

308 --- Q200002080002
Scientific Notebook # 173 (Thermal Effects on
Flow KTI)

THERMAL

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Flow KTI)

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Melissa Hill MH

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5/1/96 JP

Thermal Effects on Flow KTI

Initial entry 5/1/96 by James D. Pugh JP

This notebook chronicles the laboratory investigations for the Thermal Effects on Flow KTI.

5/1/96 gff

Preparation of crushed rock for thermal conductivity experiments.

Objective - prepare size graded crushed rock for use in thermal conductivity experiments.

Method - crushing using hammer and anvil and size grading by sieving.

Materials and Equipment

- Apache heap tuff
- Steel hammer and anvil
- plastic bags
- plastic containers
- Grieve drying oven Model PL-326
- Rubber bands
- Ro-Tap sieve shaker
- Bronze 8 inch sieves; 5/8", No. 5, and No. 10

Jim Peckoyl & Ronald Green are investigators on this project
R. Green 6/12/97

Procedure

a) Break up bulk pieces of Apache heap tuff into pieces 4 cm in diameter or smaller using hammer and anvil.

b) Separate the broken pieces into 3 size fractions by sieving.

The sizing of the fractions are as follows:

4 - 1.6 cm
 1.6 - 0.4 cm
 0.4 - 0.2 cm

c) Place the crushed rock in plastic containers and place in drying oven set at 90°C for at least two days.

d) Remove rock from drying oven and immediately place in double plastic bags. Secure tops of bags with rubber bands so that air cannot enter.

e) label bags with size fraction of the material.

6/3/96

Construction of thermal conductivity cell

Obj: build apparatus to measure the thermal conductivity of unconsolidated or crushed rock.

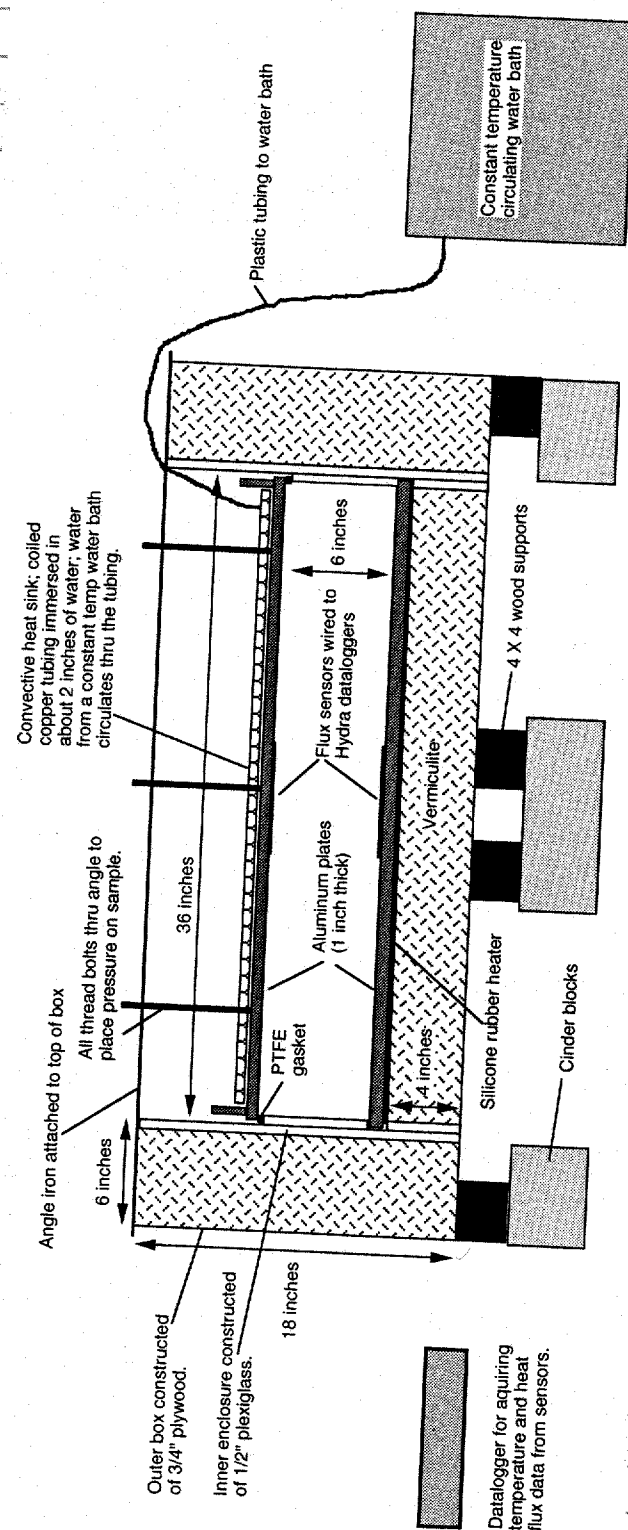
Method: measure heat flux and temperature difference over distance

Materials and equipment:

- 1/2 inch plexiglass
- 3/4" plywood
- 2x4 and 4x4 lumber
- 1" steel bolts
- Micro-Foil Heat Flow Sensors - 8 total - ^{4 each in} 6"x6" Al plates
Serial nos. 96041631, 96041632, 96041630, 96041633, 95J0642, 95J0641, 95J0639, 95J0640
- FLUKE Hydra data loggers
Serial nos 5777650 and 5832651 ^{Calibration not required}
- Hydra starter software
- OMEGA Type T copper-constantin thermocouples
length 6 inch
- Vermiculite
- 1/2" copper tubing
- 2 36"x36"x1" Aluminum plates -
- 34"x36" silicone rubber heater
- Statco energy variable transformer
- Angle iron 2"x2"x1/8"
- C clamps

- bolts, all tread, 8"
- fittings and tubing as necessary
- PTFE joint sealant
- silicone rubber sealant
- exocal water bath (ser no. 89BML 93540-11)
- exocal temperature controller
- Neslab cooler (ser no 910ML 74800-23)
- Aluminium tape
- 36"x34" silicone rubber heater
- torque wrench
- tygon tubing
- Dayton 1 ton mobil crane Model 32672
- HP 3458A multimeter (s/n 2823A02203)

A schematic diagram of the thermal conductivity system is shown below:



Description & Procedure

① A 4'x4'x18" box made of 3/4" plywood. The box was supported by an inner frame of 2"x2" wood and 4"x4" wood on the outside bottom.

② A 3'x3'x18" enclosure made of 1/2" plexiglass was constructed as shown in the schematic diagram. This consisted of an 18" high outer enclosure and 6" and 4" inside enclosures. These enclosures are placed in the middle of the plywood box.

③ 6 1/8" x 6 1/8" x 1/8" areas were milled out in the centers of the two 1" aluminum plates. The 6" x 6" x 1/8" flux sensors were mounted in the milled areas with Al tape so that the microfoil meters are approximately flush with the plate surfaces.

④ A 34" x 36" silicone rubber heater was mounted to the surface of one of the Al plates; opposite to the surface with the flux sensor. (4a) Wiring for heater runs thru a hole drilled in the bottom of the box and then to a variable transformer.

⑤ Vermiculite was placed between the inside ^{plexiglass} and outside ^{plywood} enclosures and in the bottom of the 4" high inside plexiglass enclosure. Before placing the vermiculite in the inside plexiglass enclosure a layer of 1/8" Kelvar material was placed in the bottom and two type T thermocouples were placed in the wood below the Kelvar to monitor the temperature at the base

of the box. Location of these thermocouples will be shown in following diagrams.

(6) The bottom Al plate was placed in the box supported by the 4" high plexiglass enclosure as shown in the diagram.

(7) The bottom Al plate was bolted to the outside 18" high plexiglass enclosure to add support.

(8) Wiring for the Flux sensor on the bottom Al plate was run along a groove milled in the plate, thru the holes drilled in the plexiglass and plywood enclosure, and thru to a datalogger. Location of the individual microfoil sensors will be shown in following diagrams.

(9) A bead of silicone rubber sealant was placed around the outside edge of the bottom Al plate and then the 6" high plexiglass enclosure was placed on the Al plate as shown in the diagram. The silicone will act as a watertight sealant between the plexiglass + Al.

(10) A 1/8" PTFE gasket was mounted on the top edge of the 6" high plexiglass enclosure as shown in the diagram.

(11) A ~36" x 36" x 1/16" sheet of Al was placed on top of the bottom Al plate and will act of protect the microfoil sensors

(12a) Wiring for the Flux sensors on the top Al plate were run along a groove milled in the plate and thru to a datalogger. Location of individual sensors will be shown in following diagrams.

(12) The top Al plate is placed in the plexiglass enclosure supported by the 6" high plexiglass as shown in the diagram. Note: When a sample is loaded in the system a ~36" x 36" x 1/16" sheet of Al will be placed on top of the sample to protect the microfoil sensors in the top Al plate.

(13) A 4" lip of Al has been welded to the top of the upper Al plate as shown in the diagram. This was done so that water could be ponded on the top plate to act as a heat sink.

(14) 1/2" coiled copper tubing was placed on the top Al plate. The tubing was immersed in about 2" of water. Water was circulated thru the copper tubing via a constant temperature circulating water bath.

(15) Type T thermocouples were mounted on the outside of the top + bottom Al plates to monitor the temperature differences of the systems. Location of these thermocouples will be shown in following diagrams.

(16) The 4' long pieces of 2" x 2" x 1/8" angle iron were attached to the top of the box with C clamps. Each piece of angle iron has 3 evenly spaced all thread bolts attached as shown in the diagram. The bolts are torqued down on the top Al plate to apply a pressure to the sample.

- (17) Sample is loaded in the system by removing the top Al plate using a hand operated crane, loading the sample on top of the bottom Al plate and then placing the top Al plate on the sample.

Pressure is applied to the sample using the all three bolts.

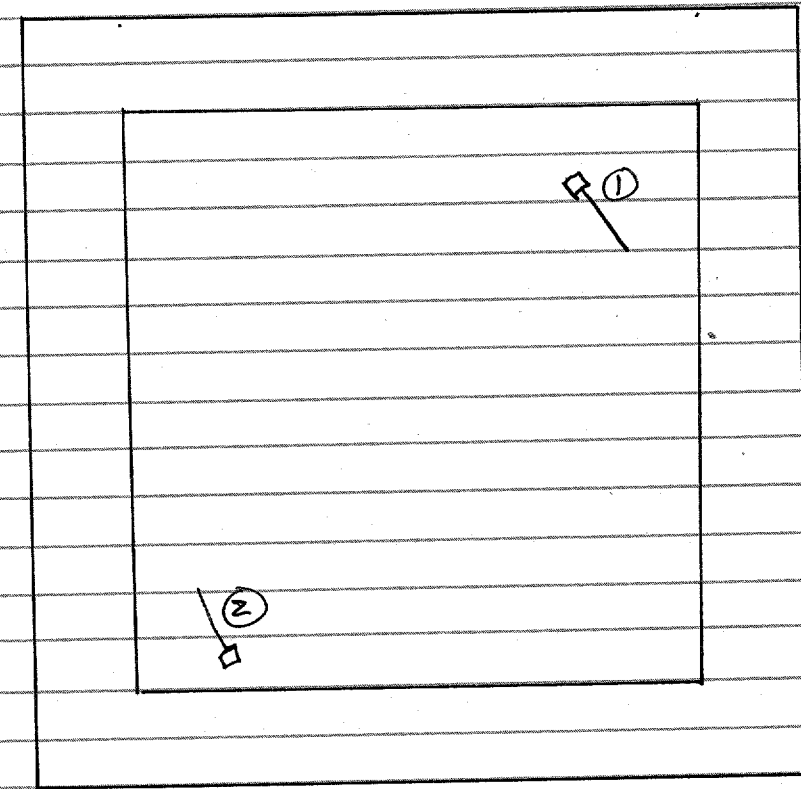
Heat is applied to the system via the silicone heater by applying voltage using the variable transformer.

Temperature of top plate is controlled by the circulating water bath.

A thermal conductivity measurement is taken when system reaches equilibrium; i.e. constant temperature at both top and bottom of system as measured by flux + temperature sensors.

Diagrams showing locations of monitoring thermocouples and flux sensors.

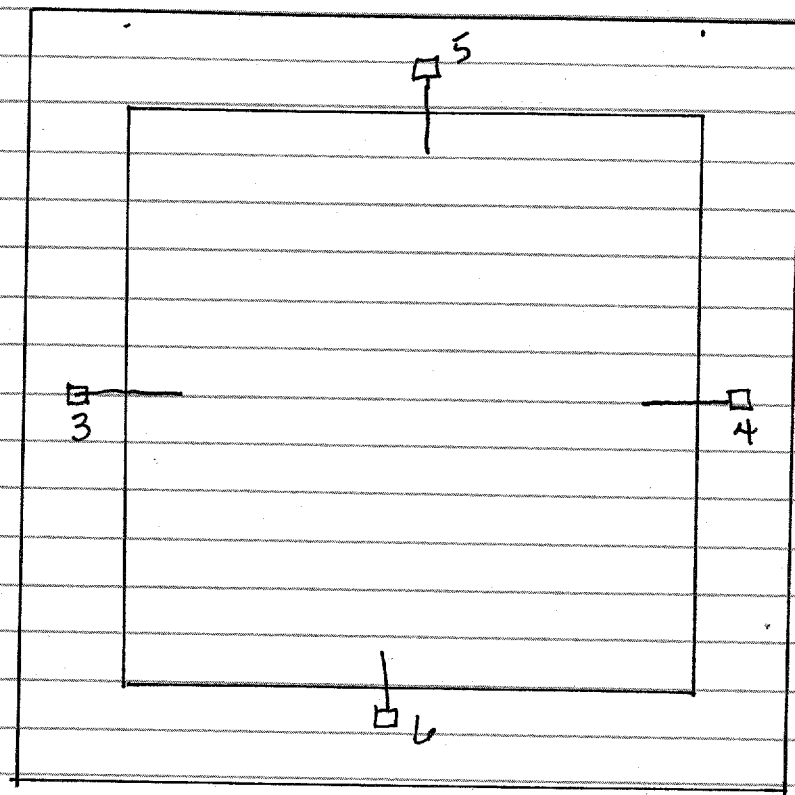
Monitoring thermocouples in bottom of box.



Front of box

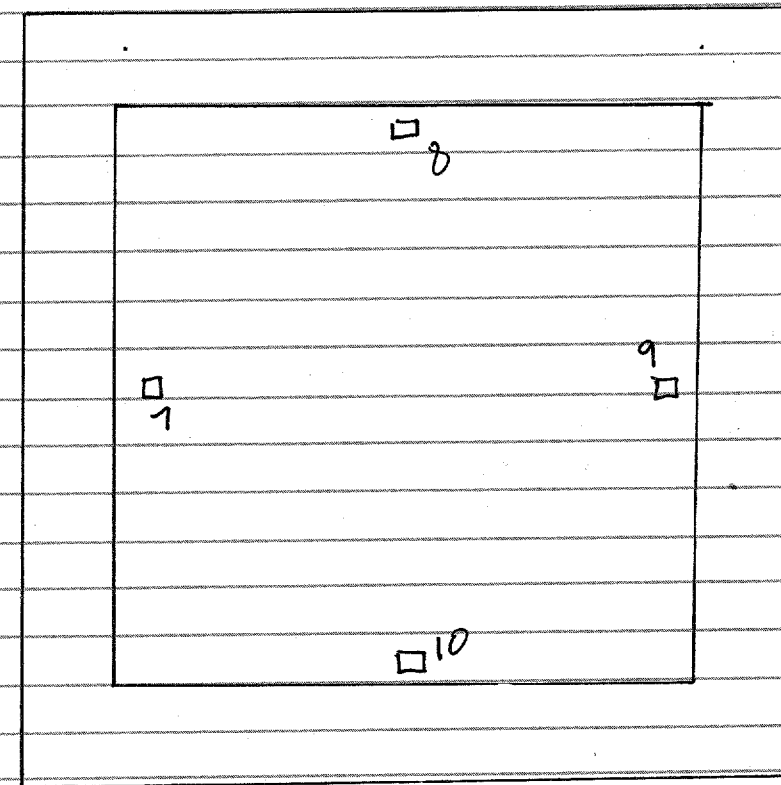
* Numbers correspond to channel numbers of datalogger to which these thermocouples are attached.

Monitoring thermocouples in bottom Al plate



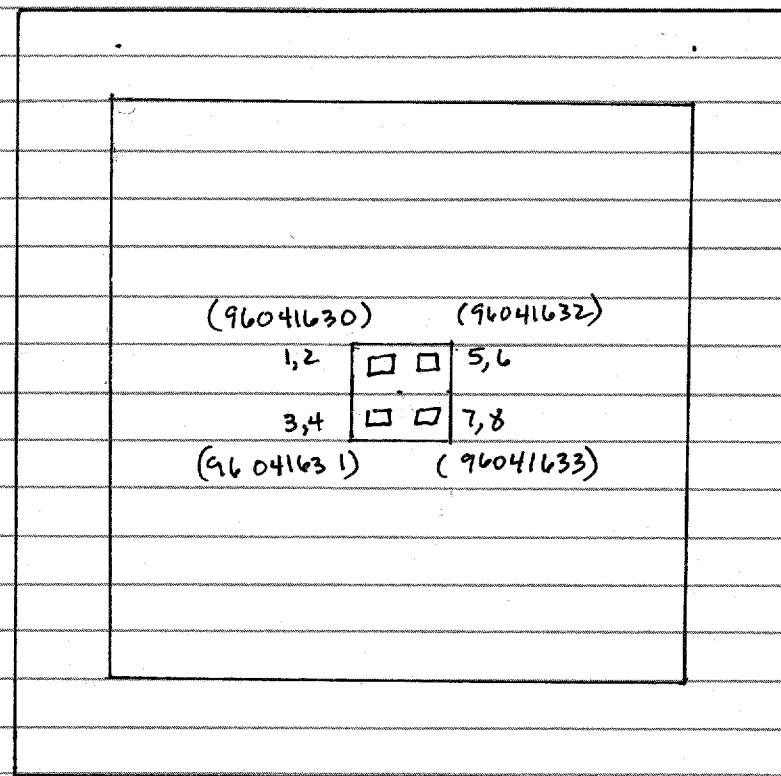
Front of box

Monitoring thermocouples in top Al plate



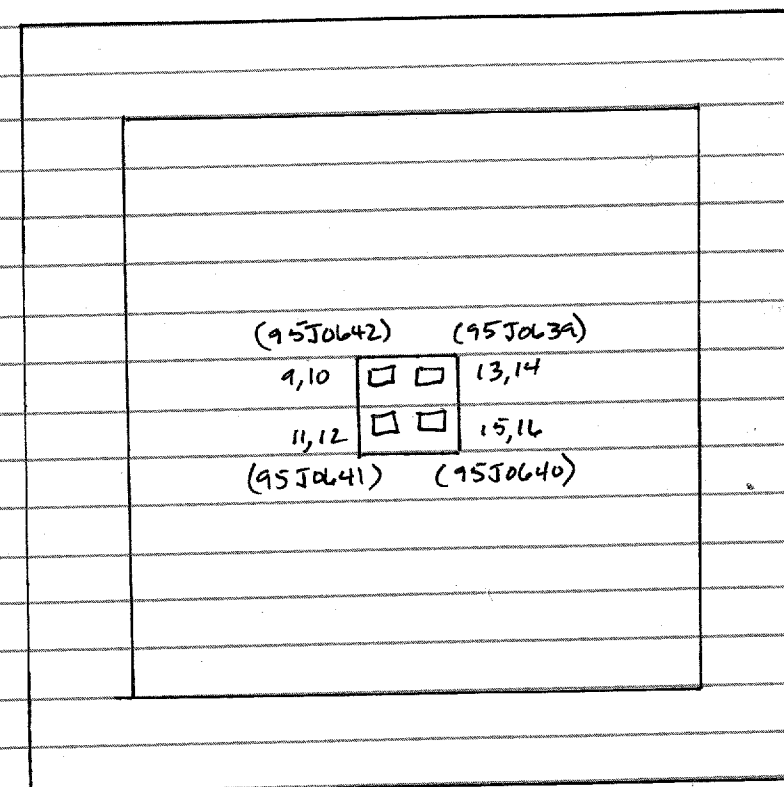
Front of box

Flux meter on bottom Al plate
 Serial nos. of each microfoil sensor are shown in parentheses.



Front of box

Flux meters on top Al plate
 (when plate is in place)



Front of box

Following are certificates of calibration
for each microfoil sensor



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Q-116-12

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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1SERIAL NO. 96041630

HEAT FLOW SENSOR:

Output at 70°F: 3.39 microvolts/Btu-Ft⁻² - Hr⁻¹Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² - Hr⁻¹ (Typ)*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

BY: Elaine TardifDATE: 4-19-96

Specialists in Temperature Measurement



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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1SERIAL NO. 96041631

HEAT FLOW SENSOR:

Output at 70°F: 3.30 microvolts/Btu-Ft⁻² - Hr⁻¹Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² - Hr⁻¹ (Typ)*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1SERIAL NO. 96041632

HEAT FLOW SENSOR:

Output at 70°F: 3.23 microvolts/Btu-Ft⁻² - Hr⁻¹Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² -Hr⁻¹ (Typ)*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1SERIAL NO. 96041633

HEAT FLOW SENSOR:

Output at 70°F: 3.42 microvolts/Btu-Ft⁻² - Hr⁻¹Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² -Hr⁻¹ (Typ)*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1

SERIAL NO. 95J0639

HEAT FLOW SENSOR:

Output at 70°F: 3.28 microvolts/Btu-Ft⁻² - Hr⁻¹

Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² -Hr⁻¹ (Typ)

*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)

Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

BY: Elaine Tardy DATE: 9-28-95
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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1

SERIAL NO. 95J0640

HEAT FLOW SENSOR:

Output at 70°F: 3.26 microvolts/Btu-Ft⁻² - Hr⁻¹

Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² -Hr⁻¹ (Typ)

*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)

Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

BY: Elaine Tardy DATE: 9-28-95
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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1SERIAL NO. 95J0641

HEAT FLOW SENSOR:

Output at 70°F: 3.20 microvolts/Btu-Ft⁻² - Hr⁻¹

Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² -Hr⁻¹ (Typ)*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)Response Time: 0.60 sec. (62% response to step function) (Typ)

THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

BY: Elaine Tardy DATE: 9-28-85
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MICRO-FOIL™ HEAT FLOW SENSOR

CALIBRATION

RdF PART NO. 27070-1SERIAL NO. 95J0642

HEAT FLOW SENSOR:

Output at 70°F: 3.43 microvolts/Btu-Ft⁻² - Hr⁻¹

Polarity: (For heat flow into surface)
White - Positive (+)
Red - Negative (-)

Temperature Multiplication Factor: See Attached Graph

*Thermal Resistance: 0.01 °F/Btu-Ft⁻² -Hr⁻¹ (Typ)*Heat Capacity: 0.03 Btu-Ft⁻²/°F (Typ)Response Time: 0.60 sec. (62% response to step function) (Typ)

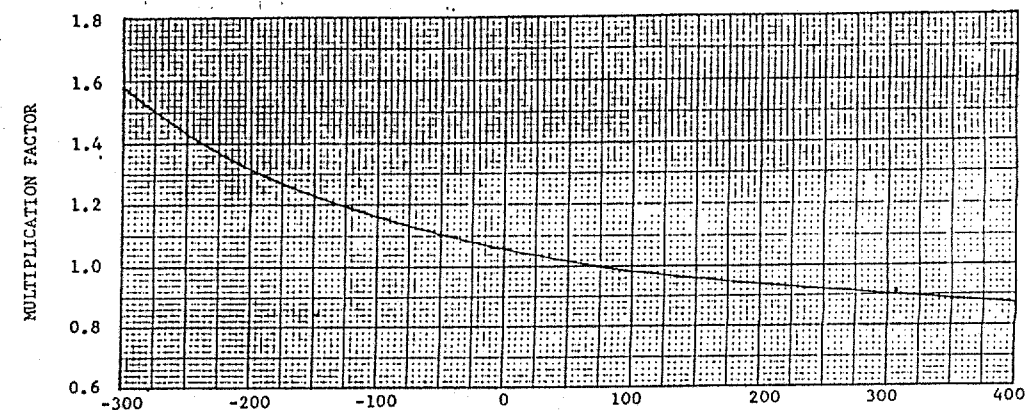
THERMOCOUPLE:

ANSI Type	Material	Polarity	Color
K	Chromel Alumel	Pos. (+) Neg. (-)	Yellow Red

Output per ANSI MC96.1-1975 and NBS Monograph 125

* Thermal resistance is the temperature difference between the front surface and rear mounting surface of the sensor per unit of heat flow through the sensor. Heat capacity is the amount of heat required to raise the mean temperature of the sensor 1°F. Typical values of these two properties are given primarily to indicate sensor capabilities and are required for heat flow calculations only in very rare instances.

BY: Elaine Tardy DATE: 9-28-85
Specialists in Temperature Measurement



SURFACE TEMPERATURE, DEGREES FAHRENHEIT
MICRO-FOIL HEAT FLOW SENSOR
OUTPUT MULTIPLICATION FACTOR VS RECEIVING SURFACE TEMPERATURE
(70°F Base)

RdF CORPORATION
Hudson, New Hampshire

0-116-12

6/4/96 JP

Initial readings of flux sensors before
heat was applied to the system
Sample was not loaded at this point

Bottom Al plate

Serial NO	mV	Temp °C
96041630	0	21.5
96041631	0	21.4
96041632	0	21.4
96041633	0	21.4

Top Al plate

Serial NO	mV	Temp °C
95J0642	0	21.4
95J0641	0	21.4
95J0639	0	21.5
95J0640	0	21.5

Monitoring thermocouples are for monitoring
heat loss from the sides of
the system and these temperatures
will not be used in determining the
thermal conductivity of the sample.
Therefore, these thermocouples do not
require calibration.

6/5/95 gf

Thermal Conductivity Measurements of crushed Apache Leap Tuff

Objective: determine thermal conductivity of crushed Apache Leap tuff at different saturation states (e.g., dry, fully saturated, matrix saturated, etc.).

Method: measure using thermal conductivity system (see p 4-10).

Equipment + materials

- thermal conductivity cell
- Apache Leap tuff crushed to 1.6 to 4 cm size (see p 2-3).
- Hewlett Packard 3458 A Multimeter (SN 2823A 02203)

Procedure - Dry rock

0915

- ① Remove top Al plate from thermal conductivity cell and load the 1.6 to 4 cm size fraction of Apache Leap tuff evenly into the cell.

1015

- ② Replace top Al plate, set up heat sink (i.e., copper tubing attached to circulating water bath immersed in about 2" of water), and attach angle iron with all-thread bolts to top of box. Begin experiment using following parameters.

Variable transformer setpoint - 40
 Waterbath temperature setpoint - 23°C
 Torque or pressure on top Al plate - 5 ft-lbs.
 Scan interval for acquiring
 Temperature + heat flow readings - 3 min

- ③ Allow system to reach steady state which will be achieved when heat flowing into the box as recorded by microvolt readings from sensors on bottom Al plate equal heat flowing out of box as recorded by mV readings from sensors on top Al plate.

- ④ Temperature & heat flow (mVDC) readings from the sensors will be downloaded from the datalogger to a computer. This data will be kept in a 3-ring binder entitled "Thermal Conductivity Data".

⑤ Final heat flow + temperature readings for each sample at different saturation states will be recorded and the thermal conductivity will be calculated.

⑥ This experiment was referred to as Run 1

gf 6/10/96
0900hrs.

The thermal conductivity cell with the dry Apache Leap tuff inside appears not to be working properly. Heat flow readings as measured in μV for sensors mounted in the top Al plate are lower than readings from sensors mounted in the lower Al plate.

Apparently some process (e.g., air pockets between sensor and sample or inadequate contact between sensor + sample) is causing thermal impedance.

1400hrs. To solve this problem steel wool (a good heat conductor) was placed between the sensor and the top $\frac{1}{16}$ " Al sheet to form a better contact between sample + sensor. However, heat flow readings from the top sensor were still lower than from the bottom sensor.

6/10/96 JP

1000hrs As Alumin pad made of sheets of Al Soil was placed between the flux sensor and the $\frac{1}{16}$ " Al top sheet to form a better contact between the sensor & sample. Again heat flow readings remained lower than those in the bottom Al plate.

6/12/96 JP

0900hrs Pieces of Al Soil were crumpled and mashed into open voids at the top surface of the rock (Apache Leap tuff) in the cell. This was done to provide a better contact between the sample & sensor. Except for one sensor in the top plate, again readings were lower than for the bottom plate sensors.

1400hrs Additional pieces of Al Soil were crumpled and mashed into remaining voids on top surface of sample. A film of vacuum grease was smeared on the surface of the top flux sensor to form a wet contact between the sensor and top $\frac{1}{16}$ " Al sheet. Heat flow readings from the top Al plate sensors are now very similar to those of the lower Al plate.

6/13/96 gp

0815hr Results of thermal conductivity experiment on dry Apache heap tuff. (Rm)

Heat Flow + Temperature readings are recorded below. Heat Flow (mV) readings were taken on a Hewlett Packard 3458A Multimeter (S/N 2823A 02203) for better sensitivity.

Bottom Al plate

Serial No.	mV	Temp °C
96041630	^{gp 6/13/96} 0.0885 .0728	70.0
96041631	.0819	70.0
96041632	.0786	70.0
96041633	.0986	70.0

Top Al plate

95J0642	.0620	22.2
95J0641	.0685	22.2
95J0639	.0815	22.3
95J0640	.0905	22.3

Monitoring thermocouples

Channel No	Temp °C
1	35.6
2	35.4
3	69.7
4	69.6
5	69.7
6	^{gp 6/13/96} 60.0
7	22.0
8	22.2
9	22.0
10	22.0

6/14/96 gp
0900hr

The tuff sample inside the thermal conductivity cell was removed and then loaded again to see if repacking of the crushed rock has any effect on thermal conductivity measurements.

Procedure on pp 26-28 was followed. In addition pieces of Al foil were crumpled and placed in voids on top surface of sample. Also the top 3'x3' sheet of 1/16" Al was not used; instead a 6"x6" piece of 1/16" Al was taped over the top flux sensor with Al tape. Vacuum grease was used to provide a even contact between the sensor and the 6"x6" Al plate.

This experiment had the following parameters

Variable temperature setpoint	- 40
Waterbath setpoint	- 23°C
Pressure on top Al plate	- 5.5±lbs
Scan interval	- 10 min

This experiment will be referred to as Rm 2.

6/17/96 gp

0815hr Results of thermal conductivity experiment
on dry Apache Leap Tuff (Run 2)

Bottom Al plate

Serial No	mV	Temp °C
96041630	.0795	69.5
96041631	.0856	69.4
96041632	.0771	69.4
96041633	.0770	69.3

Top Al plate

95J0642	.0724	22.4
95J0641	.0834	22.5
95J0639	.1182	22.5
95J0640	.0810	22.4

Monitoring thermocouples

Channel no	Temp °C
1	36.2
2	22.4 36.0 gp 6/17/96
3	69.1
4	69.1
5	69.1
7	22.4
8	22.3
9	22.4
10	22.3

6/17/96 gp

0900hr

Thermal conductivity experiment on dry
Apache Leap Tuff Run 3In this experiment the tuff sample was
left in the cell but the temperature
at the top of the cell was changed
to 40°C.

Parameters were as follows.

Variable transducer setpoint	- 40
Waterbath setpoint	- 40°C
Pressure on top Al plate	- 5 ft-lbs
Scan interval	- 10 min

6/19/96 JP

1100hr Results of TC experiment Run 3 on
dry Apache Leap tuff.

Bottom Al plate

Serial No	mV	Temp °C
96041630	.0663	76.6
96041631	.0717	76.6
96041632	.0654	76.6
96041633	.0643	76.6

Top Al plate

95J0642	.0606	39.6
95J0641	.0692	39.6
95J0639	.1001	39.5
95J0640	.0694	39.5

Monitoring Thermocouples

Channel No	Temp °C
1	39.2
2	38.0
3	76.2
4	76.2
5	76.2
7	38.8
8	39.0
9	39.0
10	38.8

6/19/96 JP

1130hr

Thermal conductivity experiment Run 4
using dry Apache Leap tuff.

In this run the tuff sample was
again left in the cell and the
temperature at the bottom of the
cell was increased to 90°C.

Parameters are as follows:

Variable transducer setpoint	= 50
Waterbath setpoint	= 40°C
Pressure to top Al plate	= 5 ft-lbs
Scan interval	= 10 min

6/20/96 gp

1320 ^{hr} Results of ^{TC} experiment Run 4 on dry Apache Leap tuff.

Bottom Al plate

Serial no	mV	Temp °C
96041630	.0993	94.3
96041631	.1093	94.3
96041632	.1000	94.4
96041633	.0971	94.3

Top Al plate

9550642	.0917	40.1
9550641	.1042	40.0
9550639	.1488	40.0
9550640	.1032	40.0

Monitoring Thermocouples

Channel No	Temp °C
1	44.1
2	42.4
3	93.8
4	93.8
5	93.8
7	39.1
8	39.4
9	39.3
10	39.1

6/20/96 gp

1330hr Thermal Conductivity experiment Run 5 using dry Apache Leap tuff

In this run the tuff sample was again left in the cell and the temperature at the top of the cell was decreased to 20°C

Parameters are as follows

Variable transducer setpoint = 50
 Waterbath setpoint = 20°C
 Pressure on top of Al plate = 5 ft-lbs
 Scan interval = 10 min

6/21/96 JP

1500hrs Results of TC experiment Run 5 on dry
JP Apache heap tuff

Bottom Al plate

Serial no	MV	Temp °C
96041630	.1166	86.5
96041631	.1268	86.5
96041632	.1169	86.6
96041633	.1125	86.5

Top Al plate

95J0642	.1023	20.2
95J0641	.1174	20.1
95J0639	.1647	20.2
95J0640	.1144	20.2

Monitoring thermocouples

Channel No	Temp °C
1	41.1
2	40.2
3	86.2
4	86.1
5	86.2
7	20.1
8	20.0
9	20.1
10	20.1

6/21/96 JP

1530hrs

Thermal Conductivity experiment Run 6 using
dry Apache heap tuff.

In this run the tuff sample ^{was left} in the cell and the temperature on the bottom Al plate was decreased to about 30°C

Parameters are as follows:

Variable tungsten setpoint -
Watertrub setpoint - 20°C
Pressure on top Al plate - 5 ft-lbs
Scan interval - 10 min

6/27/96 gp

0945hr Results of TC experiment Run 6

Bottom Al plate

Serial no	mV	Temp °C
96041630	.0227	32.1
96041631	.0239	32.1
96041632	.0211	32.2
96041633	.0203	32.2

Top Al plate

95J0642	.0174	18.8
95J0641	.0204	18.7
95J0639	.0287	18.8
95J0640	.0196	18.8

Monitoring thermocouples

Channel no	Temp °C
1	26.0
2	25.7
3	32.1
4	32.2
5	32.2
7	19.0
8	18.9
9	19.0
10	18.9

6/27/96 gp

1000hr Thermal Conductivity calculation

The thermal conductivity of the dry Apache heap tuff using data from Run 1 is calculated below using the Fourier equation.

$$Q = K_f \frac{\Delta T}{\Delta L}$$

where

Q = heat transfer per unit area (W/Ft^2)

K_f = thermal conductivity ($W/m \cdot K$)

ΔT = temperature difference between bottom and top sensors ($^{\circ}K$)

ΔL = distance between bottom and top sensors (m)

W = watts; K = degrees Kelvin

Run 1 sensor readings

Serial no	Temp °C	Temp °K = °C + 273.2	Heat Flow μV	Heat Flow cal. constant (pt 16-23) $\mu V/Btu/Ft^2 \cdot Hr$
Bottom				
96041630	70	343.2	72.8	3.39
96041631	70	343.2	81.9	3.3
96041632	70	343.2	78.6	3.23
96041633	70	343.2	98.6	3.42
Top				
95J0642	22.2	295.4	62	3.43
95J0641	22.2	295.4	68.5	3.2
95J0639	22.2	295.5	81.5	3.28
95J0640	22.3	295.5	90.5	3.26

Heat flow^(Q) for each sensor is calculated by dividing measured heat flow by the calibration constant.

Serial no	Btu/Ft ² -Hr	W/Ft ² (1 Btu/Hr = 0.293 W)
96041630	72.8 / 3.39 = 21.47	6.29
96041631	81.9 / 3.3 = 24.82	7.27
96041632	78.6 / 3.23 = 24.33	7.13
96041633	98.6 / 3.42 = 28.83	8.45
95J0642	62 / 3.43 = 18.08	5.30
95J0641	68.5 / 3.2 = 21.41	6.27
95J0639	81.5 / 3.28 = 24.85	7.28
95J0640	90.5 / 3.26 = 27.76	8.13

Heat flow for entire system is determined by averaging values from all the sensors.

$$Q = (6.29 + 7.27 + 7.13 + 8.45 + 5.30 + 6.27 + 7.28 + 8.13) / 8 = 7.015 \text{ W/Ft}^2$$

$$\text{convert to W/m}^2 = 7.015 / 0.0929 = 75.51 \text{ W/m}^2$$

$$\Delta T = (343.2 + 343.2 + 343.2 + 343.2) / 4 - (295.4 + 295.4 + 295.5 + 295.5) / 4$$

$$= 47.75 \text{ K}$$

$$\Delta L = 0.5 \text{ Ft} \quad \text{convert to m} = .5 \times .3048 = .1524 \text{ m}$$

$$K_T = 75.51 \text{ W/m}^2 \left(\frac{.1524 \text{ m}}{47.75 \text{ K}} \right) = .241 \text{ W/m-K}$$

Subsequent thermal conductivity calculation will be done using a Microsoft Excel v. 5.0 spreadsheet.

The spreadsheet calculation for Run 1 is shown below.

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap tuff (dry) Run 1						
$Q = K_T (\Delta T / \Delta L)$						
where						
Q = heat transfer per unit area (W/Ft ²)						
K _T = thermal conductivity (W/m-K)						
ΔT = temperature difference between bottom and top sensors (K)						
ΔL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp °C	Temp °K	Heat flow μ V	Cal. constant μ V/Btu/Ft ² -Hr	Heat flow Btu/Ft ² -Hr	Convert to W/Ft ² 1 Btu/Hr = 0.293 W
Bottom						
96041630	70	343.2	72.8	3.39	21.475	6.292
96041631	70	343.2	81.9	3.3	24.818	7.272
96041632	70	343.2	78.6	3.23	24.334	7.130
96041633	70	343.2	98.6	3.42	28.830	8.447
Top						
95J0642	22.2	295.4	62	3.43	18.076	5.296
95J0641	22.2	295.4	68.5	3.2	21.406	6.272
95J0639	22.3	295.5	81.5	3.28	24.848	7.280
95J0640	22.3	295.5	90.5	3.26	27.761	8.134
Summary						
Q =	7.015 W/Ft ²		75.516 W/m ²			
ΔT =	47.75 K					
ΔL =	0.5 Ft		0.1524 m			
K _T =	0.241 W/m-K					

2/27/16 Thermal conductivity spreadsheet calculations
for dry Apache Leap Tuff Run 2 thru 6
are shown on following pages.

Run 2

Thermal Conductivity calculation using Fourier equation

Sample =	Apache Leap tuff (dry) Run 2
----------	------------------------------

$$Q = K_T (dT/dL)$$

where

Q = heat transfer per unit area (W/ft^2)

K_T = thermal conductivity (W/m-K)

dT = temperature difference between bottom and top sensors (K)

dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp ⁰ C	Temp ⁰ K	Heat flow μ V	Cal. constant μ V/Btu/Ft ² -Hr	Heat flow Btu/Ft ² -Hr	Convert to W/Ft ² 1Btu/Hr = 0.293W
Bottom						
96041630	69.5	342.7	79.5	3.39	23.451	6.871
96041631	69.4	342.6	85.6	3.3	25.939	7.600
96041632	69.4	342.6	77.1	3.23	23.870	6.994
96041633	69.3	342.5	77	3.42	22.515	6.597
Top						
95J0642	22.4	295.6	72.4	3.43	21.108	6.185
95J0641	22.5	295.7	83.4	3.2	26.063	7.636
95J0639	22.5	295.7	118.2	3.28	36.037	10.559
95J0640	22.4	295.6	81	3.26	24.847	7.280

Q =	7.465 W/Ft ²	80.358 W/m ²
dT =	46.95 K	
dL =	0.5 Ft	0.1524 m

 $K_T = 0.261 \text{ W/m-K}$

Run 3

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap tuff (dry) Run 3

$$Q = K_T (dT/dL)$$

where

Q = heat transfer per unit area (W/Ft^2)

K_T = thermal conductivity (W/m-K)

dT = temperature difference between bottom and top sensors (K)

dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp °C	Temp °K	Heat flow μV	Cal. constant $\mu\text{V/Btu/Ft}^2\text{-Hr}$	Heat flow $\text{Btu/Ft}^2\text{-Hr}$	Convert to W/Ft^2 $1\text{Btu/Hr} = 0.293\text{W}$
Bottom						
96041630	76.6	349.8	66.3	3.39	19.558	5.730
96041631	76.6	349.8	71.7	3.3	21.727	6.366
96041632	76.6	349.8	65.4	3.23	20.248	5.933
96041633	76.6	349.8	64.3	3.42	18.801	5.509
Top						
95J0642	39.6	312.8	60.6	3.43	17.668	5.177
95J0641	39.6	312.8	69.2	3.2	21.625	6.336
95J0639	39.5	312.7	100.1	3.28	30.518	8.942
95J0640	39.5	312.7	69.4	3.26	21.288	6.237

$$Q = 6.279 \text{ W/Ft}^2 \quad 67.586 \text{ W/m}^2$$

dT =	37.05 K
------	---------

dL =	0.5 Ft	0.1524 m
------	--------	----------

$$K_T = 0.278 \text{ W/m-K}$$

Run 4

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap tuff (dry) Run 4

$$Q = K_T(dT/dL)$$

where Q = heat transfer per unit area (W/Ft^2)
 K_T = thermal conductivity ($W/m-K$)
 dT = temperature difference between bottom and top sensors (K)
 dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp $^{\circ}C$	Temp $^{\circ}K$	Heat flow μV	Cal. constant $\mu V/Btu/Ft^2-Hr$	Heat flow Btu/Ft^2-Hr	Convert to W/Ft^2 $1Btu/Hr = 0.293W$
Bottom						
96041630	94.3	367.5	99.3	3.39	29.292	8.583
96041631	94.3	367.5	109.3	3.3	33.121	9.705
96041632	94.4	367.6	100	3.23	30.960	9.071
96041633	94.3	367.5	97.1	3.42	28.392	8.319
Top						
95J0642	40.1	313.3	91.7	3.43	26.735	7.833
95J0641	40	313.2	104.2	3.2	32.563	9.541
95J0639	40	313.2	148.8	3.28	45.366	13.292
95J0640	40	313.2	103.2	3.26	31.656	9.275

$Q = 9.452 W/Ft^2$
 $dT = 54.3 K$
 $dL = 0.5 Ft$
 $K_T = 0.286 W/m-K$

101.747 W/m^2

0.1524 m

Run 5

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap tuff (dry) Run 5

$$Q = K_T(dT/dL)$$

where Q = heat transfer per unit area (W/Ft^2)
 K_T = thermal conductivity ($W/m-K$)
 dT = temperature difference between bottom and top sensors (K)
 dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp $^{\circ}C$	Temp $^{\circ}K$	Heat flow μV	Cal. constant $\mu V/Btu/Ft^2-Hr$	Heat flow Btu/Ft^2-Hr	Convert to W/Ft^2 $1Btu/Hr = 0.293W$
Bottom						
96041630	86.5	359.7	116.6	3.39	34.395	10.078
96041631	86.5	359.7	126.8	3.3	38.424	11.258
96041632	86.6	359.8	116.9	3.23	36.192	10.604
96041633	86.5	359.7	112.5	3.42	32.895	9.638
Top						
95J0642	20.2	293.4	102.3	3.43	29.825	8.739
95J0641	20.1	293.3	117.4	3.2	36.688	10.749
95J0639	20.2	293.4	164.7	3.28	50.213	14.713
95J0640	20.2	293.4	114.4	3.26	35.092	10.282

$Q = 10.758 W/Ft^2$
 $dT = 66.35 K$
 $dL = 0.5 Ft$
 $K_T = 0.266 W/m-K$

115.798 W/m^2

0.1524 m

Run 6

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap tuff (dry) Run 6						
$Q = K_T(dT/dL)$						
where						
Q = heat transfer per unit area (W/Ft ²)						
K _T = thermal conductivity (W/m-K)						
dT = temperature difference between bottom and top sensors (K)						
dL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp °C	Temp °K	Heat flow μV	Cal. constant	Heat flow	Convert to W/Ft ²
				μV/Btu/Ft ² -Hr	Btu/Ft ² -Hr	1Btu/Hr = 0.293W
Bottom						
96041630	32.1	305.3	22.7	3.39	6.696	1.962
96041631	32.1	305.3	23.9	3.3	7.242	2.122
96041632	32.2	305.4	21.1	3.23	6.533	1.914
96041633	32.2	305.4	20.3	3.42	5.936	1.739
Top						
95J0642	18.8	292	17.4	3.43	5.073	1.486
95J0641	18.7	291.9	20.4	3.2	6.375	1.868
95J0639	18.8	292	28.7	3.28	8.750	2.564
95J0640	18.8	292	19.6	3.26	6.012	1.762
Q = 1.927 W/Ft ² 20.744 W/m ²						
dT = 13.375 K						
dL = 0.5 Ft 0.1524 m						
K _T = 0.236 W/m-K						

7/2/96 gp

Shown below is the certificate for calibration for the HP 3458A multimeter. This meter has been used to take mV readings from flux sensors in the thermal conductivity system. The meter was received in tolerance. Therefore, readings taken before calibration will be considered good.



Southwest Research Institute
6220 Culebra Road
San Antonio, TX 78238
Department of Quality Assurance
Calibration Laboratory

Certificate of Calibration

26 June 1996

Issued to: RON GREEN DIV20 B57
Manufacturer/Model: HP 3458A
Description: DIGITAL MULTIMETER
Serial Number: 2823A02203
Asset Number: 001436

Environmental Conditions

Temperature: 73.0 Humidity: 40%

Calibration Information

Calibration was in accordance with requirements of MIL-STD-45662A and ANSI/NCSS Z540-1-1994. Measurements are traceable to the National Institute of Standards and Technology (NIST). This report may not be reproduced except in full without written approval of the originator. Inspection and test data are on file and available for inspection.

Calibration Date: 25 Jun 96 Calibration Procedure: MFG
Interval: 12 months Accuracy: MFGR SPECS
Next Calibration Due: 25 Jun 97 Received: In Tolerance

Remarks: CAL BY ROTHE DEV., SAN ANTONIO, TX
CERT# 43931

Certificate # 21799

Signed: 

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Total Pages Printed: 1

8/27/96 gp

Modification of thermal conductivity cell

Obj: prepare thermal conductivity cell for high temperature ($>90^{\circ}\text{C}$) measurements

Method: replace inner plexiglass enclosure with a fiberglass enclosure

Materials - fiberglass enclosure constructed by Mac's Custom Fiberglass.

Procedure:

- ① The inner plexiglass enclosure of the thermal conductivity cell as shown on p 6 was removed.
- ② An enclosure made of $\frac{1}{2}$ " fiberglass was placed in thermal conductivity cell so that high temperature ($>90^{\circ}\text{C}$) measurements could be taken on samples. All other components of the cell remained the same.

8/29/96 gp

0830 hrs gp

Thermal Conductivity experiment Run 7 on Dry Apache Reef Tuff.

In this run the tuff sample was loaded in the newly modified thermal conductivity cell.

Parameters are as follows:

Variable Transformer setpoint	- 80
Waterbath setpoint	- 23°C
Pressure on top of Al plate	- 5 ft. lbs
Scan interval	- 10 min

9/3/96 gp

0800hr Results of TC experiment Run 7

Bottom Al plate	BTU/Ft ² ·hr	
Serial No	Heat Flux	Temp °C
96041630	118.7656	174.0
96041631	104.8063	174.0
96041632	114.4042	174.1
96041633	90.5774	174.1

Top Al plate		
9550642	58.5726	24.2
9550641	84.3077	24.5
9550639	99.6924	24.2
9550640	91.0304	24.4

Monitor Thermocouples (Channel no)	Temp °C
1	67.5
2	66.6
3	172.6
4	173.0
5	173.6
6	173.6
7	23.9
8	24.8
9	24.5
10	23.9

9/3/96 gp

0820hr

Thermal Conductivity experiment Run 8 on
dry Apache heap Tuff

Parameters are as follows:

Variable transducer setpoint - 90
 Waterbath setpoint - 23 °C
 Pressure on top Al plate - 5 ft²/lb
 Scan Interval - 10 min

9/5/96 gp

0800hr Results of TC experiment Run 8

Bottom Al plate	BTU/ft ² -hr	Temp °C
Serial No	Heat flux	
96041630	136.5523	205.2
" 31	126.6837	205.3
" 32	1268.5006	205.3
" 33	79.112.0310	205.3

Top Al plate		
9580642	79.7509	25.0
" 41	110.1680	25.5
" 39	111.5908	25.2
" 40	102.7014	25.4

Monitoring Thermocouples	
Channel no	Temp °C
1	29.1
2	28.1
3	204.2
4	204.0
5	205.1
6	205.0
7	24.8
8	25.5
9	25.3
10	24.8

9/5/96 gp

0810 hr

Thermal Conductivity experiment Run 9
on dry Apache Leap tuff

Parameters are as follows:

Variable temperature setpoint	-80
Waterbath setpoint	-23.0°C
Pressure on top plate	-5 ft lbs
Scan Interval	-10 min

9/6/96 JP

Results of TC experiment Run 9

Bottom Al plate	BTU/ft ² -hr	Temp °C
Serial No	Heat Flux	
96041630	99.1475	174.9
" 31	101.8552	174.9
" 32	—	175.0
" 33	87.1884	174.9
24 JP 9/9/96		
Top Al plate		
95J0642	63.7063	24.4
" 41	86.5999	24.7
" 39	87.5334	24.5
" 40	81.3310	24.7

Monitoring Thermocouples
Channel No

Channel No	Temp °C
1	67.6
2	67.1
3	173.8
4	174.0
5	174.7
6	174.5
7	24.3
8	24.9
9	25.0
10	24.3

9/9/96 JP

0800 hrs

Thermal Conductivity experiment Run 10
on dry Apache Leap Tuff

Parameters are as follows:

Variable temperature setpoint	- 70
Waterbath setpoint	- 23°C
Pressure on top plate	- 5 psia
Scan Interval	- 10 min

9/11/96 JP

0840 hrs

Results of TC Experiment Run 10

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	76.0859	145.5
" 31	77.4744	145.5
" 32	—	145.6
" 33	65.1570	145.6

Top Al plate		
95J0642	48.7880	23.6
" 41	67.3827	23.9
" 39	66.9175	23.8
" 40	62.3581	23.9

Monitoring Thermocouples (Channel No)	Temp °C
1	59.0
2	58.0
3	144.2
4	144.5
5	144.9
6	144.8
7	23.6
8	24.1
9	24.1
10	23.6

9/11/96 JP

0845hr

Thermal Conductivity Experiment Run 11
on dry Apache Leap Tuff

Parameters are as follows:

Variable transformer setpoint - 60
 Waterbath setpoint - 23°C
 Pressure on top Al plate - 5.5 ± 1.6
 Scan Interval - 10 min

9/16/96 JP

1540hr Results of TC Experiment Run 11

Bottom Al plate Serial No	Heat flux BTU/hr ² -in	Temp °C
96041630	58.6125	121.9
" 31	58.8450	122.0
" 32	—	122.0
" 33	49.4404	122.0

Top Al plate		
95J0642	38.5830	23.4
" 41	54.2689	23.6
" 39	53.5807	23.5
" 40	49.3327	23.7

Monitoring Thermocouple Channel No	Temp °C
1	52.3
2	51.5
3	120.7
4	121.0
5	121.4
6	121.3
7	23.6
8	23.9
9	23.9
10	23.5

9/14/96 gp

1545

Thermal Conductivity Experiment Run 12
on dry Apollo Leap Tuff

Parameters

Variable transformer setpoint - 50
 Waterbath setpoint - 23°C
 Pressure on top Al plate - 5 ft/lb
 Spec Interval - 10 min

9/18/96 gp

0800hr Results of TC Experiment Run 12

Bottom Al plate Serial No	Heat flux BTU/ft ² -hr	Temp °C
96041630	41.8428	94.9
" 31	40.0429	95.0
" 32	—	95.0
" 33	32.7399	94.9

Top Al plate Serial No	Heat flux BTU/ft ² -hr	Temp °C
9550642	27.0595	22.5
" 41	37.7668	22.7
" 39	38.0184	22.6
" 40	34.5651	22.7

Monitoring Thermocouples Channel No	Temp °C
1	43.1
2	42.6
3	94.1
4	94.3
5	94.7
6	94.6
7	22.6
8	22.8
9	22.7
10	22.5

9/18/96 JP

0800hr

Thermal Conductivity Experiment Run 13
on dry Apache Leap Tuff

Parameters

Variable transducer output - 40
 Watertank output - 23°C
 Pressure on top Al plate - 5 ft 16
 Scan Interval - 10 min

9/20/96 JP

0800hr Results of TC experiment Run 13

Bottom Al plate Serial No	Heat Flux BTU/Ft ² -hr	Temp °C
76041630	28.1665	69.9
" 31	21.9637	69.9
" 32	—	69.9
" 33	18.0905	69.9

Top Al plate		
955042	17.1918	21.9
" 41	23.9464	22.0
" 39	24.1767	22.0
" 40	21.9712	22.0

Monitoring Thermocouples Channel No	Temp °C
1	36.2
2	35.5
3	69.3
4	69.4
5	69.7
6	69.6
7	22.0
8	22.2
9	22.1
10	21.9

9/20/96 gp

0800 hrs

Thermal Conductivity Experiment Run 14
dry Apache Leap Tuff

Parameters

Variable transformer setpoint - 30
 Waterbath setpoint - 23°C
 Pressure on top Al plate - 5 ft/lb
 Scan Interval - 10 min

9/23/96 gp

0805 hrs

Results of TC Experiment Run 14 gp 9/23/96

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	16.7014	49.6
" 31	12.3603	49.6
" 32	—	49.6
" 33	9.6621	49.7

Top Al plate		
95J042	9.7431	21.5
" 41	13.9539	21.6
" 39	13.6951	21.6
" 40	12.6049	21.6

Mounting Thermocouples Channel No	Temp °C
1	36.9
2	30.1
3	49.3
4	49.4
5	49.6
6	49.5
7	21.7
8	21.8
9	21.7
10	21.6

9/23/96 gp

0810hr

Thermal Conductivity Experiment Run 15
Dry Apache Deep Tug

Parameters

Variable frequency setpoint - 90
 Watertrub setpoint - 23°C
 Pressure on top Al plate - 5 Fx16
 Scan Interval - 15 min

9/25/96 gp

0800hr

Results of TC Experiment Run 15

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	119.5305	202.2
" 31	130.7246	202.3
" 32	-	202.4
" 33	108.7493	202.4

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
955042	78.3287	25.3
" 41	111.9055	25.7
" 39	107.5794	25.5
" 40	98.8020	25.7

Monitor Thermocouples Channel No	Temp °C
1	80.4
2	76.1
3	201.1
4	201.1
5	202.2
6	202.0
7	25.2
8	25.8
9	25.4
10	24.8

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 10)						
$Q = K_T(dT/dL)$						
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	145.5	0.96	139.68	412.88	76.086	22.293
96041631	145.5	0.96	139.68	412.88	77.474	22.700
96041632	145.6	0.96	139.776	412.976	0.000	0.000
96041633	145.6	0.96	139.776	412.976	65.157	19.091
Top						
95J0642	23.6	1.04	24.544	297.744	48.788	14.295
95J0641	23.9	1.04	24.856	298.056	67.383	19.743
95J0639	23.8	1.04	24.752	297.952	66.918	19.607
95J0640	23.9	1.04	24.856	298.056	62.358	18.271
$Q =$	19.429 W/Ft^2	209.134 W/m^2				
$dT =$	114.98 K					
$dL =$	0.5208 Ft	0.15873984 m				
$K_T =$	0.289 \pm	0.03017 $W/m-K$				

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 11)						
$Q = K_T(dT/dL)$						
where						
Q = heat transfer per unit area (W/Ft^2)						
K_T = thermal conductivity ($W/m-K$)						
dT = temperature difference between bottom and top sensors (K)						
dL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	121.9	0.97	118.243	391.443	58.613	17.173
96041631	122	0.97	118.34	391.54	58.845	17.242
96041632	122	0.97	118.34	391.54	0.000	0.000
96041633	122	0.97	118.34	391.54	49.440	14.486
Top						
95J0642	23.4	1.04	24.336	297.536	38.583	11.305
95J0641	23.6	1.04	24.544	297.744	54.269	15.901
95J0639	23.5	1.04	24.44	297.64	53.581	15.699
95J0640	23.7	1.04	24.648	297.848	49.333	14.454
$Q =$	15.180 W/Ft^2					163.402 W/m^2
$dT =$	93.824 K					
$dL =$	0.5208 Ft					0.15873984 m
$K_T =$	0.276 \pm		0.02895 $W/m-K$			

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 12)						
$Q = K_T(dT/dL)$						
where Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/Ft ² -Hr	Convert to W/Ft ² 1Btu/Hr = 0.293W
Bottom						
96041630	94.9	0.98	93.002	366.202	41.843	12.260
96041631	95	0.98	93.1	366.3	40.043	11.733
96041632	95	0.98	93.1	366.3	0.000	0.000
96041633	94.9	0.98	93.002	366.202	32.740	9.593
Top						
95J0642	22.5	1.04	23.4	296.6	27.060	7.928
95J0641	22.7	1.04	23.608	296.808	37.767	11.066
95J0639	22.6	1.04	23.504	296.704	38.018	11.139
95J0640	22.7	1.04	23.608	296.808	34.565	10.128
Q =	10.549 W/Ft ²					113.557 W/m ²
dT =	69.521 K					
dL =	0.5208 Ft					0.15873984 m
K _T =	0.259 ± 0.02723 W/m-K					

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 13)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1 Btu/Hr = 0.293W	
Bottom							
96041630	69.9	1	69.9	343.1	28.167	8.253	
96041631	69.9	1	69.9	343.1	21.964	6.435	
96041632	69.9	1	69.9	343.1	0.000	0.000	
96041633	69.9	1	69.9	343.1	18.091	5.301	
Top							
95J0642	21.9	1.04	22.776	295.976	17.192	5.037	
95J0641	22	1.04	22.88	296.08	23.946	7.016	
95J0639	22	1.04	22.88	296.08	24.177	7.084	
95J0640	22	1.04	22.88	296.08	21.971	6.438	
Q =		6.509 W/Ft^2				70.065 W/m^2	
dT =		47.046 K					
dL =		0.5208 Ft				0.15873984 m	
K _T =		0.236 ±		0.02494 W/m-K			

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap Tuff (Run 14)

$$Q = K_T(dT/dL)$$

where

Q = heat transfer per unit area (W/Ft^2)

K_T = thermal conductivity ($W/m-K$)

dT = temperature difference between bottom and top sensors (K)

dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1 Btu/Hr = 0.293W
Bottom						
96041630	49.6	1.02	50.592	323.792	16.701	4.894
96041631	49.6	1.02	50.592	323.792	12.360	3.622
96041632	49.6	1.02	50.592	323.792	0.000	0.000
96041633	49.7	1.02	50.694	323.894	9.662	2.831
Top						
95J0642	21.5	1.04	22.36	295.56	9.743	2.855
95J0641	21.6	1.04	22.464	295.664	13.954	4.088
95J0639	21.6	1.04	22.464	295.664	13.695	4.013
95J0640	21.6	1.04	22.464	295.664	12.605	3.693

$$Q = 3.714 \text{ W/Ft}^2$$

$$39.974 \text{ W/m}^2$$

$$dT = 28.18 \text{ K}$$

$$dL = 0.5208 \text{ Ft}$$

$$0.15873984 \text{ m}$$

$$K_T = 0.225 \pm 0.02382 \text{ W/m-K}$$

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap Tuff (Run 15)

$$Q = K_T(dT/dL)$$

where

Q = heat transfer per unit area (W/Ft^2)

K_T = thermal conductivity ($W/m-K$)

dT = temperature difference between bottom and top sensors (K)

dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1 Btu/Hr = 0.293W
Bottom						
96041630	202.2	0.94	190.068	463.268	119.531	35.022
96041631	202.3	0.94	190.162	463.362	130.725	38.302
96041632	202.4	0.94	190.256	463.456	0.000	0.000
96041633	202.4	0.94	190.256	463.456	108.449	31.776
Top						
95J0642	25.3	1.04	26.312	299.512	78.329	22.950
95J0641	25.7	1.04	26.728	299.928	111.910	32.789
95J0639	25.5	1.04	26.52	299.72	107.579	31.521
95J0640	25.7	1.04	26.728	299.928	98.802	28.949

$$Q = 31.616 \text{ W/Ft}^2$$

$$340.320 \text{ W/m}^2$$

$$dT = 163.61 \text{ K}$$

$$dL = 0.5208 \text{ Ft}$$

$$0.15873984 \text{ m}$$

$$K_T = 0.330 \pm 0.03432 \text{ W/m-K}$$

9/25/96 gp

0800hr

Thermal Conductivity Experiment Run 16
Dry Apache heap tuff

Parameter

Variable transducer setpoint - 90
 Waterbath setpoint - 90°C
 Pressure on top Al plate - 55 ± 1b
 Scan Interval - 15 min

9/27/96 gp

0800hr.

Results of TC experiment Run 16

Bottom Al plate Serial No	Heat flux BTU/ft ² -hr	Temp °C
96041630	96.8734	217.8
" 31	89.2305	217.9
" 32	-	218.0
" 33	121.5890	217.9

Top Al plate	Heat flux	Temp °C
95J042	86.8202	60.2
" 41	114.8026	60.1
" 39	111.1999	60.1
" 40	104.2579	60.0

Monitoring Thermocouple Channel No	Temp °C
1	86.4
2	81.5
3	216.7
4	216.5
5	217.8
6	217.5
7	57.7
8	56.8
9	57.4
10	58.4

8/27/96 gp

0800

Thermal conductivity experiment Run 17
Dry Apache Leap Tuzo

Parameters

Variable frequency output - 70
 Waterbath output - 30°C
 Pressure on top Al plate - 5 ft lb
 Scan Interval - 15 min

8/30/96 gp

0800 hrs

Results of TC experiment Run 17

Bottom Al plate Sens No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	57.2942	150.8
" 31	54.8957	150.9
" 32	-	150.9
" 33	74.3767	150.9

Top Al plate

95T 042	50.8228	31.0
" 41	70.0422	31.3
" 39	69.5393	31.2
" 40	64.4171	31.3

Monitor Thermocouples

Channel No

Temp °C

1	62.2
2	62
3	149.5
4	149.7
5	150.3
6	150.3
7	30.5
8	30.4
9	30.9
10	31.0

9/30/96 JF

0800hr

Thermal Conductivity Experiment Run 18
Dry Apache Leap tuff

Parameters

Variable temperature setpoint - 70
 Waterbath temperature - 95°C
 Pressure on top Al plate - 5.5 ± 1.6
 Scan Interval - 15 min

10/1/96 JF

0930hr

Results of TC Experiment Run 18

Bottom Al plate Serial No	Heat flux BTU/ft ² /hr	Temp °C
96041630	51.2334	159.3
" 31	46.1556	159.4
" 32	-	159.4
" 33	68.1088	159.4

Top Al plate

955042	46.8882	56.8
" 41	66.4480	56.7
" 39	63.9321	56.7
" 40	60.4193	56.7

Monitoring Thermocouple Channel No	Temp °C
1	66.3
2	60.6
3	158.0
4	158.0
5	158.8
6	158.7
7	54.6
8	54.2
9	54.4
10	55.5

10/1/96 JP

0930hr

Thermal Conductivity Experiment Run 19
Dry Apache Deep Tuff

Parameter

Variable temperature setpoint - 60
 Water bath setpoint - 95°C
 Pressure - top Al plate - 5 Fx1b
 Scan Interval - 15 min

10/3/96 JP

0800hr

Results of TC experiment Run 19

Bottom Al plate Serial no	Heat Flux BTU/Ft ² /hr	Temp °C
96041630	37.1212	134.2
" 31	37.1564	134.2
" 32	-	134.2
" 33	47.8006	134.2

Top Al plate		
953042	34.1604	56.2
" 41	49.6176	56.0
" 36	46.9747	56.1
" 40	45.1120	56.0

Monitoring Thermocouples Channel no	Temp °C
--	---------

1	58.6
2	53.7
3	132.8
4	132.9
5	133.5
6	133.3
7	54.1
8	53.5
9	53.8
10	54.8

10/3/96 JP

0800hrs.

Thermal Conductivity Experiment Run 20
Dry 45hr long Tuff

Parameters

Variable tungsten output	-50
Waterbath temp	-95°C
Pressure on top Al plate	-5 ft/lb
Scan interval	-15 min

10/5/96 JP

0800 Results of TC experiment Run 20

Bottom Al plate Sens No	Heat Flux BTU/Fe ² -hr	Temp ° C
96041630	24.5847	111.1
" 31	24.8986	111.1
" 32	—	111.1
" 33	32.7451	111.1

Top Al plate Sens No	Heat Flux BTU/Fe ² -hr	Temp ° C
955042	24.8690	54.0
" 41	36.9489	53.8
" 39	34.0667	53.9
" 40	33.8169	53.8

Mounting Thermocouple Channel No	Temp ° C
1	51.5
2	47.0
3	109.9
4	110.1
5	110.5
6	110.5
7	51.7
8	51.1
9	52.0
10	52.9

10/5/96 JP

0805hr

Thermal Conductivity Experiment Run 21
Dry Asphalt heap top

Parameters:

Variable frequency setpoint - 40
 Waterback temp - 95°C
 Pressure on top Al plate - 5.5 ft lb
 Scan Interval - 25°C

10/7/96 JP

0820hr Results of TC experiment Run 21

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	12.4210	86.1
" 31	13.0401	86.1
" 32	-	86.1
" 33	16.9400	86.1

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
955042	13.7815	53.1
" 41	21.7042	52.9
" 35	19.1449	53.1
" 40	19.3879	52.9

Monitoring Thermocouples Channel No	Temp °C
1	43.5
2	40.1
3	85.4
4	85.5
5	85.9
6	85.7
7	51.1
8	50.3
9	51.2
10	52.1

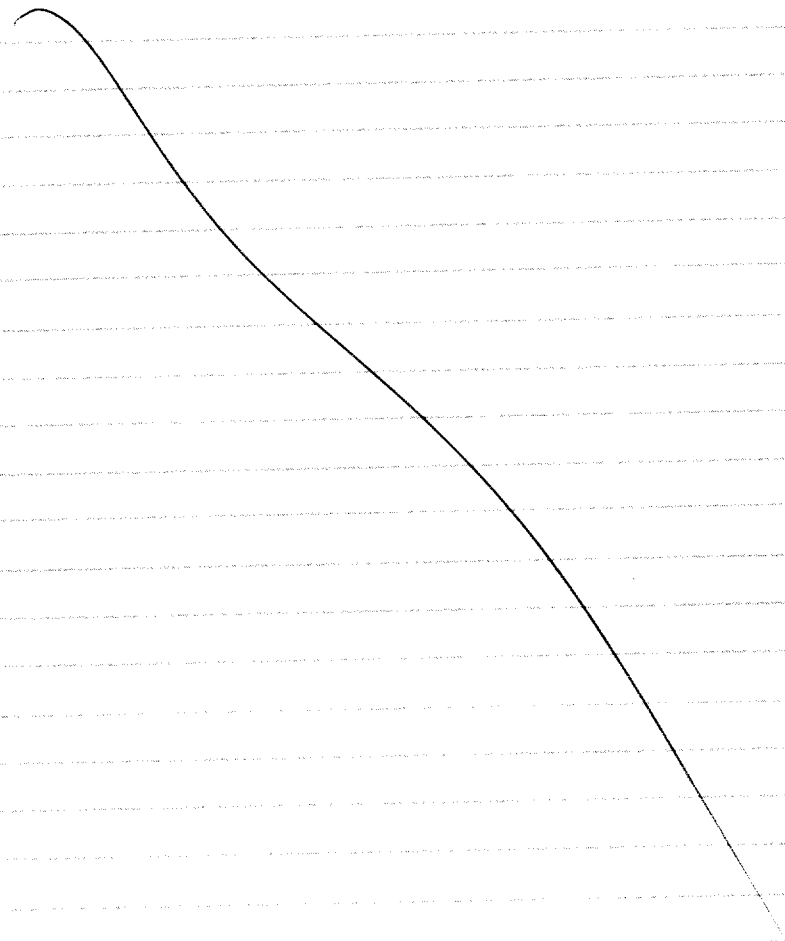
10/7/96 JP

0830 hr

Thermal Conductivity Experiment Run 22

Parameters

Variable temperature setpoint - 40
 Waterbath temperature - 40°C
 Membrane on top Al plate - 5 ft-lb
 Scan Interval - 15 min



10/9/96 JP

0800 hr

Results of TC experiment Run 22

Bottom Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	14.4430	76.9
" 31	15.0579	76.9
" 32	—	76.9
" 33	19.8084	76.9

Top Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
955042	15.0065	38.1
" 41	21.3092	38.0
" 39	20.3588	38.1
" 40	19.3534	38.1

Monitoring Thermocouples Channel No	Temp °C
1	39.0
2	35.4
3	76.2
4	76.3
5	76.6
6	76.6
7	37.7
8	37.1
9	37.4
10	37.6

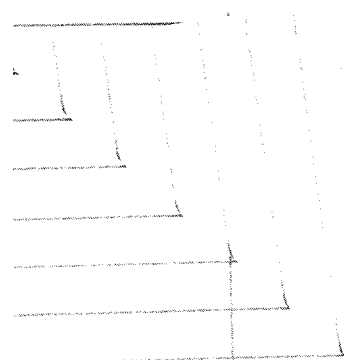
10/9/96 JP

0800 hr

Thermal Conductivity Experiment Run 23
Dry Apple heap temp

Parameters:

Variable transducer output - 80 JP 10/9/96
 Waterbath output - ~~40°C~~ 95°C
 Power on top Al plate - 5 ft/lb
 Scan Interval - 15 min



10/10/96 JP

0810 hr

Results of TC experiment Run 23

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp ^o C
96041030	64.6628	173.6
" 31	62.4705	173.6
" 32	-	173.6
" 33	88.2036	173.6

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp ^o C
955042	54.4511	54.7
" 41	75.2109	54.7
" 39	75.6271	54.6
" 40	69.8402	54.6

Monitoring thermocouples Channel No	Temp ^o C
1	20.8
2	64.6
3	172.3
4	172.1
5	173.2
6	173.2
7	52.7
8	51.6
9	52.4
10	53.7

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap Tuff (Run 17)

$$Q=K_T(dT/dL)$$

where

Q =heat transfer per unit area (W/Ft^2)

K_T = thermal conductivity ($W/m-K$)

dT = temperature difference between bottom and top sensors (K)

dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	150.8	0.96	144.768	417.968	57.294	16.787
96041631	150.9	0.96	144.864	418.064	54.896	16.084
96041632	150.9	0.96	144.864	418.064	0.000	0.000
96041633	150.9	0.96	144.864	418.064	74.377	21.792
Top						
95J0642	31	1.035	32.085	305.285	50.823	14.891
95J0641	31.3	1.035	32.3955	305.596	70.042	20.522
95J0639	31.2	1.035	32.292	305.492	69.539	20.375
95J0640	31.3	1.035	32.3955	305.596	64.417	18.874
Q =	18.475 W/Ft^2	198.872 W/m^2				
dT =	112.55 K					
dL =	0.5208 Ft	0.15873984 m				
$K_T =$	0.280 ±	0.02935 $W/m-K$				

Thermal Conductivity calculation using Fourier equation

Sample = Apache Leap Tuff (Run 19)

$$Q = K_T (dT/dL)$$

where

- Q = heat transfer per unit area (W/Ft^2)
- K_T = thermal conductivity ($W/m-K$)
- dT = temperature difference between bottom and top sensors (K)
- dL = distance between bottom and top sensors (m)

Sensor readings

Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	134.2	0.97	130.174	403.374	37.121	10.877
96041631	134.2	0.97	130.174	403.374	37.156	10.887
96041632	134.2	0.97	130.174	403.374	0.000	0.000
96041633	134.2	0.97	130.174	403.374	47.801	14.006
Top						
95J0642	56.2	1.02	57.324	330.524	34.160	10.009
95J0641	56	1.02	57.12	330.32	49.618	14.538
95J0639	56.1	1.02	57.222	330.422	46.975	13.764
95J0640	56	1.02	57.12	330.32	45.112	13.218
Q =	12.471 W/Ft^2					
dT =	72.977 K					
dL =	0.5208 Ft					
		0.15873984 m				
$K_T =$	0.292 \pm	0.03050 $W/m-K$				

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 20)						
$Q = K_T(dT/dL)$						
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	111.1	0.97	107.767	380.967	24.585	7.203
96041631	111.1	0.97	107.767	380.967	24.899	7.295
96041632	111.1	0.97	107.767	380.967	0.000	0.000
96041633	111.1	0.97	107.767	380.967	32.745	9.594
Top						
95J0642	54	1.02	55.08	328.28	24.869	7.287
95J0641	53.8	1.02	54.876	328.076	36.949	10.826
95J0639	53.9	1.02	54.978	328.178	34.067	9.982
95J0640	53.8	1.02	54.876	328.076	33.817	9.908
$Q =$	8.871 W/Ft^2				95.487 W/m^2	
$dT =$	52.815 K					
$dL =$	0.5208 Ft				0.15873984 m	
$K_T =$	0.287 \pm		0.03000 $W/m-K$			

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 21)						
$Q = K_T (dT/dL)$						
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1 Btu/Hr = 0.293W
Bottom						
96041630	86.1	0.99	85.239	358.439	12.421	3.639
96041631	86.1	0.99	85.239	358.439	13.040	3.821
96041632	86.1	0.99	85.239	358.439	0.000	0.000
96041633	86.1	0.99	85.239	358.439	16.940	4.963
Top						
95J0642	53.1	1.02	54.162	327.362	13.782	4.038
95J0641	52.9	1.02	53.958	327.158	21.704	6.359
95J0639	53.1	1.02	54.162	327.362	19.145	5.609
95J0640	52.9	1.02	53.958	327.158	19.388	5.681
$Q =$		4.873 W/Ft^2			52.454 W/m^2	
$dT =$		31.179 K				
$dL =$		0.5208 Ft			0.15873984 m	
$K_T =$		0.287 \pm			0.02801 $W/m-K$	

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 22)						
$Q=K_T(dT/dL)$						
where Q =heat transfer per unit area (W/ft^2)						
K_T = thermal conductivity (W/m-K)						
dT = temperature difference between bottom and top sensors (K)						
dL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp °C	Multi- factor	Correct Temp	Temp °K	Heat flow Btu/ ft^2 -Hr	Convert to W/ ft^2 1 Btu/Hr = 0.293W
Bottom						
96041630	76.9	0.99	76.131	349.331	14.443	4.232
96041631	76.9	0.99	76.131	349.331	15.058	4.412
96041632	76.9	0.99	76.131	349.331	0.000	0.000
96041633	76.9	0.99	76.131	349.331	19.808	5.804
Top						
95J0642	38.1	1.02	38.862	312.062	15.007	4.397
95J0641	38	1.02	38.76	311.96	21.309	6.244
95J0639	38.1	1.02	38.862	312.062	20.399	5.977
95J0640	38.1	1.02	38.862	312.062	19.393	5.682
Summary:						
Q =		5.250 W/ft^2			56.508 W/m^2	
dT =		37.295 K				
dL =		0.5208 Ft			0.15873984 m	
Final Results:						
K_T =		0.241 ±			0.02535 W/m-K	

Thermal Conductivity calculation using Fourier equation									
Sample = Apache Leap Tuff (Run 23)									
$Q = K_T(dT/dL)$									
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)							
Sensor readings									
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W			
Bottom									
96041630	173.6	0.95	164.92	438.12	64.663	18.946			
96041631	173.6	0.95	164.92	438.12	62.471	18.304			
96041632	173.6	0.95	164.92	438.12	0.000	0.000			
96041633	173.6	0.95	164.92	438.12	88.204	25.844			
Top									
95J0642	54.7	1.02	55.794	328.994	54.451	15.954			
95J0641	54.7	1.02	55.794	328.994	75.211	22.037			
95J0639	54.6	1.02	55.692	328.892	75.027	21.983			
95J0640	54.6	1.02	55.692	328.892	69.840	20.463			
$Q =$	20.504 W/Ft^2		220.715 W/m^2						
$dT =$	109.18 K								
$dL =$	0.5208 Ft		0.15873984 m						
$K_T =$	0.321 \pm		0.03339 $W/m-K$						

11/1/96 JF

Apache Leap Tuff Saturation

Obj - saturate Apache leap tuff with water in order to perform saturated thermal conductivity measurements.

Method - saturation using vacuum suction.

Equipment & materials

- crushed Apache Leap Tuff (1.6 - 4 cm size)
- vacuum chamber
- vacuum pump
- CO_2 (gas)
- deaerated H_2O

Procedure

- ① loaded crushed tuff into vacuum chamber and sealed chamber.
- ② Pulled a vacuum of about -30 inches of Hg for 15 minutes.
- ③ Release vacuum & introduce CO_2 gas for about 15 min.
- ④ Repeat steps 2 & 3 several times.
- ⑤ Introduce deaerated water into chamber until full.
- ⑥ Repeated steps 2 & 3 several times over about 2 weeks.
- ⑦ Removed crushed tuff from chamber and placed in DI water to maintain saturation.

12/13/96 JP

Thermal conductivity cell was modified for saturated measurements by sealing with silicon sealant. Before loading the crushed rock sample the cell was filled with water and heated to ensure that no loads developed.

Saturated thermal conductivity measurements on Apache Leap crushed tuff will be conducted in the same manner as those for the dry Apache Leap tuff.

12/16/96 JP

0930 hr

Thermal Conductivity Experiment Run 24
Totally saturated Apache heap Thg

Parameter:

Variable transducer setpoint - 40-100 JP 1/6/97
Waterbath temp - 23°C 5°C JP 1/6/97
Pressure on top AI plate - 55 ± 165
Scan Interval - 15 min



1/6/97

0800 hr

Results of TC experiment Run 24

Bottom AI plate	Heat Flux	Temp
Serial No	BTU/Ft ² ·hr	°C
96041630	289.8323	49
31	352.3846	49.2
32	—	49.2
33	379.3643	49.6

Top AI plate		
Serial No	Heat Flux	Temp
955642	198.7233	35.4
41	245.8960	35.9
39	180.3267	35.6
40	176.6103	35.6

Monitor Thermocouples	Temp °C
Channel No	
1	89.2
2	35.6
3	48.3
4	47.8
5	47.0
6	52.5
7	38.7
8	36.9
9	37.3
10	38.4

1/6/97 JP

0830hr JP
Thermal Conductivity Experiment Run 25
Saturated Asphaltic base Taff

Parameter JP 1/9/97
Variable temperature setpoint - ~~100~~ 108
Waterbath Temperature - ~~23°C~~ 15°C
Pressure ~ top Al plate - 5 ft lbs
Scan interval - 15 min

1/9/97 JP

1030hr
Results of TC experiment Run 25

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	109.1316	35.4
31	154.1018	35.4
32	169.5197 JP 1/9/96	35.3
33	169.5197	35.3
Top Al plate 955042	179.5019	29.7
41	209.3699	30.0
39	168.3686	29.6
40	152.5256	29.4

Monitor Thermocouple Cable No	Temp °C
1	55.2
2	25.5
3	34.1
4	33.6
5	34.2
6	36.6
7	28.3
8	28.6
9	28.2
10	28.9

I have reviewed this notebook
and find it in general
compliance with QAP-001.
There is adequate information
for another qualified
person to repeat the
activities.

E.C. Perry
1/8/87

1/9/97

1030 hrs off Thermal Conductivity Experiment Run 26
Submerged Apache Leap Tuff

Parameters

Variable temperature setpoint - 100
Waterbath Temp - 3°C
Pressure on top Al plate - 5.5 ± 1.6
Soak Interval - 15 min

1/13/97

0950 hrs Results of TC experiment Run 26

Bottom Al plate Serial No	Heat Flux BTU/ft ² hr	Temp °C
96.041630	-	46.3
31	348.3167	46.2
32	-	46.1
33	407.5022	46.1

Top Al plate Serial No	Heat Flux BTU/ft ² hr	Temp °C
95.5042	341.4901	34.9
41	340.5578	35.1
39	347.0437	35.1
40	295.2863	34.7

Monitoring Thermocouples

Thermocouple	Temp °C
1	85.14
2	31.6
3	44.5
4	44.4
5	45.2
6	49.0
7	34.9
8	35.4
9	34.6
10	35.4

1/13/97 1000hr Thermal Conductivity Experiment Run 27
Saturated Apache Leap Tuff

Parameters

Variable Transducer setpoint 80
Waterbath Temp 3°C
Pressure ~ Top AI plate 5 ft lbs.

1/14/97 0825hr

Results of TC experiment Run 27

Bottom AI plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	208.5381	37.6
31	265.9650	37.4
32	—	37.3
33	317.8670	37.5

Top AI plate

955042	302.8864	28.9
41	295.3244	29.2
39	263.8976	28.7
40	241.8084	28.5

Monitoring Thermocouples

	Temp °C
1	12.3
2	31.2
3	36.0
4	36.3
5	35.3
6	39.1
7	21.7
8	28.1
9	27.4
10	23.0

1/14/97 0830hr Thermal Conductivity Experiment Run 28
Saturated Apache Leap Tuff

Parameters

Variable Transducer setpoint 60
Waterbath Temp setpoint 3°C
Pressure ~ Top AI plate 5 ft lbs

1/15/97 0900hr

Results of TC experiment Run 28

Bottom AI plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	137.6004	21.2
31	163.5164	21.3
32	—	21.3
33	177.2036	21.3

Top AI plate

955042	106.5424	14.7
41	106.8520	14.9
39	95.7082	14.8
40	105.8362	14.8

Monitoring Thermocouples

	Temp °C
1	47.0
2	24.7
3	21.6
4	20.9
5	21.7
6	22.7
7	15.2
8	15.5
9	14.9
10	15.2

1/15/97 JP 0905hr Thermal Conductivity Experiment Run 29
Saturated Apache Leap Tuff

Parameters

Variable Transducer setpoint 60
Waterbath Temp setpoint 20°C
Pressure on Top Al plate 5 ft/lb

1/16/97 JP 1030hr Results of TC experiment Run 29

Bottom Al plate Serial No	Heat Flux BTU/HR ² ft	Temp °C
96041630	125.4369	29.8
31	149.0790	29.9
32	—	29.9
33	163.4704	29.9

Top Al plate Serial No	Heat Flux BTU/HR ² ft	Temp °C
955042	103.9139	24.4
41	106.3123	24.4
39	118.2999	24.5
40	94.8534	24.3

Monitoring Thermocouple	Temp °C
1	47.7
2	24.9
3	30.0
4	24.5
5	30.0
6	31.3
7	24.8
8	25.0
9	24.8
10	25.1

1/16/97 JP 1030hr Thermal Conductivity Experiment Run 30
Saturated Apache Leap Tuff

Parameters

Variable Transducer setpoint 50
Waterbath Temp setpoint 20°C
Pressure on Top Al plate 5 ft/lb

1/17/97 JP 0905hr Results of TC Experiment Run 30

Bottom Al plate Serial No	Heat Flux BTU/HR ² ft	Temp °C
96041630	80.6433	27.3
31	73.8381	27.2
32	116.1280 JP 11/17/97	27.2
33	116.1280	27.2

Top Al plate Serial No	Heat Flux BTU/HR ² ft	Temp °C
955042	98.2664	23.1
41	81.2476	23.0
39	95.6430	23.0
40	81.0470	22.9

Monitoring Thermocouple	Temp °C
1	42.9
2	25.6
3	27.2
4	27.0
5	27.0
6	28.1
7	23.0
8	23.0
9	23.1
10	23.1

1/17/97 pp 0910hr Thermal Conductivity Experiment Run 31
Saturated Asphalt Leach Tuff

Parameters

Variable Transformer Setpoint 45
Waterbath Temperature Setpoint 20°C
Pressure on Top plate 5 ft lbs

1/20/97 pp 0800hr Results of TC experiment Run 31

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	77.4291	25.8
31	86.8512	25.8
32	—	25.8
33	102.1762	25.8

Top Al plate

95J042	57.4254	22.1
41	57.6572	22.1
39	53.6021	22.1
40	62.4510	22.1

Monitoring Thermocouples

	Temp °C
40.0	
2	26.2
3	25.9
4	25.7
5	25.9
6	26.6
7	22.3
8	22.4
9	22.3
10	22.3

1/20/97 pp 0800hr Thermal Conductivity Experiment Run 32
Saturated Asphalt Leach Tuff

Parameters

Variable Transformer Setpoint 40
Waterbath Temp Setpoint 20°C
Pressure on Top Al plate 5 ft lbs

1/21/97 pp 0910hr Results of TC experiment Run 32

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	59.4150	24.4
31	49.4574	24.5
32	—	24.5
33	80.3687	24.4

Top Al plate

95J042	36.6105	21.3
41	50.8361	21.4
39	47.4361	21.4
40	51.2005	21.3

Monitoring Thermocouples

	Temp °C
1	36.6
2	25.6
3	24.6
4	24.4
5	24.6
6	25.2
7	21.6
8	21.6
9	21.5
10	21.6

1/21/97 gp 0915hr Thermal Conductivity Experiment Run 33
Saturated Asphalt Leep Tuff

Parameters
Variable Transducer setpoint 70
Waterbath temp setpoint 20°C
Pressure on top Al plate 5 ft/lb.

1/23/97 gp 1540hr Results of TC experiment Run 33

Bottom Al plate Serial No	Heat Flux BTU/Ft ² -hr	Temp °C
96041630	140.6570	35.7
31	252.3840	35.7
32	—	35.7
33	194.0759	35.6

Top Al plate Serial No	Heat Flux BTU/Ft ² -hr	Temp °C
955042	227.4126	29.4
41	227.9807	29.5
39	210.4418	29.4
40	174.5569	29.1

Monitoring Thermocouples	Temp °C
1	60.0
2	31.0
3	34.6
4	34.2
5	34.7
6	36.8
7	28.6
8	28.8
9	28.5
10	28.9

1/23/97 gp 1545hr Thermal Conductivity Experiment Run 34
Saturated Asphalt Leep Tuff

Parameters
Variable Transducer setpoint 90
Waterbath temp setpoint 20°C
Pressure on top Al plate 5 ft/lb

1/24/97 gp 1030hr Results of TC experiment Run 34

Bottom Al plate Serial No	Heat Flux BTU/Ft ² -hr	Temp °C
96041630	207.5612	46.9
31	244.7297	47.1
32	—	46.9
33	286.9400	47.0

Top Al plate Serial No	Heat Flux BTU/Ft ² -hr	Temp °C
955042	321.8171	38.2
41	328.2229	38.7
39	334.5226	38.5
40	294.8330	38.2

Monitoring Thermocouples	Temp °C
1	80.6
2	36.8
3	44.9
4	44.7
5	45.2
6	49.3
7	37.1
8	37.2
9	37.1
10	38.2

1/21/97 1200hr JP

Sample was removed from thermal conductivity cell. Both water & rock was removed. The matrix saturated Apache Leap tuff was immediately reloaded into the cell in separate of matrix saturated rock measurements. Alumina soil was placed to top of loaded sample to insure good contact between sample & Slur meter.

1/24/97 JP 1245hr Thermal Conductivity Experiment Run 35
Matrix Saturated Apache Leap Tuff

Parameters

Variable transducer setpoint 15
Watchdog temp setpoint 20°C
Pressure on top Al plate 5 ft 16

1/27/97 JP 0800hr Results of TC experiment Run 35

Bottom Al plate Serial No	Heat Flux DTU / Ft ² -h	Temp °C
96041630	12.1950	33
31	12.9861	33
32	+7.5 JP 1/27/97	33
33	17.5283	33

Top Al plate

Serial No	Heat Flux DTU / Ft ² -h	Temp °C
955042	14.9338	18.7
41	16.2295	18.7
39	12.3435	18.7
40	18.6482	18.7

Monitoring Thermocouples

Thermocouple	Temp °C
1	27.6
2	25.2
3	33.0
4	33.0
5	33.1
6	33.2
7	18.9
8	18.9
9	18.7
10	18.8

1/27/97 0805hr Thermal Conductivity Experiment Run 36
Matrix Substrate Apache Leap Tuff

Parameters

Variable transformer setpoint 25
Waterbath temperature setpoint 20°C
Pressure on top Al plate 5 ft lb

1/28/97 0805hr Results of TC experiment Run 36

Bottom Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	31.7899	46.1
31	34.6315	46.2
32	—	46.1
33	37.4044	46.2

Top Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
955042	23.1975	19.9
41	32.9430	20.0
39	18.0756	19.9
40	37.9512	20.0

Mounting Thermocouples Channel No	Temp °C
1	33.3
2	27.9
3	45.8
4	45.7
5	45.6
6	46.4
7	20.1 45.6
8	20.2 45.7
9	19.8
10	19.9

1/28/97 0810hr Thermal Conductivity Experiment Run 37
Matrix Substrate Apache Leap Tuff

Parameters

Variable transformer setpoint 35
Waterbath temperature setpoint 20°C
Pressure on Top Al plate 5 ft lb

1/29/97 0900hr Results of TC experiment Run 37

Bottom Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	63.4800	59.7
31	58.8665	59.9
32	—	60.0
33	60.1333	60.2

Top Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
955042	43.2547	23.0
41	86.3885	23.2
39	43.6202	23.0
40	76.3139	23.0

Mounting Thermocouples Channel No	Temp °C
1	42.1
2	32.7
3	39.0
4	60.4
5	58.8
6	60.8
7	23.0
8	23.4
9	21.8
10	22.7

1/29/97 JP 0900hr Thermal Conductivity Experiment Run 38
Mantle Saturated Apache Leap Tuff

Parameters
Variable Transformer Setpoint 30
Waterbath Temp Setpoint 20°C
Pressure on top Al plate 55 ± 16

1/30/97 JP 0800hr Results of TC experiment Run 38

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96 041630	47.0257	53.7
31	44.6665	53.9
32	—	53.9
33	53.5479	54.1

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
95 J042	27.9730	21.2
41	50.3687	21.3
39	30.1693	21.2
40	48.5736	21.2

Mounting Thermocouples	Temp °C
1	38.0
2	31.0
3	53.2
4	54.3
5	53.1
6	54.5
7	21.2
8	21.4
9	20.5
10	21.0

1/30/97 JP 0800hr Thermal Conductivity Experiment Run 39
Mantle Saturated Apache Leap Tuff

Parameters
Variable Transformer setpoint 40
Waterbath temp setpoint 20°C
Pressure on top Al plate 55 ± 16

1/31/97 JP 0800hr Results of TC experiment Run 39

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	88.2223	65.6
31	76.6760	65.7
32	—	65.9
33	82.9456	66.2

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
95 J042	47.7706	24.2
41	83.9961	24.4
39	57.0656	24.2
40	73.1280	24.1

Mounting Thermocouples	Temp °C
1	46.6
2	35.2
3	64.6
4	67.2
5	64.9
6	67.1
7	24.2
8	24.9
9	22.8
10	24.0

1/31/97 pp 0810hr Thermal Conductivity Experiment Run 40
Matrix Saturated Apache Leap Tuff

Parameters

Variable temperature setpoint 45
Waterbath temperature setpoint 20°C
Pressure on top Al plate 5.5 ± 1.6

2/1/97 pp 1200hr Results of TC experiment Run 40

Bottom Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	111.5246	70.1
31	134.6685	70.2
32	—	70.4
33	99.4483	70.9

Top Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
955042	59.0969	22.9
41	102.6903	23.3
39	71.3740	23.0
40	86.6941	22.9

Monitoring Thermocouples	Temp °C
1	50.7
2	37.5
3	69.0
4	72.6
5	69.2
6	72.2
7	23.0
8	24.2
9	24.3
10	22.9

2/1/97 pp 1205hr Thermal Conductivity Experiment Run 41
Matrix Saturated Apache Leap Tuff

Parameters

Variable temperature setpoint 50
Waterbath temp setpoint 20°C
Pressure on top Al plate 5.5 ± 1.6

2/2/97 pp 1200hr Results of TC experiment Run 41

Bottom Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
96041630	141.3503	74.5
31	144.4607	74.7
32	—	74.9
33	141.3194	75.4

Top Al plate Serial No	Heat Flux BTU/ft ² ·hr	Temp °C
955042	69.1566	24.9
41	146.4549	25.6
39	88.9339	25.0
40	120.9533	25.0

Monitoring Thermocouples	Temp °C
1	55.6
2	39.7
3	73.3
4	77.9
5	73.5
6	77.3
7	24.8
8	26.4
9	22.7
10	24.7

2/2/97 1205hr Thermal Conductivity Experiment Run 42
Matrix Saturated Apache Leap Tuff

Parameters
Variable transformer setpoint 60
Waterbath temp setpoint 20°C
Pressure on top Al plate 55 ± 1b

2/3/97 0805hr Results of TC experiment Run 42

Bottom Al plate Serial No	Heat Flux BTU/ft ² /hr	Temp °C	CH
96041630	241.9771	80.5	1
31	206.9798	81.1	2
32	—	81.2	3
33	171.3626	81.9	4
Top Al plate			
955042	159.6835	28.5	5
41	354.3392	29.8	6
39	164.2487	28.2	7
40	327.0279	28.7	8

Monitoring Thermocouples	Temp °C
1	62.5
2	41.4
3	78.9
4	85.9
5	79.1
6	84.4
7	27.1
8	29.3
9	24.7
10	27.5

2/3/97 0915hr Thermal Conductivity Experiment Run 43
Matrix Saturated Apache Leap Tuff

Parameters
Variable transformer setpoint 70
Waterbath temperature setpoint 5°C
Pressure on top Al plate 55 ± 1b

2/4/97 Results of TC experiment Run 43

Bottom Al plate Serial No	Heat Flux BTU/ft ² /hr	Temp °C
96041630	380.7802	88.7
31	281.9293	90.9
32	—	90.8
33	192.6807	94.5
Top Al plate		
955042	142.5125	19.9
41	112.6541	19.4
39	189.8350	19.7
40	104.4709	18.2

Monitoring Thermocouples	Temp °C
1	73.3
2	46.0
3	84.9
4	102.3
5	84.8
6	104.7
7	21.4
8	21.9
9	15.7
10	16.7

2/4/97 pp 0820hr Thermal Conductivity Experiment Run 44
Matrix Saturated Apache Leap Tuff

Parameters

Variable Transducer setpt 10
Waterbath temperature setpt 20°C
Pressure on Top Al plate 5 ft lb

Results of TC experiment Run 44

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C	Ch
96041630	7.3000	3.8737	1
31	1.8182	5.9087	2
32	-	-	3
33	6.0597	7.2859	4

Top Al plate

953042	-9.0060	-8.7447	5
41	-8.9966	-9.5192	6
39	-8.0553	7.3002	7
40	-9.3608	1.8182	8

Monitoring Thermocouples

Monitoring Thermocouples	Temp °C
1	25.6
2	24.5
3	28.6
4	28.8
5	28.7
6	28.9
7	18.6
8	18.6
9	18.5
10	18.4

2/6/97 M.H. 13:40 Thermal Conductivity Experiment Run 45
Matrix Saturated Apache Leap Tuff

Parameters

Variable Transducer setpt 20
H₂O bath temp setpt 20°C
Pressure on Top Al plate 5 ft lb

2/10/97 pp 0815hr Results of TC experiment Run 45

Bottom Al plate Serial #	Heat flux BTU/ft ² -hr	Temp °C
96041630	26.6430	43.6
31	14.9284	43.7
32	-	43.7
33	19.6783	43.9

Top Al plate

955042	19.4031	19.1
41	20.6916	19.1
39	17.8096	19.0
40	18.4103	19.0

Monitoring Thermocouples

Monitoring Thermocouples	Temp °C
1	31.8
2	28.5
3	43.3
4	44.1
5	43.3
6	44.3
7	19.3
8	19.4
9	18.8
10	19.0

2/10/97 gp 0820hr Thermal Conductivity Experiment Run 46
Matryx Saturated Apache Leaps Tuff

Parameters
Variable transformer setpoint 28
Waterbath temperature setpoint 20°C
Pressure - Top Al plate 5 ft + 16

2/11/97 gp 1435hr Results of TC experiment Run 46

Bottom Al plate Serial No	Heat Flux BTU/Fe ² -hr	Temp °C
96041630	52.4236	54.3
31	56.5790	54.6
32	—	54.6
33	36.0717	54.9

Top Al plate Serial No	Heat Flux BTU/Fe ² -hr	Temp °C
955042	29.2552	19.8
41	30.0276	19.8
39	29.6428	19.7
40	26.1327	19.6

Monitoring Thermocouple	Temp °C
1	37.1
2	31.4
3	53.5
4	55.4
5	53.5
6	56.0
7	20.2
8	20.3
9	19.4
10	19.5

2/11/97 gp 1435hr Thermal Conductivity Experiment Run 47
Matryx Saturated Apache Leaps Tuff

Parameters
Variable transformer setpoint 37
Waterbath temperature setpoint 20°C
Pressure - Top Al plate 5 ft + 16

2/13/97 gp 0800hr Results of TC experiment Run 47

Bottom Al plate Serial No	Heat Flux BTU/Fe ² -hr	Temp °C
96041630	103.6047	65.8
31	75.1815	66.4
32	—	66.5
33	58.3685	67.3

Top Al plate Serial No	Heat Flux BTU/Fe ² -hr	Temp °C
955042	58.0328	21.1
41	44.9997	20.9
39	51.1326	20.8
40	38.3499	20.5

Monitoring Thermocouple	Temp °C
1	44.8
2	35.3
3	64.3
4	68.7
5	67.2
6	69.6
7	21.7
8	21.6
9	20.0
10	20.3

2/13/97 JP Thermal Conductivity Experiment Run 48
Matry Substrate Apache Loop Tuff

Parameters

Variable transducer output 52470 JP 2/15/97
Waterbath temperature output 20°C
Pressure on Top Al plate 5 ftlb

2/15/97 JP 0920hr Results of TC experiment Run 48

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	162.6415	74.8
31	110.5683	76.0
32	—	76.0
33	85.1841	77.5

Top Al plate

Serial No	Heat Flux BTU/ft ² -hr	Temp °C
955042	77.7888	22.5
41	47.0360	22.0
39	82.3225	22.1
40	51.3370	21.5

Monitoring Thermocouples Temp °C

1	53.0
2	38.8
3	72.3
4	80.2
5	72.2
6	81.9
7	23.6
8	23.8
9	20.9
10	21.2

2/15/97 JP 0930hr Thermal Conductivity Experiment Run 49
Matry Substrate Apache Loop Tuff

Parameters

Variable transducer output 57
Waterbath Temp output 20°C
Pressure on Top Al plate 5 ftlb

2/17/95 JP 0800hr Results of TC experiment Run 49

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	272.4855	87.9
31	82.8858	91.9
32	—	89.5
33	148.3004	93.3

Top Al plate

Serial No	Heat Flux BTU/ft ² -hr	Temp °C
955042	151.4614	24.9
41	90.1441	23.7
39	166.1160	24.4
40	71.6752	23.0

Monitoring Thermocouples Temp °C

1	64.0
2	44.6
3	82.7
4	99.6
5	82.4
6	102.8
7	27.3
8	26.1
9	21.9
10	22.3

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 28)						
$Q = K_T(dT/dL)$						
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	21.2	1.04	22.048	295.248	137.600	40.317
96041631	21.3	1.04	22.152	295.352	163.516	47.910
96041632	21.3	1.04	22.152	295.352	0.000	0.000
96041633	21.3	1.04	22.152	295.352	177.204	51.921
Top						
95J0642	14.7	1.045	15.3615	288.562	106.592	31.232
95J0641	14.9	1.045	15.5705	288.771	106.852	31.308
95J0639	14.8	1.045	15.466	288.666	95.708	28.043
95J0640	14.8	1.045	15.466	288.666	105.836	31.010
$Q =$	37.391 W/Ft^2					402.491 W/m^2
$dT =$	6.66 K					
$dL =$	0.5 Ft					0.1524 m
$K_T =$	9.210 \pm		0.92231 $W/m-K$			

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 29)							
$Q = K_T(dT/dL)$							
where		Q =heat transfer per unit area (W/Ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors (K)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W	
Bottom							
96041630	29.8	1.038	30.9324	304.132	125.437	36.753	
96041631	29.9	1.038	31.0362	304.236	149.079	43.680	
96041632	29.9	1.038	31.0362	304.236	0.000	0.000	
96041633	29.9	1.038	31.0362	304.236	163.470	47.897	
Top							
95J0642	24.4	1.04	25.376	298.576	103.914	30.447	
95J0641	24.4	1.04	25.376	298.576	106.312	31.150	
95J0639	24.5	1.04	25.48	298.68	118.300	34.662	
95J0640	24.3	1.04	25.272	298.472	94.853	27.792	
Q =	36.054 W/Ft^2					388.098 W/m^2	
dT =	5.6343 K						
dL =	0.5 Ft					0.1524 m	
K_T =	10.498 \pm		1.05108 $W/m-K$				

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 30)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors (K)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1 Btu/Hr = 0.293W	
Bottom							
96041630	27.3	1.038	28.3374	301.537	80.643	23.628	
96041631	27.2	1.038	28.2336	301.434	73.838	21.635	
96041632	27.2	1.038	28.2336	301.434	0.000	0.000	
96041633	27.2	1.038	28.2336	301.434	116.128	34.026	
Top							
95J0642	23.1	1.04	24.024	297.224	98.266	28.792	
95J0641	23	1.04	23.92	297.12	81.248	23.806	
95J0639	23	1.04	23.92	297.12	95.643	28.023	
95J0640	22.9	1.04	23.816	297.016	81.047	23.747	
$Q =$	26.237 W/Ft^2					282.418 W/m^2	
$dT =$	4.3396 K						
$dL =$	0.5 Ft					0.1524 m	
$K_T =$	9.918 \pm		0.99312 $W/m-K$				

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 31)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors ($^{\circ}K$)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W	
Bottom							
96041630	25.8	1.038	26.7804	299.98	77.429	22.687	
96041631	25.8	1.038	26.7804	299.98	86.851	25.447	
96041632	25.8	1.038	26.7804	299.98	0.000	0.000	
96041633	25.8	1.038	26.7804	299.98	102.176	29.938	
Top							
95J0642	22.1	1.04	22.984	296.184	57.425	16.826	
95J0641	22.1	1.04	22.984	296.184	57.657	16.894	
95J0639	22.1	1.04	22.984	296.184	53.602	15.706	
95J0640	22.1	1.04	22.984	296.184	62.451	18.298	
$Q =$		20.828 W/Ft^2				224.196 W/m^2	
$dT =$		3.7964 K					
$dL =$		0.5 Ft				0.1524 m	
$K_T =$		9.000 \pm		0.90130 $W/m-K$			

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 32)						
$Q = K_T(dT/dL)$						
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/Ft^2-Hr	Convert to W/Ft^2 $1 Btu/Hr = 0.293W$
Bottom						
96041630	24.4	1.038	25.3272	298.527	59.415	17.409
96041631	24.5	1.038	25.431	298.631	49.457	14.491
96041632	24.5	1.038	25.431	298.631	0.000	0.000
96041633	24.4	1.038	25.3272	298.527	80.369	23.548
Top						
95J0642	21.3	1.04	22.152	295.352	36.611	10.727
95J0641	21.4	1.04	22.256	295.456	50.836	14.895
95J0639	21.4	1.04	22.256	295.456	47.436	13.899
95J0640	21.3	1.04	22.152	295.352	51.201	15.002
$Q =$	15.710	W/Ft^2		169.107 W/m^2		
$dT =$	3.1751	K				
$dL =$	0.5	Ft		0.1524 m		
$K_T =$	8.117 \pm	0.81299 $W/m-K$				

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 33)						
$Q = K_T(dT/dL)$						
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	35.7	1.03	36.771	309.971	140.657	41.213
96041631	35.7	1.03	36.771	309.971	252.384	73.949
96041632	35.7	1.03	36.771	309.971	0.000	0.000
96041633	35.6	1.03	36.668	309.868	194.076	56.864
Top						
95J0642	29.4	1.038	30.5172	303.717	227.413	66.632
95J0641	29.5	1.038	30.621	303.821	227.981	66.798
95J0639	29.4	1.038	30.5172	303.717	210.442	61.659
95J0640	29.1	1.038	30.2058	303.406	174.557	51.145
$Q =$	59.751 W/Ft^2					643.180 W/m^2
$dT =$	6.2799 K					
$dL =$	0.5 Ft					0.1524 m
$K_T =$	15.609 \pm		1.56215 $W/m-K$			

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 34)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors (K)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ ft^2 -Hr	Convert to W/ft^2 1Btu/Hr = 0.293W	
Bottom							
96041630	46.9	1.02	47.838	321.038	207.561	60.815	
96041631	47.1	1.02	48.042	321.242	244.730	71.706	
96041632	46.9	1.02	47.838	321.038	0.000	0.000	
96041633	47	1.02	47.94	321.14	286.590	83.971	
Top							
95J0642	38.2	1.022	39.0404	312.24	321.817	94.292	
95J0641	38.7	1.022	39.5514	312.751	328.223	96.169	
95J0639	38.5	1.022	39.347	312.547	334.523	98.015	
95J0640	38.2	1.022	39.0404	312.24	294.833	86.386	
$Q =$	84.479 W/ft^2					909.357 W/m^2	
$dT =$	8.6697 K						
$dL =$	0.5 Ft					0.1524 m	
$K_T =$	15.985 \pm		1.59981 $W/m-K$				

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 35)							
$Q = K_T(dT/dL)$							
where		Q =heat transfer per unit area (W/F ²) K_T = thermal conductivity (W/m-K) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/Ft ² -Hr	Convert to W/F ² 1Btu/Hr = 0.293W	
Bottom							
96041630	33	1.03	33.99	307.19	12.195	3.573	
96041631	33	1.03	33.99	307.19	12.986	3.805	
96041632	33	1.03	33.99	307.19	0.000	0.000	
96041633	33	1.03	33.99	307.19	17.528	5.136	
Top							
95J0642	18.7	1.04	19.448	292.648	14.934	4.376	
95J0641	18.7	1.04	19.448	292.648	16.230	4.755	
95J0639	18.7	1.04	19.448	292.648	12.344	3.617	
95J0640	18.7	1.04	19.448	292.648	18.648	5.464	
Q =		4.389 W/Ft ²				47.248 W/m ²	
dT =		14.542 K					
dL =		0.5 Ft				0.1524 m	
K _T =		0.495 ±		0.05082 W/m-K			

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 36)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W	
Bottom							
96041630	46.1	1.02	47.022	320.222	31.790	9.314	
96041631	46.2	1.02	47.124	320.324	34.632	10.147	
96041632	46.1	1.02	47.022	320.222	0.000	0.000	
96041633	46.2	1.02	47.124	320.324	37.404	10.959	
Top							
95J0642	19.9	1.04	20.696	293.896	23.198	6.797	
95J0641	20	1.04	20.8	294	32.943	9.652	
95J0639	19.9	1.04	20.696	293.896	18.076	5.296	
95J0640	20	1.04	20.8	294	37.951	11.120	
$Q =$	9.041 W/Ft^2					97.318 W/m^2	
$dT =$	26.325 K						
$dL =$	0.5 Ft					0.1524 m	
$K_T =$	0.563 \pm		0.05764 $W/m-K$				

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 37)							
$Q = K_T(dT/dL)$							
where		Q =heat transfer per unit area (W/Ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors (K)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi- factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/Ft^2-Hr	Convert to W/Ft^2 $1Btu/Hr = 0.293W$	
Bottom							
96041630	59.7	1.01	60.297	333.497	63.480	18.600	
96041631	59.9	1.01	60.499	333.699	58.867	17.248	
96041632	60	1.01	60.6	333.8	0.000	0.000	
96041633	60.2	1.01	60.802	334.002	60.133	17.619	
Top							
95J0642	23	1.04	23.92	297.12	43.255	12.674	
95J0641	23.2	1.04	24.128	297.328	86.389	25.312	
95J0639	23	1.04	23.92	297.12	43.620	12.781	
95J0640	23	1.04	23.92	297.12	76.394	22.383	
Q = 18.088 W/Ft^2 194.704 W/m^2							
dT = 36.577 K							
dL = 0.5 Ft 0.1524 m							
K _T = 0.811 ± 0.08242 W/m-K							

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 38)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors (K)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/Ft^2-Hr	Convert to W/Ft^2 $1 Btu/Hr = 0.293W$	
Bottom							
96041630	53.7	1.015	54.5055	327.706	47.026	13.779	
96041631	53.9	1.015	54.7085	327.909	44.667	13.087	
96041632	53.9	1.015	54.7085	327.909	0.000	0.000	
96041633	54.1	1.015	54.9115	328.112	53.548	15.690	
Top							
95J0642	21.2	1.04	22.048	295.248	27.973	8.196	
95J0641	21.3	1.04	22.152	295.352	50.369	14.758	
95J0639	21.2	1.04	22.048	295.248	30.169	8.840	
95J0640	21.2	1.04	22.048	295.248	48.574	14.232	
$Q =$	12.654	W/Ft^2				136.216 W/m^2	
$dT =$	32.635	K					
$dL =$	0.5	Ft				0.1524 m	
$K_T =$	0.636 \pm	0.06491 $W/m-K$					

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 39)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors ($^{\circ}C$) dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W	
Bottom							
96041630	65.6	1	65.6	338.8	88.222	25.849	
96041631	65.7	1	65.7	338.9	76.676	22.466	
96041632	65.9	1	65.9	339.1	0.000	0.000	
96041633	66.2	1	66.2	339.4	82.946	24.303	
Top							
95J0642	24.2	1.04	25.168	298.368	47.771	13.997	
95J0641	24.4	1.04	25.376	298.576	83.996	24.611	
95J0639	24.2	1.04	25.168	298.368	57.066	16.720	
95J0640	24.1	1.04	25.064	298.264	73.128	21.427	
$Q =$	21.339 W/Ft^2					229.698 W/m^2	
$dT =$	40.656 K						
$dL =$	0.5 Ft					0.1524 m	
$K_T =$	0.861 \pm		0.08740 $W/m-K$				

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 40)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W	
Bottom							
96041630	70.1	1	70.1	343.3	111.525	32.677	
96041631	70.2	1	70.2	343.4	134.669	39.458	
96041632	70.4	1	70.4	343.6	0.000	0.000	
96041633	70.9	1	70.9	344.1	99.448	29.138	
Top							
95J0642	22.9	1.04	23.816	297.016	59.097	17.315	
95J0641	23.3	1.04	24.232	297.432	102.690	30.088	
95J0639	23	1.04	23.92	297.12	71.374	20.913	
95J0640	22.9	1.04	23.816	297.016	86.694	25.401	
$Q =$	27.856 W/Ft^2					299.847 W/m^2	
$dT =$	46.454 K						
$dL =$	0.5 Ft					0.1524 m	
$K_T =$	0.984 \pm		0.09967 $W/m-K$				

Thermal Conductivity calculation using Fourier equation							
Sample = Apache Leap Tuff (Run 41)							
$Q = K_T(dT/dL)$							
where		Q = heat transfer per unit area (W/Ft^2)					
		K_T = thermal conductivity ($W/m-K$)					
		dT = temperature difference between bottom and top sensors (K)					
		dL = distance between bottom and top sensors (m)					
Sensor readings							
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/Ft^2-Hr	Convert to W/Ft^2 $1 Btu/Hr = 0.293W$	
Bottom							
96041630	74.5	1	74.5	347.7	141.350	41.416	
96041631	74.7	1	74.7	347.9	144.461	42.327	
96041632	74.9	1	74.9	348.1	0.000	0.000	
96041633	75.4	1	75.4	348.6	141.319	41.407	
Top							
95J0642	24.9	1.04	25.896	299.096	69.157	20.263	
95J0641	25.6	1.04	26.624	299.824	146.455	42.911	
95J0639	25	1.04	26	299.2	88.934	26.058	
95J0640	25	1.04	26	299.2	120.953	35.439	
$Q =$	35.689 W/Ft^2					384.162 W/m^2	
$dT =$	48.745 K						
$dL =$	0.5 Ft					0.1524 m	
$K_T =$	1.201 \pm		0.12141 $W/m-K$				

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 42)						
$Q = K_T(dT/dL)$						
where	Q = heat transfer per unit area (W/Ft^2) K_T = thermal conductivity ($W/m-K$) dT = temperature difference between bottom and top sensors (K) dL = distance between bottom and top sensors (m)					
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	80.5	0.99	79.695	352.895	241.977	70.899
96041631	81.1	0.99	80.289	353.489	206.980	60.645
96041632	81.2	0.99	80.388	353.588	0.000	0.000
96041633	81.9	0.99	81.081	354.281	171.363	50.209
Top						
95J0642	28.5	1.038	29.583	302.783	159.684	46.787
95J0641	29.8	1.038	30.9324	304.132	354.339	103.821
95J0639	28.1	1.038	29.1678	302.368	164.249	48.125
95J0640	28.7	1.038	29.7906	302.991	327.028	95.819
Q =	68.044	W/Ft^2			732.441 W/m^2	
dT =	50.495	K				
dL =	0.5	Ft				
K_T =	2.211 \pm	0.22236 $W/m-K$				

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 43)						
$Q = K_T(dT/dL)$						
where		Q =heat transfer per unit area (W/Ft^2)				
		K_T = thermal conductivity ($W/m-K$)				
		dT = temperature difference between bottom and top sensors (K)				
		dL = distance between bottom and top sensors (m)				
Sensor readings						
Serial no.	Temp $^{\circ}C$	Multi-factor	Correct Temp	Temp $^{\circ}K$	Heat flow Btu/ Ft^2 -Hr	Convert to W/Ft^2 1Btu/Hr = 0.293W
Bottom						
96041630	88.7	0.995	88.2565	361.457	380.780	111.569
96041631	90.9	0.995	90.4455	363.646	281.929	82.605
96041632	90.8	0.995	90.346	363.546	0.000	0.000
96041633	94.5	0.995	94.0275	367.228	192.681	56.455
Top						
95J0642	19.9	1.04	20.696	293.896	142.513	41.756
95J0641	19.4	1.04	20.176	293.376	112.654	33.008
95J0639	19.7	1.04	20.488	293.688	189.835	55.622
95J0640	18.2	1.04	18.928	292.128	104.471	30.610
Q = 58.804 W/Ft^2 632.977 W/m^2						
dT = 70.697 K						
dL = 0.5 Ft 0.1524 m						
K _T = 1.364 ± 0.13775 W/m-K						

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 48)						
$Q = K_T(dT/dL)$						
where Q = heat transfer per unit area (W/Ft^2)						
K_T = thermal conductivity ($W/m-K$)						
dT = temperature difference between bottom and top sensors (K)						
dL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/Ft ² -Hr	Convert to W/Ft ² 1Btu/Hr = 0.293W
Bottom						
96041630	74.8	1	74.8	348	162.642	47.654
96041631	76	1	76	349.2	110.568	32.397
96041632	76	1	76	349.2	0.000	0.000
96041633	77.5	1	77.5	350.7	85.184	24.959
Top						
95J0642	22.5	1.04	23.4	296.6	77.789	22.792
95J0641	22	1.04	22.88	296.08	47.036	13.782
95J0639	22.1	1.04	22.984	296.184	82.323	24.120
95J0640	21.5	1.04	22.36	295.56	51.337	15.042
Q =	25.821 W/Ft ²		277.941 W/m ²			
dT =	53.189 K					
dL =	0.5 Ft		0.1524 m			
K _T =	0.797 ±		0.08097 W/m-K			

Thermal Conductivity calculation using Fourier equation						
Sample = Apache Leap Tuff (Run 49)						
$Q = K_T(dT/dL)$						
where Q = heat transfer per unit area (W/Ft^2)						
K_T = thermal conductivity ($W/m-K$)						
dT = temperature difference between bottom and top sensors (K)						
dL = distance between bottom and top sensors (m)						
Sensor readings						
Serial no.	Temp °C	Multi-factor	Correct Temp	Temp °K	Heat flow Btu/Ft ² -Hr	Convert to W/Ft ² 1Btu/Hr = 0.293W
Bottom						
96041630	87.9	0.985	86.5815	359.782	272.486	79.838
96041631	91.9	0.985	90.5215	363.722	82.886	24.286
96041632	89.5	0.985	88.1575	361.358	0.000	0.000
96041633	93.3	0.985	91.9005	365.101	148.300	43.452
Top						
95J0642	24.9	1.04	25.896	299.096	151.461	44.378
95J0641	23.7	1.04	24.648	297.848	90.144	26.412
95J0639	24.4	1.04	25.376	298.576	166.116	48.672
95J0640	23	1.04	23.92	297.12	71.675	21.001
Q =	41.148 W/Ft ²		442.933 W/m ²			
dT =	64.33 K					
dL =	0.5 Ft		0.1524 m			
K _T =	1.049 ±		0.10623 W/m-K			

17/2/97 Apache Leap Samples Removed from thermal conductivity apparatus for porosity measurements. Mass measured using the Mettler PM480 Delta range Balance which was calibrated on 5 Feb. '97 SN # N45601

Sample ID	Mass (g)	
# 1	22.187	1-5 visually wet
# 2	17.039	
# 3	23.528	
# 4	19.878	
# 5	22.962	
# 6	26.244	6-10 visually dry
# 7	25.224	
# 8	19.513	
# 9	20.870	
# 10	26.092	

Note: Measurements of mass were performed immediately upon removal from the thermal conductivity apparatus. Samples # 1-5 were visually wet upon removal and samples # 6-10 were visually dry upon removal. Samples # 1-10 were then placed in a Blue M oven @ 80°C in order to desiccate the samples for porosity measurements. W. Hies 17/2/97

2/17/96 JP

Apache Leap tuff sample was removed from thermal conductivity cell. A series of measurements will now be conducted without a crushed tuff specimen in the cell.

2/17/96 JP Thermal Conductivity Experiment Run 50
Air - no rock sample

Parameters

Variable temperature setpoint 5.0
Waterbath temp setpoint 20°C
Pressure on top Al plate 55 ± 1 lb

2/19/97 JP Results of TC experiment Run 50

Bottom Al plate Serial No.	Heat Slip BTU/F ² -h	Temp °C
96041630	2.2833	22.3
31	2.1311	22.3
32	—	22.3
33	3.3786	22.3

Top Al plate

955042	3.2961	18.5
41	3.5163	18.5
39	3.6940	18.5
40	4.0906	18.5

Monitoring thermocouples	Temp °C
1	23.8
2	23.5
3	22.4
4	22.5
5	22.5
6	22.5
7	18.7
8	18.7
9	18.7
10	18.6

2/19/97pp Thermal Conductivity Experiment Run 51
Air

Parameter
Variable temperature setpoint 15
Waterbath temp setpoint 20°C
Pressure on top Al plate 55 ± 1 lb

2/20/97pp 0815hr Results of TC experiment run 51

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	12.7225	32.6
31	13.2397	32.6
32	—	32.6
33	15.5448	32.7

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
955042	14.8248	18.9
41	15.1390	18.9
39	13.7819	18.9
40	14.7785	18.9

Monitoring Thermocouples	Temp °C
1	28.2
2	26.1
3	32.7
4	32.8
5	32.7
6	32.8
7	19.1
8	19.1
9	19.0
10	19.0

2/20/97pp 0820hr Thermal Conductivity Experiment Run 52
Air

Parameter
Variable temperature setpoint 25
Waterbath temp. setpoint 20°C
Pressure on top Al plate 55 ± 1 lb

2/21/97pp 0800hr Results of TC experiment Run 52

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	33.7541	50.3
31	38.2840	50.4
32	—	50.4
33	41.0433	50.4

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
955042	39.4913	19.6
41	39.6863	19.4
39	37.0467	19.5
40	39.6551	19.6

Monitoring Thermocouples	Temp °C
1	35.2
2	30.3
3	50.4
4	50.4
5	50.4
6	56.7
7	19.6
8	19.7
9	19.5
10	19.6

2/21/97 0800hr Thermal Conductivity Experiment Run 53
Air

Parameters

Variable frequency setpoint 35
Waterbath Temp setpoint 20°C
Pump ~ Top Al plate 5 ft/lb

2/23/97 0900hr Results of TC experiment Run 53

Bottom Al plate Serial No.	Heat Flux BTU/ft ² -hr	Temp °C
96041630	72.5711	75.2 74.7
31	73.6655	75.3 74.8
32	—	75.2 74.7
33	84.7000	75.3 74.8

Top Al plate
95J042

Heat Flux BTU/ft ² -hr	Temp °C
84.1112	20.7 20.7
75.0551	21.1 20.8
73.4692	21.0 20.8
76.7270	21.0 20.8

Monitoring Thermopiles Temp °C

1
2
3
4
5
6
7
8
9
10

2/21/97 On 18/2/97 the volume of the 10 Apache
heap samples removed from the thermal
conductivity apparatus on 17/2/97 p 145 of this
lab notebook were obtained using Archimedes
principle which states that the volume of an
irregularly shaped object is equal to that of
the volume of water it displaces when
totally submerged.

Samples	Volume (cm ³)	Volume in cylinder without sample (cm ³)	Volume in cylinder with sample (cm ³)
1	10	70	80
2	7	50	57
3	10	70	80
4	8	61	69
5	9.5	90	99.5
6	11	61	72
7	10	50	60
8	8	52	60
9	10	50	60
10	10	60	72

The volumes for samples # 2 & 7 were measured
using Fisherbrand 100 ml graduated cylinder
cat. # 03-5570. Samples # 1, 3, 4, 5, 6, 8, 9 & 10
however were too large to fit through the aperture
of the Fisherbrand graduated cylinder, therefore
measurements for those samples were obtained
using the KIMAX 250 ml graduated cylinder
cat. # 20024-D. All measurements were performed
using deionized H₂O in the graduated cylinders
were emptied and refilled prior to each
measurement of sample volume. Samples were
carefully submerged to prevent the loss of
any H₂O. Samples # 1-10 were then placed back
into a blue M oven set @ 80°C.

On 21/2/97 the 10 Apache heap samples were removed from the Blue M oven so that measurements of mass could be performed. The procedures are adopted from Rasmussen et al., (1990) and Green, Rice & Meyer-James, (1995). The procedures are as follows: samples #1-10 were removed from the oven and immediately placed in a desiccator filled with drierite and were allowed to reach ambient temperature. The mass was then measured using the Mettler PM400 electronic balance with a deviation of ± 0.001 g.

Sample ID	Mass (g)
1	21.488
2	16.511
3	22.885
4	19.551
5	22.230
6	26.220
7	25.113 g mill 21/2/97
8	19.424
9	20.520
10	25.886

Samples #1-10 were then placed in a Blue M oven set @ 105°C as described in Green, Rice, & Meyer-James (1995). M. J. 21/2/97

2/23/97pp Thermal Conductivity Experiment Run 54
Air

Parameters

Variable temperature	setpoint	45
Water bath temp	setpoint	20°C
Pressure on top Al plate		5 ft + 16

2/24/97 Results of TC experiment Run 54

Bottom Al plate	Heat Flux	Temp $^{\circ}\text{C}$
Serial No	BTU/ft ² -hr	
96041630	148.4404	102.0
31	109.0847	102.1
32	—	102.5
33	156.8277	102.4

Top Al plate

955042	138.8945	22
41	129.0570	22.1
39	126.2520	22
40	134.6505	22

Monitoring Thermocouples	Temp $^{\circ}\text{C}$
1	58.4
2	45.7
3	102.7
4	102.8
5	102.3
6	103.7
7	21.7
8	21.8
9	21.5
10	21.6

2/24/97 JF Thermal Conductivity Experiment Run 55
Air

Parameter

Variable frequency output 55
Waterbath temp output 20°C
Pressure on top Al plate 5.8 ± 1.6

2/25/97 JF Results of TC experiment Run 55

Bottom Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
96041630	160.9347	133.4
31	141.8063	132.9
32	—	133.7
33	209.1439	133.9

Top Al plate Serial No	Heat Flux BTU/ft ² -hr	Temp °C
553042	201.4121	23.8
41	178.9639	23.9
35	177.5692	23.9
40	192.7924	23.9

Monting Thermocouple	Temp °C
1	72.9
2	56.0
3	134.2
4	134.2
5	133.2
6	134.5
7	23.1
8	23.2
9	22.9
10	23.2

On 2/24/97 the 10 Apache heap samples were removed from the Blue M oven so that measurements of mass could be performed. Procedures were the same as those discussed on page 152 of this lab notebook.

Sample ID	Mass (g)
1	21.473
2	16.500
3	22.868
4	19.317
5	22.271
6	26.198
7	25.153
8	19.397
9	20.801
10	25.867

Samples # 1-10 were then placed back into the Blue M oven set @ 105°C.

M. Hill 2/24/97

On 2/25/97 the 10 Apache heap samples were removed from the Blue M oven so that measurements of mass could again be performed. Procedures followed were the same as those discussed on p 152 of this lab notebook.

Sample ID	Mass (g)
1	21.471
2	16.500
3	22.868
4	19.317
5	22.269
6	26.198
7	25.151
8	19.398
9	20.800
10	25.866

Samples # 1-10 were then placed back into
the Blue M oven set @ 105°C.
M. Hill 2/25/97

2/25/97 JF Thermal Conductivity Experiment Run 56
Air

Parameter
Variable temperature setpoint 65
Waterbath temp setpoint 20°C
Pressure on top Al plate 59±16s.

2/26/97 JF Results of TC experiment Run 56

Bottom Al plate Serial No	Heat Flux BTU/F ² h	Temp °C
96041630	217.6270	166.5
31	149.3888	165.5
32	—	167.0
33	308.0383	167.1

Top Al plate		
955042	275.3286	29.7
41	246.4913	29.9
39	235.5250	29.9
40	268.9242	29.9

Monitoring Thermocouple	Temp °C
1	88.7
2	68.2
3	168.1
4	168.3
5	164.8
6	169.8
7	28.7
8	28.8
9	28.4
10	28.8

2/26/97 *gp* Thermal Conductivity Experiment Run 57
Air

Parameters
Variable temperature output 70
Waterbath temp output 10°C
Pressure on top Al plate 55 ± 16

2/27/97 *gp* Results of TC Experiment Run ~~58~~ 57 *gp* 3/18/97

Bottom Al plate Serial No	Heat Flux BTU/ft ² hr	Temp °C
46041630	344.849	183.1
31	270.0653	182.0
32	—	183.4
33	273.667	183.7

Top Al plate 95J042	Heat Flux BTU/ft ² hr	Temp °C
41	320.249	32.8
39	289.7161	32.9
40	269.7220	33.0
	330.1518	33.0

Monitor Thermocouples	Temp °C
1	97.6
2	75.3
3	185.2
4	185.2
5	184.3
6	187.1
7	31.5
8	31.8
9	30.9
10	31.7

2/27/96 *gp* Thermal Conductivity Experiment Run 58
Water

Parameters
Variable temperature output 25
Waterbath temp output 20°C
Pressure on top Al plate 55 ± 16

3/4/97
~~2/23/96~~ *gp* Results of TC experiment Run 58

Bottom Al plate Serial No	Heat Flux BTU/ft ² hr	Temp °C
46041630	20.3985	21.7
31	27.1484	21.7
32	—	21.7
33	—	21.7

Top Al plate 95J042	Heat Flux BTU/ft ² hr	Temp °C
41	25.3725	19.9
39	19.2339	19.9
40	20.9362	20.0
	25.5265	19.7 20.0 <i>gp</i> 3/4/97

Monitor Thermocouples	Temp °C
1	26.9
2	22.0
3	21.8
4	21.7
5	21.8
6	22.1
7	20.0
8	20.2
9	20.0
10	20.0

2/28/97 JF

Entries for data collected from
the Thermal Effects on Flow
KTI are contained in Scientific
Notebooks #212.

This continues in Notebook #212 R. L. H. 6/12/97

Final Entry!
This Notebook appears to
comply w/ QAP-001.

P. C. R.
2/8/2000