795D+03 | 1.21090D+02 | 0. | 3.56038D+02 | 4.77129D+02 | 8.17253D-01 | -5.96013D-04 | 1.57166D-06 1.19801D-08 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 1.9305D+05 LBM/HR ENERGY BTU/HR = 3.4197D+07 (NORMAL= 3.4197D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.2677D-01 STEP AIR= 5.1356D+00 NET VAPOR= 1.0821D+00 NET AIR= 2.6604D+01 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.660403D+01 WATER VAPOR(LBM)= 1.082080D+00 | | | | | | | | |

***** TIME = 2.500000E-04 HR = 1.500000E-02 MIN = 9.000000E-01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|--------------|-------------------------|
| 3 | 1.49578D+01 | 1.03567D+00 | 1.09126D+02 | 2.12497D+02 | 3.92377D+05 | 7.23498D+04 | 4.64726D+05 | -2.10264D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT | | | | | | | | |
| 3 | 2.69272D+03 | 1.24719D+02 | 0. | 4.00561D+02 | 5.25281D+02 | 8.32692D-01 | -5.97591D-04 | 1.57088D-06 1.21139D-08 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 2.0473D+05 LBM/HR ENERGY BTU/HR = 3.6547D+07 (NORMAL= 3.6547D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.4790D-01 STEP AIR= 5.4389D+00 NET VAPOR= 1.3300D+00 NET AIR= 3.2043D+01 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.204296D+01 WATER VAPOR(LBM)= 1.329981D+00 | | | | | | | | |

***** TIME = 2.777778E-04 HR = 1.666667E-02 MIN = 1.000000E+00 SEC *****

HEAT STRUCTURE 1 BETWEEN COMPARTMENTS 3 AND 0 1.5 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 5.648926D+04 3.229177D+00 7.883234D+01 OLIIQUID 0. 0. 0.
LEFT FILM COEF. H = 2.996083E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.038999E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.042566D+02 1.041065D+02 1.039980D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 2 BETWEEN COMPARTMENTS 3 AND 0 2 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 3.638400D+04 2.079871D+00 5.077489D+01 OLIIQUID 0. 0. 0.
LEFT FILM COEF. H = 2.996083E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.038999E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.042566D+02 1.041065D+02 1.039980D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 3 BETWEEN COMPARTMENTS 3 AND 0 3 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR 3.901339D+03 2.230179D-01 5.444429D+00 OLIIQUID 0. 0. 0.
LEFT FILM COEF. H = 2.996083E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.038999E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.042566D+02 | 1.041065D+02 | 1.039980D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 4 BETWEEN COMPARTMENTS 3 AND 0 3.5 FT CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|--------------|---------------|----------------|-----------------|----------|---------------|
| 3 VAPOR | 5.814599D+03 | 3.323883D-01 | 8.114436D+00 | OLIQUID | 0. | 0. | 0. |

LEFT FILM COEF., H = 2.996083E+01 BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT.F BULK TEMP = 1.038999E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.042566D+02 | 1.041065D+02 | 1.039980D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 5 BETWEEN COMPARTMENTS 3 AND 0 4 FT THICK CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|--------------|---------------|----------------|-----------------|----------|---------------|
| 3 VAPOR | 3.762388D+03 | 2.150748D-01 | 5.250518D+00 | OLIQUID | 0. | 0. | 0. |

LEFT FILM COEF., H = 2.996083E+01 BTU/HR.FT².F FIRST MESH K = 2.100000E-01 BTU/HR.FT.F BULK TEMP = 1.038999E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.042566D+02 | 1.041065D+02 | 1.039980D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 6 BETWEEN COMPARTMENTS 3 AND 0 4.5 FT THICK CONCRETE FLOOR

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|---------------|---------------|----------------|-----------------|----------|---------------|
| 3 LIQUID | -9.549972D+04 | -2.652313D+00 | -2.514604D+01 | OLIQUID | 0. | 0. | 0. |

LEFT FILM COEF., H = 4.000000E-01 BTU/HR.FT².F FIRST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 2.125317E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT².F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.040093D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

SUMMARY OF HEAT TRANSFER TO COMPARTMENTS BY HEAT STRUCTURES - UNITS ARE BTU

| COMP. | STEP-LIQUID | STEP-VAPOR | NET-LIQUID | NET-VAPOR |
|-------|---------------|--------------|---------------|--------------|
| 0 | 0. | 0. | 0. | 0. |
| 1 | 0. | 0. | 0. | 0. |
| 2 | 0. | 0. | 0. | 0. |
| 3 | -2.652313D+00 | 6.079530D+00 | -2.514604D+01 | 1.484166D+02 |
| 4 | 0. | 0. | 0. | 0. |

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE DE/E |
|----------|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.49688D+01 | 1.06624D+00 | 1.09488D+02 | 2.12535D+02 | 3.95799D+05 | 8.04090D+04 | 4.76208D+05 | -1.76193D-04 |

| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | |
|--|--|-----------------------------------|----|-----------------|-------------|-------------|--------------|------------------------|-------------|---|--|
| 3 | 2.68724D+03 | 1.28327D+02 | 0. | 4.45087D+02 | 5.73414D+02 | 8.48377D-01 | -5.95509D-04 | 1.57015D-06 | 1.21181D-08 | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.1428D+05 LBM/HR ENERGY BTU/HR = 3.8544D+07 (NORMAL= 3.8544D+07 PENETRATION= 0.) | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.6724D-01 STEP AIR= 5.6851D+00 NET VAPOR= 1.5972D+00 NET AIR= 3.7728D+01 | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.772808D+01 WATER VAPOR(LBM)= 1.597216D+00 | | | | | | | | | | | |

***** TIME = 3.888889E-04 HR = 2.333333E-02 MIN = 1.400000E+00 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE DE/E | TRANSFER COEFFICIENTS | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|--|--|-----------------------------------|---------------------------|-----------------|-------------------|-------------|---------------------|------------------------|-------------|---|--|-----------------------------------|--|-----------------|--|----------|--|------------------------|--|---|--|---|-------------|-------------|----|-------------|-------------|-------------|--------------|-------------|-------------|--|--|-------|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|---|--|--|--|--|--|--|--|--|--|--|--|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | | MASS | HEAT | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 3 | 1.49674D+01 | 1.16231D+00 | 1.10228D+02 | 2.12594D+02 | 4.05935D+05 | 9.95898D+04 | 5.05525D+05 | 2.62513D-05 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <table border="1"> <thead> <tr> <th colspan="2">AIR MASS (LBM)</th> <th colspan="2">W A T E R VAPOR--ATMOS--LIQUID</th> <th colspan="2">M A S S POOL</th> <th colspan="2">HUMIDITY</th> <th colspan="2">CONDENSATION (LB/S)</th> <th colspan="2">TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R)</th> </tr> </thead> <tbody> <tr> <td>3</td> <td>2.66492D+03</td> <td>1.39737D+02</td> <td>0.</td> <td>5.51077D+02</td> <td>6.90813D+02</td> <td>9.05392D-01</td> <td>-5.21565D-04</td> <td>1.56849D-06</td> <td>9.78900D-09</td> <td></td> <td></td> </tr> <tr> <td>COMP.</td> <td colspan="11">3 LEAKAGE OUTFLOW- MASS= 2.1583D+05 LBM/HR ENERGY BTU/HR = 3.9783D+07 (NORMAL= 3.9783D+07 PENETRATION= 0.)</td> </tr> <tr> <td colspan="12">STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.9539D-01 STEP AIR= 5.7000D+00 NET VAPOR= 2.7573D+00 NET AIR= 6.0877D+01</td> </tr> <tr> <td colspan="12">TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 6.087726D+01 WATER VAPOR(LBM)= 2.757328D+00</td> </tr> </tbody> </table> | | | | | | | | | | AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | 3 | 2.66492D+03 | 1.39737D+02 | 0. | 5.51077D+02 | 6.90813D+02 | 9.05392D-01 | -5.21565D-04 | 1.56849D-06 | 9.78900D-09 | | | COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.1583D+05 LBM/HR ENERGY BTU/HR = 3.9783D+07 (NORMAL= 3.9783D+07 PENETRATION= 0.) | | | | | | | | | | | STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.9539D-01 STEP AIR= 5.7000D+00 NET VAPOR= 2.7573D+00 NET AIR= 6.0877D+01 | | | | | | | | | | | | TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 6.087726D+01 WATER VAPOR(LBM)= 2.757328D+00 | | | | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 3 | 2.66492D+03 | 1.39737D+02 | 0. | 5.51077D+02 | 6.90813D+02 | 9.05392D-01 | -5.21565D-04 | 1.56849D-06 | 9.78900D-09 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.1583D+05 LBM/HR ENERGY BTU/HR = 3.9783D+07 (NORMAL= 3.9783D+07 PENETRATION= 0.) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.9539D-01 STEP AIR= 5.7000D+00 NET VAPOR= 2.7573D+00 NET AIR= 6.0877D+01 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 6.087726D+01 WATER VAPOR(LBM)= 2.757328D+00 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

***** TIME = 5.000000E-04 HR = 3.000000E-02 MIN = 1.800000E+00 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE DE/E | TRANSFER COEFFICIENTS | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|--|--|-----------------------------------|---------------------------|-----------------|-------------------|-------------|---------------------|------------------------|-------------|---|--|-----------------------------------|--|-----------------|--|----------|--|------------------------|--|---|--|---|-------------|-------------|----|-------------|-------------|-------------|--------------|-------------|-------------|--|--|-------|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|---|--|--|--|--|--|--|--|--|--|--|--|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | | MASS | HEAT | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 3 | 1.49616D+01 | 1.25192D+00 | 1.10882D+02 | 2.12605D+02 | 4.15294D+05 | 1.16946D+05 | 5.32239D+05 | 6.19776D-05 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <table border="1"> <thead> <tr> <th colspan="2">AIR MASS (LBM)</th> <th colspan="2">W A T E R VAPOR--ATMOS--LIQUID</th> <th colspan="2">M A S S POOL</th> <th colspan="2">HUMIDITY</th> <th colspan="2">CONDENSATION (LB/S)</th> <th colspan="2">TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R)</th> </tr> </thead> <tbody> <tr> <td>3</td> <td>2.64347D+03</td> <td>1.50364D+02</td> <td>0.</td> <td>6.47074D+02</td> <td>7.97437D+02</td> <td>9.57134D-01</td> <td>-4.78039D-04</td> <td>1.56668D-06</td> <td>8.49123D-09</td> <td></td> <td></td> </tr> <tr> <td>COMP.</td> <td colspan="11">3 LEAKAGE OUTFLOW- MASS= 2.0906D+05 LBM/HR ENERGY BTU/HR = 3.9381D+07 (NORMAL= 3.9381D+07 PENETRATION= 0.)</td> </tr> <tr> <td colspan="12">STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.0938D-01 STEP AIR= 5.4979D+00 NET VAPOR= 3.9733D+00 NET AIR= 8.3151D+01</td> </tr> <tr> <td colspan="12">TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 8.315145D+01 WATER VAPOR(LBM)= 3.973348D+00</td> </tr> </tbody> </table> | | | | | | | | | | AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | 3 | 2.64347D+03 | 1.50364D+02 | 0. | 6.47074D+02 | 7.97437D+02 | 9.57134D-01 | -4.78039D-04 | 1.56668D-06 | 8.49123D-09 | | | COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.0906D+05 LBM/HR ENERGY BTU/HR = 3.9381D+07 (NORMAL= 3.9381D+07 PENETRATION= 0.) | | | | | | | | | | | STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.0938D-01 STEP AIR= 5.4979D+00 NET VAPOR= 3.9733D+00 NET AIR= 8.3151D+01 | | | | | | | | | | | | TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 8.315145D+01 WATER VAPOR(LBM)= 3.973348D+00 | | | | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 3 | 2.64347D+03 | 1.50364D+02 | 0. | 6.47074D+02 | 7.97437D+02 | 9.57134D-01 | -4.78039D-04 | 1.56668D-06 | 8.49123D-09 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.0906D+05 LBM/HR ENERGY BTU/HR = 3.9381D+07 (NORMAL= 3.9381D+07 PENETRATION= 0.) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.0938D-01 STEP AIR= 5.4979D+00 NET VAPOR= 3.9733D+00 NET AIR= 8.3151D+01 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 8.315145D+01 WATER VAPOR(LBM)= 3.973348D+00 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

***** TIME = 6.111111E-04 HR = 3.666667E-02 MIN = 2.200000E+00 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE DE/E | TRANSFER COEFFICIENTS | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|--|--|-----------------------------------|---------------------------|-----------------|-------------------|-------------|---------------------|------------------------|-------------|---|--|-----------------------------------|--|-----------------|--|----------|--|------------------------|--|---|--|---|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|--|--|-------|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|--|---|--|--|--|--|--|--|--|--|--|--|--|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | | MASS | HEAT | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 3 | 1.49610D+01 | 1.33980D+00 | 1.11722D+02 | 2.12582D+02 | 4.24463D+05 | 1.34318D+05 | 5.58781D+05 | 5.59934D-05 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <table border="1"> <thead> <tr> <th colspan="2">AIR MASS (LBM)</th> <th colspan="2">W A T E R VAPOR--ATMOS--LIQUID</th> <th colspan="2">M A S S POOL</th> <th colspan="2">HUMIDITY</th> <th colspan="2">CONDENSATION (LB/S)</th> <th colspan="2">TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R)</th> </tr> </thead> <tbody> <tr> <td>3</td> <td>2.62256D+03</td> <td>1.60704D+02</td> <td>5.79452D-02</td> <td>7.43290D+02</td> <td>9.03994D+02</td> <td>1.00000D+00</td> <td>5.78936D-01</td> <td>1.56280D-06</td> <td>9.86521D-09</td> <td></td> <td></td> </tr> <tr> <td>COMP.</td> <td colspan="11">3 LEAKAGE OUTFLOW- MASS= 2.0855D+05 LBM/HR ENERGY BTU/HR = 4.0129D+07 (NORMAL= 4.0129D+07 PENETRATION= 0.)</td> </tr> <tr> <td colspan="12">STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3149D-01 STEP AIR= 5.4615D+00 NET VAPOR= 5.2569D+00 NET AIR= 1.0489D+02</td> </tr> <tr> <td colspan="12">TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.048910D+02 WATER VAPOR(LBM)= 5.256856D+00</td> </tr> </tbody> </table> | | | | | | | | | | AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | 3 | 2.62256D+03 | 1.60704D+02 | 5.79452D-02 | 7.43290D+02 | 9.03994D+02 | 1.00000D+00 | 5.78936D-01 | 1.56280D-06 | 9.86521D-09 | | | COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.0855D+05 LBM/HR ENERGY BTU/HR = 4.0129D+07 (NORMAL= 4.0129D+07 PENETRATION= 0.) | | | | | | | | | | | STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3149D-01 STEP AIR= 5.4615D+00 NET VAPOR= 5.2569D+00 NET AIR= 1.0489D+02 | | | | | | | | | | | | TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.048910D+02 WATER VAPOR(LBM)= 5.256856D+00 | | | | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S POOL | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 3 | 2.62256D+03 | 1.60704D+02 | 5.79452D-02 | 7.43290D+02 | 9.03994D+02 | 1.00000D+00 | 5.78936D-01 | 1.56280D-06 | 9.86521D-09 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 2.0855D+05 LBM/HR ENERGY BTU/HR = 4.0129D+07 (NORMAL= 4.0129D+07 PENETRATION= 0.) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3149D-01 STEP AIR= 5.4615D+00 NET VAPOR= 5.2569D+00 NET AIR= 1.0489D+02 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.048910D+02 WATER VAPOR(LBM)= 5.256856D+00 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

***** TIME = 7.222222E-04 HR = 4.333333E-02 MIN = 2.600000E+00 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE DE/E |
|--|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.49783D+01 | 1.42152D+00 | 1.13792D+02 | 2.12453D+02 | 4.33058D+05 | 1.51775D+05 | 5.84833D+05 | 1.25621D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 2.60073D+03 1.69901D+02 4.21223D-01 8.40499D+02 1.01040D+03 1.00000D+00 4.21154D+00 1.55463D-06 1.67093D-08 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 2.2171D+05 LBM/HR ENERGY BTU/HR = 4.3553D+07 (NORMAL= 4.3553D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7470D-01 STEP AIR= 5.7838D+00 NET VAPOR= 6.6909D+00 NET AIR= 1.2755D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.275540D+02 WATER VAPOR(LBM)= 6.690850D+00 | | | | | | | | |

***** TIME = 8.33333E-04 HR = 5.00000E-02 MIN = 3.00000E+00 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE DE/E |
|--|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.49870D+01 | 1.50229D+00 | 1.15740D+02 | 2.12359D+02 | 4.41187D+05 | 1.69238D+05 | 6.10425D+05 | 2.18261D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 2.57815D+03 1.78968D+02 6.27093D-02 9.37697D+02 1.11666D+03 1.00000D+00 6.26320D-01 1.54767D-06 2.14494D-08 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 2.2584D+05 LBM/HR ENERGY BTU/HR = 4.5248D+07 (NORMAL= 4.5248D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.0376D-01 STEP AIR= 5.8695D+00 NET VAPOR= 8.2657D+00 NET AIR= 1.5096D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.509581D+02 WATER VAPOR(LBM)= 8.265747D+00 | | | | | | | | |

***** TIME = 9.44444E-04 HR = 5.66667E-02 MIN = 3.40000E+00 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE DE/E |
|--|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.49898D+01 | 1.58045D+00 | 1.17594D+02 | 2.12265D+02 | 4.48964D+05 | 1.86725D+05 | 6.35689D+05 | 3.04292D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 2.55551D+03 1.87701D+02 0. 1.03513D+03 1.22283D+03 9.98517D-01 -8.34360D-04 1.54127D-06 2.56304D-08 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 2.2540D+05 LBM/HR ENERGY BTU/HR = 4.6028D+07 (NORMAL= 4.6028D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.2482D-01 STEP AIR= 5.8363D+00 NET VAPOR= 9.9392D+00 NET AIR= 1.7443D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.744291D+02 WATER VAPOR(LBM)= 9.939176D+00 | | | | | | | | |

***** TIME = 1.05556E-03 HR = 6.33333E-02 MIN = 3.80000E+00 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE DE/E |
|--|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.49886D+01 | 1.65629D+00 | 1.19339D+02 | 2.12172D+02 | 4.56474D+05 | 2.04233D+05 | 6.60707D+05 | 3.81231D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 2.53317D+03 1.96150D+02 0. 1.13278D+03 1.32893D+03 9.96627D-01 -8.80409D-04 1.53525D-06 2.94341D-08 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 2.2187D+05 LBM/HR ENERGY BTU/HR = 4.6145D+07 (NORMAL= 4.6145D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.3938D-01 STEP AIR= 5.7237D+00 NET VAPOR= 1.1683D+01 NET AIR= 1.9760D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.975971D+02 WATER VAPOR(LBM)= 1.168329D+01 | | | | | | | | |

***** TIME = 1.11111E-03 HR = 6.66667E-02 MIN = 4.00000E+00 SEC *****

HEAT STRUCTURE 1 BETWEEN COMPARTMENTS 3 AND 0 1.5 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -6.271143D+06 -1.706450D+02 -2.280258D+03 OLIVID 0. 0. 0.
LEFT FILM COEF. H = 1.198433E+02 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.199592E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.100580D+02 1.073080D+02 1.046702D+02 1.040019D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 2 BETWEEN COMPARTMENTS 3 AND 0 2 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -4.039162D+06 -1.099102D+02 -1.468684D+03 OLIVID 0. 0. 0.
LEFT FILM COEF. H = 1.198433E+02 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.199592E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.100580D+02 1.073080D+02 1.046702D+02 1.040019D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 3 BETWEEN COMPARTMENTS 3 AND 0 3 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -4.331064D+05 -1.178532D+01 -1.574823D+02 OLIVID 0. 0. 0.
LEFT FILM COEF. H = 1.198433E+02 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.199592E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.100580D+02 1.073080D+02 1.046702D+02 1.040019D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 4 BETWEEN COMPARTMENTS 3 AND 0 3.5 FT CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -6.455065D+05 -1.756497D+01 -2.347134D+02 OLIVID 0. 0. 0.
LEFT FILM COEF. H = 1.198433E+02 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.199592E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.100580D+02 1.073080D+02 1.046702D+02 1.040019D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 5 BETWEEN COMPARTMENTS 3 AND 0 4 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -4.176807D+05 -1.136557D+01 -1.518734D+02 OLIVID 0. 0. 0.
LEFT FILM COEF. H = 1.198433E+02 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.199592E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.100580D+02 1.073080D+02 1.046702D+02 1.040019D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 6 BETWEEN COMPARTMENTS 3 AND 0 4.5 FT THICK CONCRETE FLOOR

TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU

3 LIQUID -9.509994D+04 -2.641945D+00 -1.046455D+02 0. 0. 0.
LEFT FILM COEF. H = 4.000000E-01 BTU/HR.FT2.F FIRST MESH K = 5.500000E-01 BTU/HR.FT. BULK TEMP = 2.121068E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.040387D+02 | 1.040001D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

SUMMARY OF HEAT TRANSFER TO COMPARTMENTS BY HEAT STRUCTURES - UNITS ARE BTU

| COMP. | STEP-LIQUID | STEP-VAPOR | NET-LIQUID | NET-VAPOR |
|-------|---------------|---------------|---------------|---------------|
| 0 | 0. | 0. | 0. | 0. |
| 1 | 0. | 0. | 0. | 0. |
| 2 | 0. | 0. | 0. | 0. |
| 3 | -2.641945D+00 | -3.212711D+02 | -1.046455D+02 | -4.293011D+03 |
| 4 | 0. | 0. | 0. | 0. |

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|------------------------|-------------------------|---------------------------|-------------|-------------------|---------------------|--------------|-------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.49870D+01 | 1.69359D+00 | 1.20166D+02 | 2.12128D+02 | 4.60147D+05 | 2.12993D+05 | 6.73140D+05 | 4.16766D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | | W A T E R M A S S (LBM) | | HUMIDITY | | CONDENSATION (LB/S) | | MASS HEAT (BTU/S FT2 R) |
| 3 | 2.52218D+03 | 2.00299D+02 | 0. | 1.18166D+03 | 1.38196D+03 | 9.95890D-01 | -8.99639D-04 | 1.53236D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 2.1951D+05 LBM/HR ENERGY BTU/HR = 4.6063D+07 (NORMAL= 4.6063D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.4509D-01 STEP AIR= 5.6524D+00 NET VAPOR= 1.2576D+01 NET AIR= 2.0900D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.089986D+02 WATER VAPOR(LBM)= 1.257557D+01 | | | | | | | | |

***** TIME = 1.666667E-03 HR = 1.000000E-01 MIN = 6.000000E+00 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|------------------------|-------------------------|---------------------------|-------------|-------------------|---------------------|-------------|-------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.48252D+01 | 1.84212D+00 | 1.23062D+02 | 2.11846D+02 | 4.72082D+05 | 2.22831D+05 | 6.94912D+05 | 2.34998D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | | W A T E R M A S S (LBM) | | HUMIDITY | | CONDENSATION (LB/S) | | MASS HEAT (BTU/S FT2 R) |
| 3 | 2.45104D+03 | 2.16855D+02 | 1.38743D-01 | 1.23818D+03 | 1.45504D+03 | 1.00000D+00 | 6.92982D-01 | 1.51288D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 9.7928D+04 LBM/HR ENERGY BTU/HR = 2.1382D+07 (NORMAL= 2.1382D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.4010D-01 STEP AIR= 5.0003D+00 NET VAPOR= 1.8892D+01 NET AIR= 2.8428D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.842785D+02 WATER VAPOR(LBM)= 1.889163D+01 | | | | | | | | |

***** TIME = 2.222222E-03 HR = 1.333333E-01 MIN = 8.000000E+00 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|----------|------------------------|-------------|---------------------------|-------------|-------------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.48061D+01 | 1.97667D+00 | 1.25643D+02 | 2.11655D+02 | 4.85003D+05 | 2.29117D+05 | 7.14120D+05 | 1.50792D-04 |

| W A T E R M A S S (L B M) | | | | | | HUMIDITY | CONDENSATION | TRANSFER COEFFICIENTS | |
|--|--|----------------------|-------------|-------------|-------------|-------------|--------------|------------------------------|----------------------------|
| AIR MASS (L B M) | | VAPOR--ATMOS--LIQUID | | POOL TOTAL | | (L B / S) | (L B / S) | MASS (L B M O L / S F T 2) | HEAT (B T U / S F T 2 R) |
| 3 | 2.41136D+03 | 2.31721D+02 | 1.57793D-01 | 1.27448D+03 | 1.50620D+03 | 1.00000D+00 | 7.88145D-01 | 1.50167D-06 | 2.90304D-08 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 8.1118D+04 LBM/HR ENERGY BTU/HR = 1.8272D+07 (NORMAL= 1.8272D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.9339D-01 STEP AIR= 4.1132D+00 NET VAPOR= 2.2928D+01 NET AIR= 3.2810D+02 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 3.281038D+02 WATER VAPOR(LBM)= 2.292824D+01 | | | | | | | | | |

***** TIME = 2.777778E-03 HR = 1.666667E-01 MIN = 1.000000E+01 SEC *****

| COMP NO. | P R E S S U R E (P S I A) | | T E M P E R A T U R E (F) | | E N E R G Y (B T U) | | CONVERGENCE | | |
|--|--|-----------------------------|-----------------------------|-------------|-----------------------|--------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E | |
| 3 | 1.48028D+01 | 2.11178D+00 | 1.28087D+02 | 2.11474D+02 | 4.98204D+05 | 2.35413D+05 | 7.33618D+05 | | 1.59095D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (L B M) | | W A T E R M A S S (L B M) | | HUMIDITY | | CONDENSATION | | MASS HEAT | |
| | | VAPOR--ATMOS--LIQUID | | POOL TOTAL | | (L B / S) | | (L B M O L / S F T 2) (B T U / S F T 2 R) | |
| 3 | 2.37543D+03 | 2.46567D+02 | 1.29530D-01 | 1.31083D+03 | 1.55740D+03 | 1.00000D+00 | 6.46738D-01 | 1.49195D-06 | 3.71473D-08 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 7.7878D+04 LBM/HR ENERGY BTU/HR = 1.8075D+07 (NORMAL= 1.8075D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.0523D-01 STEP AIR= 3.9213D+00 NET VAPOR= 2.6929D+01 NET AIR= 3.6818D+02 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 3.681753D+02 WATER VAPOR(LBM)= 2.692947D+01 | | | | | | | | | |

***** TIME = 3.333333E-03 HR = 2.000000E-01 MIN = 1.200000E+01 SEC *****

| COMP NO. | P R E S S U R E (P S I A) | | T E M P E R A T U R E (F) | | E N E R G Y (B T U) | | CONVERGENCE | | |
|--|--|-----------------------------|-----------------------------|-------------|-----------------------|--------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E | |
| 3 | 1.48008D+01 | 2.24500D+00 | 1.30370D+02 | 2.11299D+02 | 5.11178D+05 | 2.41729D+05 | 7.52907D+05 | | 1.63211D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (L B M) | | W A T E R M A S S (L B M) | | HUMIDITY | | CONDENSATION | | MASS HEAT | |
| | | VAPOR--ATMOS--LIQUID | | POOL TOTAL | | (L B / S) | | (L B M O L / S F T 2) (B T U / S F T 2 R) | |
| 3 | 2.34103D+03 | 2.61131D+02 | 8.76849D-02 | 1.34732D+03 | 1.60846D+03 | 1.00000D+00 | 4.37432D-01 | 1.48312D-06 | 4.57623D-08 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 7.5857D+04 LBM/HR ENERGY BTU/HR = 1.8119D+07 (NORMAL= 1.8119D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.2133D-01 STEP AIR= 3.7930D+00 NET VAPOR= 3.1076D+01 NET AIR= 4.0672D+02 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.067174D+02 WATER VAPOR(LBM)= 3.107573D+01 | | | | | | | | | |

***** TIME = 3.888889E-03 HR = 2.333333E-01 MIN = 1.400000E+01 SEC *****

| COMP NO. | P R E S S U R E (P S I A) | | T E M P E R A T U R E (F) | | E N E R G Y (B T U) | | CONVERGENCE | | |
|--|--|-----------------------------|-----------------------------|-------------|-----------------------|--------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E | |
| 3 | 1.47992D+01 | 2.37610D+00 | 1.32505D+02 | 2.11128D+02 | 5.23902D+05 | 2.48063D+05 | 7.71965D+05 | | 1.89863D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (L B M) | | W A T E R M A S S (L B M) | | HUMIDITY | | CONDENSATION | | MASS HEAT | |
| | | VAPOR--ATMOS--LIQUID | | POOL TOTAL | | (L B / S) | | (L B M O L / S F T 2) (B T U / S F T 2 R) | |
| 3 | 2.30793D+03 | 2.75407D+02 | 7.33644D-02 | 1.38395D+03 | 1.65936D+03 | 1.00000D+00 | 3.65760D-01 | 1.47500D-06 | 5.49000D-08 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 7.3884D+04 LBM/HR ENERGY BTU/HR = 1.8139D+07 (NORMAL= 1.8139D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.3603D-01 STEP AIR= 3.6686D+00 NET VAPOR= 3.5371D+01 NET AIR= 4.4396D+02 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.439616D+02 WATER VAPOR(LBM)= 3.537124D+01 | | | | | | | | | |

***** TIME = 4.444444E-03 HR = 2.666667E-01 MIN = 1.600000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------------------------|--------------------------|---------------------|-----------------------|------------------------|------------------------|-----------------------|
| 3 | 1.47966D+01 | 2.50423D+00 | 1.34498D+02 | 2.10959D+02 | 5.36368D+05 | 2.54425D+05 | 7.90793D+05 | 3.24086D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MAS S POOL | (LBM) TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 2.27599D+03 | 2.89324D+02 | 3.06569D-01 | 1.42079D+03 | 1.71012D+03 | 1.00000D+00 | 1.53172D+00 | 1.46742D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 7.2291D+04 LBM/HR | ENERGY BTU/HR = | 1.8223D+07 (NORMAL= | 1.8223D+07 | PENETRATION= | O. |) |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.5141D-01 STEP AIR= 3.5648D+00 NET VAPOR= 3.9814D+01 NET AIR= 4.8004D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.800443D+02 WATER VAPOR(LBM)= 3.981377D+01 | | | | | | | | |

***** TIME = 5.000000E-03 HR = 3.000000E-01 MIN = 1.800000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------------------------|--------------------------|---------------------|-----------------------|------------------------|------------------------|-----------------------|
| 3 | 1.48000D+01 | 2.63268D+00 | 1.36550D+02 | 2.10806D+02 | 5.48603D+05 | 2.60784D+05 | 8.09387D+05 | 3.62288D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MAS S POOL | (LBM) TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 2.24508D+03 | 3.03167D+02 | O. | 1.45756D+03 | 1.76073D+03 | 9.96313D-01 | -1.17356D-03 | 1.46024D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 6.8947D+04 LBM/HR | ENERGY BTU/HR = | 1.7827D+07 (NORMAL= | 1.7827D+07 | PENETRATION= | O. |) |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.5407D-01 STEP AIR= 3.3763D+00 NET VAPOR= 4.4403D+01 NET AIR= 5.1509D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 5.150936D+02 WATER VAPOR(LBM)= 4.440301D+01 | | | | | | | | |

***** TIME = 5.555556E-03 HR = 3.333333E-01 MIN = 2.000000E+01 SEC *****

HEAT STRUCTURE 1 BETWEEN COMPARTMENTS 3 AND 0 1.5 FT THICK CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---|-----------------|---------------|---------------|----------------|-----------------|--------------|---------------|
| 3 VAPOR | -2.590884D+06 | -1.434833D+02 | -1.046325D+04 | OLIQUID | O. | O. | O. |
| LEFT FILM COEF. H = 1.698514E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.381495E+02 F | | | | | | | |
| RIGHT FILM COEF. H = O. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F | | | | | | | |
| MESH POINT TEMPERATURES (F), LEFT TO RIGHT | | | | | | | |
| 1.092871D+02 | 1.081256D+02 | 1.069837D+02 | 1.040797D+02 | 1.040015D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 2 BETWEEN COMPARTMENTS 3 AND 0 2 FT THICK CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---|-----------------|---------------|---------------|----------------|-----------------|--------------|---------------|
| 3 VAPOR | -1.668755D+06 | -9.241574D+01 | -6.739241D+03 | OLIQUID | O. | O. | O. |
| LEFT FILM COEF. H = 1.698514E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.381495E+02 F | | | | | | | |
| RIGHT FILM COEF. H = O. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F | | | | | | | |
| MESH POINT TEMPERATURES (F), LEFT TO RIGHT | | | | | | | |
| 1.092871D+02 | 1.081256D+02 | 1.069837D+02 | 1.040797D+02 | 1.040015D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 3 BETWEEN COMPARTMENTS 3 AND 0 3 FT THICK CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---|-----------------|---------------|---------------|----------------|-----------------|----------|---------------|
| 3 VAPOR | -1.789352D+05 | -9.909444D+00 | -7.226272D+02 | OLIQUID | O. | O. | O. |
| LEFT FILM COEF. H = 1.698514E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.381495E+02 F | | | | | | | |
| RIGHT FILM COEF. H = O. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F | | | | | | | |

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.092871D+02 | 1.081256D+02 | 1.069837D+02 | 1.040797D+02 | 1.040015D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 4 BETWEEN COMPARTMENTS 3 AND 0 3.5 FT CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|---------------|---------------|----------------|-----------------|----------|---------------|
| 3 VAPOR | -2.666870D+05 | -1.476914D+01 | -1.077012D+03 | OLIQUID | 0. | 0. | 0. |

LEFT FILM COEF. $h = 1.698514E+01$ BTU/HR.FT².F FIRST MESH $K = 2.100000E-01$ BTU/HR.FT. BULK TEMP = $1.381495E+02$ F
RIGHT FILM COEF. $h = 0.$ BTU/HR.FT².F LAST MESH $K = 5.500000E-01$ BTU/HR.FT.F BULK TEMP = $1.040000D+02$ F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.092871D+02 | 1.081256D+02 | 1.069837D+02 | 1.040797D+02 | 1.040015D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 5 BETWEEN COMPARTMENTS 3 AND 0 4 FT THICK CONCRETE WALLS

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|---------------|---------------|----------------|-----------------|----------|---------------|
| 3 VAPOR | -1.725622D+05 | -9.556505D+00 | -6.968898D+02 | OLIQUID | 0. | 0. | 0. |

LEFT FILM COEF. $h = 1.698514E+01$ BTU/HR.FT².F FIRST MESH $K = 2.100000E-01$ BTU/HR.FT. BULK TEMP = $1.381495E+02$ F
RIGHT FILM COEF. $h = 0.$ BTU/HR.FT².F LAST MESH $K = 5.500000E-01$ BTU/HR.FT.F BULK TEMP = $1.040000D+02$ F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.092871D+02 | 1.081256D+02 | 1.069837D+02 | 1.040797D+02 | 1.040015D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

HEAT STRUCTURE 6 BETWEEN COMPARTMENTS 3 AND 0 4.5 FT THICK CONCRETE FLOOR

| TO LEFT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU | TO RIGHT COMP. | END STEP BTU/HR | STEP BTU | TOTAL NET BTU |
|---------------|-----------------|---------------|---------------|----------------|-----------------|----------|---------------|
| 3 LIQUID | -9.367478D+04 | -5.204573D+00 | -5.239121D+02 | OLIQUID | 0. | 0. | 0. |

LEFT FILM COEF. $h = 4.000000E-01$ BTU/HR.FT².F FIRST MESH $K = 5.500000E-01$ BTU/HR.FT. BULK TEMP = $2.106402E+02$ F
RIGHT FILM COEF. $h = 0.$ BTU/HR.FT².F LAST MESH $K = 5.500000E-01$ BTU/HR.FT.F BULK TEMP = $1.040000D+02$ F

MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.041915D+02 | 1.040014D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

SUMMARY OF HEAT TRANSFER TO COMPARTMENTS BY HEAT STRUCTURES - UNITS ARE BTU

| COMP. | STEP-LIQUID | STEP-VAPOR | NET-LIQUID | NET-VAPOR |
|-------|---------------|---------------|---------------|---------------|
| 0 | 0. | 0. | 0. | 0. |
| 1 | 0. | 0. | 0. | 0. |
| 2 | 0. | 0. | 0. | 0. |
| 3 | -5.204573D+00 | -2.701341D+02 | -5.239121D+02 | -1.969902D+04 |
| 4 | 0. | 0. | 0. | 0. |

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|----------|------------------------|-------------|---------------------------|-------------|-------------------|-------------|-------------|------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47934D+01 | 2.75575D+00 | 1.38168D+02 | 2.10648D+02 | 5.60575D+05 | 2.67185D+05 | 8.27761D+05 | 3.38930D-04 |

TRANSFER COEFFICIENTS

| AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS POOL | (LBM) TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
|--|-------------------------------|-------------------|-----------------|---------------------|------------------------|------------------------|-----------------------|
| 3 | 2.21515D+03 | 3.16532D+02 | 2.43737D-01 | 1.49467D+03 | 1.81120D+03 | 1.00000D+00 | 1.21747D+00 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 6.9413D+04 LBM/HR | ENERGY BTU/HR = | 1.8395D+07 (NORMAL= | 1.8395D+07 | PENETRATION= | 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 4.8066D-01 STEP AIR= 3.3756D+00 NET VAPOR= 4.9132D+01 NET AIR= 5.4916D+02 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 5.491634D+02 WATER VAPOR(LBM)= 4.913218D+01 | | | | | | | |

***** TIME = 6.666667E-03 HR = 4.000000E-01 MIN = 2.400000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|-------------------------------|--------------------------|-----------------|---------------------|------------------------|------------------------|-----------------------|---------------------|
| 3 | 1.48008D+01 | 3.00107D+00 | 1.41774D+02 | 2.10355D+02 | 5.83892D+05 | 2.80025D+05 | 8.63917D+05 | 6.58724D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS POOL | (LBM) TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) | |
| 3 | 2.15835D+03 | 3.42722D+02 | 0. | 1.56908D+03 | 1.91181D+03 | 9.92439D-01 | -1.30135D-03 | 1.44120D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 6.8343D+04 LBM/HR | ENERGY BTU/HR = | 1.8940D+07 (NORMAL= | 1.8940D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.0338D+00 STEP AIR= 6.5599D+00 NET VAPOR= 5.8924D+01 NET AIR= 6.1425D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 6.142490D+02 WATER VAPOR(LBM)= 5.892398D+01 | | | | | | | | |

***** TIME = 7.777778E-03 HR = 4.666667E-01 MIN = 2.800000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|-------------------------------|--------------------------|-----------------|---------------------|------------------------|------------------------|-----------------------|---------------------|
| 3 | 1.47933D+01 | 3.23202D+00 | 1.44641D+02 | 2.10063D+02 | 6.06098D+05 | 2.92988D+05 | 8.99086D+05 | 5.96031D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS POOL | (LBM) TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) | |
| 3 | 2.10469D+03 | 3.67485D+02 | 0. | 1.64442D+03 | 2.01190D+03 | 9.93832D-01 | -1.36506D-03 | 1.42974D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 7.0291D+04 LBM/HR | ENERGY BTU/HR = | 2.0342D+07 (NORMAL= | 2.0342D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.1543D+00 STEP AIR= 6.6558D+00 NET VAPOR= 6.9226D+01 NET AIR= 6.7619D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 6.761946D+02 WATER VAPOR(LBM)= 6.922590D+01 | | | | | | | | |

***** TIME = 8.888889E-03 HR = 5.333333E-01 MIN = 3.200000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|-------------------------------|--------------------------|-----------------|---------------------|------------------------|------------------------|-----------------------|---------------------|
| 3 | 1.47973D+01 | 3.45938D+00 | 1.47470D+02 | 2.09799D+02 | 6.27582D+05 | 3.06002D+05 | 9.33584D+05 | 7.49545D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS POOL | (LBM) TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) | |
| 3 | 2.05442D+03 | 3.91610D+02 | 0. | 1.72003D+03 | 2.11164D+03 | 9.90725D-01 | -1.41834D-03 | 1.41922D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 6.4344D+04 LBM/HR | ENERGY BTU/HR = | 1.9383D+07 (NORMAL= | 1.9383D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.1383D+00 STEP AIR= 6.0110D+00 NET VAPOR= 7.9893D+01 NET AIR= 7.3475D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 7.347461D+02 WATER VAPOR(LBM)= 7.989312D+01 | | | | | | | | |

***** TIME = 1.000000E-02 HR = 6.000000E-01 MIN = 3.600000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|------------------------|--------------------------------|--|-----------------|-------------------|-------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47978D+01 | 3.67750D+00 | 1.50009D+02 | 2.09547D+02 | 6.48165D+05 | 3.19109D+05 | 9.67273D+05 | 1.40430D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 2.00659D+03 | 4.14663D+02 | 0. | 1.79626D+03 | 2.21092D+03 | 9.88706D-01 | -1.45574D-03 | 1.40851D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- | MASS= 5.7684D+04 LBM/HR | ENERGY BTU/HR = 1.8043D+07 (NORMAL= 1.8043D+07 | PENETRATION= 0. | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.0918D+00 STEP AIR= 5.3176D+00 NET VAPOR= 9.1009D+01 NET AIR= 7.9086D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 7.90855D+02 WATER VAPOR(LBM)= 9.10092D+01 | | | | | | | | |

***** TIME = 1.11111E-02 HR = 6.66667E-01 MIN = 4.00000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|------------------------|--------------------------------|--|-----------------|-------------------|-------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47934D+01 | 3.88600D+00 | 1.52226D+02 | 2.09307D+02 | 6.67861D+05 | 3.32309D+05 | 1.00017D+06 | 8.44536D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 1.96105D+03 | 4.36682D+02 | 0. | 1.87311D+03 | 2.30979D+03 | 9.89200D-01 | -1.49511D-03 | 1.39943D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- | MASS= 6.2596D+04 LBM/HR | ENERGY BTU/HR = 2.0291D+07 (NORMAL= 2.0291D+07 | PENETRATION= 0. | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.2606D+00 STEP AIR= 5.6946D+00 NET VAPOR= 1.0254D+02 NET AIR= 8.4468D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 8.446833D+02 WATER VAPOR(LBM)= 1.025364D+02 | | | | | | | | |

***** TIME = 1.22222E-02 HR = 7.33333E-01 MIN = 4.40000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|------------------------|--------------------------------|--|-----------------|-------------------|-------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47956D+01 | 4.09000D+00 | 1.54357D+02 | 2.09087D+02 | 6.86984D+05 | 3.45566D+05 | 1.03255D+06 | 1.28777D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 1.91809D+03 | 4.58127D+02 | 0. | 1.95027D+03 | 2.40840D+03 | 9.88234D-01 | -1.52161D-03 | 1.38991D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- | MASS= 5.5975D+04 LBM/HR | ENERGY BTU/HR = 1.8756D+07 (NORMAL= 1.8756D+07 | PENETRATION= 0. | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.1933D+00 STEP AIR= 5.0261D+00 NET VAPOR= 1.1433D+02 NET AIR= 8.9593D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 8.959279D+02 WATER VAPOR(LBM)= 1.143317D+02 | | | | | | | | |

***** TIME = 1.33333E-02 HR = 8.00000E-01 MIN = 4.80000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|------------------------|--------------------------------|--|-----------------|-------------------|-------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47930D+01 | 4.28567D+00 | 1.56215D+02 | 2.08881D+02 | 7.05334D+05 | 3.58898D+05 | 1.06423D+06 | 1.25405D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 1.87688D+03 | 4.78722D+02 | 0. | 2.02789D+03 | 2.50661D+03 | 9.89852D-01 | -1.54519D-03 | 1.38097D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- | MASS= 5.4518D+04 LBM/HR | ENERGY BTU/HR = 1.8855D+07 (NORMAL= 1.8855D+07 | PENETRATION= 0. | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.2256D+00 STEP AIR= 4.8319D+00 NET VAPOR= 1.2652D+02 NET AIR= 9.4542D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 9.454203D+02 WATER VAPOR(LBM)= 1.265216D+02 | | | | | | | | |

***** TIME = 1.44444E-02 HR = 8.66667E-01 MIN = 5.20000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|------------------------|--------------------------------|---------------------------|--------------------|-------------------|----------------|--------------|---------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47901D+01 | 4.47371D+00 | 1.57970D+02 | 2.08684D+02 | 7.22966D+05 | 3.72320D+05 | 1.09529D+06 | 1.25005D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | | HUMIDITY TOTAL | | CONDENSATION (LB/S) |
| 3 | 1.83753D+03 | 4.98431D+02 | 0. | 2.10608D+03 | 2.60451D+03 | 9.90477D-01 | -1.56390D-03 | 1.37223D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 5.3805D+04 LBM/HR ENERGY BTU/HR = 1.9173D+07 (NORMAL= 1.9173D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.2705D+00 STEP AIR= 4.7079D+00 NET VAPOR= 1.3902D+02 NET AIR= 9.9305D+02 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 9.930468D+02 WATER VAPOR(LBM)= 1.390214D+02 | | | | | | | | |

***** TIME = 1.555556E-02 HR = 9.333333E-01 MIN = 5.600000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|------------------------|--------------------------------|---------------------------|--------------------|-------------------|----------------|--------------|---------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47907D+01 | 4.65611D+00 | 1.59739D+02 | 2.08498D+02 | 7.39969D+05 | 3.85821D+05 | 1.12579D+06 | 1.45147D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | | HUMIDITY TOTAL | | CONDENSATION (LB/S) |
| 3 | 1.80000D+03 | 5.17386D+02 | 0. | 2.18476D+03 | 2.70214D+03 | 9.88082D-01 | -1.57756D-03 | 1.36354D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 5.0740D+04 LBM/HR ENERGY BTU/HR = 1.8596D+07 (NORMAL= 1.8596D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.2538D+00 STEP AIR= 4.3841D+00 NET VAPOR= 1.5179D+02 NET AIR= 1.0389D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.038861D+03 WATER VAPOR(LBM)= 1.517874D+02 | | | | | | | | |

***** TIME = 1.666667E-02 HR = 1.000000E+00 MIN = 6.000000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|------------------------|--------------------------------|---------------------------|--------------------|-------------------|----------------|--------------|---------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47952D+01 | 4.83365D+00 | 1.61581D+02 | 2.08324D+02 | 7.56370D+05 | 3.99394D+05 | 1.15576D+06 | 1.54209D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | | HUMIDITY TOTAL | | CONDENSATION (LB/S) |
| 3 | 1.76401D+03 | 5.35620D+02 | 0. | 2.26387D+03 | 2.79949D+03 | 9.81714D-01 | -1.58862D-03 | 1.35511D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 5.1457D+04 LBM/HR ENERGY BTU/HR = 1.9372D+07 (NORMAL= 1.9372D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.3267D+00 STEP AIR= 4.3907D+00 NET VAPOR= 1.6484D+02 NET AIR= 1.0831D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.083133D+03 WATER VAPOR(LBM)= 1.648445D+02 | | | | | | | | |

***** TIME = 1.777778E-02 HR = 1.066667E+00 MIN = 6.400000E+01 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|------------------------|--------------------------------|---------------------------|--------------------|-------------------|----------------|--------------|---------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47908D+01 | 5.00502D+00 | 1.62761D+02 | 2.08170D+02 | 7.72381D+05 | 4.12981D+05 | 1.18536D+06 | 1.43220D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) | | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | | HUMIDITY TOTAL | | CONDENSATION (LB/S) |
| 3 | 1.72960D+03 | 5.53662D+02 | 0. | 2.34294D+03 | 2.89660D+03 | 9.88559D-01 | -1.59848D-03 | 1.34718D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.9512D+04 LBM/HR ENERGY BTU/HR = 1.9122D+07 (NORMAL= 1.9122D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.3291D+00 STEP AIR= 4.1723D+00 NET VAPOR= 1.7813D+02 NET AIR= 1.1258D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.125829D+03 WATER VAPOR(LBM)= 1.781275D+02 | | | | | | | | |

***** TIME = 1.888889E-02 HR = 1.133333E+00 MIN = 6.800000E+01 SEC *****

COMP NO. 3
PRESSURE (PSIA) TOTAL 1.47934D+01 STEAM 5.17134D+00 ATMOS 1.64438D+02 POOL 2.08019D+02
TEMPERATURE (F) ATMOS 7.87664D+05 POOL 4.26676D+05
ENERGY (BTU) TOTAL 1.21434D+06
CONVERGENCE DE/E 1.46283D-03
TRANSFER COEFFICIENTS
AIR MASS (LBM) 1.69610D+03 WATER VAPOR--ATMOS--LIQUID POOL 2.42272D+03 TOTAL 2.99332D+03 HUMIDITY 9.81839D-01 CONDENSATION (LB/S) -1.60381D-03 MASS (LB MOL/S FT2) 1.33889D-06 HEAT (BTU/S FT2 R) 4.38063D-07
COMP. 3 LEAKAGE OUTFLOW- MASS= 4.9635D+04 LBM/HR ENERGY BTU/HR = 1.9644D+07 (NORMAL= 1.9644D+07 PENETRATION= 0.)
STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.3836D+00 STEP AIR= 4.1314D+00 NET VAPOR= 1.9181D+02 NET AIR= 1.1676D+03
TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.167611D+03 WATER VAPOR(LBM)= 1.918134D+02

***** TIME = 2.000000E-02 HR = 1.200000E+00 MIN = 7.200000E+01 SEC *****

COMP NO. 3
PRESSURE (PSIA) TOTAL 1.47876D+01 STEAM 5.33136D+00 ATMOS 1.65456D+02 POOL 2.07885D+02
TEMPERATURE (F) ATMOS 8.02570D+05 POOL 4.40387D+05
ENERGY (BTU) TOTAL 1.24296D+06
CONVERGENCE DE/E 1.35270D-03
TRANSFER COEFFICIENTS
AIR MASS (LBM) 1.66416D+03 WATER VAPOR--ATMOS--LIQUID POOL 2.50250D+03 TOTAL 3.08988D+03 HUMIDITY 9.88416D-01 CONDENSATION (LB/S) -1.60866D-03 MASS (LB MOL/S FT2) 1.33113D-06 HEAT (BTU/S FT2 R) 4.71550D-07
COMP. 3 LEAKAGE OUTFLOW- MASS= 4.8014D+04 LBM/HR ENERGY BTU/HR = 1.9450D+07 (NORMAL= 1.9450D+07 PENETRATION= 0.)
STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.3873D+00 STEP AIR= 3.9477D+00 NET VAPOR= 2.0565D+02 NET AIR= 1.2078D+03
TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.207836D+03 WATER VAPOR(LBM)= 2.056464D+02

***** TIME = 2.111111E-02 HR = 1.266667E+00 MIN = 7.600000E+01 SEC *****

COMP NO. 3
PRESSURE (PSIA) TOTAL 1.47903D+01 STEAM 5.48874D+00 ATMOS 1.66692D+02 POOL 2.07757D+02
TEMPERATURE (F) ATMOS 8.17033D+05 POOL 4.54172D+05
ENERGY (BTU) TOTAL 1.27121D+06
CONVERGENCE DE/E 1.57195D-03
TRANSFER COEFFICIENTS
AIR MASS (LBM) 1.63371D+03 WATER VAPOR--ATMOS--LIQUID POOL 2.58272D+03 TOTAL 3.18633D+03 HUMIDITY 9.88670D-01 CONDENSATION (LB/S) -1.61065D-03 MASS (LB MOL/S FT2) 1.32331D-06 HEAT (BTU/S FT2 R) 5.02807D-07
COMP. 3 LEAKAGE OUTFLOW- MASS= 4.7343D+04 LBM/HR ENERGY BTU/HR = 1.9607D+07 (NORMAL= 1.9607D+07 PENETRATION= 0.)
STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.4144D+00 STEP AIR= 3.8459D+00 NET VAPOR= 2.1960D+02 NET AIR= 1.2466D+03
TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.246567D+03 WATER VAPOR(LBM)= 2.196038D+02

***** TIME = 2.222222E-02 HR = 1.333333E+00 MIN = 8.000000E+01 SEC *****

COMP NO. 3
PRESSURE (PSIA) TOTAL 1.47889D+01 STEAM 5.63718D+00 ATMOS 1.68148D+02 POOL 2.07630D+02
TEMPERATURE (F) ATMOS 8.30478D+05 POOL 4.68078D+05
ENERGY (BTU) TOTAL 1.29856D+06
CONVERGENCE DE/E 1.40559D-03
TRANSFER COEFFICIENTS
AIR MASS (LBM) 1.60365D+03 WATER VAPOR--ATMOS--LIQUID POOL 2.66372D+03 TOTAL 3.28228D+03 HUMIDITY 9.81593D-01 CONDENSATION (LB/S) -1.61114D-03 MASS (LB MOL/S FT2) 1.31547D-06 HEAT (BTU/S FT2 R) 5.34408D-07
COMP. 3 LEAKAGE OUTFLOW- MASS= 4.6727D+04 LBM/HR ENERGY BTU/HR = 1.9768D+07 (NORMAL= 1.9768D+07 PENETRATION= 0.)
STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.4411D+00 STEP AIR= 3.7508D+00 NET VAPOR= 2.3405D+02 NET AIR= 1.2849D+03
TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.284913D+03 WATER VAPOR(LBM)= 2.340532D+02

***** TIME = 2.333333E-02 HR = 1.400000E+00 MIN = 8.400000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.47888D+01 | 5.78380D+00 | 1.69242D+02 | 2.07518D+02 | 8.43879D+05 | 4.81984D+05 | 1.32586D+06 | 1.46528D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 1.57521D+03 6.33616D+02 0. 2.74462D+03 3.37824D+03 9.81984D-01 -1.61046D-03 1.30790D-06 5.65416D-07 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.5699D+04 LBM/HR ENERGY BTU/HR = 1.9729D+07 (NORMAL= 1.9729D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.4525D+00 STEP AIR= 3.6252D+00 NET VAPOR= 2.4849D+02 NET AIR= 1.3216D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.321638D+03 WATER VAPOR(LBM)= 2.484944D+02 | | | | | | | | |

***** TIME = 2.444444E-02 HR = 1.466667E+00 MIN = 8.800000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.47857D+01 | 5.92506D+00 | 1.70003D+02 | 2.07415D+02 | 8.57147D+05 | 4.95932D+05 | 1.35308D+06 | 1.43447D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 1.54808D+03 6.48406D+02 0. 2.82572D+03 3.47413D+03 9.88565D-01 -1.60947D-03 1.30072D-06 5.98147D-07 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.4910D+04 LBM/HR ENERGY BTU/HR = 1.9767D+07 (NORMAL= 1.9767D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.4689D+00 STEP AIR= 3.5210D+00 NET VAPOR= 2.6301D+02 NET AIR= 1.3571D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.357056D+03 WATER VAPOR(LBM)= 2.630052D+02 | | | | | | | | |

***** TIME = 2.555556E-02 HR = 1.533333E+00 MIN = 9.200000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.47882D+01 | 6.06497D+00 | 1.71036D+02 | 2.07320D+02 | 8.69953D+05 | 5.09915D+05 | 1.37987D+06 | 1.63347D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 1.52158D+03 6.62720D+02 0. 2.90698D+03 3.56970D+03 9.88188D-01 -1.60610D-03 1.29324D-06 6.26776D-07 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.3323D+04 LBM/HR ENERGY BTU/HR = 1.9428D+07 (NORMAL= 1.9428D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.4562D+00 STEP AIR= 3.3575D+00 NET VAPOR= 2.7783D+02 NET AIR= 1.3918D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.391836D+03 WATER VAPOR(LBM)= 2.778303D+02 | | | | | | | | |

***** TIME = 2.666667E-02 HR = 1.600000E+00 MIN = 9.600000E+01 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.47872D+01 | 6.19973D+00 | 1.71965D+02 | 2.07232D+02 | 8.82270D+05 | 5.23938D+05 | 1.40621D+06 | 1.58876D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| 3 1.49568D+03 6.76540D+02 0. 2.98842D+03 3.66496D+03 9.88915D-01 -1.60245D-03 1.28595D-06 6.57314D-07 | | | | | | | | |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.3369D+04 LBM/HR ENERGY BTU/HR = 1.9805D+07 (NORMAL= 1.9805D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.4966D+00 STEP AIR= 3.3221D+00 NET VAPOR= 2.9297D+02 NET AIR= 1.4260D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.426013D+03 WATER VAPOR(LBM)= 2.929687D+02 | | | | | | | | |

***** TIME = 2.777778E-02 HR = 1.666667E+00 MIN = 1.000000E+02 SEC *****

HEAT STRUCTURE 1 BETWEEN COMPARTMENTS 3 AND 0 1.5 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -6.686100D+06 -7.425904D+02 -1.245641D+05 OLIIQUID 0. 0.
LEFT FILM COEF., H = 3.990835E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.722795E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.405792D+02 1.375765D+02 1.346043D+02 1.072428D+02 1.042575D+02 1.040164D+02 1.040009D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
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1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 2 BETWEEN COMPARTMENTS 3 AND 0 2 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -4.306430D+06 -4.782928D+02 -8.023012D+04 OLIIQUID 0. 0.
LEFT FILM COEF., H = 3.990835E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.722795E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.405792D+02 1.375765D+02 1.346043D+02 1.072428D+02 1.042575D+02 1.040164D+02 1.040009D+02 1.040000D+02 1.040000D+02
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HEAT STRUCTURE 3 BETWEEN COMPARTMENTS 3 AND 0 3 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -4.617647D+05 -5.128581D+01 -8.602819D+03 OLIIQUID 0. 0.
LEFT FILM COEF., H = 3.990835E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.722795E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.405792D+02 1.375765D+02 1.346043D+02 1.072428D+02 1.042575D+02 1.040164D+02 1.040009D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
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1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 4 BETWEEN COMPARTMENTS 3 AND 0 3.5 FT CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -6.882192D+05 -7.643693D+01 -1.282174D+04 OLIIQUID 0. 0.
LEFT FILM COEF., H = 3.990835E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.722795E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.405792D+02 1.375765D+02 1.346043D+02 1.072428D+02 1.042575D+02 1.040164D+02 1.040009D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
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1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 5 BETWEEN COMPARTMENTS 3 AND 0 4 FT THICK CONCRETE WALLS
TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 VAPOR -4.453183D+05 -4.945919D+01 -8.296417D+03 OLIIQUID 0. 0.
LEFT FILM COEF., H = 3.990835E+01 BTU/HR.FT2.F FIRST MESH K = 2.100000E-01 BTU/HR.FT. BULK TEMP = 1.722795E+02 F
RIGHT FILM COEF., H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT
1.405792D+02 1.375765D+02 1.346043D+02 1.072428D+02 1.042575D+02 1.040164D+02 1.040009D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02
1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02 1.040000D+02

HEAT STRUCTURE 6 BETWEEN COMPARTMENTS 3 AND 0 4.5 FT THICK CONCRETE FLOOR

TO LEFT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU TO RIGHT COMP. END STEP BTU/HR STEP BTU TOTAL NET BTU
3 LIQUID -8.998756D+04 -9.999201D+00 -2.556859D+03 0 LIQUID 0 0
LEFT FILM COEF. H = 4.000000E-01 BTU/HR.FT2.F FIRST MESH K = 5.500000E-01 BTU/HR.FT. BULK TEMP = 2.071408E+02 F
RIGHT FILM COEF. H = 0. BTU/HR.FT2.F LAST MESH K = 5.500000E-01 BTU/HR.FT.F BULK TEMP = 1.040000D+02 F
MESH POINT TEMPERATURES (F), LEFT TO RIGHT

| | | | | | | | | | |
|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|
| 1.048822D+02 | 1.040325D+02 | 1.040008D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |
| 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 | 1.040000D+02 |

SUMMARY OF HEAT TRANSFER TO COMPARTMENTS BY HEAT STRUCTURES - UNITS ARE BTU

| COMP. | STEP-LIQUID | STEP-VAPOR | NET-LIQUID | NET-VAPOR |
|-------|---------------|---------------|---------------|---------------|
| 0 | 0. | 0. | 0. | 0. |
| 1 | 0. | 0. | 0. | 0. |
| 2 | 0. | 0. | 0. | 0. |
| 3 | -9.999201D+00 | -1.398065D+03 | -2.556859D+03 | -2.345152D+05 |
| 4 | 0. | 0. | 0. | 0. |

| COMP NO. | PRESSURE (PSIA) | TEMPERATURE (F) | ENERGY (BTU) | | | CONVERGENCE | | |
|--|-----------------|----------------------------|--------------|-------------|-------------|---------------------|---------------------|--------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47850D+01 | 6.32703D+00 | 1.73180D+02 | 2.07144D+02 | 8.93907D+05 | 5.38091D+05 | 1.43200D+06 | 1.33892D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | POOL TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 1.47031D+03 | 6.89177D+02 | 0. | 3.07071D+03 | 3.75989D+03 | 9.81608D-01 | -1.59794D-03 | 1.27869D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.3736D+04 LBM/HR ENERGY BTU/HR = 2.0324D+07 (NORMAL= 2.0324D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.5474D+00 STEP AIR= 3.3121D+00 NET VAPOR= 3.0844D+02 NET AIR= 1.4597D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.459676D+03 WATER VAPOR(LBM)= 3.084426D+02 | | | | | | | | |

***** TIME = 3.333333E-02 HR = 2.000000E+00 MIN = 1.200000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | TEMPERATURE (F) | ENERGY (BTU) | | | CONVERGENCE | | |
|--|-----------------|----------------------------|--------------|-------------|-------------|---------------------|---------------------|--------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47852D+01 | 6.93956D+00 | 1.77243D+02 | 2.06832D+02 | 9.49616D+05 | 6.08819D+05 | 1.55844D+06 | 1.38589D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | POOL TOTAL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 1.35516D+03 | 7.51505D+02 | 0. | 3.48056D+03 | 4.23206D+03 | 9.82296D-01 | -1.56560D-03 | 1.24343D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.1742D+04 LBM/HR ENERGY BTU/HR = 2.0991D+07 (NORMAL= 2.0991D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.6511D+00 STEP AIR= 2.9869D+00 NET VAPOR= 3.8827D+02 NET AIR= 1.6162D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.616237D+03 WATER VAPOR(LBM)= 3.882661D+02 | | | | | | | | |

***** TIME = 3.888889E-02 HR = 2.333333E+00 MIN = 1.400000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | TEMPERATURE (F) | ENERGY (BTU) | | | CONVERGENCE | | |
|----------|-----------------|-----------------|--------------|-------------|-------------|-------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47871D+01 | 7.49108D+00 | 1.80642D+02 | 2.06647D+02 | 9.93222D+05 | 6.79988D+05 | 1.67931D+06 | 1.47098D-03 |

| AIR MASS (LBM) | | | | | | WATER MASS (LBM) | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS | |
|--|--|-------------|----|-------------|-------------|------------------|--------------|-------------|-------------|---------------------|--|-----------------------------|--|
| VAPOR--ATMOS--LIQUID | | | | | | POOL | | TOTAL | | TOTAL | | MASS HEAT | |
| | | | | | | | | | | | | (LB MOL/S FT2)(BTU/S FT2 R) | |
| 3 | 1.25354D+03 | 8.07061D+02 | 0. | 3.89157D+03 | 4.69863D+03 | 9.82748D-01 | -1.52384D-03 | 1.20947D-06 | 9.46529D-07 | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.0484D+04 LBM/HR ENERGY BTU/HR = 2.1793D+07 (NORMAL= 2.1793D+07 PENETRATION= 0.) | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.7585D+00 STEP AIR= 2.7397D+00 NET VAPOR= 4.7370D+02 NET AIR= 1.7593D+03 | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.759273D+03 WATER VAPOR(LBM)= 4.736966D+02 | | | | | | | | | | | | | |

***** TIME = 4.444444E-02 HR = 2.666667E+00 MIN = 1.600000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | CONVERGENCE | |
|----------|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47865D+01 | 7.98975D+00 | 1.83578D+02 | 2.06554D+02 | 1.04456D+06 | 7.51272D+05 | 1.79583D+06 | 1.36224D-03 |

| AIR MASS (LBM) | | | | | | WATER MASS (LBM) | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS | |
|--|--|-------------|----|-------------|-------------|------------------|--------------|-------------|-------------|---------------------|--|-----------------------------|--|
| VAPOR--ATMOS--LIQUID | | | | | | POOL | | TOTAL | | TOTAL | | MASS HEAT | |
| | | | | | | | | | | | | (LB MOL/S FT2)(BTU/S FT2 R) | |
| 3 | 1.16243D+03 | 8.57545D+02 | 0. | 4.30182D+03 | 5.15936D+03 | 9.82904D-01 | -1.47745D-03 | 1.17685D-06 | 1.05859D-06 | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.0171D+04 LBM/HR ENERGY BTU/HR = 2.2961D+07 (NORMAL= 2.2961D+07 PENETRATION= 0.) | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 1.8917D+00 STEP AIR= 2.5718D+00 NET VAPOR= 5.6497D+02 NET AIR= 1.8918D+03 | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 1.891804D+03 WATER VAPOR(LBM)= 5.649665D+02 | | | | | | | | | | | | | |

***** TIME = 5.000000E-02 HR = 3.000000E+00 MIN = 1.800000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | CONVERGENCE | |
|----------|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47875D+01 | 8.45083D+00 | 1.86140D+02 | 2.06531D+02 | 1.08599D+06 | 8.22418D+05 | 1.90841D+06 | 1.35771D-03 |

| AIR MASS (LBM) | | | | | | WATER MASS (LBM) | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS | |
|--|--|-------------|----|-------------|-------------|------------------|--------------|-------------|-------------|---------------------|--|-----------------------------|--|
| VAPOR--ATMOS--LIQUID | | | | | | POOL | | TOTAL | | TOTAL | | MASS HEAT | |
| | | | | | | | | | | | | (LB MOL/S FT2)(BTU/S FT2 R) | |
| 3 | 1.07944D+03 | 9.03821D+02 | 0. | 4.70985D+03 | 5.61367D+03 | 9.83191D-01 | -1.42858D-03 | 1.14509D-06 | 1.15761D-06 | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 3.9664D+04 LBM/HR ENERGY BTU/HR = 2.3923D+07 (NORMAL= 2.3923D+07 PENETRATION= 0.) | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.0053D+00 STEP AIR= 2.4018D+00 NET VAPOR= 6.6266D+02 NET AIR= 2.0162D+03 | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.016210D+03 WATER VAPOR(LBM)= 6.626594D+02 | | | | | | | | | | | | | |

***** TIME = 5.555556E-02 HR = 3.333333E+00 MIN = 2.000000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | CONVERGENCE | |
|----------|-----------------|-------------|-----------------|-------------|--------------|-------------|-------------|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47846D+01 | 8.86956D+00 | 1.88078D+02 | 2.06549D+02 | 1.12389D+06 | 8.93513D+05 | 2.01741D+06 | 1.21774D-03 |

| AIR MASS (LBM) | | | | | | WATER MASS (LBM) | | HUMIDITY | | CONDENSATION (LB/S) | | TRANSFER COEFFICIENTS | |
|--|--|-------------|----|-------------|-------------|------------------|--------------|-------------|-------------|---------------------|--|-----------------------------|--|
| VAPOR--ATMOS--LIQUID | | | | | | POOL | | TOTAL | | TOTAL | | MASS HEAT | |
| | | | | | | | | | | | | (LB MOL/S FT2)(BTU/S FT2 R) | |
| 3 | 1.00460D+03 | 9.46093D+02 | 0. | 5.11646D+03 | 6.06255D+03 | 9.89571D-01 | -1.37890D-03 | 1.11483D-06 | 1.25131D-06 | | | | |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 3.8820D+04 LBM/HR ENERGY BTU/HR = 2.4559D+07 (NORMAL= 2.4559D+07 PENETRATION= 0.) | | | | | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.0889D+00 STEP AIR= 2.2244D+00 NET VAPOR= 7.6578D+02 NET AIR= 2.1325D+03 | | | | | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.132463D+03 WATER VAPOR(LBM)= 7.657798D+02 | | | | | | | | | | | | | |

***** TIME = 6.111111E-02 HR = 3.666667E+00 MIN = 2.200000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE |
|--|--------------------------|-------------|-------------------|-------------|-----------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47860D+01 | 9.25887D+00 | 1.90038D+02 | 2.06600D+02 | 1.15870D+06 | 9.64281D+05 | 2.12298D+06 | 1.18907D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | | WATER MASS (LBM) | | HUMIDITY (LB/S) | | CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) | |
| | VAPOR--ATMOS--LIQUID | | POOL | | TOTAL | | | |
| 3 | 9.35898D+02 | 9.84981D+02 | 0. | 5.52007D+03 | 6.50505D+03 | 9.90444D-01 | -1.32905D-03 | 1.08543D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.8890D+04 LBM/HR | | ENERGY BTU/HR = | | 2.5692D+07 (NORMAL= 2.5692D+07 PENETRATION= 0.) | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.2127D+00 STEP AIR= 2.1084D+00 NET VAPOR= 8.7528D+02 NET AIR= 2.2426D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.242583D+03 WATER VAPOR(LBM)= 8.752826D+02 | | | | | | | | |

***** TIME = 6.666667E-02 HR = 4.000000E+00 MIN = 2.400000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE |
|--|--------------------------|-------------|-------------------|-------------|-----------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47904D+01 | 9.61941D+00 | 1.92159D+02 | 2.06673D+02 | 1.19062D+06 | 1.03473D+06 | 2.22535D+06 | 1.18965D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | | WATER MASS (LBM) | | HUMIDITY (LB/S) | | CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) | |
| | VAPOR--ATMOS--LIQUID | | POOL | | TOTAL | | | |
| 3 | 8.72736D+02 | 1.02032D+03 | 0. | 5.92086D+03 | 6.94118D+03 | 9.83406D-01 | -1.27980D-03 | 1.05697D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.9477D+04 LBM/HR | | ENERGY BTU/HR = | | 2.7128D+07 (NORMAL= 2.7128D+07 PENETRATION= 0.) | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.3613D+00 STEP AIR= 2.0250D+00 NET VAPOR= 9.9115D+02 NET AIR= 2.3472D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.347162D+03 WATER VAPOR(LBM)= 9.911538D+02 | | | | | | | | |

***** TIME = 7.222222E-02 HR = 4.333333E+00 MIN = 2.600000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE |
|--|--------------------------|-------------|-------------------|-------------|-----------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47946D+01 | 9.95301D+00 | 1.93724D+02 | 2.06763D+02 | 1.22028D+06 | 1.10474D+06 | 2.32502D+06 | 1.43078D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | | WATER MASS (LBM) | | HUMIDITY (LB/S) | | CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) | |
| | VAPOR--ATMOS--LIQUID | | POOL | | TOTAL | | | |
| 3 | 8.15180D+02 | 1.05349D+03 | 0. | 6.31818D+03 | 7.37167D+03 | 9.84354D-01 | -1.23234D-03 | 1.02975D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.8765D+04 LBM/HR | | ENERGY BTU/HR = | | 2.7606D+07 (NORMAL= 2.7606D+07 PENETRATION= 0.) | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.4253D+00 STEP AIR= 1.8819D+00 NET VAPOR= 1.1127D+03 NET AIR= 2.4461D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.446134D+03 WATER VAPOR(LBM)= 1.112657D+03 | | | | | | | | |

***** TIME = 7.777778E-02 HR = 4.666667E+00 MIN = 2.800000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) | | TEMPERATURE (F) | | ENERGY (BTU) | | | CONVERGENCE |
|--|--------------------------|-------------|-------------------|-------------|-----------------|-------------|---|-------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47887D+01 | 1.02486D+01 | 1.94777D+02 | 2.06858D+02 | 1.24689D+06 | 1.17458D+06 | 2.42147D+06 | 1.07813D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | | WATER MASS (LBM) | | HUMIDITY (LB/S) | | CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) | |
| | VAPOR--ATMOS--LIQUID | | POOL | | TOTAL | | | |
| 3 | 7.63183D+02 | 1.08335D+03 | 0. | 6.71397D+03 | 7.79731D+03 | 9.91407D-01 | -1.18300D-03 | 1.00388D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.9493D+04 LBM/HR | | ENERGY BTU/HR = | | 2.9035D+07 (NORMAL= 2.9035D+07 PENETRATION= 0.) | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.5717D+00 STEP AIR= 1.8164D+00 NET VAPOR= 1.2390D+03 NET AIR= 2.5395D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.539548D+03 WATER VAPOR(LBM)= 1.239018D+03 | | | | | | | | |

***** TIME = 8.333333E-02 HR = 5.000000E+00 MIN = 3.000000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--------------------------|--------------------------------|---------------------------|-----------------|-------------------|---------------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47954D+01 | 1.05245D+01 | 1.96403D+02 | 2.06956D+02 | 1.27094D+06 | 1.24428D+06 | 2.51522D+06 | 1.18007D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 7.16163D+02 | 1.10997D+03 | | 7.10836D+03 | 8.21833D+03 | | 9.83826D-01 | -1.13792D-03 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 4.0236D+04 LBM/HR | ENERGY BTU/HR = | | 3.0442D+07 (NORMAL= | 3.0442D+07 | PENETRATION= 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.7147D+00 STEP AIR= 1.7560D+00 NET VAPOR= 1.3700D+03 NET AIR= 2.6280D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.627985D+03 WATER VAPOR(LBM)= 1.370001D+03 | | | | | | | | |

***** TIME = 8.888889E-02 HR = 5.333333E+00 MIN = 3.200000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--------------------------|--------------------------------|---------------------------|-----------------|-------------------|---------------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47957D+01 | 1.07709D+01 | 1.97495D+02 | 2.07055D+02 | 1.29298D+06 | 1.31372D+06 | 2.60670D+06 | 1.28404D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 6.73765D+02 | 1.13431D+03 | | 7.50079D+03 | 8.63509D+03 | | 9.84165D-01 | -1.09510D-03 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.9070D+04 LBM/HR | ENERGY BTU/HR = | | 3.0328D+07 (NORMAL= | 3.0328D+07 | PENETRATION= 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.7209D+00 STEP AIR= 1.6202D+00 NET VAPOR= 1.5052D+03 NET AIR= 2.7118D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.711800D+03 WATER VAPOR(LBM)= 1.505236D+03 | | | | | | | | |

***** TIME = 9.444444E-02 HR = 5.666667E+00 MIN = 3.400000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--------------------------|--------------------------------|---------------------------|-----------------|-------------------|---------------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47901D+01 | 1.09915D+01 | 1.98138D+02 | 2.07155D+02 | 1.31277D+06 | 1.38282D+06 | 2.69558D+06 | 9.58981D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 6.35294D+02 | 1.15664D+03 | | 7.89078D+03 | 9.04742D+03 | | 9.91034D-01 | -1.05039D-03 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.9364D+04 LBM/HR | ENERGY BTU/HR = | | 3.1271D+07 (NORMAL= | 3.1271D+07 | PENETRATION= 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.8207D+00 STEP AIR= 1.5530D+00 NET VAPOR= 1.6449D+03 NET AIR= 2.7917D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.791688D+03 WATER VAPOR(LBM)= 1.644914D+03 | | | | | | | | |

***** TIME = 1.000000E-01 HR = 6.000000E+00 MIN = 3.600000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--------------------------|--------------------------------|---------------------------|-----------------|-------------------|---------------------|---------------------|----------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47974D+01 | 1.11991D+01 | 1.99369D+02 | 2.07252D+02 | 1.33065D+06 | 1.45176D+06 | 2.78241D+06 | 1.19720D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) |
| 3 | 6.00652D+02 | 1.17644D+03 | | 8.27954D+03 | 9.45598D+03 | | 9.84194D-01 | -1.01244D-03 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | | 3.9521D+04 LBM/HR | ENERGY BTU/HR = | | 3.2057D+07 (NORMAL= | 3.2057D+07 | PENETRATION= 0. |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.9046D+00 STEP AIR= 1.4865D+00 NET VAPOR= 1.7884D+03 NET AIR= 2.8677D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.867746D+03 WATER VAPOR(LBM)= 1.788351D+03 | | | | | | | | |

***** TIME = 1.055556E-01 HR = 6.333333E+00 MIN = 3.800000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|--|--------------------------------|---------------------------|--------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47968D+01 | 1.13806D+01 | 2.00156D+02 | 2.07347D+02 | 1.34672D+06 | 1.52053D+06 | 2.86725D+06 | 1.14305D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 5.69585D+02 | 1.19423D+03 | | 0.8.66703D+03 | 9.83983D-01 | | -9.73947D-04 | 8.94493D-07 1.79837D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 3.9708D+04 LBM/HR ENERGY BTU/HR = 3.2812D+07 (NORMAL= 3.2812D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.9851D+00 STEP AIR= 1.4269D+00 NET VAPOR= 1.9351D+03 NET AIR= 2.9402D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 2.940229D+03 WATER VAPOR(LBM)= 1.935073D+03 | | | | | | | | |

* * * * * TIME = 1.11111E-01 HR = 6.66667E+00 MIN = 4.00000E+02 SEC * * * * *

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|--|--------------------------------|---------------------------|--------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47914D+01 | 1.15401D+01 | 2.00458D+02 | 2.07440D+02 | 1.36115D+06 | 1.58911D+06 | 2.95026D+06 | 9.23123D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 5.41847D+02 | 1.21061D+03 | | 0.9.05317D+03 | 1.02638D+04 | | 9.91677D-01 | -9.36811D-04 8.76450D-07 1.83966D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 3.8712D+04 LBM/HR ENERGY BTU/HR = 3.2520D+07 (NORMAL= 3.2520D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 2.9693D+00 STEP AIR= 1.3320D+00 NET VAPOR= 2.0846D+03 NET AIR= 3.0094D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.009384D+03 WATER VAPOR(LBM)= 2.084554D+03 | | | | | | | | |

* * * * * TIME = 1.16667E-01 HR = 7.00000E+00 MIN = 4.20000E+02 SEC * * * * *

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|--|--------------------------------|---------------------------|--------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.47919D+01 | 1.16867D+01 | 2.01098D+02 | 2.07528D+02 | 1.37408D+06 | 1.65761D+06 | 3.03169D+06 | 9.04349D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 5.16992D+02 | 1.22492D+03 | | 0.9.43860D+03 | 1.06635D+04 | | 9.91100D-01 | -9.03740D-04 8.59819D-07 1.87138D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 3.9287D+04 LBM/HR ENERGY BTU/HR = 3.3494D+07 (NORMAL= 3.3494D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.0677D+00 STEP AIR= 1.2976D+00 NET VAPOR= 2.2368D+03 NET AIR= 3.0757D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.075656D+03 WATER VAPOR(LBM)= 2.236814D+03 | | | | | | | | |

* * * * * TIME = 1.22222E-01 HR = 7.33333E+00 MIN = 4.40000E+02 SEC * * * * *

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE DE/E |
|--|--|--------------------------------|---------------------------|--------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | |
| 3 | 1.48020D+01 | 1.18264D+01 | 2.01985D+02 | 2.07614D+02 | 1.38594D+06 | 1.72592D+06 | 3.11186D+06 | 1.27623D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 4.94755D+02 | 1.23798D+03 | | 0.9.82276D+03 | 1.10607D+04 | | 9.84729D-01 | -8.77618D-04 8.45003D-07 1.88682D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 3.9424D+04 LBM/HR ENERGY BTU/HR = 3.4060D+07 (NORMAL= 3.4060D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.1277D+00 STEP AIR= 1.2528D+00 NET VAPOR= 2.3916D+03 NET AIR= 3.1393D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.139310D+03 WATER VAPOR(LBM)= 2.391591D+03 | | | | | | | | |

* * * * * TIME = 1.27777E-01 HR = 7.66667E+00 MIN = 4.60000E+02 SEC * * * * *

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|---------------------|
| 3 | 1.48020D+01 | 1.19450D+01 | 2.02475D+02 | 2.07696D+02 | 1.39634D+06 | 1.79403D+06 | 3.19037D+06 |
| TRANSFER COEFFICIENTS | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS (LB MOL/S FT2) (BTU/S FT2 R) HEAT | | | | | | | |
| 3 | 4.74677D+02 | 1.24957D+03 | 0. | 1.02056D+04 | 1.14551D+04 | 9.84670D-01 | -8.49417D-04 |
| 3 | 4.74677D+02 | 1.24957D+03 | 0. | 1.02056D+04 | 1.14551D+04 | 9.84670D-01 | -8.49417D-04 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 3.9460D+04 LBM/HR ENERGY BTU/HR = 3.4498D+07 (NORMAL= 3.4498D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.1755D+00 STEP AIR= 1.2089D+00 NET VAPOR= 2.5492D+03 NET AIR= 3.2008D+03 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 3.200804D+03 WATER VAPOR(LBM)= 2.549191D+03 | | | | | | | |

***** TIME = 1.333333E-01 HR = 8.000000E+00 MIN = 4.800000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|---------------------|
| 3 | 1.47941D+01 | 1.20453D+01 | 2.02564D+02 | 2.07775D+02 | 1.40561D+06 | 1.86195D+06 | 3.26755D+06 |
| TRANSFER COEFFICIENTS | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS (LB MOL/S FT2) (BTU/S FT2 R) HEAT | | | | | | | |
| 3 | 4.56651D+02 | 1.26003D+03 | 0. | 1.05871D+04 | 1.18472D+04 | 9.91212D-01 | -8.19176D-04 |
| 3 | 4.56651D+02 | 1.26003D+03 | 0. | 1.05871D+04 | 1.18472D+04 | 9.91212D-01 | -8.19176D-04 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 3.9913D+04 LBM/HR ENERGY BTU/HR = 3.5265D+07 (NORMAL= 3.5265D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.2533D+00 STEP AIR= 1.1815D+00 NET VAPOR= 2.7092D+03 NET AIR= 3.2602D+03 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 3.260247D+03 WATER VAPOR(LBM)= 2.709174D+03 | | | | | | | |

***** TIME = 1.388889E-01 HR = 8.333333E+00 MIN = 5.000000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|---------------------|
| 3 | 1.48030D+01 | 1.21481D+01 | 2.03298D+02 | 2.07851D+02 | 1.41412D+06 | 1.92974D+06 | 3.34386D+06 |
| TRANSFER COEFFICIENTS | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS (LB MOL/S FT2) (BTU/S FT2 R) HEAT | | | | | | | |
| 3 | 4.40569D+02 | 1.26942D+03 | 0. | 1.09678D+04 | 1.22373D+04 | 9.84682D-01 | -8.00312D-04 |
| 3 | 4.40569D+02 | 1.26942D+03 | 0. | 1.09678D+04 | 1.22373D+04 | 9.84682D-01 | -8.00312D-04 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 3.9761D+04 LBM/HR ENERGY BTU/HR = 3.5468D+07 (NORMAL= 3.5468D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.2779D+00 STEP AIR= 1.1400D+00 NET VAPOR= 2.8711D+03 NET AIR= 3.3177D+03 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 3.317746D+03 WATER VAPOR(LBM)= 2.871073D+03 | | | | | | | |

***** TIME = 1.444444E-01 HR = 8.666667E+00 MIN = 5.200000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|---------------------|
| 3 | 1.48032D+01 | 1.22339D+01 | 2.03644D+02 | 2.07923D+02 | 1.42169D+06 | 1.99737D+06 | 3.41906D+06 |
| TRANSFER COEFFICIENTS | | | | | | | |
| AIR MASS (LBM) WATER MASS (LBM) HUMIDITY CONDENSATION MASS (LB MOL/S FT2) (BTU/S FT2 R) HEAT | | | | | | | |
| 3 | 4.26134D+02 | 1.27780D+03 | 0. | 1.13475D+04 | 1.26253D+04 | 9.84646D-01 | -7.79113D-04 |
| 3 | 4.26134D+02 | 1.27780D+03 | 0. | 1.13475D+04 | 1.26253D+04 | 9.84646D-01 | -7.79113D-04 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 3.9844D+04 LBM/HR ENERGY BTU/HR = 3.5845D+07 (NORMAL= 3.5845D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3182D+00 STEP AIR= 1.1089D+00 NET VAPOR= 3.0350D+03 NET AIR= 3.3736D+03 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 3.373598D+03 WATER VAPOR(LBM)= 3.035020D+03 | | | | | | | |

***** TIME = 1.500000E-01 HR = 9.000000E+00 MIN = 5.400000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|-----------------|---------------------|-----------------------|---------------------|---------------------|---------------------|
| 3 | 1.48032D+01 | 1.23107D+01 | 2.03953D+02 | 2.07993D+02 | 1.42850D+06 | 2.06485D+06 | 3.49335D+06 | 1.16049D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | POOL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 4.13201D+02 | 1.28529D+03 | 0. | 1.17263D+04 | 1.30116D+04 | 9.84611D-01 | -7.60176D-04 | 7.84591D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 3.9864D+04 LBM/HR | ENERGY BTU/HR = | 3.6136D+07 (NORMAL= | 3.6136D+07 | PENETRATION= | 0. |) |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3501D+00 STEP AIR= 1.0792D+00 NET VAPOR= 3.2008D+03 NET AIR= 3.4279D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.427947D+03 WATER VAPOR(LBM)= 3.200778D+03 | | | | | | | | |

***** TIME = 1.555556E-01 HR = 9.333333E+00 MIN = 5.600000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|-----------------|---------------------|-----------------------|---------------------|---------------------|---------------------|
| 3 | 1.47988D+01 | 1.23752D+01 | 2.04229D+02 | 2.08059D+02 | 1.43447D+06 | 2.13227D+06 | 3.56674D+06 | 9.84001D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | POOL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 4.01612D+02 | 1.29155D+03 | 0. | 1.21046D+04 | 1.33961D+04 | 9.84211D-01 | -7.43183D-04 | 7.75508D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 3.8681D+04 LBM/HR | ENERGY BTU/HR = | 3.5301D+07 (NORMAL= | 3.5301D+07 | PENETRATION= | 0. |) |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.2770D+00 STEP AIR= 1.0209D+00 NET VAPOR= 3.3682D+03 NET AIR= 3.4810D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.480953D+03 WATER VAPOR(LBM)= 3.368228D+03 | | | | | | | | |

***** TIME = 1.611111E-01 HR = 9.666667E+00 MIN = 5.800000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|-----------------|---------------------|-----------------------|---------------------|---------------------|---------------------|
| 3 | 1.48035D+01 | 1.24418D+01 | 2.04470D+02 | 2.08123D+02 | 1.43999D+06 | 2.19939D+06 | 3.63939D+06 | 1.15471D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | POOL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 3.91218D+02 | 1.29808D+03 | 0. | 1.24810D+04 | 1.37791D+04 | 9.84657D-01 | -7.29194D-04 | 7.67419D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 3.9689D+04 LBM/HR | ENERGY BTU/HR = | 3.6444D+07 (NORMAL= | 3.6444D+07 | PENETRATION= | 0. |) |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3871D+00 STEP AIR= 1.0228D+00 NET VAPOR= 3.5372D+03 NET AIR= 3.5328D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.532764D+03 WATER VAPOR(LBM)= 3.537240D+03 | | | | | | | | |

***** TIME = 1.666667E-01 HR = 1.000000E+01 MIN = 6.000000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|-----------------|---------------------|-----------------------|---------------------|---------------------|---------------------|
| 3 | 1.47991D+01 | 1.24934D+01 | 2.04709D+02 | 2.08184D+02 | 1.44430D+06 | 2.26647D+06 | 3.71077D+06 | 9.02660D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | POOL | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 3.81802D+02 | 1.30304D+03 | 0. | 1.28572D+04 | 1.41603D+04 | 9.83949D-01 | -7.13237D-04 | 7.59485D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 3.9704D+04 LBM/HR | ENERGY BTU/HR = | 3.6658D+07 (NORMAL= | 3.6658D+07 | PENETRATION= | 0. |) |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.4105D+00 STEP AIR= 1.0011D+00 NET VAPOR= 3.7081D+03 NET AIR= 3.5836D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.583596D+03 WATER VAPOR(LBM)= 3.708081D+03 | | | | | | | | |

***** TIME = 1.722222E-01 HR = 1.033333E+01 MIN = 6.200000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE |
|--|--|--------------------------------|---------------------------|---------------|-------------------|-------------|---------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.47998D+01 | 1.25432D+01 | 2.04931D+02 | 2.08242D+02 | 1.44877D+06 | 2.33346D+06 | 3.78223D+06 |
| | TRANSFER COEFFICIENTS | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) | | HUMIDITY | CONDENSATION (LB/S) |
| 3 | 3.73527D+02 | 1.30785D+03 | 0. | 1.32328D+04 | 1.45407D+04 | 9.83420D-01 | -6.97195D-04 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.2473D+04 LBM/HR ENERGY BTU/HR = 3.9406D+07 (NORMAL= 3.9406D+07 PENETRATION= 0.) | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6695D+00 STEP AIR= 1.0497D+00 NET VAPOR= 3.8797D+03 NET AIR= 3.6333D+03 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.633287D+03 WATER VAPOR(LBM)= 3.879657D+03 | | | | | | | |

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--|--------------------------|-------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.47960D+01 | 1.26929D+01 | 2.05042D+02 | 2.08453D+02 | 1.46242D+06 | 2.60010D+06 | 4.06252D+06 | 7.65408D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT | | | | | | | | |
| 3 | 3.48075D+02 | 1.32345D+03 | 0. | 1.47273D+04 | 1.60507D+04 | 9.93058D-01 | -6.68971D-04 | 7.32529D-07 |
| 3 | LEAKAGE OUTFLOW- MASS= 4.0148D+04 LBM/HR ENERGY BTU/HR = 3.7804D+07 (NORMAL= 3.7804D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.5306D+00 STEP AIR= 9.3026D-01 NET VAPOR= 4.5776D+03 NET AIR= 3.8244D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.824406D+03 WATER VAPOR(LBM)= 4.577620D+03 | | | | | | | | |

***** TIME = 2.000000E-01 HR = 1.200000E+01 MIN = 7.200000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--|--------------------------|-------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.47963D+01 | 1.27220D+01 | 2.05147D+02 | 2.08500D+02 | 1.46496D+06 | 2.66653D+06 | 4.13149D+06 | 7.64513D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT | | | | | | | | |
| 3 | 3.43258D+02 | 1.32630D+03 | 0. | 1.50995D+04 | 1.64258D+04 | 9.93200D-01 | -6.64462D-04 | 7.28924D-07 |
| 3 | LEAKAGE OUTFLOW- MASS= 4.0215D+04 LBM/HR ENERGY BTU/HR = 3.7973D+07 (NORMAL= 3.7973D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.5483D+00 STEP AIR= 9.2000D-01 NET VAPOR= 4.7545D+03 NET AIR= 3.8706D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.870640D+03 WATER VAPOR(LBM)= 4.754547D+03 | | | | | | | | |

***** TIME = 2.055556E-01 HR = 1.233333E+01 MIN = 7.400000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--|--------------------------|-------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.48056D+01 | 1.27555D+01 | 2.05691D+02 | 2.08545D+02 | 1.46741D+06 | 2.73293D+06 | 4.20035D+06 | 1.12459D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT | | | | | | | | |
| 3 | 3.38966D+02 | 1.32868D+03 | 0. | 1.54715D+04 | 1.68002D+04 | 9.84774D-01 | -6.68110D-04 | 7.27067D-07 |
| 3 | LEAKAGE OUTFLOW- MASS= 3.9856D+04 LBM/HR ENERGY BTU/HR = 3.7733D+07 (NORMAL= 3.7733D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.5270D+00 STEP AIR= 9.0142D-01 NET VAPOR= 4.9322D+03 NET AIR= 3.9163D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.916348D+03 WATER VAPOR(LBM)= 4.932155D+03 | | | | | | | | |

***** TIME = 2.111111E-01 HR = 1.266667E+01 MIN = 7.600000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--|--------------------------|-------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.48067D+01 | 1.27800D+01 | 2.05781D+02 | 2.08589D+02 | 1.46950D+06 | 2.79917D+06 | 4.26867D+06 | 1.15929D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT | | | | | | | | |
| 3 | 3.35057D+02 | 1.33108D+03 | 0. | 1.58425D+04 | 1.71736D+04 | 9.84865D-01 | -6.65683D-04 | 7.24346D-07 |
| 3 | LEAKAGE OUTFLOW- MASS= 4.0143D+04 LBM/HR ENERGY BTU/HR = 3.8092D+07 (NORMAL= 3.8092D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.5620D+00 STEP AIR= 8.9826D-01 NET VAPOR= 5.1107D+03 NET AIR= 3.9617D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 3.961674D+03 WATER VAPOR(LBM)= 5.110746D+03 | | | | | | | | |

***** TIME = 2.166667E-01 HR = 1.300000E+01 MIN = 7.800000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.48045D+01 | 1.27987D+01 | 2.05911D+02 | 2.08630D+02 | 1.47126D+06 | 2.86540D+06 | 4.33666D+06 | 6.41385D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | MASS (LBM) | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 3.31535D+02 | 1.33277D+03 | 0. | 1.62135D+04 | 1.75463D+04 | 9.83695D-01 | -6.54624D-04 | 7.20294D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 3.7176D+04 LBM/HR | ENERGY BTU/HR = | 3.5340D+07 (NORMAL= | 3.5340D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.3067D+00 STEP AIR= 8.2390D-01 NET VAPOR= 5.2901D+03 NET AIR= 4.0066D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.006613D+03 WATER VAPOR(LBM)= 5.290078D+03 | | | | | | | | |

***** TIME = 2.22222E-01 HR = 1.33333E+01 MIN = 8.00000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.47984D+01 | 1.28125D+01 | 2.05973D+02 | 2.08671D+02 | 1.47222D+06 | 2.93148D+06 | 4.40370D+06 | 6.77653D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | MASS (LBM) | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 3.28223D+02 | 1.33409D+03 | 0. | 1.65836D+04 | 1.79177D+04 | 9.83508D-01 | -6.55838D-04 | 7.18575D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 4.0465D+04 LBM/HR | ENERGY BTU/HR = | 3.8548D+07 (NORMAL= | 3.8548D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6074D+00 STEP AIR= 8.8879D-01 NET VAPOR= 5.4706D+03 NET AIR= 4.0513D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.051341D+03 WATER VAPOR(LBM)= 5.470646D+03 | | | | | | | | |

***** TIME = 2.27777E-01 HR = 1.36667E+01 MIN = 8.20000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.48002D+01 | 1.28313D+01 | 2.06030D+02 | 2.08710D+02 | 1.47386D+06 | 2.99748D+06 | 4.47134D+06 | 7.73442D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | MASS (LBM) | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 3.25393D+02 | 1.33595D+03 | 0. | 1.69532D+04 | 1.82892D+04 | 9.83817D-01 | -6.57065D-04 | 7.17139D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 4.0279D+04 LBM/HR | ENERGY BTU/HR = | 3.8434D+07 (NORMAL= | 3.8434D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.5978D+00 STEP AIR= 8.7763D-01 NET VAPOR= 5.6512D+03 NET AIR= 4.0956D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.095588D+03 WATER VAPOR(LBM)= 5.651158D+03 | | | | | | | | |

***** TIME = 2.33333E-01 HR = 1.40000E+01 MIN = 8.40000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|----------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|---------------------|
| 3 | 1.48023D+01 | 1.28486D+01 | 2.06083D+02 | 2.08747D+02 | 1.47538D+06 | 3.06341D+06 | 4.53878D+06 | 8.68154D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | WATER VAPOR--ATMOS--LIQUID | MASS (LBM) | MASS (LBM) | HUMIDITY | CONDENSATION (LB/S) | MASS (LB MOL/S FT2) | HEAT (BTU/S FT2 R) |
| 3 | 3.22839D+02 | 1.33767D+03 | 0. | 1.73224D+04 | 1.86601D+04 | 9.84097D-01 | -6.58398D-04 | 7.15880D-07 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= | 4.0352D+04 LBM/HR | ENERGY BTU/HR = | 3.8562D+07 (NORMAL= | 3.8562D+07 | PENETRATION= | 0. | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6107D+00 STEP AIR= 8.7282D-01 NET VAPOR= 5.8323D+03 NET AIR= 4.1396D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.139559D+03 WATER VAPOR(LBM)= 5.832264D+03 | | | | | | | | |

***** TIME = 2.38889E-01 HR = 1.43333E+01 MIN = 8.60000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E | |
|---|--|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|-------------|
| 3 | 1.48041D+01 | 1.28643D+01 | 2.06131D+02 | 2.08783D+02 | 1.47675D+06 | 3.12926D+06 | 4.60600D+06 | 9.53032D-04 | |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY (LB/S) CONDENSATION (LB/S) MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | |
| 3 | 3.20523D+02 | 1.33923D+03 | 0. | 1.76911D+04 | 1.90304D+04 | 9.84345D-01 | -6.60016D-04 | 7.14812D-07 | 1.94248D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.0444D+04 LBM/HR ENERGY BTU/HR = 3.8703D+07 (NORMAL= 3.8703D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6248D+00 STEP AIR= 8.6898D-01 NET VAPOR= 6.0140D+03 NET AIR= 4.1833D+03 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.183291D+03 WATER VAPOR(LBM)= 6.013961D+03 | | | | | | | | | |

***** TIME = 2.444444E-01 HR = 1.466667E+01 MIN = 8.800000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E | |
|---|--|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|-------------|
| 3 | 1.47966D+01 | 1.28705D+01 | 2.05746D+02 | 2.08818D+02 | 1.47807D+06 | 3.19504D+06 | 4.67311D+06 | 6.67557D-04 | |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY (LB/S) CONDENSATION (LB/S) MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | |
| 3 | 3.18440D+02 | 1.34072D+03 | 0. | 1.80595D+04 | 1.94002D+04 | 9.92655D-01 | -6.55188D-04 | 7.12726D-07 | 1.94690D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.0633D+04 LBM/HR ENERGY BTU/HR = 3.8928D+07 (NORMAL= 3.8928D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6471D+00 STEP AIR= 8.6769D-01 NET VAPOR= 6.1961D+03 NET AIR= 4.2268D+03 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.226791D+03 WATER VAPOR(LBM)= 6.196130D+03 | | | | | | | | | |

***** TIME = 2.500000E-01 HR = 1.500000E+01 MIN = 9.000000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E | |
|---|--|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|-------------|
| 3 | 1.48002D+01 | 1.28848D+01 | 2.06257D+02 | 2.08851D+02 | 1.47861D+06 | 3.26084D+06 | 4.73945D+06 | 6.53170D-04 | |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY (LB/S) CONDENSATION (LB/S) MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | |
| 3 | 3.16436D+02 | 1.34112D+03 | 0. | 1.84279D+04 | 1.97690D+04 | 9.83385D-01 | -6.55700D-04 | 7.11621D-07 | 1.94012D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.1887D+04 LBM/HR ENERGY BTU/HR = 4.0178D+07 (NORMAL= 4.0178D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7646D+00 STEP AIR= 8.8949D-01 NET VAPOR= 6.3793D+03 NET AIR= 4.2702D+03 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.270212D+03 WATER VAPOR(LBM)= 6.379295D+03 | | | | | | | | | |

***** TIME = 2.555556E-01 HR = 1.533333E+01 MIN = 9.200000E+02 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E | |
|---|--|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|-------------|
| 3 | 1.47985D+01 | 1.28938D+01 | 2.06294D+02 | 2.08883D+02 | 1.47929D+06 | 3.32650D+06 | 4.80579D+06 | 6.01245D-04 | |
| TRANSFER COEFFICIENTS | | | | | | | | | |
| AIR MASS (LBM) WATER VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY (LB/S) CONDENSATION (LB/S) MASS (LB MOL/S FT2) HEAT (BTU/S FT2 R) | | | | | | | | | |
| 3 | 3.14633D+02 | 1.34200D+03 | 0. | 1.87955D+04 | 2.01375D+04 | 9.83356D-01 | -6.58087D-04 | 7.11013D-07 | 1.93015D-06 |
| COMP. | 3 LEAKAGE OUTFLOW- MASS= 4.0894D+04 LBM/HR ENERGY BTU/HR = 3.9266D+07 (NORMAL= 3.9266D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6798D+00 STEP AIR= 8.6391D-01 NET VAPOR= 6.5628D+03 NET AIR= 4.3134D+03 | | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.313432D+03 WATER VAPOR(LBM)= 6.562822D+03 | | | | | | | | | |

***** TIME = 2.611111E-01 HR = 1.566667E+01 MIN = 9.400000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--|--------------------------------|---------------------------|--------------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.48074D+01 | 1.29114D+01 | 2.06293D+02 | 2.08914D+02 | 1.48109D+06 | 3.39207D+06 | 4.87316D+06 | 1.07516D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL TOTAL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 3.13201D+02 | 1.34386D+03 | 0. | 1.91626D+04 | 2.05065D+04 | 9.84722D-01 | -6.67018D-04 | 7.11785D-07 1.90711D-06 |
| COMP. 3 | LEAKAGE OUTFLOW- MASS= 4.0757D+04 LBM/HR ENERGY BTU/HR = 3.9170D+07 (NORMAL= 3.9170D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6714D+00 STEP AIR= 8.5714D-01 NET VAPOR= 6.7459D+03 NET AIR= 4.3563D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.35628D+03 WATER VAPOR(LBM)= 6.745864D+03 | | | | | | | | |

***** TIME = 2.666667E-01 HR = 1.600000E+01 MIN = 9.600000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--|--------------------------------|---------------------------|--------------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.48010D+01 | 1.29147D+01 | 2.06354D+02 | 2.08944D+02 | 1.48104D+06 | 3.45761D+06 | 4.93865D+06 | 7.27528D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL TOTAL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 3.11579D+02 | 1.34407D+03 | 0. | 1.95295D+04 | 2.08736D+04 | 9.83749D-01 | -6.63816D-04 | 7.10266D-07 1.90947D-06 |
| COMP. 3 | LEAKAGE OUTFLOW- MASS= 4.0812D+04 LBM/HR ENERGY BTU/HR = 3.9258D+07 (NORMAL= 3.9258D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.6803D+00 STEP AIR= 8.5441D-01 NET VAPOR= 6.9308D+03 NET AIR= 4.3993D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.399318D+03 WATER VAPOR(LBM)= 6.930759D+03 | | | | | | | | |

***** TIME = 2.722222E-01 HR = 1.633333E+01 MIN = 9.800000E+02 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--|--------------------------------|---------------------------|--------------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.48059D+01 | 1.29270D+01 | 2.06400D+02 | 2.08973D+02 | 1.48220D+06 | 3.52309D+06 | 5.00529D+06 | 4.71823D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL TOTAL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 3.10332D+02 | 1.34527D+03 | 0. | 1.98961D+04 | 2.12413D+04 | 9.83770D-01 | -6.62593D-04 | 7.09353D-07 1.90883D-06 |
| COMP. 3 | LEAKAGE OUTFLOW- MASS= 3.8076D+04 LBM/HR ENERGY BTU/HR = 3.6647D+07 (NORMAL= 3.6647D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.4366D+00 STEP AIR= 7.9403D-01 NET VAPOR= 7.1150D+03 NET AIR= 4.4420D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.441982D+03 WATER VAPOR(LBM)= 7.114987D+03 | | | | | | | | |

***** TIME = 2.777778E-01 HR = 1.666667E+01 MIN = 1.000000E+03 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | | CONVERGENCE |
|--|--|--------------------------------|---------------------------|--------------------------|-------------------|-------------|---------------------|---------------------------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | TOTAL | DE/E |
| 3 | 1.47819D+01 | 1.29128D+01 | 2.05550D+02 | 2.09001D+02 | 1.48274D+06 | 3.58858D+06 | 5.07132D+06 | 3.76873D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL TOTAL | HUMIDITY | | CONDENSATION (LB/S) | MASS (LB MOL/S FT2)(BTU/S FT2 R) HEAT |
| 3 | 3.09095D+02 | 1.34562D+03 | 4.94459D-01 | 2.02627D+04 | 2.16083D+04 | 1.00000D+00 | 1.23549D+00 | 7.08053D-07 1.91163D-06 |
| COMP. 3 | LEAKAGE OUTFLOW- MASS= 4.2891D+04 LBM/HR ENERGY BTU/HR = 4.1315D+07 (NORMAL= 4.1315D+07 PENETRATION= 0.) | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.8746D+00 STEP AIR= 8.9103D-01 NET VAPOR= 7.3000D+03 NET AIR= 4.4846D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.484636D+03 WATER VAPOR(LBM)= 7.300034D+03 | | | | | | | | |

***** TIME = 2.833333E-01 HR = 1.700000E+01 MIN = 1.020000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.48045D+01 | 1.29397D+01 | 2.06427D+02 | 2.09029D+02 | 1.48353D+06 | 3.65393D+06 | 5.13746D+06 | 8.83799D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| VAPOR--ATMOS--LIQUID POOL TOTAL (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.07995D+02 | 1.34656D+03 | 0. | 2.06285D+04 | 2.19751D+04 | 9.84210D-01 | -6.72877D-04 | 7.09809D-07 |
| 3 | 3.07995D+02 | 1.34656D+03 | 0. | 2.06285D+04 | 2.19751D+04 | 9.84210D-01 | -6.72877D-04 | 7.09809D-07 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.0997D+04 LBM/HR ENERGY BTU/HR = 3.9519D+07 (NORMAL= 3.9519D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7062D+00 STEP AIR= 8.4905D-01 NET VAPOR= 7.4853D+03 NET AIR= 4.5272D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.527153D+03 WATER VAPOR(LBM)= 7.485280D+03 | | | | | | | | |

***** TIME = 2.888889E-01 HR = 1.733333E+01 MIN = 1.040000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.47988D+01 | 1.29411D+01 | 2.06476D+02 | 2.09055D+02 | 1.48336D+06 | 3.71924D+06 | 5.20261D+06 | 5.70624D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| VAPOR--ATMOS--LIQUID POOL TOTAL (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.06809D+02 | 1.34660D+03 | 0. | 2.09941D+04 | 2.23407D+04 | 9.83330D-01 | -6.70594D-04 | 7.08716D-07 |
| 3 | 3.06809D+02 | 1.34660D+03 | 0. | 2.09941D+04 | 2.23407D+04 | 9.83330D-01 | -6.70594D-04 | 7.08716D-07 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.1093D+04 LBM/HR ENERGY BTU/HR = 3.9637D+07 (NORMAL= 3.9637D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7177D+00 STEP AIR= 8.4817D-01 NET VAPOR= 7.6716D+03 NET AIR= 4.5698D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.569756D+03 WATER VAPOR(LBM)= 7.671645D+03 | | | | | | | | |

***** TIME = 2.944444E-01 HR = 1.766667E+01 MIN = 1.060000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.48079D+01 | 1.29550D+01 | 2.06462D+02 | 2.09081D+02 | 1.48483D+06 | 3.78449D+06 | 5.26932D+06 | 1.04419D-03 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| VAPOR--ATMOS--LIQUID POOL TOTAL (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.06015D+02 | 1.34809D+03 | 0. | 2.13593D+04 | 2.27074D+04 | 9.84671D-01 | -6.80073D-04 | 7.09943D-07 |
| 3 | 3.06015D+02 | 1.34809D+03 | 0. | 2.13593D+04 | 2.27074D+04 | 9.84671D-01 | -6.80073D-04 | 7.09943D-07 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.1138D+04 LBM/HR ENERGY BTU/HR = 3.9702D+07 (NORMAL= 3.9702D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7241D+00 STEP AIR= 8.4680D-01 NET VAPOR= 7.8570D+03 NET AIR= 4.6120D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.611966D+03 WATER VAPOR(LBM)= 7.856974D+03 | | | | | | | | |

***** TIME = 3.000000E-01 HR = 1.800000E+01 MIN = 1.080000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | STEAM | TEMPERATURE (F) ATMOS | POOL | ENERGY (BTU) ATMOS | POOL | TOTAL | CONVERGENCE DE/E |
|--|--------------------------|-------------|--------------------------|-------------|-----------------------|-------------|--------------|---------------------|
| 3 | 1.47941D+01 | 1.29483D+01 | 2.05932D+02 | 2.09106D+02 | 1.48512D+06 | 3.84969D+06 | 5.33482D+06 | 7.04115D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) W A T E R M A S S (LBM) HUMIDITY CONDENSATION MASS HEAT | | | | | | | | |
| VAPOR--ATMOS--LIQUID POOL TOTAL (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.05071D+02 | 1.34854D+03 | 0. | 2.17242D+04 | 2.30727D+04 | 9.94947D-01 | -6.72895D-04 | 7.08100D-07 |
| 3 | 3.05071D+02 | 1.34854D+03 | 0. | 2.17242D+04 | 2.30727D+04 | 9.94947D-01 | -6.72895D-04 | 7.08100D-07 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.2938D+04 LBM/HR ENERGY BTU/HR = 4.1460D+07 (NORMAL= 4.1460D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.8896D+00 STEP AIR= 8.8130D-01 NET VAPOR= 8.0436D+03 NET AIR= 4.6543D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.654327D+03 WATER VAPOR(LBM)= 8.043598D+03 | | | | | | | | |

***** TIME = 3.055556E-01 HR = 1.833333E+01 MIN = 1.100000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|-------------------------|
| 3 | 1.48038D+01 | 1.29614D+01 | 2.06517D+02 | 2.09130D+02 | 1.48545D+06 | 3.91494D+06 | 5.40040D+06 | 8.18271D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.04254D+02 | 1.34865D+03 | 0. | 2.20894D+04 | 2.34380D+04 | 9.84071D-01 | -6.82449D-04 | 7.09361D-07 1.84845D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.1041D+04 LBM/HR ENERGY BTU/HR = 3.9647D+07 (NORMAL= 3.9647D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7196D+00 STEP AIR= 8.4044D-01 NET VAPOR= 8.2303D+03 NET AIR= 4.6966D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.696561D+03 WATER VAPOR(LBM)= 8.230284D+03 | | | | | | | | |

***** TIME = 3.11111E-01 HR = 1.866667E+01 MIN = 1.120000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|-------------------------|
| 3 | 1.48056D+01 | 1.29678D+01 | 2.06530D+02 | 2.09153D+02 | 1.48599D+06 | 3.98006D+06 | 5.46605D+06 | 9.03008D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.03493D+02 | 1.34930D+03 | 0. | 2.24538D+04 | 2.38031D+04 | 9.84298D-01 | -6.86078D-04 | 7.09564D-07 1.83819D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.1217D+04 LBM/HR ENERGY BTU/HR = 3.9836D+07 (NORMAL= 3.9836D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7376D+00 STEP AIR= 8.4204D-01 NET VAPOR= 8.4172D+03 NET AIR= 4.7387D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.738738D+03 WATER VAPOR(LBM)= 8.417249D+03 | | | | | | | | |

***** TIME = 3.166667E-01 HR = 1.900000E+01 MIN = 1.140000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|-------------------------|
| 3 | 1.48072D+01 | 1.29737D+01 | 2.06542D+02 | 2.09176D+02 | 1.48646D+06 | 4.04512D+06 | 5.53158D+06 | 9.76467D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.02778D+02 | 1.34989D+03 | 0. | 2.28179D+04 | 2.41678D+04 | 9.84501D-01 | -6.89675D-04 | 7.09787D-07 1.82807D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 4.1329D+04 LBM/HR ENERGY BTU/HR = 3.9961D+07 (NORMAL= 3.9961D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.7497D+00 STEP AIR= 8.4244D-01 NET VAPOR= 8.6045D+03 NET AIR= 4.7809D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.780870D+03 WATER VAPOR(LBM)= 8.604534D+03 | | | | | | | | |

***** TIME = 3.22222E-01 HR = 1.93333E+01 MIN = 1.160000E+03 SEC *****

| COMP NO. | PRESSURE (PSIA) TOTAL | TEMPERATURE (F) STEAM | TEMPERATURE (F) ATMOS | TEMPERATURE (F) POOL | ENERGY (BTU) ATMOS | ENERGY (BTU) POOL | ENERGY (BTU) TOTAL | CONVERGENCE DE/E |
|--|--------------------------|--------------------------|--------------------------|-------------------------|-----------------------|----------------------|-----------------------|-------------------------|
| 3 | 1.47980D+01 | 1.29697D+01 | 2.06127D+02 | 2.09198D+02 | 1.48680D+06 | 4.11015D+06 | 5.59695D+06 | 6.32842D-04 |
| TRANSFER COEFFICIENTS | | | | | | | | |
| AIR MASS (LBM) VAPOR--ATMOS--LIQUID POOL TOTAL HUMIDITY CONDENSATION (LB/S) (LB MOL/S FT2)(BTU/S FT2 R) | | | | | | | | |
| 3 | 3.02099D+02 | 1.35038D+03 | 0. | 2.31818D+04 | 2.45322D+04 | 9.92613D-01 | -6.85789D-04 | 7.08731D-07 1.83512D-06 |
| COMP. 3 LEAKAGE OUTFLOW- MASS= 3.8733D+04 LBM/HR ENERGY BTU/HR = 3.7459D+07 (NORMAL= 3.7459D+07 PENETRATION= 0.) | | | | | | | | |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.5158D+00 STEP AIR= 7.8784D-01 NET VAPOR= 8.7922D+03 NET AIR= 4.8230D+03 | | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS O AIR(LBM)= 4.822965D+03 WATER VAPOR(LBM)= 8.792153D+03 | | | | | | | | |

***** TIME = 3.27777E-01 HR = 1.966667E+01 MIN = 1.180000E+03 SEC *****

| COMP NO. | P R E S S U R E (PSIA) | | T E M P E R A T U R E (F) | | E N E R G Y (BTU) | | CONVERGENCE |
|--|------------------------|--------------------------------|---------------------------|--------------------|-------------------|---------------------|---------------------|
| | TOTAL | STEAM | ATMOS | POOL | ATMOS | POOL | DE/E |
| 3 | 1.47998D+01 | 1.29747D+01 | 2.06608D+02 | 2.09220D+02 | 1.48640D+06 | 4.17522D+06 | 5.40550D-04 |
| | TRANSFER COEFFICIENTS | | | | | | |
| | AIR MASS (LBM) | W A T E R VAPOR--ATMOS--LIQUID | | M A S S (LBM) POOL | | HUMIDITY | CONDENSATION (LB/S) |
| 3 | 3.01350D+02 | 1.34986D+03 | 0. | 2.35459D+04 | 2.48958D+04 | 9.83241D-01 | -6.87946D-04 |
| COMP. 3 | LEAKAGE OUTFLOW- MASS= | | 4.1891D+04 LBM/HR | ENERGY BTU/HR = | | 4.0536D+07 (NORMAL= | 4.0536D+07 |
| STEP AND NET MASS LOSSES LBM STEP VAPOR= 3.8041D+00 STEP AIR= 8.5037D-01 NET VAPOR= 8.9805D+03 NET AIR= 4.8651D+03 | | | | | | | |
| TOTAL NET CONTAINMENT LOSS TO ATMOSPHERE IS 0 AIR(LBM)= 4.865131D+03 WATER VAPOR(LBM)= 8.980545D+03 | | | | | | | |

***** COMPUTER TIME FOR THIS CASE WAS 1.4525 MIN.

***** COMPUTER TIME FOR ALL JOBS WAS 1.4545 MIN.

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MFA U.C.C. NOS/BE L587 V1.7.05.4 06/03/84
11.53.19.CONTOST FROM 9V
11.53.19.IP 00000512 WORDS - FILE INPUT , DC 04
11.53.19.CONT,P2,T400,EC1000, MCONTEMPT
11.53.20.ACCOUNT,AGEIHT,*---*
11.53.21.ROUTE,OUTPUT,TID=80,DEF.
11.53.22.REWIND,OUTPUT.
11.53.22.ATTACH,LT28,CONTEMPTLT28,ID=EIUCC.
11.53.22.AT CY= 002 SN=GLOBAL
11.53.22.ATTACH,TAPE15,STEAMTABLE,ID=EIUCC.
11.53.22.AT CY= 001 SN=GLOBAL
11.53.22.RFL,EC=1000.
11.53.22.LT28.
11.53.24.*-----*
11.53.24.* CONTEMPT LT-28 FROM NESC (ARGONNE). *
11.53.24.* INCLUDES ENERGY INC. MODIFICATIONS *
11.53.24.* TO FIX THE MK I MK II MODELS, *
11.53.24.* AND THE PRESSURE-FLASH MODEL *
11.53.24.* (E.I. IDENTs PSFIX + PFLFIX , AS *
11.53.24.* IDENT PFPFL-FIX IN THIS SOURCE). *
11.53.24.* INCLUDES PLOTTING CAPABILITY VIA *
11.53.24.* UNIPLOT-UNIPLOT (IDENT UCCPLOT). *
11.53.24.* UCC INSTALLATION DATE- 14 JULY 82. *
11.53.24.*-----*
11.53.42. STOP
11.53.42. 255700 FINAL EXECUTION FL.
11.53.42. 87.311 CP SECONDS EXECUTION TIME.
11.53.43.BEGIN,PPRINT,,H=INPUT,COPIES=1.
11.53.52.
11.53.52. COPYRIGHT, 1981, UNIVERSITY COMPUTING
11.53.52. COMPANY. REPRODUCTION PROHIBITED UNLESS
11.53.52. SPECIFICALLY AUTHORIZED BY SEPARATE
11.53.52. WRITING.
11.53.52.
11.53.52.RETURN,ZZZZZIN,ZZZZZPO,DAYFILE,DAYFIL.
11.53.52.IFE(FILE(INPUT,AS),H1)
11.53.52.COPYBR,INPUT,ZZZZZIN.
11.53.53.ENDIF,H1.
11.53.53.COPY,ZZZZZP1,ZZZZZIN.
11.53.53.RETURN,ZZZZZP1.
11.53.53.UCC,BANNER(0=ZZZZZIN,,BIN,54)
11.53.53.(C) 1983, 1984 UCC
11.53.55.REWIND,OUTPUT.
11.53.55.COPY,OUTPUT,ZZZZZIN.
11.53.55.IFE((T.AND.(OT.NE.TX0)),DLOOP)
11.53.55.SUMMARY.
11.53.55.MS 76736 WORDS ( 76736 MAX USED)
11.53.55.MM 255700B MAX SCM ,1000000B MAX LCM
11.53.55.CPR 88.085
11.53.55.IOR 3.599
11.53.55.ECR 4.727
11.53.55.SRU 96.412
11.53.55.ARU .000
11.53.55.TOT 96.412
11.53.55.DAYFIL.

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